



**Calhoun: The NPS Institutional Archive**  
**DSpace Repository**

---

Theses and Dissertations

1. Thesis and Dissertation Collection, all items

---

1986-06

# Marine gas turbine modeling for modern control design

Herda, Vincent J.

---

<https://hdl.handle.net/10945/21966>

---

This publication is a work of the U.S. Government as defined in Title 17, United States Code, Section 101. Copyright protection is not available for this work in the United States.

*Downloaded from NPS Archive: Calhoun*



Calhoun is the Naval Postgraduate School's public access digital repository for research materials and institutional publications created by the NPS community. Calhoun is named for Professor of Mathematics Guy K. Calhoun, NPS's first appointed -- and published -- scholarly author.

**Dudley Knox Library / Naval Postgraduate School**  
**411 Dyer Road / 1 University Circle**  
**Monterey, California USA 93943**

<http://www.nps.edu/library>





DUDLEY MITOX LIBRARY  
NAVAL POSTGRADUATE SCHOOL  
MONTEREY, CALIFORNIA 93943-6002







# NAVAL POSTGRADUATE SCHOOL

Monterey, California



## THESIS

MARINE GAS TURBINE MODELING  
FOR  
MODERN CONTROL DESIGN

by

Vincent J. Herda

June 1986

Thesis Advisor:

David Smith

Approved for public release; distribution unlimited

T230613



REPORT DOCUMENTATION PAGE

|   |   |   |                         |
|---|---|---|-------------------------|
| REPORT SECURITY CLASSIFICATION<br>Unclassified  |   | 1b. RESTRICTIVE MARKINGS  |                         |
| 1. SECURITY CLASSIFICATION AUTHORITY  |   | 3. DISTRIBUTION / AVAILABILITY OF REPORT  |                         |
| 2. DECLASSIFICATION / DOWNGRADING SCHEDULE  |   |   |                         |
| PERFORMING ORGANIZATION REPORT NUMBER(S)  |   | 5. MONITORING ORGANIZATION REPORT NUMBER(S)                                       |                         |
| 1a. NAME OF PERFORMING ORGANIZATION<br>Naval Postgraduate School  | 6b. OFFICE SYMBOL<br>(if applicable)      | 7a. NAME OF MONITORING ORGANIZATION   |                         |
| 2. ADDRESS (City, State, and ZIP Code)<br>Monterey, California 93943-5000   |   | 7b. ADDRESS (City, State, and ZIP Code)   |                         |
| 3a. NAME OF FUNDING / SPONSORING ORGANIZATION   | 8b. OFFICE SYMBOL<br>(if applicable)      | 9. PROCUREMENT INSTRUMENT IDENTIFICATION NUMBER                                   |                         |
| 2. ADDRESS (City, State, and ZIP Code)  |   | 10. SOURCE OF FUNDING NUMBERS   |                         |
|   |   | PROGRAM ELEMENT NO.   | PROJECT NO.             |
|   |   | TASK NO.  | WORK UNIT ACCESSION NO. |
| 1. TITLE (Include Security Classification)<br>Marine Gas Turbine Modeling for Modern Control Design   |   |   |                         |
| 2. PERSONAL AUTHOR(S)<br>Vincent J. Herda   |   |   |                         |
| 3a. TYPE OF REPORT<br>Masters Thesis  | 13b. TIME COVERED<br>FROM _____ TO Jun 86 | 14. DATE OF REPORT (Year, Month, Day)<br>1986 June 19                             | 15. PAGE COUNT<br>134   |
| 6. SUPPLEMENTARY NOTATION   |   |   |                         |
| 7. COSATI CODES   |   | 18. SUBJECT TERMS (Continue on reverse if necessary and identify by block number) |                         |
| FIELD   | GROUP                                     | SUB-GROUP   |                         |
|   |   | Marine gas turbine, Modeling, Modern Control                                      |                         |
| 9. ABSTRACT (Continue on reverse if necessary and identify by block number)   |   |   |                         |
| <p>The search for improved performance of U.S. Navy ships has led to more complex propulsion systems consisting of multiple, intracting inputs. Classical control theory does not effectively exploit these interactions. Modern Control Theory provides a systematic method of dealing with multiple intracting inputs to achieve improved system performance. One of the most highly developed modern control techniques is the linear quadratic regulator (LQR) method. Essential to the application of this method is the formulation of a state space description of the plant. In this paper a nonlinear dynamic propulsion system model is developed from experimental data and used to formulate a state space model.</p> |   |   |                         |
| 20. DISTRIBUTION / AVAILABILITY OF ABSTRACT<br><input checked="" type="checkbox"/> UNCLASSIFIED/UNLIMITED <input type="checkbox"/> SAME AS RPT <input type="checkbox"/> DTIC USERS  |   | 21. ABSTRACT SECURITY CLASSIFICATION<br>Unclassified                              |                         |
| 22a. NAME OF RESPONSIBLE INDIVIDUAL   |   | 22b. TELEPHONE (Include Area Code)  | 22c. OFFICE SYMBOL      |



Approved for public release; distribution is unlimited.

Marine Gas Turbine Modeling for Modern Control Design

by

Vincent J. Herda  
Lieutenant, United States Navy  
B.S., U.S. Naval Academy, 1980

Submitted in partial fulfillment of the  
requirements for the degrees of

MASTER OF SCIENCE IN MECHANICAL ENGINEERING  
AND  
MECHANICAL ENGINEER

from the

NAVAL POSTGRADUATE SCHOOL  
June 1986

## ABSTRACT

The search for improved performance of U.S. Navy ships has led to more complex propulsion systems consisting of multiple, interacting inputs. Classical control theory does not effectively exploit these interactions. Modern control theory provides a systematic method of dealing with multiple interacting inputs to achieve improved system performance. One of the the most highly developed modern control techniques is the linear quadratic regulator (LQR) method. Essential to the application of this method is the formulation of a state space description of the plant. In this paper a nonlinear dynamic propulsion system model is developed from experimental data and used to formulate a state space model.

## TABLE OF CONTENTS

|       |   |    |
|-------|---|----|
| I.    | INTRODUCTION . . . . .                                | 9  |
| II.   | OVERVIEW . . . . .                                    | 11 |
| III.  | PLANT DESCRIPTION/CONCEPTUAL MODELING . . . . .       | 12 |
|       | A. PLANT DESCRIPTION . . . . .                        | 12 |
|       | B. THE CONCEPTUAL PLANT MODEL . . . . .               | 14 |
|       | 1. Plant Boundaries . . . . .                         | 14 |
|       | 2. Plant Components . . . . .                         | 14 |
|       | 3. Significant Dynamics . . . . .                     | 15 |
|       | 4. Model Simplification . . . . .                     | 18 |
|       | 5. Component Inputs/Outputs . . . . .                 | 20 |
| IV.   | QUANTITATIVE COMPONENT MODELING . . . . .             | 26 |
|       | A. DATA ACQUISITION . . . . .                         | 26 |
|       | B. DATA REDUCTION . . . . .                           | 28 |
| V.    | STEADY STATE PLANT MODEL . . . . .                    | 31 |
|       | A. STEADY STATE MODEL ALGORITHM . . . . .             | 31 |
|       | B. STEADY STATE MODEL RESULTS . . . . .               | 31 |
| VI.   | NONLINEAR DYNAMIC MODEL . . . . .                     | 37 |
|       | A. GAS GENERATOR INERTIA . . . . .                    | 37 |
|       | B. NONLINEAR DYNAMIC PROGRAM . . . . .                | 42 |
| VII.  | STATE SPACE MODEL . . . . .                           | 48 |
| VIII. | CONCLUSIONS AND RECOMMENDATIONS . . . . .             | 54 |
|       | APPENDIX A: DATA ACQUISITION PROGRAM . . . . .        | 55 |
|       | APPENDIX B: LEAST SQUARES CURVE FIT PROGRAM . . . . . | 67 |

|   |     |
|---|-----|
| APPENDIX C: STEADY STATE COMPUTER PROGRAM . . . . . | 73  |
| APPENDIX D: NONLINEAR DYNAMIC PROGRAM . . . . .     | 114 |
| APPENDIX E: STATE EQUATION FORMULATION . . . . .    | 127 |
| LIST OF REFERENCES . . . . .                        | 133 |
| INITIAL DISTRIBUTION LIST . . . . .                 | 134 |



LIST OF TABLES

|    |  |    |
|----|--|----|
| 1. | GAS TURBINE/DYNAMOMETER INSTRUMENTATION . . . . .  | 27 |
| 2. | GAS TURBINE DATA ACQUISITION SCHEDULE . . . . .  | 29 |
| 3. | SCALING FACTORS . . . . .  | 30 |
| 4. | COMPARISON OF STEADY STATE OUTPUT WITH RAW<br>DATA FOR NG = 25,900 RPM, NS = 970 RPM . . . . . | 34 |
| 5. | VARIATION OF 'A' AND 'B' MATRICES WITH<br>OPERATING POINT . . . . .                            | 50 |

## LIST OF FIGURES

|      |   |    |
|------|---|----|
| 3.1  | NPS Marine Propulsion Test Facility . . . . .                                     | 13 |
| 3.2  | Propulsion Plant Components . . . . .   | 16 |
| 3.3  | Reduced Component Model . . . . .   | 19 |
| 3.4  | Mechanical-Rotational Port . . . . .  | 21 |
| 3.5  | Incompressible Fluid Port . . . . .   | 21 |
| 3.6  | Thermal Port . . . . .  | 22 |
| 3.7  | Alternate Thermal Port . . . . .  | 22 |
| 3.8  | Combined Port . . . . .   | 23 |
| 3.9  | Thermodynamic Power Port . . . . .  | 23 |
| 3.10 | Complete Multiport Diagram . . . . .  | 25 |
| 5.1  | Steady State Plant Model Flowchart . . . . .                                      | 32 |
| 5.2  | Torque Differential .vs. Fuel Flowrate . . . . .                                  | 36 |
| 6.1  | Experimental Apparatus for<br>JG Determination . . . . .                          | 39 |
| 6.2  | Simplified Diagram of Experimental Apparatus . . . . .                            | 40 |
| 6.3  | Flowchart for Nonlinear Dynamic Program . . . . .                                 | 43 |
| 6.4  | Fuel Flowrate Input . . . . .   | 45 |
| 6.5  | Gas Generator Response . . . . .  | 46 |
| 6.6  | Dynamometer Response . . . . .  | 47 |
| 7.1  | Comparison of State Space vs. Nonlinear Model<br>Gas Generator Response . . . . . | 52 |
| 7.2  | Comparison of State Space vs. Nonlinear Model<br>Dynamometer Response . . . . .   | 53 |

## SYMBOLS AND ABBREVIATIONS

|     |   |   |
|-----|---|---|
| E   | = | Fuel Energy Realized at HP Turbine          |
| JD  | = | Dynamometer Inertia                         |
| JG  | = | Gas Generator Inertia                       |
| Ma  | = | Air Mass Flowrate                           |
| Maf | = | Combined Fuel and Air Mass Flowrate         |
| Mf  | = | Fuel Mass Flowrate                          |
| NG  | = | Gas Generator Speed                         |
| NS  | = | Power Turbine/Dynamometer Speed             |
| P2  | = | Compressor Discharge Pressure               |
| P4  | = | High Pressure Turbine Discharge Pressure    |
| QC  | = | Compressor Torque                           |
| QD  | = | Dynamometer Torque                          |
| QF  | = | Free Power Turbine Torque                   |
| QH  | = | High Pressure Turbine Torque                |
| t   | = | Fuel Energy Lag Time Constant               |
| T2  | = | Compressor Discharge Temperature            |
| T4  | = | High Pressure Turbine Discharge Temperature |
| V   | = | Volume Flowrate                             |
| Ww  | = | Dynamometer Water Weight                    |

## I. INTRODUCTION

The search for improved performance of U.S. Navy ships has led to increasingly complex marine propulsion systems. Controllable inputs to this system now include fuel flow rate, engine inlet guide vane and stator vane position, bleed air selection, and propeller pitch angle. Current control strategies applied to these propulsion plants, and classical control techniques in general, do not take into account the interaction between these inputs. In contrast, modern control techniques (MCT) provide a systematic method to achieve improved system performance when dealing with multiple, interacting inputs. Specifically, modern control theory methods provide the following benefits not found in classical control methods applied to multiple input, multiple output (MIMO) systems:

- (1) Effective treatment of coupled input interactions to improve performance,
- (2) Rigorous treatment of stability questions,
- (3) Systematic control design which reduce iteration and the need for extensive intuition and experience in the control design process.

The most extensive application of modern control theory to date is the F100 Turbofan Multivariable Control Synthesis Program, sponsored by the Air Force Aero Propulsion Lab and Nasa Lewis Research Center. [Ref. 1: p.43]. The results of this program demonstrated that modern control theory techniques provide an orderly, effective, systematic approach to controller design for multiple, interacting input systems.

Current work at the Naval Postgraduate School, Monterey, is aimed at investigating the application of modern control techniques to U.S. Navy ship propulsion plants. The initial phase of this effort involves the application of modern control techniques to a low power gas turbine test



facility located at the school. In the context of this effort the goals of this thesis were:

- (1) Development of an accurate digital computer model of the propulsion test facility which includes all significant plant nonlinearities and dynamic effects.
- (2) Develop a linear (state-space) model of the propulsion plant.

The nonlinear model is a valuable tool in controller design. First, it provides a means to test control strategies without risking damage to the actual plant. Second, it provides a cost effective alternative to extensive controller tests. Finally, in this work the nonlinear model provided the basis from which a linear (state space) model was derived.

The state space model of the propulsion plant is essential for future controller design work at NPS using the linear quadratic regulator (LQR) technique, which is the most highly developed modern control method. [Ref. 2: p. 653].

## II. OVERVIEW

This thesis is organized into eight chapters. In the following chapter a description of the test facility at the Naval Postgraduate School (NPS) is given. Also in that chapter, a conceptual model of the plant is developed. The plant is first divided into functional components. The significant plant dynamics are identified, and the number of plant components is reduced so that only the degree of complexity necessary to represent the significant plant processes is retained. Finally, the component interactions are defined by identifying component inputs and outputs. The component interactions link the components together and form a basis for quantitative modeling of the plant.

In Chapter 4 quantitative ( versus conceptual ) component modeling is described. Using experimental data, the input/output relations for each component (as defined in the previous chapter ) are constructed in equation form.

In Chapter 5 the individual component equations are joined together to form a steady state plant model.

In Chapter 6 the differential equations governing the plant dynamics ( identified in Chapter 3 ) are introduced into the steady state model. In this way a nonlinear dynamic plant model is developed.

In Chapter 7 the state space model is derived from the nonlinear dynamic model.

Chapter 8 contains conclusions and recommendations for further work.

### III. PLANT DESCRIPTION/CONCEPTUAL MODELING

#### A. PLANT DESCRIPTION

The test facility ( hereafter referred to as 'the plant') consists of a Boeing model 502-6A 175 horsepower gas turbine engine and a Clayton 17-300 water dynamometer. Figure 3.1 is a schematic of the test facility.

The gas turbine can be subdivided into the gas generator section and the power take-off section. The gas generator section consists of a single stage centrifugal compressor, a dual can combustor, an accessory drive section, and a single-stage axial flow high pressure turbine (HPT). The power take-off section consists of a single-stage axial flow free power turbine (FPT). Fuel enters the combustor via the fuel control, which consists of a flyball governor and an acceleration limiter. The fuel control setting is adjusted by an electric-motor driven control lever. The hot gases drive the high pressure turbine. The high pressure turbine, in turn, drives the compressor and accessory drive section. The accessory drive section extracts power from the high pressure turbine to drive the fuel pump and governor, the oil pump, and a tachometer generator. The free power turbine extracts energy from the hot gas stream and drives the dynamometer. There is no mechanical connection between the high pressure turbine and the free power turbine.

The water dynamometer acts as a power absorption unit. The power turbine torque and speed are adjusted by varying the amount of water in the dynamometer. This is analogous to changing the pitch on a controllable pitch propeller. Water enters and leaves the dynamometer via electric motor driven load and unload valves.

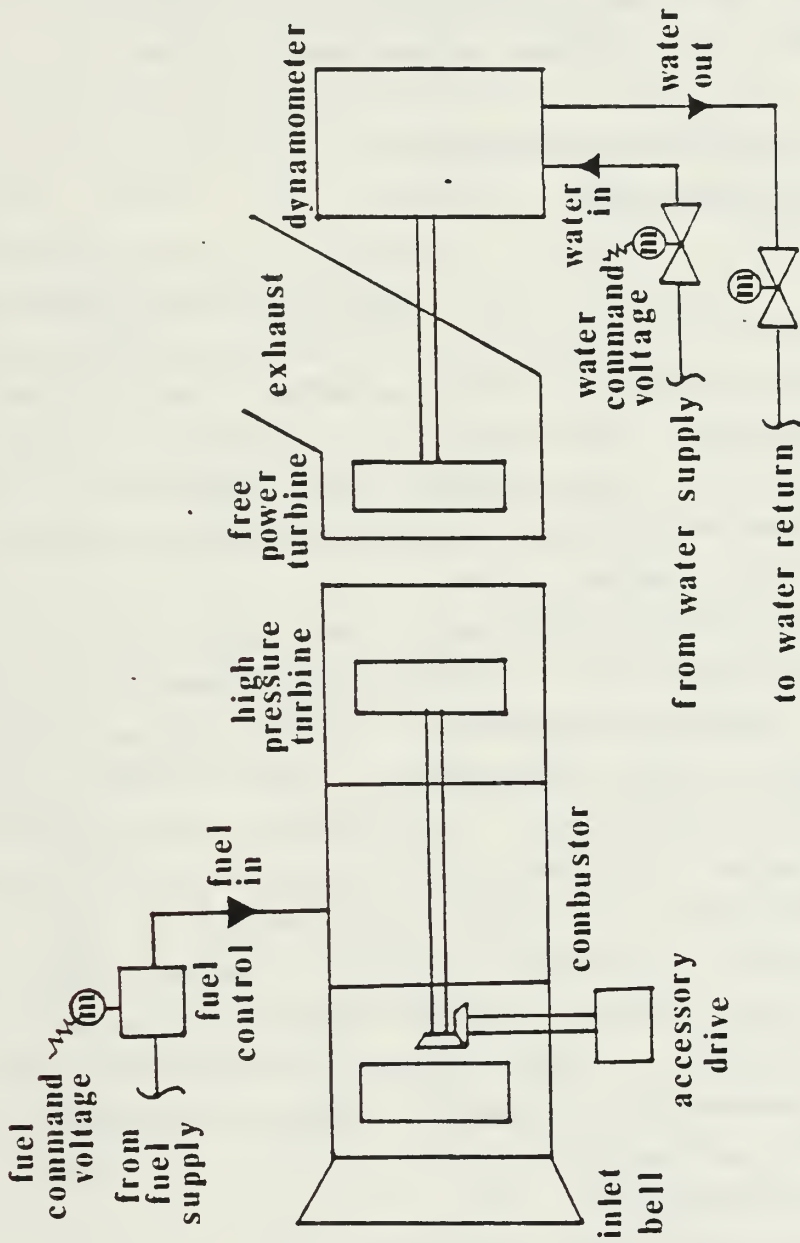


Figure 3.1 NPS Marine Propulsion Test Facility



## B. THE CONCEPTUAL PLANT MODEL

In formulating a conceptual plant model the following issues must be addressed:

- definition of plant boundaries,
- identification of significant plant dynamics,
- extent to which the plant must be divided into components and how the components selected, and
- definition of component inputs and outputs.

These issues are discussed below.

### 1. Plant Boundaries

Selection of plant boundaries is important since this selection determines the plant inputs. Because the long range goal of this project is the implementation of an improved control system, the existing fuel control was excluded from the plant model. The plant boundary was located downstream of the existing fuel control, and actual fuel flow to the combustor (versus fuel command voltage) was established as one plant input.

A model of the dynamometer was developed in earlier work by Johnson [Ref. 3]. This model accurately describes the behavior of the dynamometer during loading conditions (water addition to the dynamometer), but is less accurate during unloading conditions. The source of the dynamometer model inaccuracies is thought to involve the unload valve behavior. In order to avoid introduction of the unload valve inaccuracies into the propulsion model developed in this study, the load and unload valves were placed outside the plant boundaries. Thus, actual water to and from the dynamometer (versus water command voltage) was established as the second plant input.

### 2. Plant Components

Breaking the plant into components facilitates the identification of causal relationships and plant dynamics. Further, the plant components provide the foundation of plant model development.

The selection of components is a cut and try process. A first cut at component identification is shown in Figure 3.2.

This selection was based on a functional basis and assumptions about the significant processes occurring within the plant. The minimum number of components necessary to account for these processes is sought. If the resulting model is insufficiently accurate, then some significant process has either been overlooked or improperly described. In either case, the selection of components must be reevaluated.

### 3. Significant Dynamics

Paramount to model accuracy is the identification of significant plant dynamics. Fluid momentum and compressibility, heat transfer, energy storage, rotor inertia, and combustion effects are all possibilities. However, dynamic effects can only be considered significant in the practical sense if their time constants are neither much shorter nor extremely longer than those for the controller actuators and sensors. Previous work by Szuch [Ref. 4:p. 243] in the area of aircraft gas turbine controls indicated that fluid momentum, compressibility, and energy storage dynamics occur too rapidly to be controlled, while heat transfer dynamics occur too slowly to be important in the control problem.

The importance of combustion dynamics deserves special discussion. Szuch [Ref. 4:p. 243] and DeHoff [Ref. 5:p. 274] concluded that combustion dynamics were of too high frequency to be important in controls considerations. In contrast, Rubis [Ref. 6:p. 56] discusses significant transient effects associated with engine torque development in response to fuel flowrate changes. These effects could be due in part to combustion related delays. In the present work combustion effects were initially neglected. The resulting model produced excessive

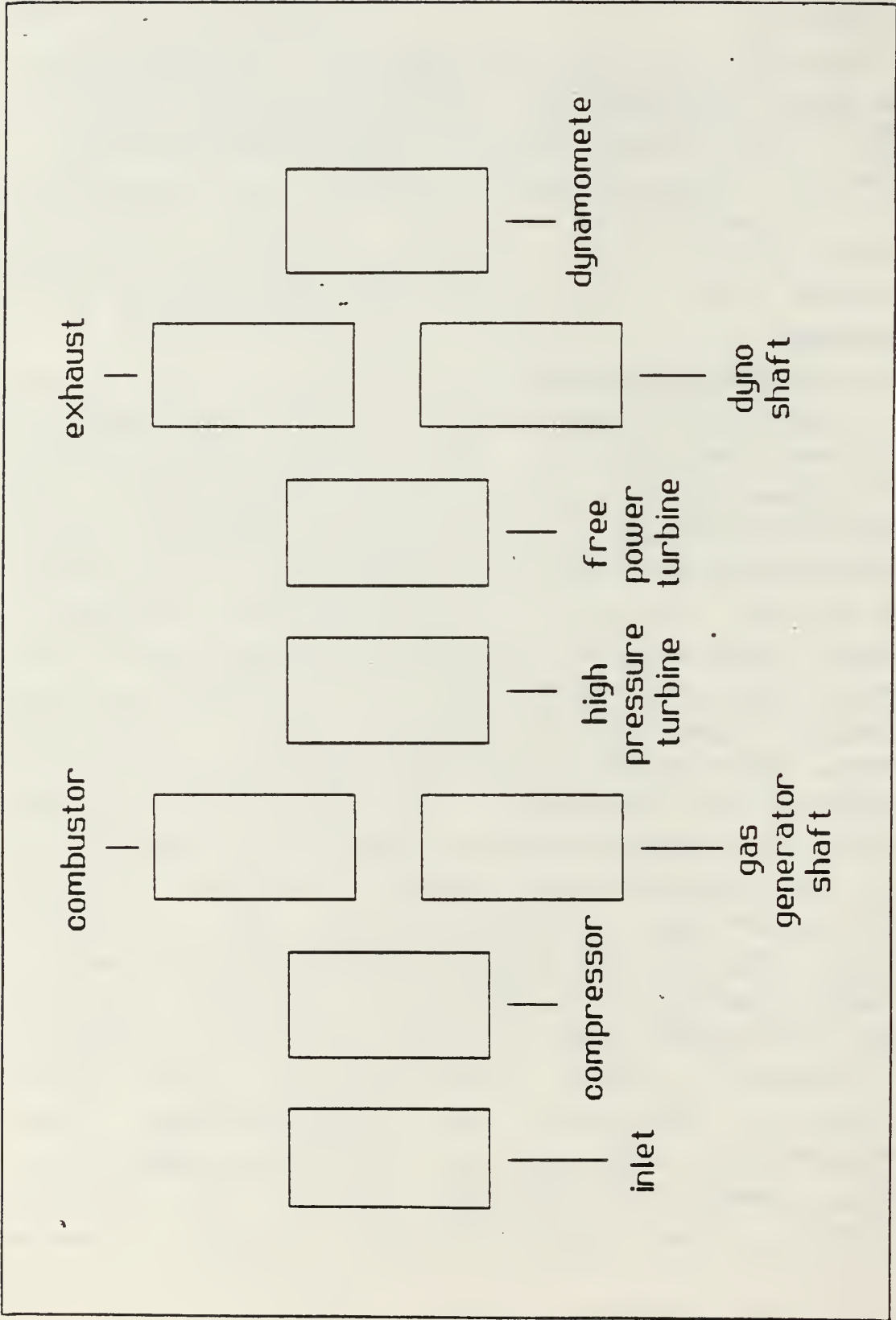


Figure 3.2 Propulsion Plant Components

accelerations when compared to experimental data. When combustion effects were modeled as a fuel energy lag accurate results were achieved. This fuel energy lag represents the delay between the time when the chemical energy in the fuel passes through the fuel nozzles and the time when the mechanical energy is realized at the high pressure turbine.

In addition to the fuel energy lag, the most significant plant dynamics are the rotor inertia effects. Thus, the equations governing the plant dynamic behavior are:

$$\dot{N}_G = (Q_H - Q_C - Q_A - Q_{FRG})/J_G$$

$$\dot{N}_S = (Q_F - Q_D - Q_{FRD})/J_D$$

$$E/M_f = 1/(t_S + 1)$$

Where

|           |  |
|-----------|--|
| $N_G$     | = gas generator acceleration,                                    |
| $N_S$     | = free power turbine acceleration,                               |
| $J_G$     | = gas generator inertia,   |
| $J_D$     | = combined free power turbine and dynamometer inertia,           |
| $Q_H$     | = high pressure turbine torque,                                  |
| $Q_C$     | = compressor torque,   |
| $Q_A$     | = accessory drive torque,  |
| $Q_{FRG}$ | = gas generator frictional torque,                               |
| $Q_F$     | = free power turbine torque,                                     |
| $Q_D$     | = dynamometer torque,  |
| $Q_{FRD}$ | = combined free power turbine and dynamometer frictional torque, |
| $M_f$     | = measured fuel flowrate at the fuel nozzles,                    |
| $E$       | = mechanical energy applied at the high pressure turbine,        |
| $t$       | = time constant associated with the combustion process.          |



In this study the auxiliary torque ( $Q_D$ ) and gas generator frictional torque ( $Q_{FRG}$ ) were lumped into the compressor torque ( $Q_D$ ). Also, the dynamometer/power turbine frictional torque ( $Q_{FRD}$ ) was lumped into the dynamometer torque ( $Q_D$ ). Having made these simplifications the governing dynamic equations become:

$$\dot{N}_G = (Q_H - Q_C) / J_G \quad (3.1)$$

..

$$\dot{N}_S = (Q_F - Q_D) / J_D \quad (3.2)$$

$$M_f/E = 1 / (t_S + 1) \quad (3.3)$$

#### 4. Model Simplification

Once the significant dynamic effects are determined and the governing equations identified, the plant model may be simplified by reducing the number of components. As noted in the overview, it will be necessary during the model development to define the input/output relationships for each component in equation form. If the dynamic effects can be lumped into isolated components, then the input/output equations for these components are already known; they are the governing differential equations for the plant dynamics. Further, if the dynamic effects are lumped into isolated components, then the input/output equations for the remaining components can be obtained from steady state data since these components are assumed to contain no dynamic effects. This approach was applied to the current modeling problem and the reduced component model of Figure 3.3 was produced.

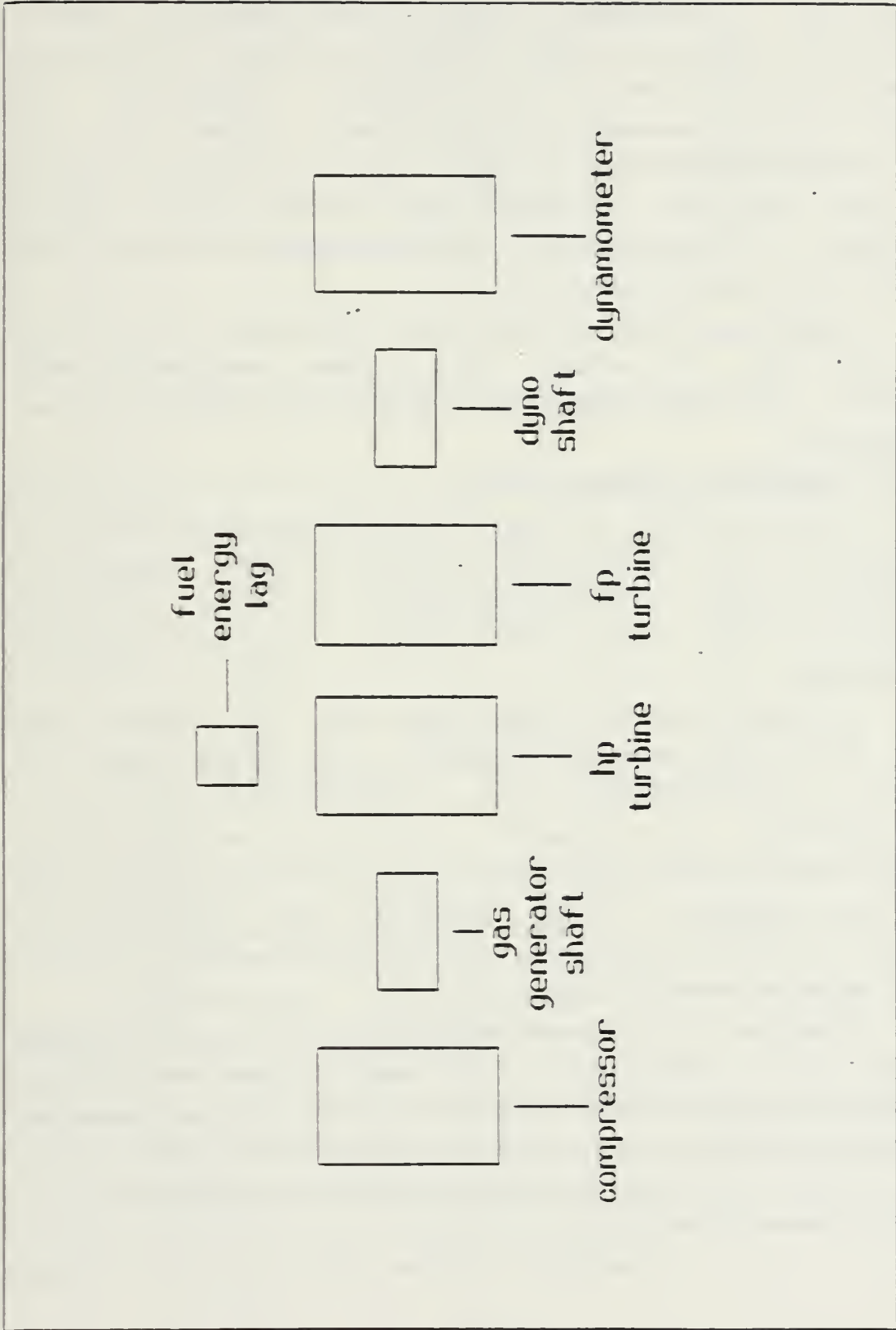


Figure 3.3 Reduced Component Model

In this work two dynamic effects are the accelerations of the gas generator and the power turbine/dynamometer. By lumping the entire gas generator inertia into the gas generator shaft, the gas generator acceleration dynamics were isolated to that component. Similarly, the power turbine/dynamometer dynamics were lumped into the power turbine/dynamometer shaft. The third dynamic effect, the fuel combustion dynamics, was lumped into a single component, a first order lag between the fuel flowrate input and the high pressure turbine.

Since no dynamic effects were considered to occur in the inlet bell or exhaust duct, these components were combined with the compressor and free power turbine, respectively.

##### 5. Component Inputs/Outputs

The next step in formulating the conceptual model is determining the inputs and outputs of each component. Multiport analysis using signal pairs at "ports" of power transfer is one useful method for studying component interaction.

At the mechanical-rotational port (gas generator and power turbine/dynamometer shafts ) the signal pair is torque,  $Q$ , and rotational speed,  $N$ , as shown in Figure 3.4. More difficult to represent is the thermofluid power transfer between the compressor, high pressure turbine, and free power turbine. If the fluid flow were incompressible the port would be represented by a pressure-volume flowrate signal pair as shown in Figure 3.5.

However, this simple representation is not adequate for the case of compressible flow since it does not account for thermal energy transfer via the fluid internal energy. One could represent this port as shown in Figure 3.6 where  $U = M * u$ , with  $M$  the mass flowrate and  $u$  the fluid specific internal energy.

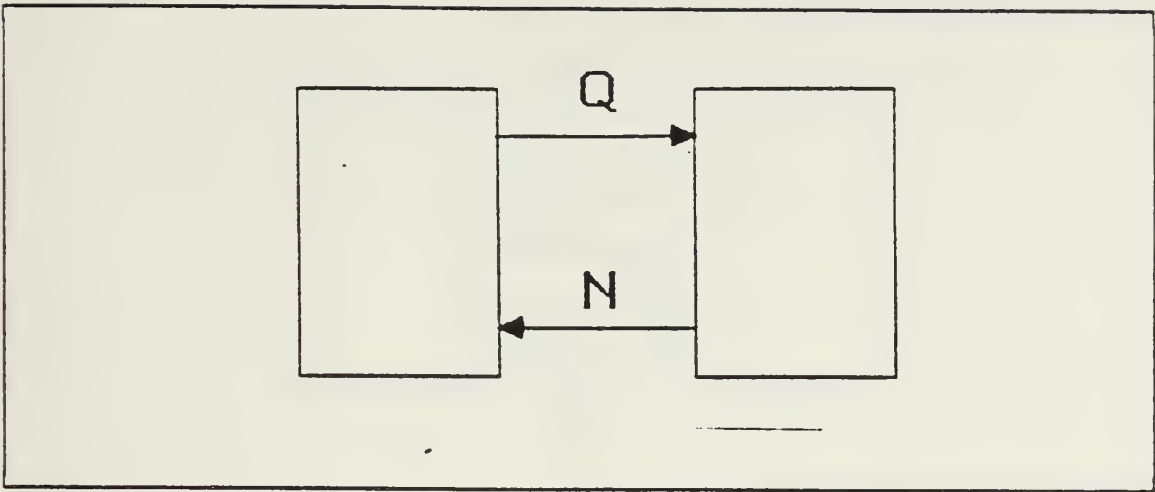


Figure 3.4 Mechanical-Rotational Port

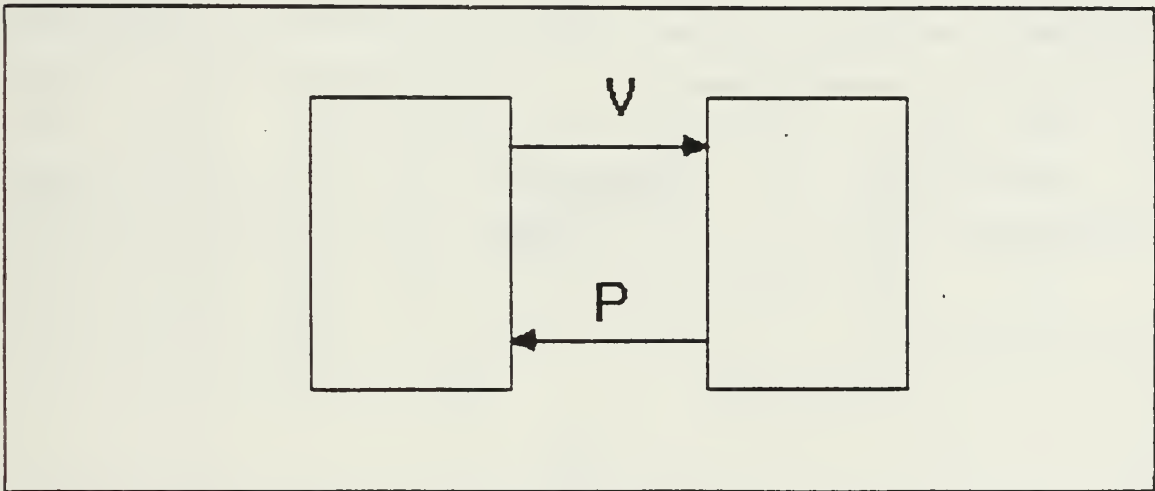


Figure 3.5 Incompressible Fluid Port

Representing internal energy as the product of specific heat ( $C_v$ ) and temperature, the port could be rewritten as shown in Figure 3.7.

One might now attempt to combine effects and describe the complete thermofluid power transfer as shown in Figure 3.8.

However, since the variables  $P, V, M,$  and  $T$  are related through the equations of state, it is redundant to measure all four in the modeling process.

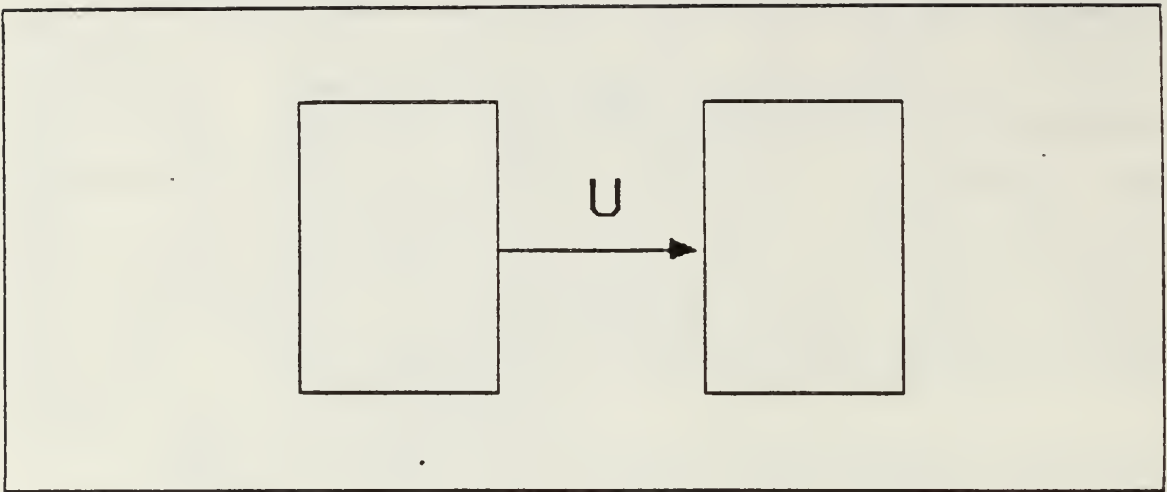


Figure 3.6 Thermal Port

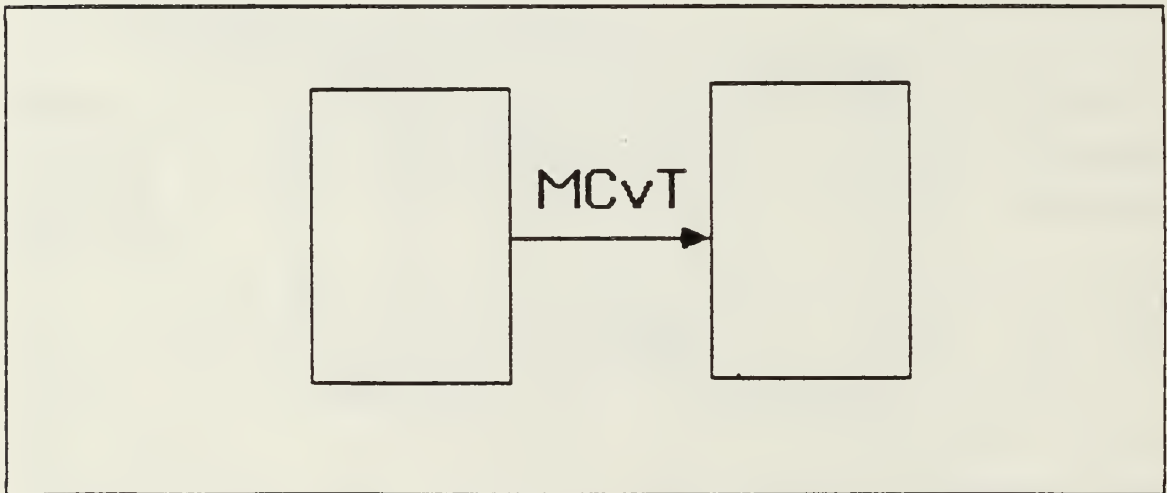


Figure 3.7 Alternate Thermal Port

In considering which variable to eliminate it should be noted that since the direction of mass flow and volume flow must be the same, and since temperature is "carried along" with the mass flow, these three variables have the same signal flow direction. Thus, elimination of the pressure variable was considered unwise since this would essentially eliminate the two-way component interaction. Elimination of temperature from the set of independent



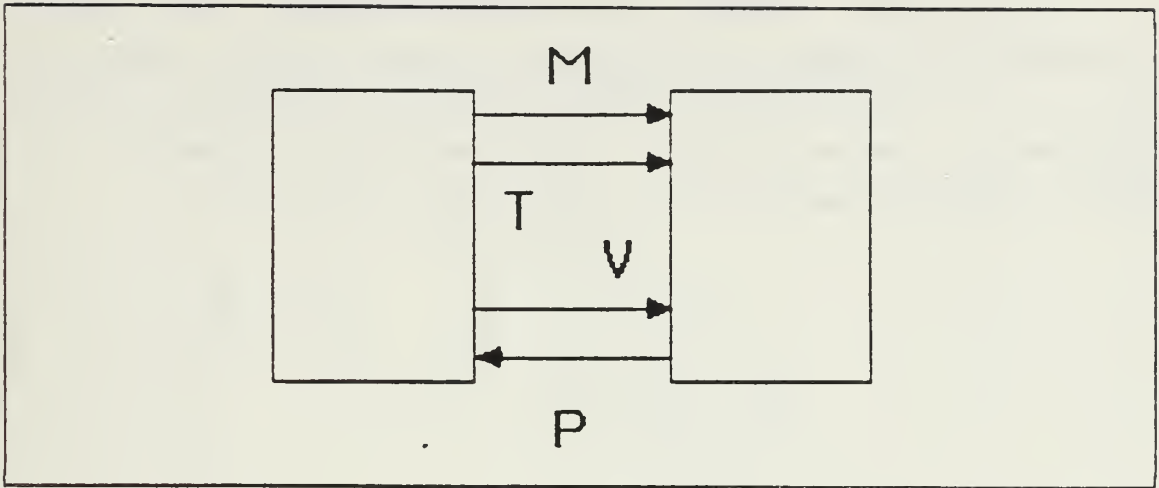


Figure 3.8 Combined Port

variables was considered a poor choice due to its ease of measurement relative to either mass or volume flowrate. Finally, since mass flowrate is conserved while volume flowrate is not, and since this conservation might lead to simplification in future measurements and calculations, it was decided that volume flowrate,  $V$ , would be eliminated. The resulting power port is shown in Figure 3.9.

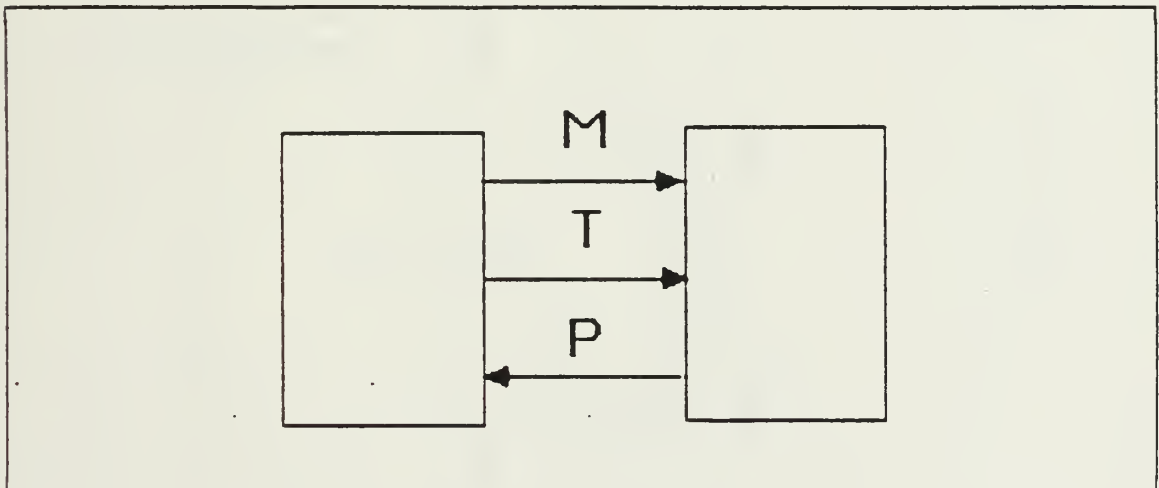


Figure 3.9 Thermodynamic Power Port

Using this concept of the thermodynamic power port the complete multiport diagram was constructed as shown in Figure 3.10. Note that variable ambient conditions were eliminated as system inputs by using corrected variables, a commonly employed technique in gas turbine analysis.

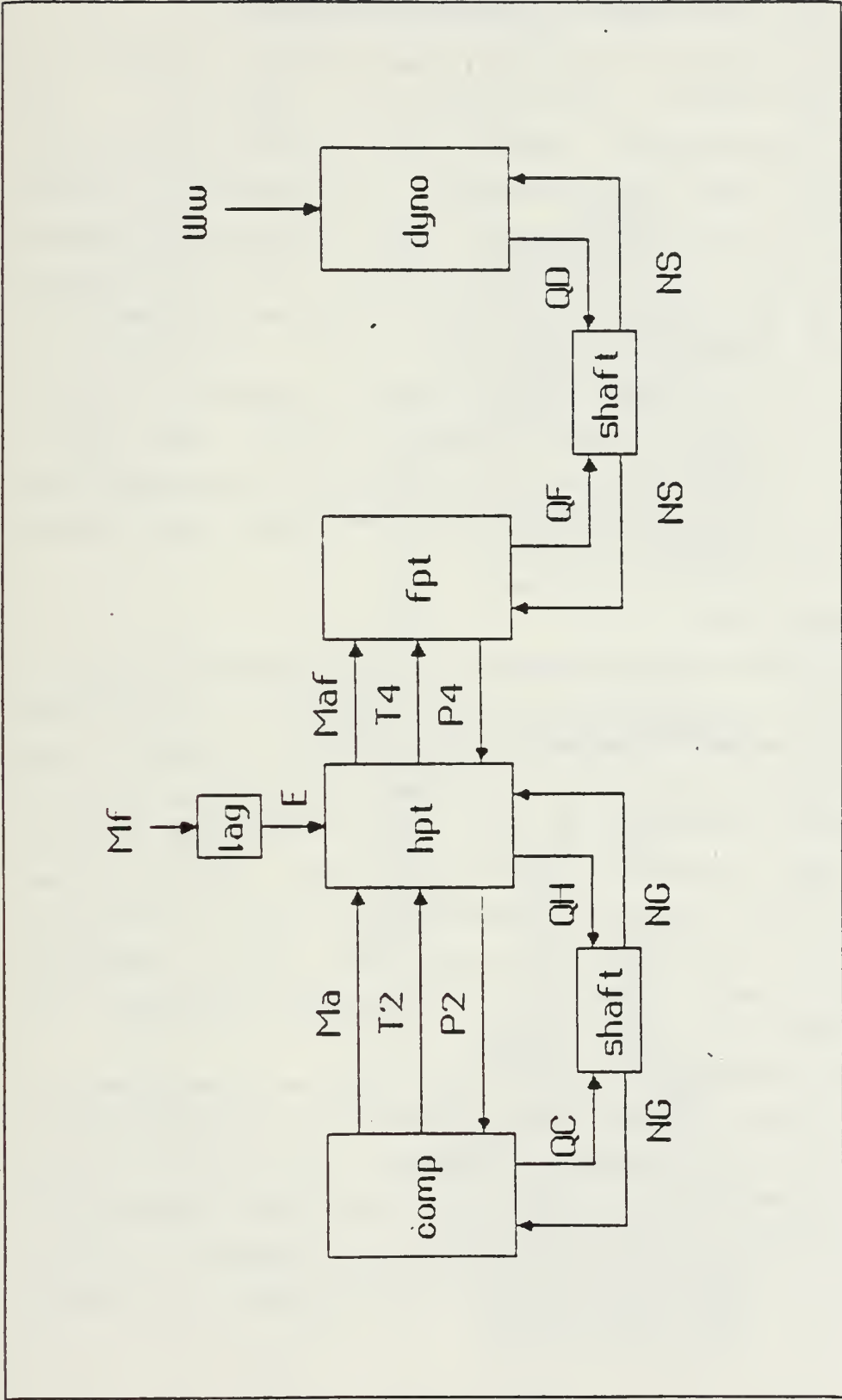


Figure 3.10 Complete Multipoint Diagram

#### IV. QUANTITATIVE COMPONENT MODELING

From the multiport diagram of the previous chapter the component input/output relationships are identified. The next step in the modeling process is to obtain quantitative expressions for these relationships. In this model we have assumed that the gas generator and power turbine/dynamometer shafts, and the fuel energy lag contain the plant dynamic effects. The quantitative relation for these components is the governing differential equations 3.1 , 3.2 and 3.3. Further, since it has been assumed that the remaining components contain no significant dynamic effect, the input/output equations for these components can be obtained from steady state data. The following describes how these equations were obtained.

##### A. DATA ACQUISITION

The gas turbine and dynamometer is instrumented as indicated in Table 1. The data acquisition system is controlled by an HP-85 personal computer. Temperature, speeds, and torques are taken using an HP-3497A Data Acquisition/Control Unit. Pressure readings are taken using a Pressure Systems DPT-6400. Fuel flowrate is obtained by the operator from two rotometers and entered interactively or from a turbine flowmeter. An HP-82902M flexible disk drive provides program/data storage capability. A Digital DECWRITER IV printer provides hard copy output.

Data was taken at 93 operating points as indicated in Table 2. These points were selected to provide full coverage of the plant operating envelope. At each operating point temperature, speed, and torque values were sampled 30 times and averaged. Pressure values were sampled 8 times and averaged. A copy of the acquisition program is included as Appendix A.

TABLE 1  
GAS TURBINE/DYNAMOMETER INSTRUMENTATION

| Parameter                           | Symbol | Instrumentation          |
|-------------------------------------|--------|--------------------------|
| Compressor Inlet Temp.              | T1     | 4 type T thermocouples   |
| Compressor Disch. Temp.             | T2     | 4 type T thermocouples   |
| High Pressure Turbine Inlet Temp.   | T3     | 4 type K thermocouples   |
| High Pressure Turbine Disch. Temp.  | T4     | 4 type K thermocouples   |
| Cell Pressure                       | P0     | 2 static pressure probes |
| Inlet Bell Pressure                 | P1     | 2 static pressure probes |
| Compressor Disch. Pressure          | P2     | 2 static pressure probes |
| High Pressure Turbine Disch. Press. | P4     | 1 static pressure probes |
| Gas Generator Speed                 | NG     | 1 tachometer generator   |
| Dynamometer Speed                   | NS     | 1 RF speed sensor        |
| Dynamometer Torque                  | OD     | 1 RF torque sensor       |
| Fuel Flowrate                       | MF     | 2 Rotometers             |
| Fuel Flowrate                       | ME     | 1 Turbine Flowmeter      |



## B. DATA REDUCTION

Data reduction took place in two phases. In the first phase average values, generator torque, air mass flowrate, and corrected values were computed. These calculations are part of the data acquisition program (Appendix A).

In the second phase, curve fits were obtained for the input/output relations of each turbine component using the method of least squares [Ref. 7:p. 153] The program which performed the least squares fit is included as Appendix B. Using this program, three types of curve fit were obtained for each input/output relation. The first is a "complete quadratic" curve fit shown in equation 4.1,

$$Y = C1*X1^2 + C2*X1*X2 + C3*X2^2 + C4*X1 + C5*X2 + C6 \quad (4.1)$$

where Y = output (dependent) variable,

X1,X2 = input (independent) variables,

C1,C2,C3,C4,C5,C6, = constant coefficients.

The second type of curve fit obtained was a "reduced quadratic", so called because the cross product terms (ie., X1\*X2) found in the "complete quadratic" curve fit were excluded. Equation 4.2 is an example of this format.

$$Y = C1*X1^2 + C2*X2^2 + C3*X1 + C4*X2 + C5 \quad (4.2)$$

The third curve fit type was a linear curve fit. Equation 4.3 is an example of this format.

$$Y = C1*X1 + C2*X2 + C3 \quad (4.3)$$

In each case the result of the curve fit program is the coefficients of the curve fit equation. Because the magnitude of some variables is much larger than others (ie., NG = 30,000 rpm, P4 = 17 psia ) it was necessary to scale the

TABLE 2  
GAS TURBINE DATA ACQUISITION SCHEDULE

| GAS GENERATOR<br>SPEED, NG<br>(RPM) | DYNAMOMETER<br>SPEED, NS<br>(RPM) | GAS GENERATOR<br>SPEED, NG<br>(RPM) | DYNAMOMETER<br>SPEED, NS<br>(RPM) |
|-------------------------------------|-----------------------------------|-------------------------------------|-----------------------------------|
| 19078.73                            | 549.12                            | 19400.72                            | 563.30                            |
| 21128.36                            | 557.66                            | 21829.68                            | 557.98                            |
| 22547.57                            | 562.21                            | 23208.31                            | 563.58                            |
| 23891.30                            | 566.05                            | 24584.86                            | 569.89                            |
| 25280.03                            | 565.37                            | 25922.19                            | 573.93                            |
| 26665.44                            | 567.74                            | 27331.84                            | 569.30                            |
| 28726.66                            | 576.29                            | 29382.51                            | 580.98                            |
| 30067.85                            | 580.45                            | 30825.73                            | 587.61                            |
| 31525.20                            | 582.29                            | 32533.96                            | 584.86                            |
| 33488.27                            | 593.19                            | 19080.00                            | 935.15                            |
| 19254.72                            | 946.33                            | 21160.08                            | 958.80                            |
| 21854.58                            | 954.31                            | 22570.12                            | 952.79                            |
| 23270.02                            | 957.89                            | 23968.66                            | 953.97                            |
| 24516.74                            | 954.13                            | 25285.25                            | 959.41                            |
| 25988.33                            | 968.10                            | 26635.89                            | 965.15                            |
| 27296.90                            | 964.39                            | 28080.53                            | 969.07                            |
| 28796.48                            | 971.97                            | 29448.34                            | 976.55                            |
| 30080.00                            | 989.08                            | 30824.83                            | 979.37                            |
| 31543.90                            | 977.28                            | 32476.51                            | 978.31                            |
| 33490.05                            | 981.56                            | 34504.89                            | 983.94                            |
| 35372.62                            | 996.06                            | 19088.39                            | 1428.13                           |
| 21112.06                            | 1441.88                           | 21852.49                            | 1431.24                           |
| 22577.27                            | 1444.77                           | 23202.79                            | 1436.46                           |
| 23896.71                            | 1445.22                           | 24476.83                            | 1438.68                           |
| 25259.17                            | 1442.62                           | 25919.51                            | 1442.97                           |
| 26508.37                            | 1455.67                           | 27302.78                            | 1453.57                           |
| 27917.37                            | 1452.72                           | 28612.59                            | 1446.09                           |
| 29370.06                            | 1468.75                           | 30036.55                            | 1458.07                           |
| 30694.21                            | 1460.35                           | 31568.65                            | 1456.94                           |
| 32464.30                            | 1459.62                           | 33358.12                            | 1461.41                           |
| 23925.74                            | 1934.28                           | 24574.83                            | 1953.73                           |
| 25269.44                            | 1943.66                           | 25845.15                            | 1943.32                           |
| 26637.27                            | 1944.69                           | 27287.50                            | 1946.16                           |
| 27807.57                            | 1944.34                           | 28665.43                            | 1947.56                           |
| 29131.64                            | 1933.95                           | 29985.26                            | 1954.42                           |
| 30443.17                            | 1939.51                           | 31485.56                            | 1961.59                           |
| 32379.32                            | 1974.51                           | 33144.56                            | 1938.01                           |
| 34523.04                            | 1951.02                           | 35366.35                            | 1963.19                           |
| 27344.96                            | 2432.68                           | 28000.63                            | 2421.92                           |
| 28696.43                            | 2441.53                           | 29346.11                            | 2433.45                           |
| 30057.51                            | 2436.86                           | 30736.87                            | 2429.97                           |
| 31489.43                            | 2431.06                           | 32441.26                            | 2441.16                           |
| 33358.05                            | 2440.31                           | 29370.30                            | 2922.37                           |
| 30060.52                            | 2918.94                           | 30653.77                            | 2906.41                           |
| 31528.78                            | 2927.09                           | 32413.38                            | 2917.06                           |
| 33291.47                            | 2930.93                           | 34366.77                            | 2917.24                           |

variables to prevent algorithmic singularities during the least squares solution. This was accomplished by dividing each variable by a scaling factor. The scaling factors, shown in table 3, were selected so that each variable had a range of 0.0 to 1.0 when scaled.

TABLE 3  
SCALING FACTORS

| Variable                                   | Scaling Factor |
|--|----------------|
| Gas Generator Speed, NG                    | 36,000 rpm.    |
| Compressor Torque, Qc                      | 130 ft. lb.    |
| Air Mass Flowrate, Ma                      | 13,000 lb/hr.  |
| Compressor Discharge Temperature, T2       | 800 deg. R.    |
| Compressor Discharge Pressure, P2          | 43.0 psia.     |
| Fuel Mass Flowrate, Mf                     | 240 lb/hr.     |
| High Pressure Turbine Torque, QH           | 130 ft. lb.    |
| Combined Air/Fuel Mass Flowrate, Maf       | 13,000 lb/hr.  |
| High Pressure Turbine Discharge Temp., T4  | 1800 deg. R.   |
| High Pressure Turbine Discharge Press., P4 | 20.0 psia.     |
| Dynamometer Speed, NS                      | 3,000 rpm.     |
| Free Power Turbine Torque, QF              | 480 ft. lb.    |

## V. STEADY STATE PLANT MODEL

### A. STEADY STATE MODEL ALGORITHM

With the input/output component relations defined in equation form the next step was to link these relations together to form a steady state plant model. Figure 5.1 presents the flowchart describing the steady plant state model algorithm. In this algorithm the program user inputs the gas generator and dynamometer speeds at which the plant parameters are to be evaluated. The program makes an initial guess at the steady state fuel flowrate,  $M_f$ . A guess is also made for the compressor and high pressure turbine discharge pressures,  $P_2$  and  $P_4$ . The program uses these assumed values to calculate the compressor and high pressure turbine outputs. The computed compressor discharge pressure is compared with the assumed value. If the difference between assumed and computed value exceeds the specified tolerance, the value of  $P_2$  is updated. Otherwise, the power turbine outputs are calculated and the computed high pressure turbine discharge pressure is compared with the assumed value. Convergence within the specified tolerance is again required. If this check is met the compressor and high pressure turbine torques are compared.

These torques should be equal in steady state. If they are not the assumed value of fuel flowrate is updated and the entire process is repeated. The steady state computer model is included as Appendix C.

### B. STEADY STATE MODEL RESULTS

The steady state computer program was tested at various points in the plant operating envelope. The output of the computer model was compared with the raw data for the same

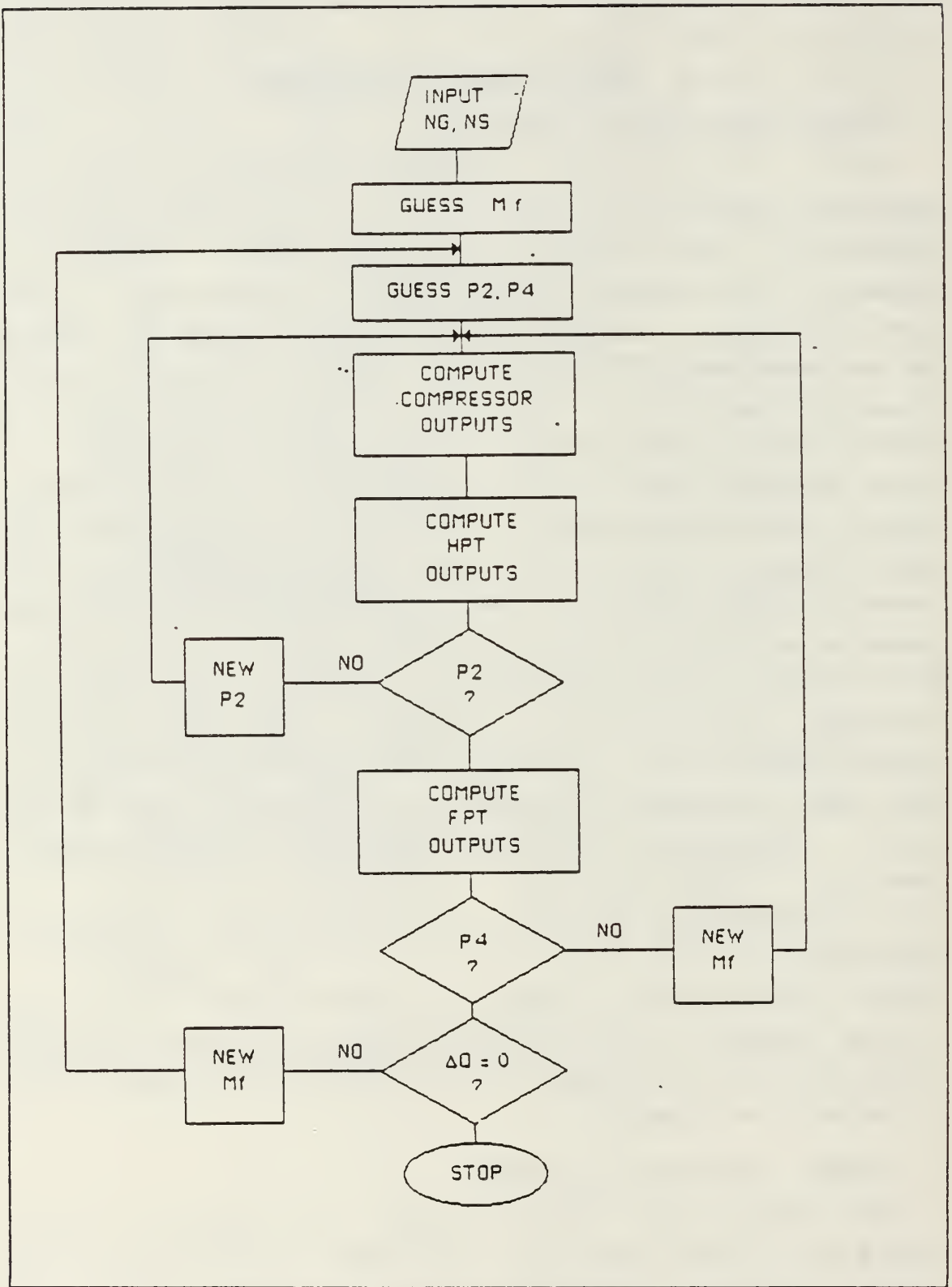


Figure 5.1 Steady State Plant Model Flowchart



operating points. The results showed excellent agreement between the steady state model and the raw data at most operating points. The only exception to this was at extremely high gas generator speeds. A typical comparison is shown in Table 4.

As indicated by the flowchart of Figure 5.1, at any given gas generator speed (NG) and dynamometer speed (NS) combination, the program must hunt for the fuel flow rate that will produce zero torque differential between the compressor and high pressure turbine. An investigation into the nature of the torque differential as a function of fuel flowrate (at fixed NG and NS) provides some interesting insights into the performance characteristics of the engine. As an example, in Figure 5.2 the torque differential is plotted versus fuel flow for NG = 30,000 rpm and NS = 1,100 rpm.

This plot has several interesting features. First, note that there are two values of fuel flowrate that lead to zero torque differential. This suggests that at a given NG/NS combination there are actually two equilibrium conditions. It is thought that the upper fuel flowrate represents a state of inefficient operation. Whatever the source of the higher fuel flowrate condition, comparison with the raw data indicates that the normal operating mode of the turbine is at the lower fuel flowrate.

A second feature of this curve is the peak torque differential. This peak is considered to be a significant characteristic of the gas generator. It is thought to be indicative of the maximum driving torque difference attainable at the specified NG/NS combination. Thus, if one wishes to accelerate the gas generator quickly, this plot indicates the limits of achievable acceleration as well as the optimal fuel input to achieve the greatest acceleration. Clearly, more fuel does not necessarily lead to greater

TABLE 4  
 COMPARISON OF STEADY STATE OUTPUT WITH RAW DATA  
 FOR NG = 25,900 RPM, NS = 970 RPM

| Parameter                           | Symbol | Steady State<br>Computer Output | Raw Data     |
|-------------------------------------|--------|---------------------------------|--------------|
| Compressor Torque                   | QC     | 69.8 ft.lb.                     | 69.4 ft.lb.  |
| Compressor Disch. Temp.             | T2     | 658 deg.R.                      | 550 deg.R.   |
| High Pressure Turbine Disch. Temp.  | T4     | 1354 deg.R.                     | 1361 deg.R.  |
| Compressor Disch. Pressure          | P2     | 27.41 psia.                     | 27.42 psia.  |
| High Pressure Turbine Disch. Press. | P4     | 16.36 psia.                     | 16.36 psia.  |
| Free Power Turbine Torque           | QE     | 151.7 ft.lb.                    | 150.5 ft.lb. |
| Fuel Flowrate                       | Mf     | 110.8 lb/hr.                    | 110.3 lb/hr. |
| Air Mass Flowrate                   | Ma     | 8696 lb/hr.                     | 8742 lb/hr.  |

acceleration. In fact, this plot suggests that too large a fuel increase can lead to deceleration. One should note, however, that this condition may be impossible to achieve practically, since it presumes that this large fuel change can be made instantly, without changing the NG/NS combination (ie., a perfect step). The fuel energy lag dynamics seem to exclude this possibility in the current application. Further, the existing fuel control devices on most gas turbine facilities would likely prevent this condition from being observed.

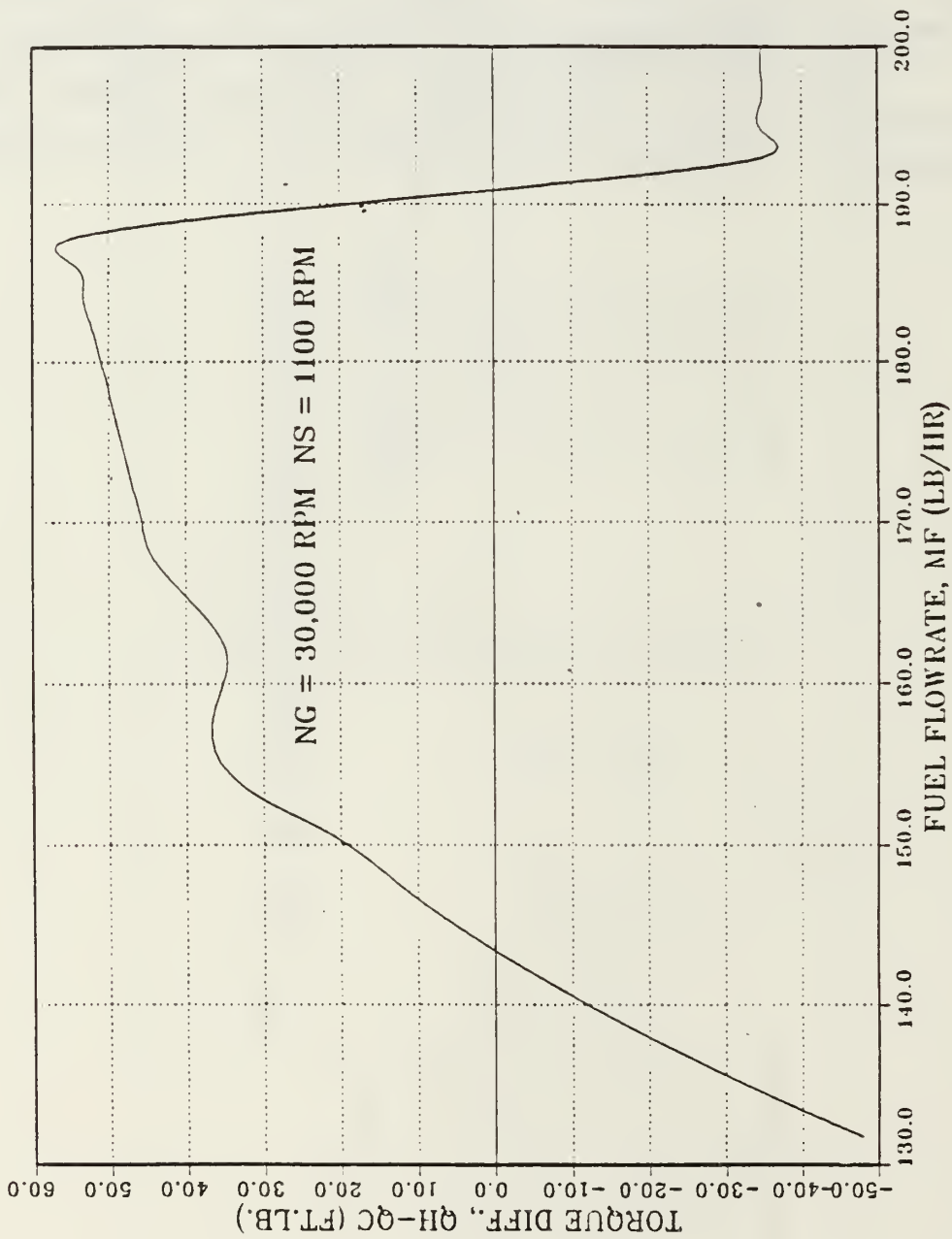


Figure 5.2 Torque Differential . vs. Fuel Flowrate

## VI. NONLINEAR DYNAMIC MODEL

The next step was to develop a nonlinear dynamic model by introducing the plant dynamic equations into the steady state model.

In order to implement the governing dynamic equations, the gas generator and power turbine/dynamometer inertias must be known. Johnson [Ref. 3:p. 56] concluded that the combined power turbine/dynamometer inertia (JD) is insensitive to dyno water weight and that a value of  $JD = 0.6738 \text{ lb. ft. s}^2$  was valid throughout the operating range.

The following section describes the determination of the gas generator inertia. Subsequently, the development and results of the nonlinear dynamic model is described.

### A. GAS GENERATOR INERTIA

The technical manual for the Boeing 502-6A gas turbine engine [Ref. 8:p. 6] lists the gas generator inertia (-JG) as  $0.11 \text{ in. lb. s}^2$ . However, it was unclear whether this inertia value included the accessory gearbox inertia. Further, the equipment configuration at the NPS test facility is somewhat different than the standard configuration described in the technical manual. Because the gas generator inertia is crucial to accurate dynamic performance prediction, it was desirable to verify the technical manual value experimentally.

In order to experimentally determine the gas generator inertia, the gas generator inlet bell and nose cone was removed. A lever arm was attached to the compressor impeller using existing bolt holes intended for impeller removal. [Ref. 8:p. VII-10]. A spring was attached at each end of the lever arm and secured to the base of the turbine. The resulting experimental set-up is shown in Figure 6.1.



Finally, a potentiometer was attached to the lever arm and aligned with the impeller shaft centerline to permit measurement of impeller angular position.

The lever was deflected and released from rest. Using a strip chart recorder the oscillatory motion of the gas generator was recorded. This procedure was repeated ten times so that good average values could be obtained.

A simplified diagram of the experimental apparatus is given in Figure 6.2, where  $K$  is the effective spring constant,  $J$  is the total polar mass moment of inertia about the gas generator axis,  $\theta$  is the angle of rotation, and  $c$  is the system damping due to friction. From this simplified diagram the differential equation for viscously damped free vibration is found to be:

$$J \ddot{\theta} + C \dot{\theta} + K \theta = 0 \quad (6.1)$$

The solution to this equation [Ref. 9:p. 25-32] for the underdamped case reveals the frequency of damped oscillation to be:

$$W_d = W_n \sqrt{1 - \zeta^2} \quad (6.2)$$

where  $W_d$  = frequency of damped oscillation  
 $W_n$  = natural frequency  
 $\zeta$  = damping ratio.

Using average values, the frequency of damped oscillation was determined from the strip chart readings to be:

$$W_d = 67.544 \text{ rad/sec}$$

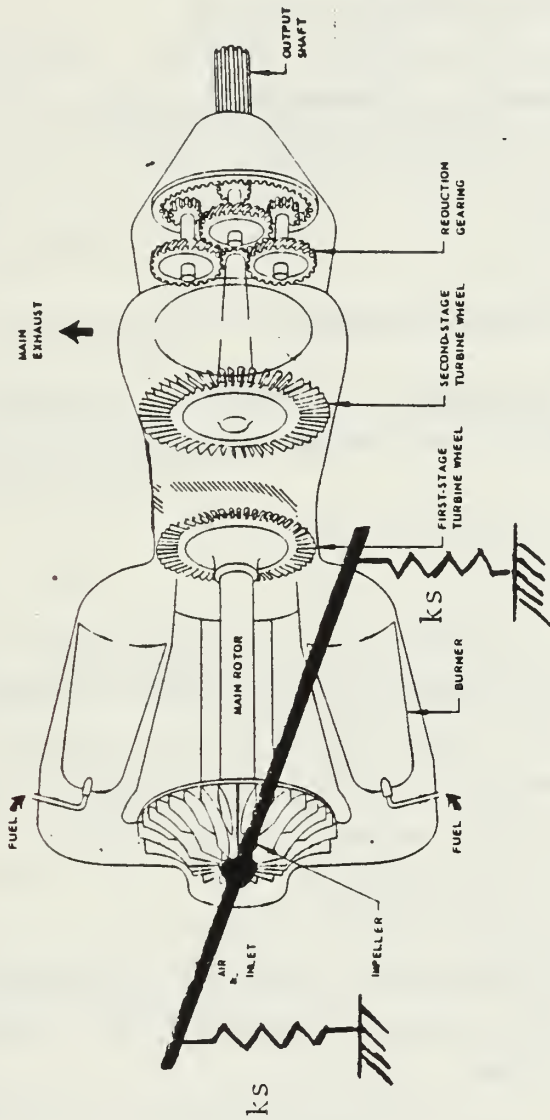


Figure 6.1 Experimental Apparatus for JG Determination  
 [Ref. 8: fig. 16., p. V-1]

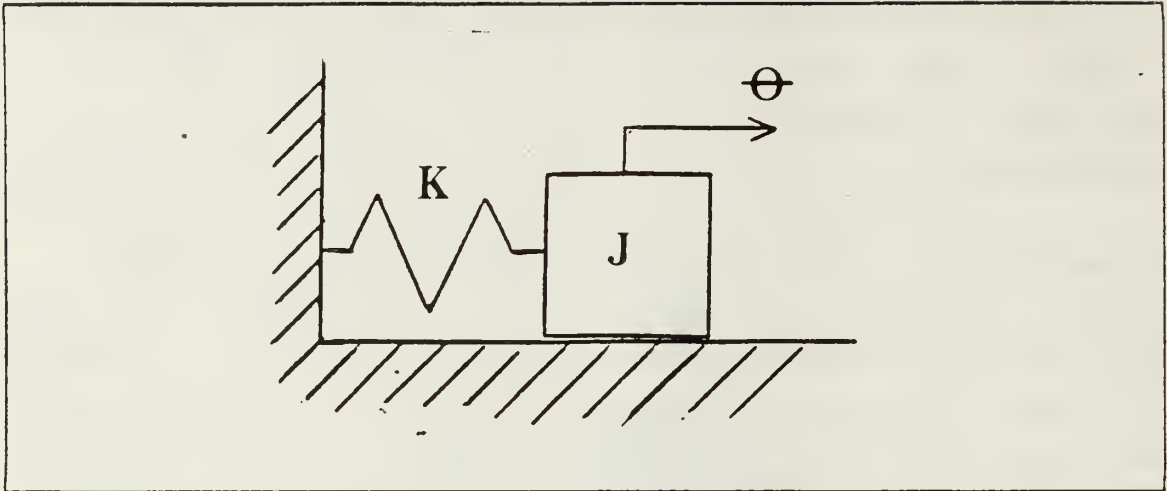


Figure 6.2 Simplified Diagram of Experimental Apparatus

Also from the solution to the free vibration equation, the following relation involving the damping ratio is found:

$$2 \pi \zeta / \sqrt{1 - \zeta^2} = (1/n) * \ln(X_0/X_n) \quad (6.3)$$

where  $n$  = number of elapsed oscillations,  
 $X_0$  = original oscillation amplitude,  
 $X_n$  = amplitude after  $n$  cycles.

Again using average experimental values, the damping ratio was determined from equation 6.3 to be:

$$\zeta = 0.0325$$

Using the experimentally obtained damping ratio and damped frequency, the natural frequency,  $\omega_n$ , was determined from equation 6.2 to be:

$$\omega_n = 67.5799 \text{ rad/sec}$$

The natural frequency of the system is also given by:

$$\omega_n = K/J. \quad (6.4)$$

For this system the effective spring constant, K, is:

$$K = 2 * k_s * R^2 \quad (6.5)$$

where  $k_s$  = individual spring constant,  
 $R$  = distance from gas generator axis to  
spring attachment point.

The individual spring constants were experimentally determined to be  $k_s = 6.891 \text{ lb./in.}$ , with  $R = 7.0 \text{ inches}$ . Solving for the effective spring constant, K, using equation 6.5 the total system inertia, J, was calculated from equation 6.4 to be:

$$J = 0.14786 \text{ in. lb. s}^2$$

The total inertia is equal to the sum of the individual inertia effects of the gas generator rotor (JG), lever arm (JL), and springs (JS):

$$J = JG + JL + JS. \quad (6.6)$$

The lever arm inertia was calculated as:

$$JL = m_l * l^2 / 12 = 0.014457 \text{ in. lb. s}^2 \quad (6.7)$$

where  $m_l$  = mass of the lever arm,  
 $l$  = length of the lever arm.

The combined inertia of both springs was calculated using Rayleigh's method to be:

$$JS = 2 * m_s * R^2 / 3 = 0.01914 \text{ in. lb. s}^2 \quad (6.8)$$

where  $m_s$  = mass of each spring.

With the total (J), spring (JS), and lever (JL) inertias determined, the gas generator inertia was found using equation 6.6 to be:

$$JG = 0.1143 \text{ in. lb. s}^2$$

## B. NONLINEAR DYNAMIC PROGRAM

The nonlinear dynamic program was formulated using Discrete Simulation Language (DSL). The flowchart describing the dynamic program algorithm is given in Figure 6.3. The user must enter the fuel flowrate and dynamometer water weight as a function of time by editing the program prior to execution. Upon execution of the program the user interactively enters the initial gas generator and dynamometer speeds. The steady state program is then called to determine the equilibrium value of fuel flowrate,  $M_{fo}$ , and dynamometer water weight,  $W_{wo}$ . A time step is then taken and the new fuel flowrate and water weight is determined. The dynamic effect of the fuel energy lag is then computed. The steady state program is again used to determine the compressor, high pressure turbine, free power turbine, and dynamometer torques ( $Q_C$ ,  $Q_H$ ,  $Q_F$ ,  $Q_D$  respectively). These torques are entered into the dynamic equations describing the gas generator and dynamometer accelerations. accelerations are integrated to obtain speeds. A check is made to determine if the run time is exceeded. If not, time is again incremented and the loop repeats. A copy of the nonlinear dynamic program is included as Appendix D.

In order to validate the nonlinear dynamic program the propulsion plant test facility was subjected to step changes in commanded fuel flowrate voltage. The resulting fuel flowrate, gas generator speed, and dynamometer speed was

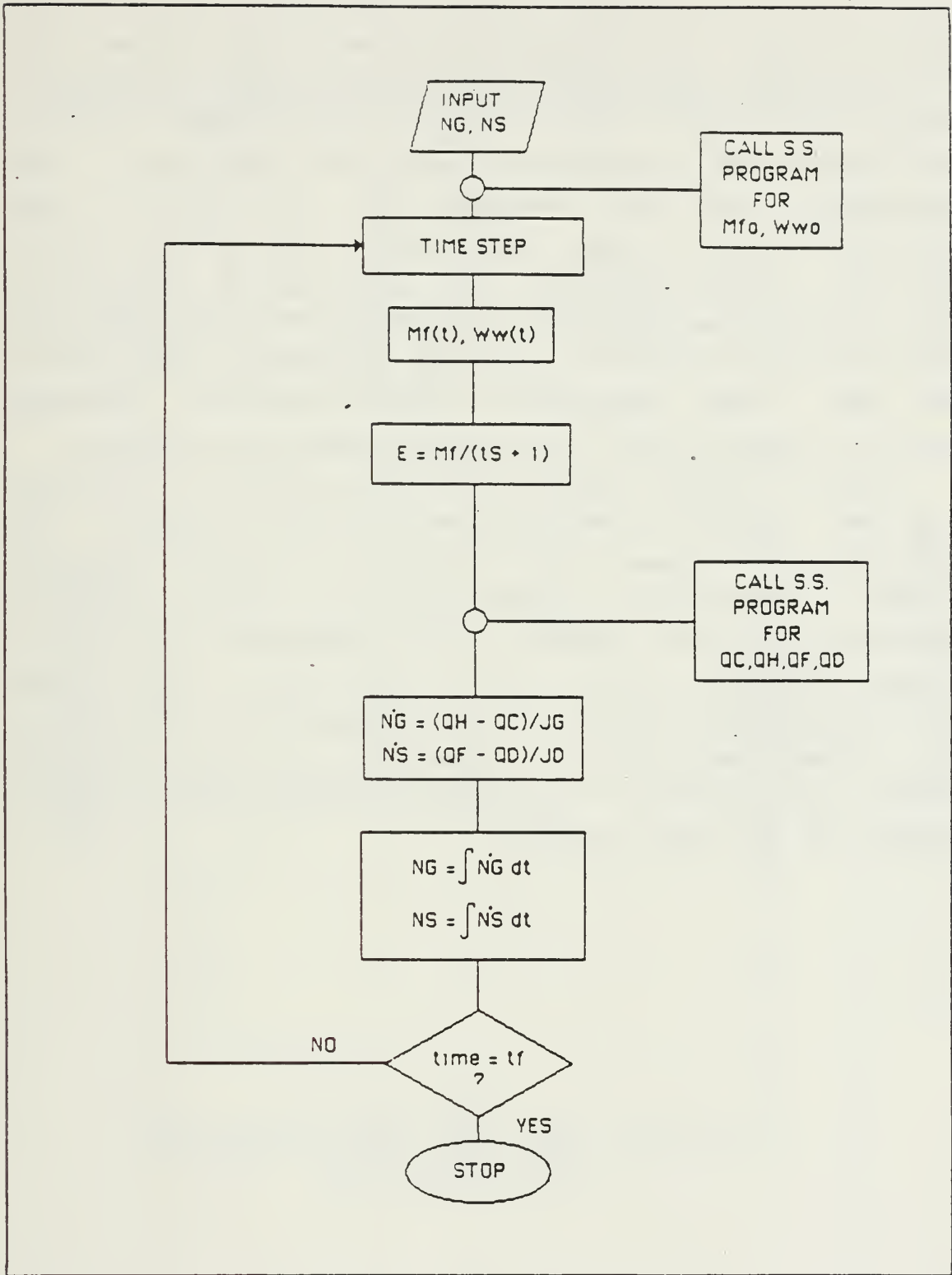


Figure 6.3 Flowchart for Nonlinear Dynamic Program



recorded using a multichannel strip chart. The recorded fuel flowrate versus time was entered into the dynamic program in tabular form and was used to exercise the program. Various acceleration and deceleration tests were conducted. The experimental data were compared with the output of the nonlinear dynamic program. Figures 6.4, 6.5, and 6.6 illustrate the results obtained. In this case an increase in fuel flowrate was applied to accelerate the gas generator from 25,000 to 29,500 rpm and the dynamometer from 960 to 1090 rpm. This represents a large transient, covering nearly one third of the gas generator operating envelope.

Figure 6.4 shows the fuel flowrate transient in response to a step change in commanded fuel flowrate voltage. The discontinuities shown result from the discrete sampling effects of the digital flowmeter, and the unsteady nature of the fuel flow at the location of the flowmeter, just downstream of the fuel control valve. Figures 6.5 and 6.6 show the resulting transients of the gas generator and dynamometer. Experimental data is plotted along with the nonlinear dynamic model results. The results show excellent agreement between the data and the model.

# FUEL FLOW INPUT

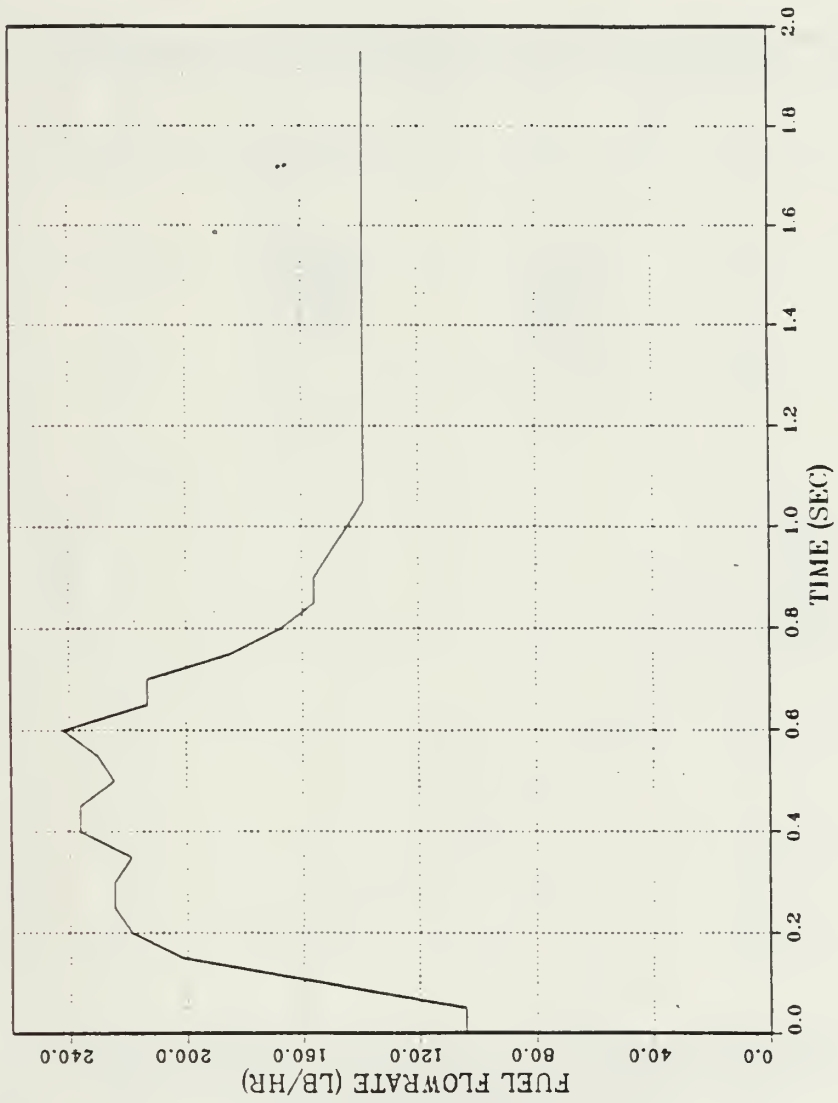


Figure 6.4 Fuel Flowrate Input

# NONLINEAR MODEL RESULTS

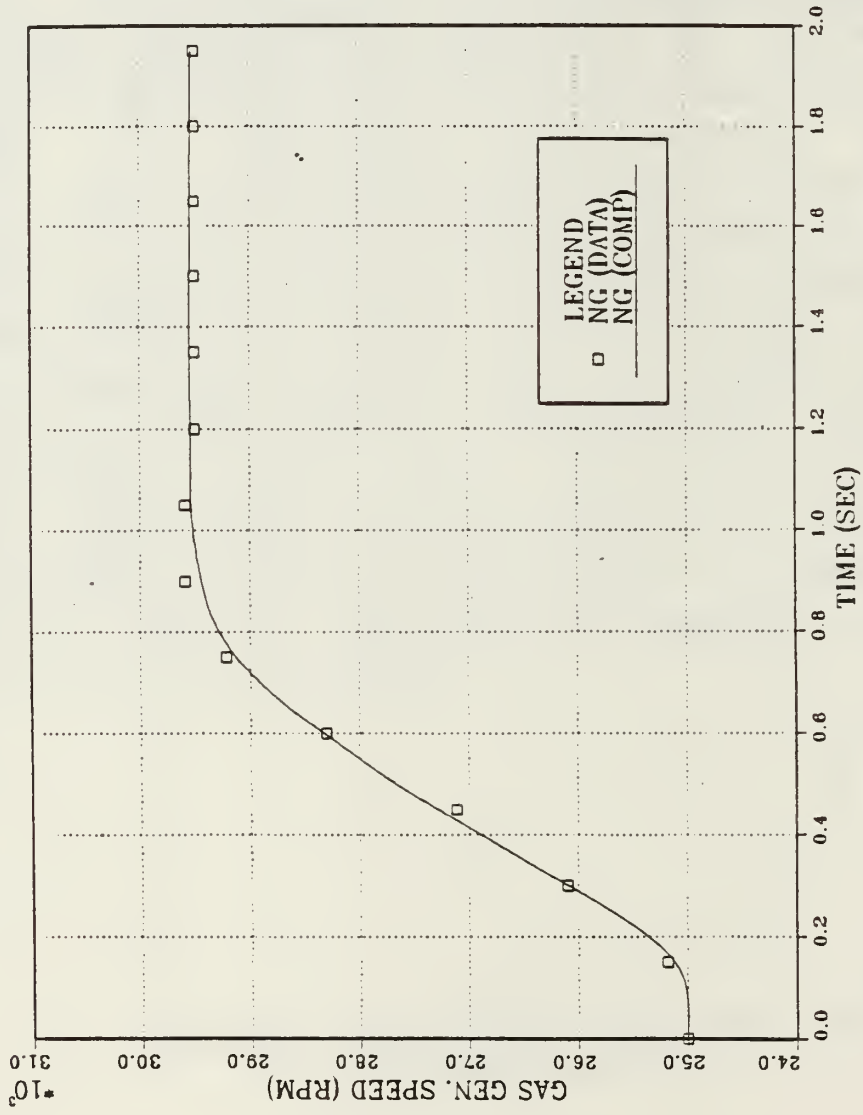


Figure 6.5 Gas Generator Response

# NONLINEAR MODEL RESULTS

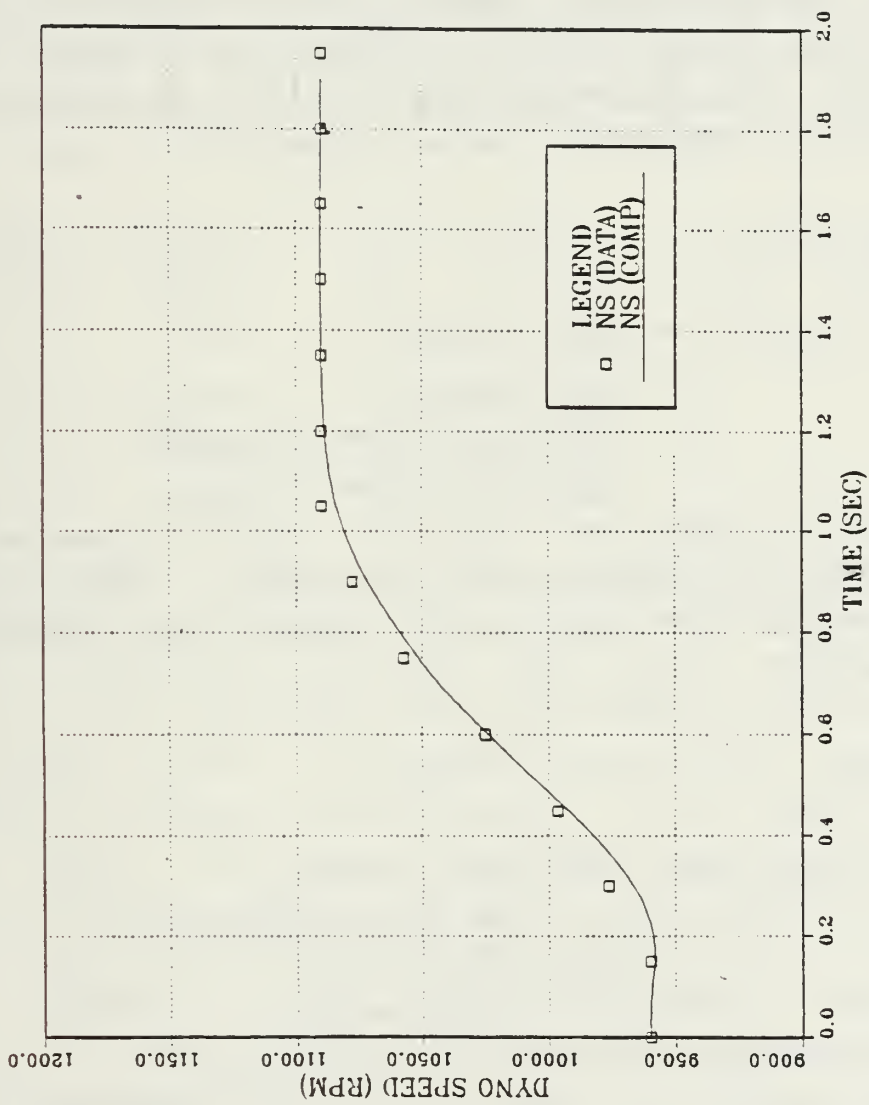


Figure 6.6 Dynamometer Response

## VII. STATE SPACE MODEL

Among modern control theory techniques, the linear quadratic regulator (LQR) method is the most highly developed. This method coordinates multiple inputs simultaneously and provides a straightforward manner in which the feedback gain matrix can be manipulated to achieve the desired system performance. The LQR method calls for the system to be represented in state space form as shown below:

$$\dot{X} = A*X + B*U \quad (7.1)$$

where  $X$  = state vector,  
 $U$  = input vector,  
 $A$  = state coefficient matrix,  
 $B$  = input coefficient matrix.

In order to arrive at the state space representation, one must resort to perturbational variables. The excursion of any variable,  $X$ , away from its initial condition can be represented by:

$$X = X_0 + x \quad (7.2)$$

where  $X_0$  = the initial value,  
 $x = dX$  = the perturbation from  
the initial value,  
 $X$  = the current value.

Any variable can be represented in this manner.

In this study the states are the gas generator speed (NG), power turbine/dynamometer speed (NS), and mechanical energy resulting fuel combustion (E). This selection is mandated by the dynamic equations of 3.1, 3.2, and 3.3, one state per derivative term [Ref. 10:p. 665]. The plant

inputs are the fuel flowrate (Mf) and the dynamometer water weight (Ww). Using perturbational variables the state space equation becomes:

$$\begin{Bmatrix} \dot{n}g \\ \dot{n}s \\ \dot{e} \end{Bmatrix} = A \begin{Bmatrix} ng \\ ns \\ e \end{Bmatrix} + B \begin{Bmatrix} mf \\ ww \end{Bmatrix} .$$

What remains to be done is to determine the elements of the 'A' and 'B' matrices, which contain the coefficients of the state equation set. We can write these elements symbolically as:

$$\begin{array}{lll} a_{11} = \partial \dot{n}g / \partial ng & a_{12} = \partial \dot{n}g / \partial ns & a_{13} = \partial \dot{n}g / \partial e \\ a_{21} = \partial \dot{n}s / \partial ng & a_{22} = \partial \dot{n}s / \partial ns & a_{23} = \partial \dot{n}s / \partial e \\ a_{31} = \partial \dot{e} / \partial ng & a_{32} = \partial \dot{e} / \partial ns & a_{33} = \partial \dot{e} / \partial e \\ \\ b_{11} = \partial \dot{n}g / \partial mf & b_{12} = \partial \dot{n}g / \partial ww & \\ b_{21} = \partial \dot{n}s / \partial mf & b_{22} = \partial \dot{n}s / \partial ww & \\ b_{31} = \partial \dot{e} / \partial mf & b_{32} = \partial \dot{e} / \partial ww & . \end{array}$$

In order to arrive at these coefficients a Taylor series expansion was carried out on each component input/output equation retaining only first order terms. The results is a set of linear equations which can be reduced to the state space form given above. A detailed solution for these coefficients is included as Appendix E. It is important to note that these coefficients vary with operating point. A subroutine was added to the steady state program which evaluates these analytic coefficient expressions at user specified operating points (SUBROUTINE PART in Appendix C). Table 5 shows how the 'A' and 'B' matrices vary with operating point.

Comparison between the state space model and nonlinear dynamic model was conducted by subjecting both to the fuel flowrate inputs used in the nonlinear dynamic program validation. Shown in Figure 7.1 and 7.2 is the response of the



TABLE 5  
 VARIATION OF 'A' AND 'B' MATRICES WITH OPERATING POINT

| NG (rpm) | NS (rpm) | 'A' matrix |        |         | 'B' matrix |      |         |
|----------|----------|------------|--------|---------|------------|------|---------|
| 21,000   | 600      | -5.800     | -0.696 | 1402.2  | 0.00       | 0.00 | 0.00    |
|          |          | 0.155      | -5.803 | 7.822   | 0.00       | 0.00 | -166.3  |
|          |          | 0.000      | 0.000  | -0.500  | 0.50       | 0.00 | 0.00    |
| 26,000   | 1,500    | -17.273    | -1.649 | 2479.4  | 0.00       | 0.00 | 0.00    |
|          |          | 0.317      | -3.430 | -0.3851 | 0.00       | 0.00 | -708.9  |
|          |          | 0.000      | 0.000  | -0.500  | 0.50       | 0.00 | 0.00    |
| 30,000   | 2,000    | -23.39     | -0.950 | 2485.4  | 0.00       | 0.00 | 0.00    |
|          |          | 0.5194     | -3.706 | -5.3616 | 0.00       | 0.00 | -1183.7 |
|          |          | 0.000      | 0.000  | -0.500  | 0.50       | 0.00 | 0.00    |

nonlinear and state space models. In this example the 'A' and 'B' matrices were evaluated at the initial condition. As expected for large perturbations such as this, the state space model, with its linear assumptions, does not accurately describe the behavior of this highly nonlinear plant. The limitations of the state space model are important in that they indicate the limits of the LQR controller design and

help to define necessary transitions between linear approximations. When an accurate global dynamic model of the plant is needed for control testing, the nonlinear model will be used.

# STATE SPACE RESULTS

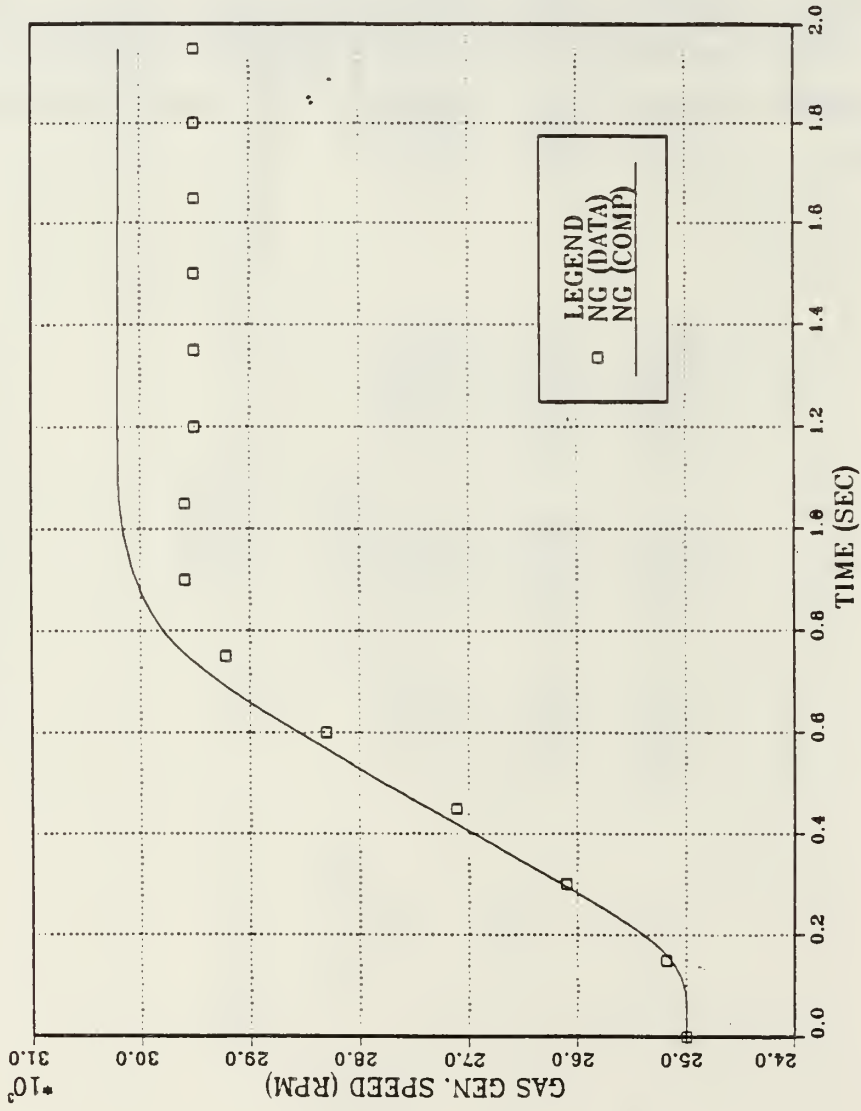


Figure 7.1 Comparison of State Space vs. Nonlinear Model  
Gas Generator Response

# STATE SPACE RESULTS

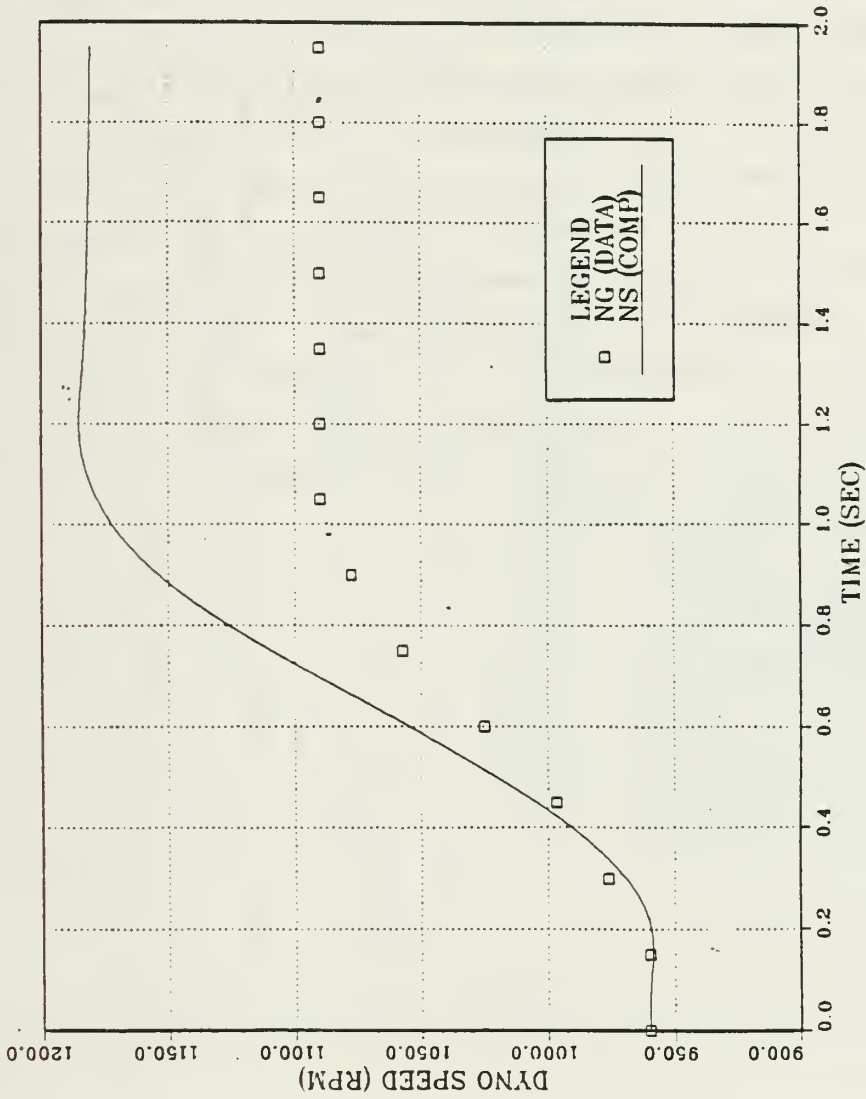


Figure 7.2 Comparison of State Space vs. Nonlinear Model  
Dynamometer Response

## VIII. CONCLUSIONS AND RECOMMENDATIONS

An accurate nonlinear dynamic computer model of the Naval Postgraduate School marine propulsion test facility has been developed. A state space model has been derived from the nonlinear model.

Prior to controller design the fuel flowrate and dynamometer water weight actuators must be accurately modeled and included in both the nonlinear dynamic program and the state space model. In conjunction with this effort, a new fuel control valve should be installed which will allow more direct control of fuel flowrate. When this is accomplished a new controller should be designed using modern control techniques, specifically the LQR method. Performance tests should then be conducted on the turbine using both the present (classical) controller and the modern controller. These tests should include power level transients as well as simulated sea state conditions.

APPENDIX A  
DATA ACQUISITION PROGRAM

```

10 | #####
20 | #
30 | #           GAS TURBINE DATA ACQUISITION/REDUCTION PROGRAM           #
40 | #           #####
50 | #           #####
60 | #
70 | # USER INSTRUCTIONS:
80 |
90 | # THIS PROGRAM IS USED TO TAKE GAS TURBINE DATA AT THE
100 | # NAVAL POSTGRADUATE SCHOOL GAS TURBINE MARINE PROPULSION TEST
110 | # FACILITY.
120 |
130 | # THE USER MUST INPUT THE FOLLOWING DATA INTRACTIVELY:
140 |
150 | #           (1) TIME ,DATE
160 | #           (2) BAROMETERIC PRESSURE
170 | #           (1) BAROMETERIC TEMPERATURE CORRECTION
180 | #           (4) UPPER AND LOWER FUEL FLOWRATE ROTOMETER READINGS.
190 | # THE FOLLOWING IS A LIST OF VARIABLE NAMES USED IN THIS PROGRAM :
200 |
210 | # A1 = AIR FUEL RATIO.
220 | # D0 = THETA CORRECTION FACTOR
230 | # D1 = DELTA CORRECTION FACTOR
240 | # D2 = DELTA PRESSURE IN THROAT.
250 | # D5 = BAROMETERIC LATITUDE CORRECTION.
260 | # D6 = BAROMETERIC TEMP CORRECTION.
270 | # K(1) = HPT INLET TEMP RIGHT A.
280 | # K(2) = HPT INLET TEMP LEFT A.
290 | # K(3) = HPT INLET TEMP RIGHT A.
300 | # K(4) = HPT INLET TEMP LEFT A.
310 | # K(5) = FPT INLET TEMP RIGHT A.
320 | # K(6) = FPT INLET TEMP LEFT A.
330 | # K(7) = FPT INLET TEMP RIGHT B.
340 | # K(8) = FPT INLET TEMP LEFT B.
350 | # M1 = MASS FLOW RATE LOWER FLOAT
360 | # M2 = MASS FLOW RATE UPPER FLOAT
370 | # M3 = CORRECTED MASS FLOW RATE UPPER FLOAT

```



380 ! M4 = CORRECTED MASS FLOW RATE LOWER FLOAT  
390 ! M5 = CORRECTED MASS FLOWRATE  
400 ! M6 = MASS FLOW RATE OF AIR.  
410 ! M7 = CORRECTED MASS FLOW RATE OF AIR  
420 ! M8 = COMBINED AIR AND FUEL FLOW RATE.  
430 ! N(1) = COMPRESSOR SPEED, VOLTS  
440 ! N(2) = DYNAMOMETER SPEED, VOLTS  
450 ! N(4) = DYNAMOMETER TORQUE, VOLTS  
460 ! N1 = COMPRESSOR SPEED  
470 ! N2 = DYNAMOMETER SPEED  
480 ! N3 = CORRECTED GAS GENERATOR SPEED.  
490 ! N4 = CORRECTED DYNAMOMETER SPEED.  
500 ! P0 = ATM. PRESSURE  
510 ! P1 = AVERAGE INLET BELL PRESS.  
520 ! P2 = AVE COMPRESSOR DISCHARGE PRESS.  
530 ! P4 = AVE FPT INLET PRESS.  
540 ! P8 = AVE CELL PRESS.  
550 ! P9 = CORRECTED CELL PRESSURE.  
560 ! P(2) = COMPRESSOR DISCHARGE PRESSURE,RIGHT.  
570 ! P(4) = FPT INLET PRESSURE.  
580 ! P(5) = COMPRESSOR DISCHARGE PRESSURE,LEFT.  
590 ! P(9) = INLET BELL PRESSURE, LEFT.  
600 ! P(14) = CELL PRESSURE,FRONT.  
610 ! P(15) = CELL PRESSURE,REAR.  
620 ! P(16) = INLET BELL PRESSURE, RIGHT.  
630 ! Q1 = HPT TORQUE.  
640 ! Q2 = DYNO TORQUE.  
650 ! Q3 = CORRECTED HPT TORQUE.  
660 ! Q4 = CORRECTED DYNO TORQUE.  
670 ! R1 = LOWER ROTOMETER READING.  
680 ! R2 = UPPER ROTOMETER READING.  
690 ! R5 = RUN COUNNER  
700 ! T0 = AVERAGE INLET TEMP.  
710 ! T2 = AVE COMPRESSOR DISCHARGE TEMP.  
720 ! T3 = AVE HPT INLET TEMP.  
730 ! T4 = AVE FPT INLET TEMP  
740 ! T(0) = COMPRESSOR INLET TEMP A.  
750 ! T(1) = COMPRESSOR INLET TEMP B.  
760 ! T(2) = COMPRESSOR INLET TEMP C.  
770 ! T(3) = COMPRESSOR INLET TEMP D.  
780 ! T(4) = COMPRESSOR DISCHARGE TEMP ,RIGHT A.  
790 ! T(5) = COMPRESSOR DISCHARGE TEMP ,LEFT A.  
800 ! T(6) = COMPRESSOR DISCHARGE TEMP ,RIGHT B.  
810 ! T(7) = COMPRESSOR DISCHARGE TEMP ,LEFT B.  
820 !  
830 ! OPTION BASE 0  
840 ! DIM B\$(10),C\$(11),P(16),T(10),K(10),N(10),K1\$(30)  
850 !

```

860 ! DECLARE TYPEWRITER PRINTER AS OUTPUT DEVICE.
870 !
880 PRINTER IS 10,120
890 !
900 ! ZERO RUN COUNTER
910 !
920 R5=0
930 !
940 CLEAR
950 DISP "ENTER TIME,DATE:";
960 INPUT K1$
970 DISP " "
980 DISP "ENTER BAROMETRIC PRESS (IN.HG.)";
990 INPUT P0
1000 ! DISP " "
1010 ! DISP "FOR NPS THE LAT. CORRECTION IS: -0.025 (IN.HG.)";
1020 D5=-.025
1030 DISP " "
1040 DISP "ENTER TEMP. CORRECTION (IN.HG.)";
10500 INPUT D6
1060 !
1070 ! ATMOSPHERIC PRESSURE CORRECTED FOR LATITUDE AND TEMP (IN.HG) , P0.
1080 !
1090 P0=P0+D5+D6
1100 CLEAR
1110 R5=R5+1
1120 DISP " "
1130 DISP "ENTER UPPER ROTOMETER READING";
1140 INPUT R2
1150 DISP " "
1160 DISP "ENTER LOWER ROTOMETER READING";
1170 INPUT R1
1180 !
1190 SETTIME 0,0
1200 !
1210 ! FORMAT THE OUTPUT STATEMENTS
1220 !
1230 IMAGE K,5D,2D,K
1240 IMAGE K,4D,2D,K
1250 IMAGE K,1D,4D,K
1260 IMAGE K,5D,D,K
1270 !
1280 ! ZERO INPUT ARRAYS .
1290 !
1300 FOR I=0 TO 16
1310 P(I)=0
1320 NEXT I
1330 FOR I=0 TO 10

```

```

1340 T(I)=0
1350 K(I)=0
1360 N(I)=0
1370 NEXT I
1380 !
1390 ! THE FOLLOWING LOOP CAUSES 'K0' READINGS TO BE TAKEN
1400 ! FOR EACH PRESSURE DATA POINT.
1410 ! THIS ENSURES THAT A GOOD AVERAGE VALUE IS OBTAINED.
1420 !
1430 K0=8
1440 K1=30
1450 FOR K5=1 TO K0
1460 !
1470 !
1480 ! TAKE PRESSURE READINGS.
1490 !
1500 ! NOTE: CHANNELS 1-8 ARE CALIBRATED IN IN.HG.
1510 !
1520 SET TIMEDUT 7:1000
1530 OUTPUT 705 "SCO 1-8 ",CHR$(13)
1540 FOR I=1 TO 8
1550 ENTER 705 USING "%,K" ; B$
1560 P(I)=P(I)+VAL(B$(3))
1570 NEXT I
1580 ABORTIO 7
1590 !
1600 ! NOTE: CHANNELS 1-8 ARE CALIBRATED IN IN.H2O.
1610 !
1620 SET TIMEDUT 7:1000
1630 OUTPUT 705 "SCO 9-16 ",CHR$(13)
1640 FOR J=9 TO 16
1650 ENTER 705 USING "%,K" ; C$
1660 P(J)=P(J)+VAL(C$(4))
1670 NEXT J
1680 ABORTIO 7
1690 !
1700 NEXT K5
1710 !
1720 !
1730 ! TAKE THERMOCOUPLE VOLTS.
1740 !
1750 ! TYPE 'T' THERMOCOUPLES.
1760 !
1770 FOR I=40 TO 49
1780 OUTPUT 709 ; "AC",I
1790 FOR J=1 TO K1
1800 ENTER 709 ; V
1810 T(I-40)=V+T(I-40)

```

```

1820 ! PRINT "V(";I-40;")=";V
1830 NEXT J
1840 NEXT I
1850 !
1860 ! TYPE 'K' THERMOCOUPLES.
1870 !
1880 FOR I=50 TO 59
1890   OUTPUT 709 ;"AC",I
1900   FOR J=1 TO K1
1910   ENTER 709 ; V
1920   K(I-49)=K(I-49)+V
1930   ! PRINT "V(";I-49;")=";V
1940   ! PRINT "K(";I-49;")=";K(I-49)
1950   NEXT J
1960 NEXT I
1970 !
1980 !
1990 ! TAKE SPEED,TORQUE VOLTS.
2000 !
2010 FOR I=20 TO 29
2020   OUTPUT 709 ;"AC",I
2030   FOR J=1 TO K1
2040   ENTER 709 ; V
2050   N(I-19)=N(I-19)+V
2060 NEXT J
2070 NEXT I
2080 !
2090 !
2100 ! DATA COLLECTION COMPLETE. NOW COMPUTE AVERAGE VALUE OF EACH DATA POINT.
2110 ! DATA POINT.
2120 BEEP
2130 BEEP
2140 BEEP
2150 BEEP
2160 !
2170 DISP "ENTER CELL PRESSURE (REMINDER, NEG NUMBER!) ";
2180 INPUT P8
2190 !
2200 !
2210 FOR I=0 TO 16
2220   P(I)=P(I)/K0
2230 NEXT I
2240 !
2250 ! CONVERT FROM VOLTS TO DEG.F FOR TYPE 'T' THERMOCOUPLE.
2260 !
2270 FOR I=0 TO 9
2280   T(I)=T(I)/K1
2290   M0=.1008609

```

```

2300 M1=25727.94369
2310 M2=-767345.8295
2320 M3=78025595.81
2330 M4=-9247486589
2340 M5=69768800000
2350 M6=-2.66192E13
2360 M7=3.94078E14
2370 T(I)=M0+T(I)*(M1+T(I)*(M2+T(I)*(M3+T(I)*(M4+T(I)*(M5+T(I)*(M6+T(I)*M7))))))
2380 T(I)=9/5*T(I)+32
2390 NEXT I
2400 I
2410 I CONVERT FROM VOLTS TO DEG.F FOR TYPE 'K' THERMOCOUPLE.
2420 I
2430 FOR I=1 TO 10
2440 K(I)=K(I)/K1
2450 I
2460 L0=.226584602
2470 L1=24152.109
2480 L2=67233.4248
2490 L3=2210340.682
2500 L4=-860963914.9
2510 L5=48350600000
2520 L6=-1.18452E12
2530 L7=1.3869E13
2540 L8=-6.33708E13
2550 K(I)=L0+K(I)*(L1+K(I)*(L2+K(I)*(L3+K(I)*(L4+K(I)*(L5+K(I)*(L6+K(I)*(L7+K(I)*L8))))))
2560 K(I)=9/5*K(I)+32
2570 NEXT I
2580 I
2590 I CONVERT SPEED, TORQUE READINGS.
2600 I
2610 FOR I=1 TO 10
2620 N(I)=N(I)/K1
2630 NEXT I
2640 I
2650 I DYND SPEED (RPM),N2.
2660 I
2670 N2=N(1)*652.728191
2680 I
2690 I GAS GENERATOR SPEED (RPM),N1.
2700 I
2710 N1=16143.31+N(2)*3778
2720 I
2730 I DYND TORQUE (FT-LBS.),Q2.
2740 I
2750 Q2=N(4)*59.254138
2760 I
2770 I COMPUTE AVERAGE VALUE FOR REDUNDANT DATA POINTS.

```

```

2780 |
2790 |
2800 | INLET BELL PRESSURE (IN.H2O),P1
2810 |
2820 P1=(P(9)+P(16))/2
2830 |
2840 | COMPRESSOR DISCHARGE PRESSURE (IN.HG.),P2.
2850 |
2860 P2=(P(2)+P(5))/2
2870 |
2880 | FPT INLET PRESSURE (IN.HG.),P4.
2890 |
2900 P4=P(4)
2910 |
2920 | COMPRESSOR INLET TEMPERATURE (DEG.F),T0.
2930 |
2940 T0=(T(0)+T(1)+T(2)+T(3))/4
2950 |
2960 | COMPRESSOR DISCHARGE TEMPERATURE (DEG.F),T2.
2970 |
2980 T2=(T(4)+T(5)+T(6)+T(7))/4
2990 |
3000 | HPT INLET TEMPERATURE (DEG.F),T3.
3010 |
3020 T3=(K(1)+K(2)+K(3)+K(4))/4
3030 |
3040 | FPT INLET TEMPERATURE (DEG.F),T3.
3050 |
3060 T4=(K(5)+K(6)+K(7)+K(8))/4
3070 |
3080 PRINT "DATE: ";K1$;" RUN: ";R5
3090 PRINT
3100 |
3110 CLEAR
3120 DISP "DETAILED REPORT ENTER '1'."
3130 DISP "SUMMARY REPORT ENTER '2'.";
3140 DISP "ANALYSIS ENTER '3'.";
3150 INPUT Z1
3160 IF Z1=3 THEN GOTO 3950
3170 |
3180 PRINT "*****"
3190 PRINT " RAW DATA "

```



```

3170 !
3180 PRINT "*****"
3190 PRINT " "
3200 PRINT "*****"
3210 PRINT "*****"
3220 PRINT "*****"
3230 IF Z1=2 THEN GOTO 3710
3240 PRINT "PRESSURES"
3250 PRINT " "
3260 PRINT " "
3270 PRINT USING 1230 ; "BAROMETERIC PRESS.,"
3280 PRINT USING 1230 ; "CELL PRESS. FRONT,"
3290 PRINT USING 1230 ; "CELL PRESS. REAR,"
3300 PRINT USING 1230 ; "CELL PRESS. AVE,"
3310 PRINT USING 1230 ; "INLET BELL PRESS. RIGHT,"
3320 PRINT USING 1230 ; "INLET BELL PRESS. LEFT,"
3330 PRINT USING 1230 ; "INLET BELL PRESS. AVE,"
3340 PRINT USING 1230 ; "COMPRESSOR DISCH. PRESS. RIGHT,"
3350 PRINT USING 1230 ; "COMPRESSOR DISCH. PRESS. LEFT,"
3360 PRINT USING 1230 ; "COMPRESSOR DISCH. PRESS. AVE,"
3370 PRINT USING 1230 ; "FPT INLET PRESS.,"
3380 PRINT " "
3390 PRINT "TEMPERATURE"
3400 PRINT " "
3410 PRINT USING 1240 ; "COMPRESSOR INLET TEMP. A,"
3420 PRINT USING 1240 ; "COMPRESSOR INLET TEMP. B,"
3430 PRINT USING 1240 ; "COMPRESSOR INLET TEMP. C,"
3440 PRINT USING 1240 ; "COMPRESSOR INLET TEMP. D,"
3450 PRINT USING 1240 ; "COMPRESSOR INLET TEMP. AVE,"
3460 PRINT USING 1240 ; "COMPRESSOR DISCH. TEMP. RIGHT A,"
3470 PRINT USING 1240 ; "COMPRESSOR DISCH. TEMP. LEFT A,"
3480 PRINT USING 1240 ; "COMPRESSOR DISCH. TEMP. RIGHT B,"
3490 PRINT USING 1240 ; "COMPRESSOR DISCH. TEMP. LEFT B,"
3500 PRINT USING 1240 ; "COMPRESSOR DISCH. TEMP. AVE,"
3510 PRINT USING 1240 ; "HPT INLET TEMP. RIGHT A,"
3520 PRINT USING 1240 ; "HPT INLET TEMP. LEFT A,"
3530 PRINT USING 1240 ; "HPT INLET TEMP. RIGHT B,"
3540 PRINT USING 1240 ; "HPT INLET TEMP. LEFT B,"
3550 PRINT USING 1240 ; "HPT INLET TEMP. AVE,"
3560 PRINT USING 1240 ; "FPT INLET TEMP. RIGHT A,"
3570 PRINT USING 1240 ; "FPT INLET TEMP. LEFT A,"
3580 PRINT USING 1240 ; "FPT INLET TEMP. RIGHT B,"
3590 PRINT USING 1240 ; "FPT INLET TEMP. LEFT B,"
3600 PRINT USING 1240 ; "FPT INLET TEMP. AVE,"
3610 PRINT " "
3620 PRINT "SPEEDS ETC."
3630 PRINT " "
3640 PRINT USING 1240 ; "UPPER ROTOMETER,"

```

```

PO = ";PO;" IN.HG."
P(13) = ",P(13)," IN.H20"
P(14) = ",P(14)," IN.H20"
PB = ",PB," IN.H20"
P(16) = ",P(16)," IN.H20"
P(9) = ",P(9)," IN.H20"
P1 = ",P1," IN.H20"
P(2) = ",P(2)," IN.HG"
P(5) = ",P(5)," IN.HG"
P2 = ",P2," IN.HG"
P4 = ",P4," IN.HG"

T(0) = ",T(0)," DEG. F"
T(1) = ",T(1)," DEG. F"
T(2) = ",T(2)," DEG. F"
T(3) = ",T(3)," DEG. F"
T0 = ",T0," DEG. F"
T(4) = ",T(4)," DEG. F"
T(5) = ",T(5)," DEG. F"
T(6) = ",T(6)," DEG. F"
T(7) = ",T(7)," DEG. F"
TZ = ",TZ," DEG. F"
K(1) = ",K(1)," DEG. F"
K(2) = ",K(2)," DEG. F"
K(3) = ",K(3)," DEG. F"
K(4) = ",K(4)," DEG. F"
T3 = ",T3," DEG. F"
K(5) = ",K(5)," DEG. F"
K(6) = ",K(6)," DEG. F"
K(7) = ",K(7)," DEG. F"
K(8) = ",K(8)," DEG. F"
T4 = ",T4," DEG. F"

R2 = ",R2"

```

```

3650 PRINT USING 1240 ; "LOWER ROTOMETER,          R1      = ",R1
3660 PRINT USING 1260 ; "GAS GENERATOR SPEED,      N1      = ",N1," RPM"
3670 PRINT USING 1260 ; "DYNAMOMETER SPEED,        N2      = ",N2," RPM"
3680 PRINT USING 1260 ; "DYNAMOMETER TORQUE,       Q2      = ",Q2," FT-LB"
3690 !
3700 GOTO 3900
3710 !
3720 !
3730 PRINT USING 1260 ; "GAS GENERATOR SPEED,      N1      = ",N1," RPM"
3740 PRINT USING 1260 ; "DYNAMOMETER SPEED,        N2      = ",N2," RPM"
3750 PRINT " "
3760 PRINT USING 1230 ; "BAROMETERIC PRESS.,      P0      = ";P0;" IN.HG."
3770 PRINT USING 1230 ; "CELL PRESS. AVE,         P8      = ",P8," IN.H2O"
3780 PRINT USING 1230 ; "INLET BELL PRESS. AVE,    P1      = ",P1," IN.H2O"
3790 PRINT USING 1230 ; "COMPRESSOR DISCH. PRESS. AVE, P2      = ",P2," IN.HG"
3800 PRINT USING 1230 ; "FPT INLET PRESS.,        P4      = ",P4," IN.HG"
3810 PRINT USING 1240 ; "COMPRESSOR INLET TEMP. AVE, T0      = ",T0," DEG. F"
3820 PRINT USING 1240 ; "COMPRESSOR DISCH. TEMP. AVE, T2      = ",T2," DEG. F"
3830 PRINT USING 1240 ; "HPT INLET TEMP. AVE,      T3      = ",T3," DEG. F"
3840 PRINT USING 1240 ; "FPT INLET TEMP. AVE,      T4      = ",T4," DEG. F"
3850 PRINT USING 1240 ; "UPPER ROTOMETER,         R2      = ",R2
3860 PRINT USING 1240 ; "LOWER ROTOMETER,         R1      = ",R1
3870 PRINT USING 1260 ; "DYNAMOMETER TORQUE,       Q2      = ",Q2," FT-LB"
3880 !
3890 !
3900 !
3910 ! DATA REDUCTION CALCULATIONS
3920 !
3930 ! ABS. COMPRESSOR INLET TEMP.(DEG.R)
3940 !
3950 T0=T0+460
3960 !
3970 ! ABS. COMPRESSOR DISCH. TEMP.(DEG.R)
3980 !
3990 T2=T2+460
4000 !
4010 ! ABS. HPT INLET TEMP.(DEG.R)
4020 !
4030 T3=T3+460
4040 !
4050 ! ABS. FPT INLET TEMP.(DEG.R)
4060 !
4070 T4=T4+460
4080 !
4090 ! TEMP. CORRECTION FACTOR
4100 !
4110 D0=D0/520
4120 !

```

4130 ! ABS.CELL PRESS.(PSIA)  
4140 !  
4150 P9=P0\*(14.696/29.92)+P8\*(14.696/406.92)  
4160 !  
4170 ! PRESSURE CORRECTION FACTOR.  
4180 !  
4190 D1=P9/14.696  
4200 !  
4210 ! CORRECTED DYNO TORQUE.(FT.LBS)  
4220 !  
4230 Q4=Q2/D1  
4240 !  
4250 ! CORRECTED GAS GENERATOR SPEED.(RPM)  
4260 !  
4270 N3=N1/SQR(D0)  
4280 !  
4290 ! CORRECTED DYNAMOMETER SPEED.(RPM)  
4300 !  
4310 N4=N2/SQR(D0)  
4320 !  
4330 ! CALCULATE MASS FLOW RATE OF FUEL.(LB/HR)  
4340 !  
4350 !  
4360 M2=.607954\*R2-4.627907  
4370 M1=1.17442\*R1-8.556818  
4380 M5=(M1+M2)/2  
4390 !  
4400 ! CALCULATE MASS FLOW RATE OF AIR  
4410 !  
4420 D2=(P8-P1)\*14.696/406.92  
4430 M6=8.02\*.98\*P9\*21.73/SQR(53.34\*T0)\*SQR(D2/P9-1.5/1.4\*(D2/P9)^2)  
4440 M7=3600\*M6  
4450 !  
4460 ! CALCULATE AIR/FUEL RATIO  
4470 !  
4480 A1=M7/M5  
4490 !  
4500 ! CALCULATE THE COMBINED AIR + FUEL FLOW RATE (LB/HR).  
4510 !  
4520 M8=M5+M7  
4530 !  
4540 ! CALCULATE THE PERCENT THEORETIC AIR.  
4550 !  
4560 W=A1\*6.7847  
4570 !  
4580 ! CALCULATE THE CORRECTED HPT TORQUE (FT-LBS.).  
4590 !  
4500 BQ=5.94

```

4610 B1=.001951
4620 B2=-.000000281
4630 !
4640 C0=-.0003657
4650 C1=-.0000004536
4660 C2=3.571E-11
4670 !
4680 X=T3-T4
4690 Y=T3-T4*T4
4700 Z=T3^3-T4^3
4710 !
4720 B3=B0*X+B1*Y/2+B2*Z/3
4730 C3=C0*X+C1*Y/2+C2*Z/3
4740 H1=(B3+M*C3)/28.954
4750 Q1=M8*H1*778/(2*3.14159*N1*60)
4760 Q3=Q1/D1
4770 !
4780 ! ABS. COMPRESSOR DISCH. PRESS. (PSIA)
4790 !
4800 P2=P0*(14.696/29.92)+P2*(14.696/29.92)
4810 !
4820 ! ABS. FPT INLET PRESS. (PSIA)
4830 P4=P0*(14.696/29.92)+P4*(14.696/29.92)
4840 !
4850 ! CORRECTED VALUES.
4860 !
4870 !
4880 T2=T2/D0
4890 T4=T4/D0
4900 M5=M5/(D1*SQR(D0)/D1)
4910 M7=M7*SQR(D0)/D1
4920 A1=M7/M5
4930 M8=M5+M7
4940 !
4950 P2=P2/D1
4960 P4=P4/D1
4970 !
4980 !
4990 PRINT " "
5000 PRINT "*****CORRECTED VALUES*****"
5010 PRINT "ANALYSIS (CORRECTED VALUES)"
5020 PRINT "*****"
5030 PRINT " "
5040 !
5050 PRINT USING 1240 ; "COMPRESSOR DISCH. TEMP.,"
5060 PRINT USING 1240 ; "FPT INLET TEMP.,"
5070 PRINT USING 1230 ; "COMPRESSOR DISCH. PRESS.,"
5080 PRINT USING 1230 ; "FPT INLET PRESSURE,"
T2 = ",T2," DEG. R."
T4 = ",T4," DEG. R."
P2 = ",P2," PSIA"
P4 = ",P4," PSIA"

```

```

5090 PRINT USING 1240 ; "CORRECTED DYNO TORQUE,"
5100 PRINT USING 1240 ; "CORRECTED HPT TORQUE,"
5110 PRINT USING 1260 ; "CORRECTED GAS GENERAOR SPEED,"
5120 PRINT USING 1260 ; "CORRECTED DYNAMOMETER SPEED,"
5130 PRINT USING 1230 ; "CORRECTED FUEL FLOW RATE,"
5140 PRINT USING 1230 ; "CORRECTED AIR FLOW RATE,"
5150 PRINT USING 1230 ; "COMBINED AIR+FUEL FLOW RATE,"
5160 PRINT "AIR FUEL RATIO,"
5170 PRINT "THETA,"
5180 PRINT "DELTA,"
5190 !
5200 FOR L=1 TO 8
5210 PRINT " "
5220 NEXT L
5230 PRINT N3:P2:M7:T2:Q3:M5:P4:M8:T4:N4:Q4
5240 CLEAR
5250 DISP "ANOTHER RUN ENTER '1'."
5260 DISP "STOP ENTER '2'."
5270 INPUT Z2
5280 IF Z2<1.5 THEN GOTO 1110
5290 END

```

|    |   |         |         |
|----|---|---------|---------|
| Q4 | = | ","Q4," | FT-LB"  |
| Q3 | = | ","Q3," | FT-LB"  |
| N3 | = | ","N3," | RPM"    |
| N4 | = | ","N4," | RPM"    |
| M5 | = | ","M5," | LBM/HR" |
| M7 | = | ","M7," | LBM/HR" |
| M8 | = | ","M8," | LBM/HR" |

|    |   |      |
|----|---|------|
| A1 | = | ":A1 |
| D0 | = | ":D0 |
| D1 | = | ":D1 |





FIT00240  
 FIT00250  
 FIT00260  
 FIT00270  
 FIT00280  
 FIT00290  
 FIT00280  
 FIT00280  
 FIT00290

WHERE X, Y, Z ARE THE INDEPENDENT VARIABLES B IS THE DEPENDENT  
 VARIABLE, AND SUBSCRIPTS 1, 2, 3, ETC., INDICATE THE RUN NUMBER.

BEFORE EXECUTING TYPE :  
 FORTVS FIT (AUTODBL(DBLPAD)  
 TO RUN THIS PROGRAM IN DOUBLE PRECISION.

ALSO BEFORE EXECUTING TYPE : IMSLSP NONIMSL  
 GLOBAL, MACLIB  
 TO GET ACCESS TO IMSL ROUTINE LEQT2F.

GOOD LUCK!!!!!!

#####

```

1 DIMENSION X(90,5) BB(90) F(90,21), B(21),
  A(21,21), WKAREA(10000)
1 DATA B/21*0.0/, A/441*0.0/, X/450*0.0/, BB/90*0.0/, F/1890*0.0/,
  WKAREA/10000*0.0/

```

```

44 WRITE(6,44)
  FORMAT(//,3X,'HOW MANY DATA RUNS ?')
  READ(5*,*) NDATA
  WRITE(6,*) NDATA

```

```

55 WRITE(6,55)
  FORMAT(//,3X,'HOW MANY INDEPENDENT VARIABLES ?')
  READ(5*,*) NIND
  WRITE(6,*) NIND

```

```

111 WRITE(6,111)
  FORMAT(2X,1) SELECT : 1 = COMPLETE, QUADRATIC', /
  12X, '2 = REDUCED QUADRATIC', /
  12X, '3 = LINEAR APPROX.' )

```

```

C READ(5,*) YY
  WRITE(6,*) YY
  IF(YY-2.0) 112, 113, 114

```

THIS IS FOR THE COMPLETE QUADRATIC

```

112 NCOEFF = (NIND)*(1 + NIND)/2 + NIND + 1
  WRITE(6,*) NCOEFF
  GO TO 115

```

FIT00300  
 FIT00310  
 FIT00320  
 FIT00330  
 FIT00340  
 FIT00350  
 FIT00360  
 FIT00370  
 FIT00380  
 FIT00390  
 FIT00400  
 FIT00410  
 FIT00420  
 FIT00430  
 FIT00440  
 FIT00450  
 FIT00460  
 FIT00470  
 FIT00480  
 FIT00490  
 FIT00500  
 FIT00510  
 FIT00520  
 FIT00530  
 FIT00540  
 FIT00550  
 FIT00560  
 FIT00570  
 FIT00580  
 FIT00590  
 FIT00600  
 FIT00610  
 FIT00620  
 FIT00630

```

FIT00640
FIT00650
FIT00660
FIT00670
FIT00680
FIT00690
FIT00700
FIT00710
FIT00720
FIT00730
FIT00740
FIT00750
FIT00760
FIT00770
FIT00780
FIT00790
FIT00800
FIT00810
FIT00820
FIT00830
FIT00840
FIT00850
FIT00860
FIT00870
FIT00880
FIT00890
FIT00900
FIT00910
FIT00920
FIT00930
FIT00940
FIT00950
FIT00960
FIT00970
FIT00980
FIT00990
FIT01000
FIT01010
FIT01020
FIT01030
FIT01040
FIT01050
FIT01060
FIT01070
FIT01080
FIT01090
FIT01100
FIT01110
FIT01120
FIT01130

```

```

THIS IS FOR THE REDUCED QUADRATIC

```

```

113 NCOEFF = NIND*2 + 1
    WRITE(6,*) 'NCOEFF=', NCOEFF
    GO TO 115

```

```

THIS IS FOR THE LINEAR CURVE FIT

```

```

114 NCOEFF = NIND + 1
    WRITE(6,*) 'NCOEFF=', NCOEFF

```

```

115 CALL COEFF(X, BB, F, B, A, WKAREA, NCOEFF, NIND, NDATA, YY)

```

```

END

```

```

*****
SUBROUTINE COEFF(X, BB, F, B, A, WKAREA, NCOEFF, NIND, NDATA, YY)
*****

```

```

1 DIMENSION X(NDATA, NIND), BB(NDATA), F(NDATA, NCOEFF), B(NCOEFF),
    A(NCOEFF, NCOEFF), WKAREA(10000)

```

```

TEST CASE

```

```

X{ 1, 1 } = -3.0
X{ 2, 1 } = -2.0
X{ 3, 1 } = 0.0
X{ 4, 1 } = 3.0
X{ 5, 1 } = 4.0

```

```

BB{ 1 } = 18.0
BB{ 2 } = 10.0
BB{ 3 } = 2.0
BB{ 4 } = 2.0
BB{ 5 } = 5.0

```

```

READ IN DATA FROM FILE 02

```

```

DO 12 I = 1, NDATA
READ(2, 88) X( I, 1 ), BB( I )
READ(2, 89) X( I, 2 )
CONTINUE
FORMAT( F10.0, 40X, F10.0 )

```

```

12
88
89

```

```

C PRINT OUT THE DATA AS A CHECK
C
377 WRITE(6,377) 'DO YOU WANT TO CHECK THE INPUT ? 1=YES, 2=NO'
    FORMAT(/,2X,*)
    READ(5,*) ZZ
    WRITE(6,*) ZZ
    IF(ZZ.GT.1.5) GO TO 378
C
    DO 201 J = 1, NDATA
    DO 191 J = 1, NIND
    WRITE(8,211) I, J, X(I, J)
    FORMAT(3X, X(, I2, , I2, ' ) = ', G15.7)
    CONTINUE
211 WRITE(8,221) I, BB(I)
191 FORMAT(3X, BB(, I2, ) = ', G15.7)
    CONTINUE
C
C CONSTRUCT THE SYSTEM OF EQUATIONS USING THE METHOD OF
C LEAST SQUARES.
C
378 DO 100 K = 1, NDATA
    L = 0.0
    IF(YY-2.0) 112, 113, 114
C
C THIS SET GETS THE COMPLETE QUADRATIC
C
112 DO 110 I = 1, NIND
    DO 120 J = 1, NIND
        L = L + 1
        F(K, L) = X(K, I) * X(K, J)
    CONTINUE
120 CONTINUE
110 DO 130 II = 1, NIND
        L = L + 1
        F(K, L) = X(K, II)
    CONTINUE
130 F(K, L) = 1.0
C
C GO TO 100
C
C THIS GETS THE REDUCED QUADRATIC
C
113 DO 810 I = 1, NIND
    L = L + 1
    F(K, L) = X(K, I) * X(K, I)
810 CONTINUE
    DO 830 II = 1, NIND

```

```

FIT01140
FIT01150
FIT01160
FIT01170
FIT01180
FIT01190
FIT01200
FIT01210
FIT01220
FIT01230
FIT01240
FIT01250
FIT01260
FIT01270
FIT01280
FIT01290
FIT01300
FIT01310
FIT01320
FIT01330
FIT01340
FIT01350
FIT01360
FIT01370
FIT01380
FIT01390
FIT01400
FIT01410
FIT01420
FIT01430
FIT01440
FIT01450
FIT01460
FIT01470
FIT01480
FIT01490
FIT01500
FIT01510
FIT01520
FIT01530
FIT01540
FIT01550
FIT01560
FIT01570
FIT01580
FIT01590
FIT01600
FIT01610
FIT01620
FIT01630

```

```

FIT01640
FIT01650
FIT01660
FIT01670
FIT01680
FIT01690
FIT01700
FIT01710
FIT01720
FIT01730
FIT01740
FIT01750
FIT01760
FIT01770
FIT01780
FIT01790
FIT01800
FIT01810
FIT01820
FIT01830
FIT01840
FIT01850
FIT01860
FIT01870
FIT01880
FIT01890
FIT01900
FIT01910
FIT01920
FIT01930
FIT01940
FIT01950
FIT01960
FIT01970
FIT01980
FIT01990
FIT02000
FIT02010
FIT02020
FIT02030
FIT02040
FIT02050
FIT02060
FIT02070
FIT02080
FIT02090
FIT02100
FIT02110
FIT02120
FIT02130

```

```

      L = L + 1
      F(K,L) = X(K,II)
      CONTINUE
      L = L + 1
      F(K,L) = 1.0
      GO TO 100
C
C
C
C
      THIS GETS THE LINEAR CURVE FIT
114 DO 930 II = 1,NIND
      L = L + 1
      F(K,L) = X(K,II)
      CONTINUE
      L = L + 1
      F(K,L) = 1.0
      CONTINUE
C
      DO 140 M = 1,NCOEFFE
      DO 150 J = 1,NCOEFFE
      DO 160 I = 1,NDATA
      A(M,J) = (F(I,J) * F(I,M)) + A(M,J)
      CONTINUE
160 CONTINUE
150 CONTINUE
140 CONTINUE
      DO 170 J = 1,NCOEFFE
      DO 180 I = 1,NDATA
      B(J) = (F(I,J) * BB(I)) + B(J)
      CONTINUE
180 CONTINUE
170 CONTINUE
C
      PRINT OUT THE 'A' AND 'B' MATRICES AS A CHECK
C
C
C
      DO 190 J = 1,NCOEFFE
      DO 200 I = 1,NCOEFFE
      WRITE(8,210) J,I,A(J,I)
      FORMAT(3X,'A(',I2,',',I2,') = ',G15.7)
      CONTINUE
210 CONTINUE
      WRITE(8,220) J,B(J)
      FORMAT(3X,'B(',I2,') = ',G15.7)
      CONTINUE
220 CONTINUE
190 CONTINUE
C
C
C
C

```

```

C C C C C C C C C C
CALL THE IMSL ROUTINE 'LEQT2F' TO SOLVE THE LINEAR SYSTEM
      A * C = B
THE SOLUTION C IS RETURNED TO THE B VECTOR, AND IS OUTPUT BELOW.
C IS THE VECTOR OF POLYNOMIAL COEFFICIENTS.
      NC = 1
      IER = 0
      IDGT = 1
      CALL LEQT2F(A, NC, NCOEFF, NCOEFF, B, IDGT, WKAREA, IER)
      DO 10 IN = 1, NCOEFF
      WRITE(8, 11) IN, B(IN)
      FORMAT(10X, 'C(', I2, ') = ', G15.7)
      CONTINUE
      END
11
10
C C
FIT02140
FIT02150
FIT02160
FIT02170
FIT02180
FIT02190
FIT02200
FIT02210
FIT02220
FIT02230
FIT02240
FIT02250
FIT02260
FIT02270
FIT02280
FIT02290
FIT02300
FIT02310
FIT02320

```







B STATE SPACE COEFFICIENT MATRIX.

C VECTOR CONTAINING THE COEFFICIENTS FOR THE QUADRATIC CURVE FIT.

MA AIR FLOW RATE, LBS/HR.

MAF COMBINED FUEL AND AIR FLOW RATE, LBS/HR.

MERR PERCENTAGE ERROR IN FUEL FLOW RATE ALLOWED DURING FUEL FLOW RATE CONVERGENCE.

MF FUEL FLOW RATE, LBS/HR.

MEDEL INCREMENTAL CHANGE IN FUEL FLOW RATE USED WHEN SEARCHING FOR UPPER AND LOWER BOUNDS ON FUEL FLOW RATE.

MFL LOWER LIMIT ON FUEL FLOW RATE.

MFMIN FUEL FLOW RATE WHICH LEADS TO THE MINIMUM GAS GENERATOR TORQUE DIFFERENTIAL.

MFU UPPER LIMIT ON FUEL FLOW RATE.

MF1 INTERMEDIATE FUEL FLOW RATE USED IN FUEL FLOW RATE CONVERGENCE.

MF2 INTERMEDIATE FUEL FLOW RATE USED IN FUEL FLOW RATE CONVERGENCE.

NG GAS GENERATOR SPEED, RPM.

NS DYNAMOMETER SPEED, RPM.

PERR PERCENTAGE ERROR IN PRESSURES (P2,P4) ALLOWED DURING PRESSURE CONVERGENCE.

P2 COMPRESSOR DISCHARGE PRESSURE, PSIA.

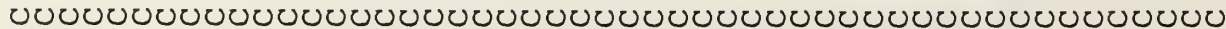
P2G GUESS FOR THE COMPRESSOR DISCHARGE PRESSURE, PSIA.

P4 HPT DISCHARGE PRESSURE, PSIA.

P4G GUESS FOR THE HPT DISCHARGE PRESSURE, PSIA.

QC COMPRESSOR TORQUE, FT-LBS.

QD DYNAMOMETER TORQUE, FT-LBS.





COMMON QC, NG, P2G, QHPT, MA, T2, ME, P4G, QEPT, MAE, T4, NS, OD, WW  
REAL NG, NS, ME, MAE, MA, NSO, NGO, MEO, MAEO, MAO, MEDEL, MEU, MEL,  
MF1, ME2, MEMIN, MERR  
DIMENSION A(2,2), B(2,2)

1

INPUT THE INITIAL GAS GENERATOR SPEED AND DYNO SPEED.

1 WRITE(6,1)  
FORMAT(/,3X,'INPUT INITIAL GAS GENERATOR SPEED,"NG".')

READ(5,\*) NG  
WRITE(6,\*) NG

3 WRITE(6,3)  
FORMAT(/,3X,'INPUT INITIAL DYNO SPEED,"NS".')

READ(5,\*) NS  
WRITE(6,\*) NS

ESTABLISH THE CONVERGENCE TOLERANCES.

WWERR = 0.05  
MERR = 0.001  
PERR = 0.05  
QERR = 0.01

FIND AN INITIAL "GOOD GUESS" FOR 'ME' GIVEN 'NG' AND 'NS'.

CALL NGNSMF(NG,NS,ME)

ME1 = ME  
XCOUNT = 0.0

CONVERGE ON 'P2' AND 'P4' FOR THE GIVEN 'ME', 'NG' AND 'NS'.

5 CALL P2P4(NG,NS,ME,PERR,QPERC,P2G,P4G)

IF(ABS(QPERC).LT.QERR) GO TO 300

ESTABLISH UPPER AND LOWER BOUNDS ON 'ME':

```

C      XCOUNT = XCOUNT + 1.0
C      X1 = 1.0
C      XSIGN = -1.0 * SIGN(X1,OPERC)
C      WRITE(6,*) QPERC = ,QPERC, XSIGN = ', XSIGN
C      MEDEL = 2.0
C      IF(XCOUNT.GT.1.5) GO TO 33
C
C      XSIGN1 = XSIGN
C      MF2 = MF1 + XSIGN * MEDEL
C      MF = MF2
C      QPERC1 = QPERC
C      GO TO 5
C
C      33  IF((XSIGN1*XSIGN).LT.0.5) GO TO 298
C
C      MF2 = MF1 + XSIGN1 * MEDEL * XCOUNT
C      MF = MF2
C      GO TO 5
C
C      USE THE GOLDEN SECTION METHOD TO FIND THE VALUE OF 'MF' THAT
C      WILL LEAD TO ZERO GAS GENERATOR TORQUE MISMATCH.
C
C      298  QPERC2 = QPERC
C
C      IF(MF2.LT.MF1) GO TO 34
C
C      MFU = MF2
C      MFL = MF1
C      QU = ABS(QPERC2)
C      QL = ABS(QPERC1)
C
C      34  MFU = MF1
C      MFL = MF2
C      QU = ABS(QPERC1)
C      QL = ABS(QPERC2)
C
C      WRITE(6,170)
C      FORMAT(/,9X,'XMF1',14X,'XMF2',14X,'XMF2',14X,'XMFU',/)
C
C      TAU = 0.381966
C      XN = -2.078 * ALOG(MERR/100.0) + 3
C      WRITE(6,*) 'XN =',XN
C      MF1 = (1.0-TAU)*MFL + TAU*(MFU)
C      CALL P2P4(NG,NS,MF1,PERR,QPERC,P2G,P4G)
C      Q1 = ABS(QPERC)
C      MF2 = (1.0-TAU)*MFU + TAU*(MFL)
C      CALL P2P4(NG,NS,ME2,PERR,QPERC,P2G,P4G)

```

```

O2 = ABS(QPERC)
XK = 3.0
XK = XK + 1.0
WRITE(6,168) MEL, MF1, ME2, MEU
FORMAT(2X,4(F15.7,3X))
MEMIN = (MEL + ME2)/2
ODIEFF = (Q1 + Q2)/2.0
WRITE(6,*) ODIFF
IF(ODIEFF.LT.QERR) GO TO 92
IF(XK.GT.XN) GO TO 92
IF(Q1.GT.Q2) GO TO 91
MEU = ME2
OU = Q2
ME2 = MF1
O2 = Q1
ME1 = (1.0-TAU)*MEL + TAU*(MEU)
CALL P2P4(NG,NS,MF1,PERR,QPERC,P2G,P4G)
O1 = ABS(QPERC)
GO TO 90
MEL = MF1
OL = Q1
MF1 = MF2
O1 = Q2
ME2 = (1.0-TAU)*MEU + TAU*(MEL)
CALL P2P4(NG,NS,ME2,PERR,QPERC,P2G,P4G)
O2 = ABS(QPERC)
GO TO 90
WRITE(6,169) MEMIN
FORMAT(2X,G.S. MEMIN = ',F15.7)
ME = MEMIN

CALL SUBMA(NG,P2G,MA)
CALL SUBT2(NG,P2G,T2)
CALL SUBQC(NG,P2G,OC)
CALL SUBQHT(NG,MA,T2,ME,P4G,QHPT)
MAF = MA + ME
CALL SUBT4(NG,MA,T2,ME,P4G,T4)
CALL SUBQET(MAF,T4,NS,QEPT)
QPERC = 100*(QHPT-QC)/QHPT

```

90

C  
C168

C  
C  
C

91

92  
169

C  
C

EQUATE, OD = OFPT FOR STEADY STATE AND SOLVE FOR 'WW' USING NEWTON'S METHOD. NOTE THAT 'WWERR' HALTS THE ITERATION.

"WW1" IS THE INITIAL GUESS FOR DYNO WATER WEIGHT. IT IS NEEDED TO START NEWTON'S SCHEME. THE VALUE IS FAIRLY ARBITRARY BUT DO NOT USE 'WW1 = 0.0'!

C  
C  
C  
C  
C  
C  
C  
C  
C  
C  
C

```

C      WW1 = 5.00
C      GG = QD - QEPT, WHERE QD = FCN(WW1)
C
C3     C5 = 1.19294E-5
C4     C3 = 4.0E-6
C4     C4 = -20.0 + C3*NS*NS
OD     OD = C4 + C5*NS*NS*(WW1**1.3)
GG     GG = QD - QEPT
GGP    GGP = 1.3*C5*NS*NS*(WW1**0.3)
WW     WW = WW1 - GG/GGP
WWDIFF WWDIFF = 100.0 * ABS((WW - WW1)/WW1)
IF(WWDIFF.LT.WWERR) GO TO 300
WW1 = WW
GO TO 37

```

```

C      SET VALUES TO INITIAL VALUES AND PRINT OUT.
C
C300

```

```

NGO = NG
NSO = NS
OCO = OC
MAO = MA
T2O = T2
P2O = P2G
QHPTO = QHPT
MFO = MF
P4O = P4G
T4O = T4
MAFO = MAF
QEPTO = QEPT
ODO = OD
WVO = WW

```

```

C      CALL SUBROUTINE 'PART' TO GET THE COEFFICIENTS OF THE STATE
C      SPACE MATRICES, 'A' AND 'B'. THE RESULTS ARE SENT TO FILE O2.
C
C      CALL PART(A,B)

```

```

C      PRINT OUTPUT TO THE SCREEN.
C
C      WRITE(6,*) 'NGO = ', NGO
C      WRITE(6,*) 'NSO = ', NSO
C      WRITE(6,*) 'OCO = ', OCO
C      WRITE(6,*) 'MAO = ', MAO
C      WRITE(6,*) 'T2O = ', T2O
C      WRITE(6,*) 'P2O = ', P2O
C      WRITE(6,*) 'QHPTO = ', QHPTO

```



```

WRITE(6,*)
WRITE(6,*)MFO
WRITE(6,*)P40
WRITE(6,*)T40
WRITE(6,*)MAFO
WRITE(6,*)QEPTO
WRITE(6,*)QDO
WRITE(6,*)WVO
WRITE(6,*)P2ERR
WRITE(6,*)P4ERR
WRITE(6,*)MERR
WRITE(6,*)WWERR

```

PRINT OUTPUT TO FILE 02.

```

WRITE(2,*)
WRITE(2,*)NGO
WRITE(2,*)NSO
WRITE(2,*)QCO
WRITE(2,*)MAO
WRITE(2,*)T20
WRITE(2,*)P20
WRITE(2,*)QHPTO
WRITE(2,*)MFO
WRITE(2,*)P40
WRITE(2,*)T40
WRITE(2,*)MAFO
WRITE(2,*)QEPTO
WRITE(2,*)QDO
WRITE(2,*)WVO
WRITE(2,*)QPERC
WRITE(2,*)P2ERR
WRITE(2,*)P4ERR

```



```

B = 0
K = 0
DO 70 J = 1, NIND
DO 71 I = J, NIND
   K = K+1
B = B+C(K)*X(J)*X(I)
CONTINUE
CONTINUE

```

71  
70

C

```

DO 72 J = 1, NIND
   K = K+1
B = B+C(K)*X(J)
CONTINUE

```

72

C

```

K = K+1
B = B+C(K)

```

C

```

WRITE(6,84) B
FORMAT(/,2X, ' THE SCALED ME IS : ', 2X,G15.7)

```

84

C

```

BR = B * Z(NIND + 1)

```

C

THE FOLLOWING ENSURES THAT THE OUTPUT STAYS IN WITHIN LIMITS.

```

XHI = 240.0
XLO = 70.0

```

C

```

BR = AMAX1(XLO, BR)
BR = AMIN1(XHI, BR)

```

C

```

WRITE(6,85) BR
FORMAT(/,2X, ' ME IS : ', 2X,G15.7)

```

85

C

```

RETURN
END

```

C

\*\*\*\*\*  
SUBROUTINE P2P4(NG,NS,ME,PERR,OPERC,P2G,P4G)  
\*\*\*\*\*

THE INPUTS TO THIS SUBROUTINE ARE 'NG', 'NS', AND 'ME', AND 'P2', AND 'P4'  
FOR THESE INPUTS THE SUBROUTINE CONVERGES ON 'P2', AND 'P4',  
AND FINDS THE "STEADY STATE" TORQUE DIFFERENTIAL, WHICH  
IS REPRESENTED IN PERCENTAGE FORM AS 'QPERC'.

REAL NG, NS, ME, MAF, MA, NSO, NGO, MFO, MAFO, MAO, MEDEL, MFU, MFL

C

P2G AND P4G ARE NOMINAL VALUES OF COMPRESSOR DISCHARGE AND FPT INLET PRESSURES. THEY PROVIDE AN INITIAL GUESS FOR THE CONVERGENCE ROUTINE. P2ERR AND P4ERR ARE THE MAXIMUM ALLOWABLE DIFFERENCES BETWEEN P2G AND P2 , AND BETWEEN P4G AND P4.

```

P2G = 31.5
P4G = 17.0
P2ERR = PERR
P4ERR = PERR
ZS = 50.0
ZX = 0.0

```

COMPUTE COMPRESSOR OUTPUTS.

```

10 ZX = ZX + 1.0

```

```

CALL SUBMA(NG,P2G,MA)
CALL SUBT2(NG,P2G,T2)
CALL SUBQC(NG,P2G,QC)

```

COMPUTE P2 AND CHECK AGAINST P2G.

```

20 CALL SUBP2(NG,MA,T2,ME,P4G,P2)
P2DIFF = 100.0 * ABS(P2 - P2G)/P2
P2G = P2
P2G = P2G + 0.5*(P2-P2G)
IF(ZX.GT.ZS) GO TO 511
IF(P2DIFF.GT.P2ERR) GO TO 10

```

```

511 ZX = 0.0

```

COMPUTE REMAINING HPT OUTPUTS.

```

MAF = MA + MF
WRITE(6,*) 'MAF = ',MAF

```

```

47 CALL SUBT4(NG,MA,T2,ME,P4G,T4)

```

COMPUTE P4 AND CHECK AGAINST P4G.

```

CALL SUBP4(MAF,T4,NS,P4)
P4DIFF = 100.0 * ABS(P4 - P4G)/P4
P4G = P4G + 0.5*(P4-P4G)

```

```

C      P4G = P4
C      IF(P4DIFF.GT.P4ERR) GO TO 20
C      COMPUTE THE TORQUE MISMATCH (QHPT-QC).
C
C      CALL SUBMA(NG,P2G,MA)
C      CALL SUBT2(NG,P2G,T2)
C      CALL SUBOC(NG,P2G,QC)
C      CALL SUBOHT(NG,MA,T2,ME,P4G,QHPT)
C      CALL SUBOET(MA,T4,NS,QEPT)
C      QPERC = 100*(QHPT-QC)/QHPT
C
C      RETURN
C      END
C*****
C      SUBROUTINE SUBMA(X1,X2,BR)
C*****
C      THIS SUBROUTINE PRODUCES OUTPUT 'MA' FOR THE GIVEN INPUTS.
C
C      DIMENSION X(5),C(21),Z(5),XR(5)
C
C      XR(1) = X1
C      XR(2) = X2
C
C      COEFFICIENTS OF THE QUADRATIC CURVE FIT.
C
C      C(1) = 1.570198
C      C(2) = -0.7270151
C      C(3) = 0.2529498
C      C(4) = 0.1880112
C      C(5) = -0.6588774
C      C(6) = 0.3668176
C
C      SCALING FACTORS.
C
C      Z(1) = 36000.0
C      Z(2) = 43.0
C      Z(3) = 13000.0
C
C      NIND = 2
C
C      DO 686 I = 1,NIND
C          X(I) = XR(I)/Z(I)
C      CONTINUE
C      686
C      CONSTRUCT THE COMPLETE QUADRATIC EQUATION.

```

```

C
B = 0
K = 0
DO 70 J = 1, NIND
DO 71 I = J, NIND
   K = K+1
B = B+C(K)*X(J)*X(I)
CONTINUE
70 CONTINUE

C
DO 72 J = 1, NIND
   K = K+1
B = B+C(K)*X(J)
CONTINUE
72 CONTINUE

C
   K = K+1
B = B+C(K)

C
WRITE(6,84) B
FORMAT(/,2X, ' THE SCALED MA IS : ', 2X, G15.7)
84

C
BR = B * Z(NIND + 1)

```

THE FOLLOWING ENSURES THAT THE OUTPUT STAYS IN WITHIN LIMITS.

```

C
XHI = 13500.0
XLO = 5500.0

C
BR = AMAX1(XLO, BR)
BR = AMIN1(XHI, BR)

C
85 WRITE(6,85) BR
FORMAT(/,2X, ' MA IS : ', 2X, G15.7)

```

```

RETURN
END

```

```

C*****
C SUBROUTINE SUBT2(X1, X2, BR)
C*****

```

THIS SUBROUTINE PRODUCES OUTPUT 'T2' FOR THE GIVEN INPUTS.

```

DIMENSION X(5), C(21), Z(5), XR(5)

```



```
XR{1} = X1
XR{2} = X2
```

```
C
C
C
```

COEFFICIENTS OF THE QUADRATIC CURVE FIT.

```
C{1} = -0.5771397
C{2} = 2.203628
C{3} = -1.040498
C{4} = 0.1354878
C{5} = -0.4898891
C{6} = 0.7473461
```

```
C
C
```

SCALING FACTORS.

```
Z{1} = 36000.0
Z{2} = 43.0
Z{3} = 800.0
```

```
C
```

NIND = 2

```
C
```

```
DO 500 I = 1, NIND
X(I) = XR(I)/Z(I)
CONTINUE
```

```
711
500
```

```
C
C
C
```

CONSTRUCT THE COMPLETE QUADRATIC EQUATION.

```
B = 0
K = 0
DO 70 J = 1, NIND
DO 71 I = J, NIND
K = K + 1
B = B + C(K) * X(J) * X(I)
CONTINUE
CONTINUE
```

```
71
70
```

```
C
```

```
DO 72 J = 1, NIND
K = K + 1
```

```
B = B + C(K) * X(J)
```

```
72
```

```
C
```

```
B = B + C(K)
K = K + 1
```

```
C
C
C
C
C
```

```
WRITE(6, 84) B
FORMAT(/, 2X, ' THE SCALED T2 IS : ', 2X, G15.7)
```

```
84
```

```
BR = B * Z(NIND + 1)
```

```
C
```

C C THE FOLLOWING ENSURES THAT THE OUTPUT STAYS IN WITHIN LIMITS.

C XHI = 850.0  
C XLO = 500.0

C BR = AMAX1(XLO, BR)  
C BR = AMIN1(XHI, BR)

C C 85 WRITE(6,85) BR  
C C FORMAT(/,2X, T2 IS : ', 2X,G15.7)

C C RETURN  
C C END

C C \*\*\*\*\*  
C C SUBROUTINE SUBOC(X1, X2, BR)  
C C \*\*\*\*\*

C C THIS SUBROUTINE PRODUCES OUTPUT 'QC' FOR THE GIVEN INPUTS.

C C DIMENSION X(5), C(21), Z(5), XR(5)

C C XR(1) = X1  
C C XR(2) = X2

C C COEFFICIENTS OF THE QUADRATIC CURVE FIT.

C C { 1 } = -9.796132  
C C { 2 } = 20.03512  
C C { 3 } = -10.70980  
C C { 4 } = 0.1464243  
C C { 5 } = 1.657819  
C C { 6 } = -0.3884839

C C SCALING FACTORS.

C C Z{ 1 } = 36000.0  
C C Z{ 2 } = 43.0  
C C Z{ 3 } = 130.0

C C NIND = 2

C C DO 500 I = 1, NIND  
C C X(I) = XR(I)/Z(I)  
C C CONTINUE

C C 711  
C C 500  
C C

```

C CC
C   CONSTRUCT THE COMPLETE QUADRATIC EQUATION.

```

```

71 B = 0
70 K = 0
   DO 70 J = 1, NIND
   DO 71 I = J, NIND
     K = K + 1
     B = B + C(K) * X(J) * X(I)
   CONTINUE
   CONTINUE

```

```

C   DO 72 J = 1, NIND
     K = K + 1
     B = B + C(K) * X(J)
   CONTINUE

```

```

C   K = K + 1
     B = B + C(K)

```

```

C   WRITE(6, 84) B
C   FORMAT(/, 2X, 'THE SCALED QC IS : ', 2X, G15.7)

```

```

C   BR = B * Z(NIND + 1)

```

```

C   THE FOLLOWING ENSURES THAT THE OUTPUT STAYS IN WITHIN LIMITS.

```

```

C   XHI = 130.0
C   XLO = 40.0

```

```

C   BR = AMAX1(XLO, BR)
C   BR = AMINI(XHI, BR)

```

```

85 WRITE(6, 85) BR
   FORMAT(/, 2X, 'QC IS : ', 2X, G15.7)

```

```

C   RETURN
C   END

```

```

C *****
C   SUBROUTINE SUBP2(X1, X2, X3, X4, X5, BR)
C *****

```

```

C   THIS SUBROUTINE PRODUCES OUTPUT 'P2' FOR THE GIVEN INPUTS.

```

C DIMENSION X(5),C(21),Z(6),XR(5)  
 C  
 C

XR(1) = X1  
 XR(2) = X2  
 XR(3) = X3  
 XR(4) = X4  
 XR(5) = X5

C COEFFICIENTS OF THE QUADRATIC CURVE FIT.  
 C

C(1) = 4.17287  
 C(2) = -2.839741  
 C(3) = 1.223014  
 C(4) = -1.854803  
 C(5) = -10.26167  
 C(6) = -0.2169524  
 C(7) = -1.156939  
 C(8) = 2.860795  
 C(9) = 5.767990  
 C(10) = -0.101891  
 C(11) = 0.2918  
 C(12) = -0.441640  
 C(13) = 0.7359644  
 C(14) = -9.559825  
 C(15) = 22.88968  
 C(16) = 4.7794  
 C(17) = -2.558953  
 C(18) = 0.272224  
 C(19) = 6.295503  
 C(20) = -28.57775  
 C(21) = 9.380198

C SCALING FACTORS.  
 C  
 C

Z(1) = 36000.0  
 Z(2) = 13000.0  
 Z(3) = 800.0  
 Z(4) = 240.0  
 Z(5) = 20.0  
 Z(6) = 43.0

C NIND = 5  
 C DO 500 I = 1,NIND  
 C X(I) = XR(1)/Z(I)  
 C CONTINUE  
 C 500  
 C

```

C
C
C
C
C
CONSTRUCT THE COMPLETE QUADRATIC EQUATION.

```

```

71 B = 0
70 K = 0
DO 70 J = 1,NIND
DO 71 I = J,NIND
   K = K+1
B = B+C(K)*X(J)*X(I)
CONTINUE
CONTINUE

```

```

C
DO 72 J = 1,NIND
   K = K+1
B = B+C(K)*X(J)
CONTINUE
72

```

```

C
   K = K+1
B = B+C(K)

```

```

C
C
C
C
C
84 WRITE(6,84) B
   FORMAT(/,2X, THE SCALED P2 IS :',2X,G15.7)

```

```

C
BR = B * Z(NIND + 1)

```

```

C
C
C
C
THE FOLLOWING ENSURES THAT THE OUTPUT STAYS IN WITHIN LIMITS.

```

```

XHI = 43.0
XLO = 20.0

```

```

C
BR = AMAX1(XLO, BR)
BR = AMIN1(XHI, BR)

```

```

C
85 WRITE(6,85) BR
   FORMAT(/,2X, P2 IS :',2X,G15.7)

```

```

C
RETURN
END

```

```

C
C
C
C
C*****
SUBROUTINE SUBT4(X1,X2,X3,X4,X5, BR)
C*****

```

```

C
C THIS SUBROUTINE PRODUCES OUTPUT 'T4' FOR THE GIVEN INPUTS.

```

CC  
CC

DIMENSION X(5), C(21), Z(6), XR(5)

XR(1) = X1  
XR(2) = X2  
XR(3) = X3  
XR(4) = X4  
XR(5) = X5

CC  
CC

COEFFICIENTS OF THE QUADRATIC CURVE FIT.

C(1) = -22.20944  
C(2) = 10.79398  
C(3) = 21.99301  
C(4) = 86.64350  
C(5) = -208.0447  
C(6) = 1.232848  
C(7) = -12.46899  
C(8) = -64.69914  
C(9) = 180.0014  
C(10) = -0.6479730  
C(11) = -11.01693  
C(12) = 20.21592  
C(13) = 16.70037  
C(14) = -121.1824  
C(15) = 183.1548  
C(16) = 138.3667  
C(17) = -17.2714  
C(18) = -18.03533  
C(19) = 72.75989  
C(20) = -229.4335  
C(21) = 73.97864

CC  
CC

SCALING FACTORS.

Z(1) = 36000.0  
Z(2) = 13000.0  
Z(3) = 800.0  
Z(4) = 240.0  
Z(5) = 20.0  
Z(6) = 1800.0

CC  
C

NIND = 5  
DO 500 I = 1, NIND



500 X(I) = XR(I)/Z(I)  
CONTINUE

CONSTRUCT THE COMPLETE QUADRATIC EQUATION.

71 B = 0  
70 K = 0  
DO 70 J = 1, NIND  
DO 71 I = J, NIND  
K = K+1  
B = B+C(K)\*X(J)\*X(I)  
CONTINUE  
CONTINUE

72 DO 72 J = 1, NIND  
K = K+1  
B = B+C(K)\*X(J)  
CONTINUE

K = K+1  
B = B+C(K)

84 WRITE(6,84) B  
FORMAT(/,2X, THE SCALED T4 IS : ', 2X,G15.7)

BR = B \* Z(NIND + 1)

THE FOLLOWING ENSURES THAT THE OUTPUT STAYS IN WITHIN LIMITS.

XHI = 1800.0  
XLO = 1300.0

BR = AMAX1(XLO, BR)  
BR = AMINI(XHI, BR)

85 WRITE(6,85) BR  
FORMAT(/,2X, T4 IS : ', 2X,G15.7)

RETURN  
END

\*\*\*\*\*  
SUBROUTINE SUBQHT(X1, X2, X3, X4, X5, BR)  
\*\*\*\*\*

C\*\*\*\*\*

THIS SUBROUTINE PRODUCES OUTPUT 'QHPT' FOR THE GIVEN INPUTS.

DIMENSION X(5),C(21),Z(6),XR(5)

XR(1) = X1  
XR(2) = X2  
XR(3) = X3  
XR(4) = X4  
XR(5) = X5

COEFFICIENTS OF THE QUADRATIC CURVE FIT.

C(1) = 343.8178  
C(2) = -562.3596  
C(3) = -23.65895  
C(4) = -54.97896  
C(5) = 98.09515  
C(6) = 217.8508  
C(7) = 3.591497  
C(8) = 119.9962  
C(9) = -248.3938  
C(10) = -0.1507291  
C(11) = 17.95723  
C(12) = -17.87346  
C(13) = -40.67739  
C(14) = 28.27711  
C(15) = 190.2205  
C(16) = -160.9423  
C(17) = 260.8458  
C(18) = 21.40023  
C(19) = -34.85067  
C(20) = -219.0661  
C(21) = 62.16870

SCALING FACTORS.

Z(1) = 36000.0  
Z(2) = 13000.0  
Z(3) = 800.0  
Z(4) = 240.0  
Z(5) = 20.0  
Z(6) = 130.0

```

NIND = 5
DO 500 I = 1, NIND
X(I) = XR(I)/Z(I)
CONTINUE

```

CONSTRUCT THE COMPLETE QUADRATIC EQUATION.

```

B = 0
K = 0
DO 70 J = 1, NIND
DO 71 I = J, NIND
    K = K+1
    B = B+C(K)*X(J)*X(I)
CONTINUE
CONTINUE
DO 72 J = 1, NIND
    K = K+1
    B = B+C(K)*X(J)
CONTINUE

```

```

K = K+1
B = B+C(K)

```

```

WRITE(6, 84) B
FORMAT(/, 2X, ' THE SCALED QHPT IS : ', 2X, G15.7)

```

```

BR = B * Z(NIND + 1)

```

THE FOLLOWING ENSURES THAT THE OUTPUT STAYS IN WITHIN LIMITS.

```

XHI = 130.0
XLO = 40.0

```

```

BR = AMAX1(XLO, BR)
BR = AMIN1(XHI, BR)

```

```

WRITE(6, 85) BR
FORMAT(/, 2X, ' QHPT IS : ', 2X, G15.7)

```

```

RETURN
END

```

C 711  
500  
C  
C  
C  
C  
C

71  
70  
C

72  
C

84  
C  
C  
C  
C  
C

C  
C  
C  
C

C  
C  
C  
C  
C

C

```

C*****
C***** SUBROUTINE SUBP4(X1, X2, X3, BR)
C*****

```

```

C THIS SUBROUTINE PRODUCES OUTPUT 'P4' FOR THE GIVEN INPUTS.

```

```

C DIMENSION X(5), C(21), Z(6), XR(5)

```

```

C XR(1) = X1
C XR(2) = X2
C XR(3) = X3

```

```

C COEFFICIENTS OF THE QUADRATIC CURVE FIT.

```

```

C C(1) = 0.1926178
C C(2) = 1.158328
C C(3) = 0.1008366
C C(4) = 6.138049E-02
C C(5) = 8.429369E-02
C C(6) = -5.136141E-02
C C(7) = -0.8789043
C C(8) = -1.171511
C C(9) = -4.834537E-02
C C(10) = 1.559548

```

```

C SCALING FACTORS.

```

```

C Z(1) = 13000.0
C Z(2) = 1800.0
C Z(3) = 3000.0
C Z(4) = 20.0

```

```

C NIND = 3

```

```

C DO 500 I = 1, NIND
C X(I) = XR(I)/Z(I)
C CONTINUE

```

```

C CONSTRUCT THE COMPLETE QUADRATIC EQUATION.

```

```

C B = 0

```

```

K = 0
DO 70 J = 1, NIND
DO 71 I = J, NIND
  K = K+1
  B = B+C(K)*X(J)*X(I)
CONTINUE
70 CONTINUE
C

DO 72 J = 1, NIND
  K = K+1
  B = B+C(K)*X(J)
CONTINUE
72 CONTINUE
C

  K = K+1
  B = B+C(K)
C

WRITE(6,84) B
84 FORMAT(/,2X, 'THE SCALED P4 IS : ',2X,G15.7)
C

BR = B * Z(NIND + 1)
C

```

THE FOLLOWING ENSURES THAT THE OUTPUT STAYS IN WITHIN LIMITS.

```

XHI = 20.0
XLO = 15.2
C

BR = AMAX1(XLO, BR)
BR = AMIN1(XHI, BR)
C

WRITE(6,85) BR
85 FORMAT(/,2X, 'P4 IS : ',2X,G15.7)
C

```

```

RETURN
END

```

```

C*****
C SUBROUTINE SUBOFT(X1,X2,X3,BR)
C*****

```

THIS SUBROUTINE PRODUCES OUTPUT 'QFT' FOR THE GIVEN INPUTS.

```

DIMENSION X(5),C(21),Z(6),XR(5)
C

```

```

XR(1) = X1
XR(2) = X2

```

XR(3) = X3  
 COEFFICIENTS OF THE QUADRATIC CURVE FIT.

```

C( 1 ) = 2.192477
C( 2 ) = 0.8755642
C( 3 ) = -0.6626919
C( 4 ) = 3.892829
C( 5 ) = -0.1769417
C( 6 ) = 1.446682E-02
C( 7 ) = -1.83825
C( 8 ) = -7.607660
C( 9 ) = 0.2095135
C(10) = 3.747696
  
```

SCALING FACTORS.

```

Z( 1 ) = 13000.0
Z( 2 ) = 1800.0
Z( 3 ) = 3000.0
Z( 4 ) = 480.00
  
```

NIND = 3

```

DO 500 I = 1, NIND
X(I) = XR(I)/Z(I)
CONTINUE
  
```

CONSTRUCT THE COMPLETE QUADRATIC EQUATION.

```

B = 0
K = 0
DO 70 J = 1, NIND
DO 71 I = J, NIND
  K = K+1
  B = B+C(K)*X(J)*X(I)
CONTINUE
CONTINUE
  
```

```

DO 72 J = 1, NIND
  K = K+1
  B = B+C(K)*X(J)
CONTINUE
  
```

K = K+1



```

B = B+C(K)
WRITE(6,84) B
FORMAT(/,2X, ' THE SCALED QFPT IS : ',2X,G15.7)
84
BR = B * Z(NIND + 1)

```

THE FOLLOWING ENSURES THAT THE OUTPUT STAYS IN WITHIN LIMITS.

```

XHI = 480.0
XLO = 25.0

```

```

BR = AMAX1(XLO, BR)
BR = AMIN1(XHI, BR)

```

```

WRITE(6,85) BR
FORMAT(/,2X, ' QFPT IS : ',2X,G15.7)
85

```

```

RETURN
END

```

```

C*****
C SUBROUTINE PART(A,B)*****
C*****

```

THIS SUBROUTINE CALCULATES THE ELEMENTS OF THE 'A' AND 'B' MATRICES IN THE STATE SPACE EQUATION:

$$XDOT = A*X + B*U .$$

```

COMMON OC, NG, P2, QH, MA, T2, ME, P4, QF, MAF, T4, NS, QD, WW
DIMENSION A(2,2), B(2,2)
REAL NG, NS, ME, MA, MAF, JG, JD

```

```

JG = 0.009525 * 2 * 3.14159 / 60.0
JD = 0.6738 * 2 * 3.14159 / 60.0

```

CALL SUBROUTINES TO GET PARTIAL DERIVATIVES.

```

CALL DMA(NG, P2, DMADNG, DMADP2)
CALL DT2(NG, P2, DT2DNG, DT2DP2)
CALL DOC(NG, P2, DOCDNG, DOCDP2)
CALL DP2(NG, MA, T2, ME, P4, DP2DNG, DP2DME, DP2DMA, DP2DT2, DP2DP4)
CALL DT4(NG, MA, T2, ME, P4, DT4DNG, DT4DME, DT4DMA, DT4DT2, DT4DP4)

```

```

CALL DOHT(NG,MA,T2,ME,P4,DOHDNG,DOHDME,DOHDMA,DOHDT2,DQHDP4)
CALL DP4(MAF,T4,NS,DP4DNS,DP4MAF,DP4DT4)
CALL DQFT(MAF,T4,NS,DQFDNS,DQFMAF,DQFDT4)
CALL DQD(NS,WW,DQDDNS,DQDDWW)

```

```

C
C
C
C

```

COMPUTE THE COEFFICIENTS OF THE STATE SPACE EQUATIONS ( I.E. THE ELEMENTS OF THE A AND B MATRICES).

```

A1 = DOHDMA
A2 = DOHDT2
A3 = DOHDME
A4 = DQHDP4
A5 = DOHDNG
A6 = DQCDP2
A7 = DQCDNG
B1 = DMADP2
B2 = DMADNG
C1 = DT2DP2
C2 = DT2DNG
D1 = DP4MAF
D2 = DP4DT4
D3 = DP4DNS
E1 = DP2DMA
E2 = DP2DT2
E3 = DP2DMF
E4 = DP2DP4
E5 = DP2DNG
F1 = DT4DMA
F2 = DT4DT2
F3 = DT4DMF
F4 = DT4DP4
F5 = DT4DNG
Z1 = DQFDNS
Z2 = DQFMAF
Z3 = DQFDT4
Z4 = DQDDNS
Z5 = DQDDWW
G1 = 1-F4*D2
G2 = (F1+F4*D1)/G1
G3 = F2/G1
G4 = (F3+F4*D1)/G1
G5 = F4*D3/G1
G6 = F5/G1
G7 = (1-E1*B1-E2*C1)
G8 = (E1*B2+E2*C2+E5)/G7
G9 = E3/G7
G10 = E4/G7
G11 = (A1*B1+A2*C1-A6)
G12 = (A1*B2+A2*C2+A5-A7)
G13 = A3

```

```

G14 = A4
G15 = G11*G8+G12
G16 = G11*G9+G13
G17 = G11*G10+G14
G18 = { D1+D2*G2 }
G19 = { D1+D2*G4 }
G20 = { D2*G3 }
G21 = { D2*G5+D3 }
G22 = D2*G6
G23 = { G18*B1+G20*C1 }
G24 = { G18*B2+G20*C2+G22 }
G25 = { 1-G23*G10 }
G26 = { G23*G8+G24 } / G25
G27 = { G23*G9+G19 } / G25
G28 = G21/G25
G29 = { G15+G17*G26 }
G30 = { G16+G17*G27 }
G31 = G17*G28
G32 = Z1+Z3*G5-Z4
G33 = Z2+Z3*G2
G34 = Z2+Z3*G4
G35 = Z3*G3
G36 = Z3*G6
G37 = G33*B1+G35*C1
G38 = G33*B2+G35*C2+G36
G39 = { G37*G8+G38 }
G40 = { G37*G9+G34 }
G41 = G37*G10
G42 = G32+G41*G28
G43 = G39+G41*G26
G44 = G40+G41*G27

```

FINAL FORM OF THE 'A' AND 'B' MATRICES.  
! NOTE ! ELEMENTS A33 AND B31 ARE NOT COMPUTED HERE BUT WERE  
DETERMINED EXPERIMENTALLY FROM GAS TURBINE TEST DATA.

FOR ACCELERATIONS USE:

A33 = -0.5  
B31 = 0.5

FOR DECELERATIONS USE:

A33 = -0.87  
B31 = 0.87

A11 = G29/JG  
A12 = G31/JC  
A13 = G30/JG  
A21 = G43/JD

CCCCCCCCCCCCCCCC



```

C C COEFFICIENTS OF THE QUADRATIC CURVE FIT.
C C

```

```

C C { 1 } = 1.570198
C C { 2 } = -0.7270151
C C { 3 } = 0.2529498
C C { 4 } = 0.1880112
C C { 5 } = -0.6588774
C C { 6 } = 0.3668176

```

```

C C SCALING FACTORS.
C C

```

```

C C { Z(1) } = 36000.0
C C { Z(2) } = 43.0
C C { Z(3) } = 13000.0

```

```

C C NIND = 2

```

```

C C DO 686 I = 1, NIND
C C X(I) = XR(I)/Z(I)
C C CONTINUE

```

```

C C 686

```

```

C C DMADNG = 2.0*C(1)*X(1) + C(2)*X(2) + C(4)
C C DMADNG = DMADNG*Z(3)/Z(1)
C C DMADP2 = C(2)*X(1) + 2.0*C(3)*X(2) + C(5)
C C DMADP2 = DMADP2*Z(3)/Z(2)

```

```

C C RETURN
C C END

```

```

C C *****
C C SUBROUTINE DT2(X1, X2, DT2DNG, DT2DP2) *****
C C *****

```

```

C C THIS SUBROUTINE PRODUCES THE FOLLOWING PARTIAL DERIVATIVES:

```

```

C C DT2/DNG, DT2/DP2

```

```

C C DIMENSION X(5), C(21), Z(5), XR(5)

```

```

C C XR(1) = X1
C C XR(2) = X2

```

C C COEFFICIENTS OF THE QUADRATIC CURVE FIT.

C { 1 } = -9.796132  
 C { 2 } = 20.03512  
 C { 3 } = -10.70980  
 C { 4 } = 0.1464243  
 C { 5 } = 1.657819  
 C { 6 } = -0.3884839

C C SCALING FACTORS.

C { Z(1) } = 36000.0  
 C { Z(2) } = 43.0  
 C { Z(3) } = 130.0

C NIND = 2

C 711 DO 500 I = 1, NIND  
 C 500 X(I) = XR(I)/Z(I)  
 C CONTINUE

C DQCDNG = 2.0\*C(1)\*X(1) + C(2)\*X(2) + C(4)  
 C DQCDNG = DQCDNG\*Z(3)/Z(1)

C DQCDP2 = C(2)\*X(1) + 2.0\*C(3)\*X(2) + C(5)  
 C DQCDP2 = DQCDP2\*Z(3)/Z(2)

C RETURN  
 C END

C \*\*\*\*\*  
 C SUBROUTINE DP2(X1, X2, X3, X4, X5, DP2DNG, DP2DME, DP2DMA, DP2DT2, DP2DP4)  
 C \*\*\*\*\*

C THIS SUBROUTINE PRODUCES THE FOLLOWING PARTIAL DERIVATIVES:

DP2/DNG, DP2/DME

DIMENSION X(5), C(21), Z(6), XR(5)

XR(1) = X1  
 XR(2) = X2  
 XR(3) = X3



XR(4) = X4  
 XR(5) = X5

COEFFICIENTS OF THE QUADRATIC CURVE FIT.

C(1) = 4.17287  
 C(2) = -2.839741  
 C(3) = 1.223014  
 C(4) = -1.854803  
 C(5) = -10.26167  
 C(6) = -0.2169524  
 C(7) = -1.156939  
 C(8) = 2.860795  
 C(9) = 5.767990  
 C(10) = -0.101891  
 C(11) = 0.2918  
 C(12) = -0.441640  
 C(13) = 0.7359644  
 C(14) = -9.559825  
 C(15) = 22.88968  
 C(16) = 4.7794  
 C(17) = -2.558953  
 C(18) = 0.272224  
 C(19) = 6.295503  
 C(20) = -28.57775  
 C(21) = 9.380198

SCALING FACTORS.

Z(1) = 36000.0  
 Z(2) = 13000.0  
 Z(3) = 800.0  
 Z(4) = 240.0  
 Z(5) = 20.0  
 Z(6) = 43.0

NIND = 5

DO 500 I = 1, NIND  
 X(I) = XR(I)/Z(I)  
 CONTINUE

DP2DNG = 2\*C(1)\*X(1) + C(2)\*X(2) + C(3)\*X(3) + C(4)\*X(4)  
 + C(5)\*X(5) + C(16)  
 DP2DNG = DP2DNG\*Z(6)/Z(1)

DP2DME = C(4)\*X(1) + C(8)\*X(2) + C(11)\*X(3) + 2\*C(13)\*X(4)  
 + C(14)\*X(5) + C(19)

```

C      DP2DMF = DP2DMF*Z(6)/Z(4)
      1  DP2DMA = C(2)*X(1) + C(7)*X(3) + C(8)*X(4) + 2*C(6)*X(2)
      C  DP2DMA = DP2DMA*Z(5) + C(17)
      C  DP2DMA = DP2DMA*Z(6)/Z(2)
      1  DP2DT2 = C(3)*X(1) + C(7)*X(2) + C(11)*X(4) + 2*C(10)*X(3)
      C  DP2DT2 = DP2DT2*X(5) + C(18)
      C  DP2DP4 = C(5)*X(1) + C(9)*X(2) + C(12)*X(3) + 2*C(15)*X(5)
      C  DP2DP4 = DP2DP4*Z(4) + C(20)
      C  DP2DP4 = DP2DP4*Z(6)/Z(5)

      RETURN
      END

C*****
C      SUBROUTINE DT4(X1, X2, X3, X4, X5, DT4DNG, DT4DMF, DT4DMA, DT4DT2, DT4DP4)
C*****

```

THIS SUBROUTINE PRODUCES THE FOLLOWING PARTIAL DERIVATIVES:

DT4/DNG, DT4/DMF  
 DIMENSION X(5), C(21), Z(6), XR(5)

```

XR(1) = X1
XR(2) = X2
XR(3) = X3
XR(4) = X4
XR(5) = X5

```

COEFFICIENTS OF THE QUADRATIC CURVE FIT.

```

C(1) = -22.20944
C(2) = 10.79398
C(3) = 21.99301
C(4) = 86.64350
C(5) = -208.0447
C(6) = 1.232848

```

```

C( 7) = -12.46899
C( 8) = -64.69914
C( 9) = 180.0014
C(10) = -0.6479730
C(11) = 20.21592
C(12) = 16.70037
C(13) = 21.1824
C(14) = 183.1548
C(15) = 138.3667
C(16) = -117.2714
C(17) = -18.03533
C(18) = 72.75989
C(19) = -229.4335
C(20) = 73.97864
C(21) =

```

CC  
CC  
CC

SCALING FACTORS.

```

Z( 1) = 36000.0
Z( 2) = 13000.0
Z( 3) = 800.0
Z( 4) = 240.0
Z( 5) = 20.0
Z( 6) = 1800.0

```

CC  
CC

NIND = 5

```

DO 500 I = 1,NIND
X(I) = XR(I)/Z(I)
CONTINUE

```

C 711  
C 500  
CC

```

1 DT4DNG = 2*C( 1)*X( 1) + C( 2)*X( 2) + C( 3)*X( 3) + C( 4)*X( 4)
+ C( 5)*X( 5) + C( 16)
DT4DNG = DT4DNG*Z( 6)/Z( 1)

1 DT4DMF = C( 4)*X( 1) + C( 8)*X( 2) + C( 11)*X( 3) + 2*C( 13)*X( 4)
+ C( 14)*X( 5) + C( 19)
DT4DMF = DT4DMF*Z( 6)/Z( 4)

1 DT4DMA = C( 2)*X( 1) + C( 7)*X( 3) + C( 8)*X( 4) + 2*C( 6)*X( 2)
+ C( 9)*X( 5) + C( 17)
DT4DMA = DT4DMA*Z( 6)/Z( 2)

1 DT4DT2 = C( 3)*X( 1) + C( 7)*X( 2) + C( 11)*X( 4) + 2*C( 10)*X( 3)
+ C( 12)*X( 5) + C( 18)
DT4DT2 = DT4DT2*Z( 6)/Z( 3)

```

C  
C  
C  
C  
C

```

1      DT4DP4 = C(5)*X(1) + C(9)*X(2) + C(12)*X(3) + 2*C(15)*X(5)
      + C(14)*X(4) + C(20)
      DT4DP4 = DT4DP4*Z(6)/Z(5)

```

```

      RETURN
      END

```

```

C*****
SUBROUTINE DQHT(X1,X2,X3,X4,X5,DQHDNG,DQHDMF,DQHDMA,DQHDT2,DQHDP4)
C*****

```

THIS SUBROUTINE PRODUCES THE FOLLOWING PARTIAL DERIVATIVES: ;

DQH/DNG, DQH/DMF, DQH/DMA, DQH/DT2, DQH/DP4

DIMENSION X(5),C(21),Z(6),XR(5)

```

XR(1) = X1
XR(2) = X2
XR(3) = X3
XR(4) = X4
XR(5) = X5

```

COEFFICIENTS OF THE QUADRATIC CURVE FIT.

```

C(1) = 343.8178
C(2) = -562.3596
C(3) = -23.65895
C(4) = -54.97896
C(5) = 98.09515
C(6) = 217.8508
C(7) = 3.591497
C(8) = 119.9962
C(9) = -248.3938
C(10) = -0.1507291
C(11) = 17.95723
C(12) = -17.87346
C(13) = -40.67739
C(14) = 28.27711
C(15) = 190.2205
C(16) = -160.9423
C(17) = 260.8458

```

```

C(18) = 21.40023
C(19) = -34.85067
C(20) = -219.0661
C(21) = 62.16870

```

SCALING FACTORS.

```

Z(1) = 36000.0
Z(2) = 13000.0
Z(3) = 800.0
Z(4) = 240.0
Z(5) = 20.0
Z(6) = 130.0

```

NIND = 5

```

DO 500 I = 1, NIND
X(I) = XR(I)/Z(I)
CONTINUE

```

```

1 DQHDNG = 2*C(1)*X(1) + C(2)*X(2) + C(3)*X(3) + C(4)*X(4)
  + C(5)*X(5) + C(16)/Z(1)
1 DQHDNG = DQHDNG*Z(6)/Z(1)
1 DQHDMF = C(4)*X(1) + C(8)*X(2) + C(11)*X(3) + 2*C(13)*X(4)
  + C(14)*X(5) + C(19)
1 DQHDMF = DQHDMF*Z(6)/Z(4)
1 DQHDMA = C(2)*X(1) + C(7)*X(3) + C(8)*X(4) + 2*C(6)*X(2)
  + C(9)*X(5) + C(17)/Z(2)
1 DQHDMA = DQHDMA*Z(6)/Z(2)
1 DQHDT2 = C(3)*X(1) + C(7)*X(2) + C(11)*X(4) + 2*C(10)*X(3)
  + C(12)*X(5) + C(18)
1 DQHDT2 = DQHDT2*Z(6)/Z(3)
1 DQHDP4 = C(5)*X(1) + C(9)*X(2) + C(12)*X(3) + 2*C(15)*X(5)
  + C(14)*X(4) + C(20)
1 DQHDP4 = DQHDP4*Z(6)/Z(5)

```

```

RETURN
END

```

\*\*\*\*\*

C\*\*\*\*\*  
 C SUBROUTINE DP4(X1 X2 X3 DP4DNS DP4MAE DP4DT4)\*\*\*\*\*  
 C\*\*\*\*\*

C THIS SUBROUTINE PRODUCES THE FOLLOWING PARTIAL DERIVATIVES:  
 C DP4/DNS

C DIMENSION X(5),C(21),Z(6),XR(5)

C XR(1) = X1  
 C XR(2) = X2  
 C XR(3) = X3

C COEFFICIENTS OF THE QUADRATIC CURVE FIT.

C C(1) = 0.1926178  
 C C(2) = 1.158328  
 C C(3) = 0.1008366  
 C C(4) = 6.138049E-02  
 C C(5) = 8.429369E-02  
 C C(6) = -5.136141E-02  
 C C(7) = -0.8789043  
 C C(8) = -1.171511  
 C C(9) = -4.834537E-02  
 C C(10) = 1.559548

C SCALING FACTORS.

C Z(1) = 13000.0  
 C Z(2) = 1800.0  
 C Z(3) = 3000.0  
 C Z(4) = 20.0

C NIND = 3

C DO 500 I = 1,NIND  
 C X(I) = XR(I)/Z(I)  
 C CONTINUE

C DP4DNS = C(3)\*X(1) + C(5)\*X(2) + 2\*C(6)\*X(3) + C(9)  
 C DP4DNS = DP4DNS\*Z(4)/Z(3)







DQDDWW = DQDDWW\*XWW/XQD

C  
C  
C

RETURN  
END

\$ENTRY



1, 144.4, .15, 201.8, .3, 224.7, .35, 219.0, .40, 236.2, ...  
 2, 219.0, .25, 224.7, .55, 230.4, .60, 241.9, ...  
 45, 236.2, .50, 224.7, .75, 184.6, .80, 167.4, .85, 155.9, ...  
 65, 213.2, .75, 184.6, .80, 167.4, .85, 155.9, ...  
 90, 155.9, .95, 150.2, 1.0, 144.4, 1.05, 138.7, ...  
 1, 1138.7, .1, 138.7, 1.2, 138.7, 1.25, 138.7  
 1, 15, 138.7, .05, 0, ...

AFGEN NGDATA = 0.0, 0, .05, 0, ...

1, 0, .15, 1, .3, 6, 35, 8, .40, 10, ...  
 2, 2, 5, .25, 4, .50, 14, .75, 23, .80, 24, .85, 25, ...  
 45, 11.5, .50, 14, .75, 23, .80, 24, .85, 25, ...  
 65, 20, .7, 21.5, .95, 25.5, 1.0, 25.5, 1.05, 25, ...  
 90, 25, .95, 25.5, 1.0, 25.5, 1.05, 25, ...

AFGEN NSDATA = 0.0, 0, 1.2, 24.5, 1.25, 24.5

1, 0, .15, 0, .3, 2, 35, 2.5, .40, 3.5, ...  
 2, 0.5, .25, 1, .55, 7, .60, 8, ...  
 45, 4.5, .50, 6, .75, 12, .80, 13, .85, 13.5, ...  
 65, 9, .7, 10.5, .95, 15, 1.0, 15.5, 1.05, 16, ...  
 90, 14.5, .95, 15, 1.0, 15.5, 1.05, 16, ...  
 1, 15, 16, 1.2, 16, 1.25, 16

THIS SET IS FOR EXPERIMENTAL RUN # 4.

AFGEN MFDATA = 0.0, 1.0, .05, 2.0, ...

1, 3, 0, .15, 6, 0, .3, 17, 0, .35, 19, 0, .40, 21, 0, ...  
 2, 13, 0, .25, 15, 0, .55, 23, 0, .60, 23, 0, .80, 20, 0, .85, 19, 0, ...  
 45, 22, 0, .50, 23, 0, .75, 21, 0, .80, 20, 0, .85, 19, 0, ...  
 65, 23, 0, .7, 22, 0, .95, 14.5, 1.0, 14.6, 1.05, 10.0, ...  
 90, 17, 0, .95, 14.5, 1.0, 14.6, 1.05, 10.0, ...  
 1, 15, 7, 0, .1, 2, 8, 0, .1, 25, 8, 0, .1, 45, 9, 0, .1, 50, 9, 0, ...  
 1, 30, 8, 0, .1, 35, 8, 0, .1, 40, 8, 0, .1, 45, 9, 0, .1, 50, 9, 0, ...  
 1, 55, 9, 50, .1, 60, 9, 50, .1, 70, 9, 50, .1, 75, 9, 50, .1, 80, 9, 50, .1, 85, 9, 50, ...  
 1, 90, 9, 50, .1, 95, 9, 50, .2, 0, 9, 50, .2, 0, 9, 50, .2, 10, 9, 50, ...

AFGEN NGDATA = 0.0, 4.0, .05, 4.0, ...

1, 4, 0, .15, 5, 0, .3, 8, 50, .35, 10, 50, .40, 13, 0, ...  
 2, 4, 15, 0, .25, 17, 5, .55, 20, 0, .60, 22, 0, .80, 30, 0, .85, 31, 0, ...  
 45, 15, 0, .50, 17, 5, .75, 26, 5, .80, 30, 0, .85, 31, 0, ...  
 65, 24, 5, .7, 26, 5, .95, 33, 6, 1.0, 34, 6, 1.05, 34, 6, ...  
 90, 32, 5, .95, 33, 6, 1.0, 34, 6, 1.05, 34, 6, ...

1, 15, 34, 6, .1, 2, 34, 0, 1.25, 33, 5, 1.3, 33, 0, 1.35, 33, 0, ...  
 1, 40, 33, 0, .1, 45, 32, 6, 1.50, 32, 6, 1.55, 32, 0, 1.60, 32, 0, ...  
 AFGEN NSDATA = 0.0, 1.0, .05, 1.0, ...

1, 1, 0, .15, 1, 0, .3, 3, 50, .35, 4, 50, .40, 6, 0, ...  
 2, 2, 0, .25, 2, 50, .3, 3, 50, .35, 4, 50, .40, 6, 0, ...

\*\*\*\*\*





```

A21 = 0.3025516
A22 = -5.2999960
A23 = 0.7975193
A31 = 0.0000000
A32 = 0.0000000
A33 = -0.5000000
B11 = 0.0000000
B12 = 0.0000000
B21 = 0.0000000
B22 = -368.9609000
B31 = 0.5000000
B32 = 0.0000000

```

```

"A" AND "B" MATRICES FOR NG = 29500.0000000
AND NS = 1090.0000000

```

```

A11 = -18.5633600
A12 = -13.8810100
A13 = 2864.8290000
A21 = 0.5190844
A22 = -7.5316480
A23 = -1.7081720
A31 = 0.0000000
A32 = 0.0000000
A33 = -0.5000000
B11 = 0.0000000
B12 = 0.0000000
B21 = 0.0000000
B22 = -503.6293000
B31 = 0.5000000
B32 = 0.0000000

```

```

AVERAGE "A" AND "B" MATRICES FOR RUN#1.

```

```

A11 = -15.686
A12 = -9.157
A13 = 2486.73
A21 = 0.4109
A22 = -6.416
A23 = -0.455
A33 = -0.5
B22 = -436.3
B31 = 0.5

```

```

ESTABLISH INITIAL CONDITIONS.

```

\*\*\*\*\*

```

11 WRITE(3,11)
   FORMAT(/,2X,'INPUT INITIAL GAS GEN. SPEED ,NGO')
10 READ(4,16) NGO
   FORMAT(F15.7)
21 WRITE(3,21) NGO
   FORMAT(F15.7)
31 WRITE(3,31)
   FORMAT(/,2X,'INPUT INITIAL DYNO SPEED, NSO')
30 READ(4,36) NSO
   FORMAT(F15.7)
41 WRITE(3,41) NSO
   FORMAT(F15.7)
*
* CALL STEADY STATE PROGRAM TO GET INITIAL FUEL FLOWRATE, MFO,
* AND DYNO WATER WEIGHT, WWO.
*
* CALL STEADY(NGO,NSO,MFO,WWO)
*
33 WRITE(3,33) MFO
   FORMAT(/,2X,'THE ORIGINAL FUEL FLOW RATE IS : ',F15.7)
34 WRITE(3,34) WWO
   FORMAT(/,2X,'THE ORIGINAL WATER WEIGHT IS : ',F15.7)
*
* SET INITIAL STATE PERTURBATION TO ZERO
*
* DNG = 0.0
* DNS = 0.0
* DE  = 0.0
*
* EO = MFO
*
*
*
* DERIVATIVE
*
* COMPUTE INPUT TO THE NONLINEAR MODEL, ME(T), WW(T).
*
* RUN #1
*
* MEM = AFGEN(MEDATA,TIME)
* WW1 = 2.263*RAMP(0.05)
* WW2 = -2.263*RAMP(0.75)
*
*
* RUN #4
*
* DIV = AFGEN(MEDATA,TIME)

```

```

MEM = MEO-4.489*(DIV-1.0)
WW1 = .7069*RAMP(0.00)
WW2 = -.7069*RAMP(1.60)

```

RUN #10

```

DIV = AEGEN(MFDATA, TIME)
MEM = MEO+5.217*(DIV-3.0)
WW1 = .6130*RAMP(0.00)
WW2 = -.6130*RAMP(1.60)

```

ALL RUNS

DYNAMIC EQUATIONS FOR NONLINEAR MODEL.

```

E = REALPL(MEO, T, MEM)
WW = WWO+WW1+WW2
NGDOT = (DELOG/JG)*60/(2*PI)
NG = INTGRL(NGO, NGDOT)
NSDOT = (DELOG/JD)*60/(2*PI)
NS = INTGRL(NSO, NSDOT)

DME = MEM-MEO
DWW = WW-WWO
DNGDOT = A11*DNG + A12*DNS + A13*DE
DNSDOT = A21*DNG + A22*DNS + A23*DE + B22*DWW
DEDOT = A33*DE + B31*DME
DNG=INTGRL(0.0, DNGDOT)
DNS=INTGRL(0.0, DNSDOT)
DE=INTGRL(0.0, DEDOT)
NGF = NGO + DNG
NSF = NSO + DNS
EF = EO + DE

```

DYNAMIC

THE STATEMENTS IN THE PREVIOUS (DERIVATIVE) SECTION YIELD VALUES OF 'NG', AND 'NS' AS CALCULATED BY THE NONLINEAR AND STATE SPACE MODELS. THE STATEMENTS BELOW COMPUTE THE VALUES OF 'NG', AND 'NS' AS RECORDED FROM GAS TURBINE TEST DATA.

RUN #1

```

NGD = NGO+183.67*AFGEN(NGDATA, TIME)
NSD = NSO+8.125*AFGEN(NSDATA, TIME)

```

RUN #4

```

NGDIV = NLEGEN(NGDATA, TIME)

```

```

NSDIV = NLFGEN(NSDATA, TIME)
NGD = NGO-185.36*(NGDIV-4)
NSD = NSO-16.27*(NSDIV-1)

```

RUN #10

```

NGDIV = NLFGEN(NGDATA, TIME)
NSDIV = NLFGEN(NSDATA, TIME)
NGD = NGO+192.96*(NGDIV-5)
NSD = NSO+10.65*(NSDIV-4)

```

CALL SUBROUTINE 'TORK' WHICH USES THE STEADY STATE MODEL TO GET COMPRESSOR AND HPT TORQUE VALUES.

```

PROCED DELOG DELQD = BLK(NG, NS, E, WW, DELQ, DELQD)
CALL TORK(NG, NS, E, WW, DELQ, DELQD)
CONTINUE

```

ENDPRO  
TERMINAL

```

METHOD STIFF
RELERR NS = 1.E-6, NG = 1.E-6, DNS = 1.E-6, DNG = 1.E-6, DQ = 1.E-6
ABSERR NS = 1.E-5, NG = 1.E-5, DNS = 1.E-5, DNG = 1.E-5, DQ = 1.E-5
CONTROL FINTIM=2.00, DELT=1.E-5
PRINT 0.05 MEM, NGD, NG, NGF, NSD, NS, NSF
* SAVE 0.05 MEM, NG, NGD, NS, NSD
SAVE 0.05, MEM, NG, NGD, NS, NSD, NGF, NSF, EF

```

RUN #1

```

GRAPH (DE=TEK618) TIME(LO=0.0, SC=0.2, TI=0.50, NI=10, UN=SEC) ...
NS(LO=900, SC=100, TI=1.6, NI=5, UN=RPM) ...
NSD(LO=900, SC=100, TI=1.6, NI=5, UN=RPM) ...
NSF(LO=900, SC=100, TI=1.6, NI=5, UN=RPM) ...
EF(LO=100, SC=10, TI=2, NI=4, UN=LB/HR) ...
MEM(LO=100, SC=10, TI=2, NI=4, UN=LB/HR) ...
NG(LO=24000, SC=1000, TI=1.1428, NI=7, UN=RPM) ...
NGD(LO=24000, SC=1000, TI=1.1428, NI=7, UN=RPM) ...
NGF(LO=24000, SC=1000, TI=1.1428, NI=7, UN=RPM) ...

```

RUN #4

```

GRAPH (DE=TEK618) TIME(LO=0.0, SC=0.2, TI=0.50, NI=10, UN=SEC) ...
NG(LO=24000, SC=1000, TI=1.33, NI=6, UN=RPM) ...
NSD(LO=24000, SC=1000, TI=1.33, NI=6, UN=RPM) ...
NS(LO=700, SC=100, TI=1.6, NI=5, UN=RPM) ...
NSD(LO=700, SC=100, TI=1.6, NI=5, UN=RPM) ...
MEM(LO=100, SC=10, TI=1.6, NI=5, UN=LB/HR) ...

```

RUN #4

```

* GRAPH (DE=TEK618) TIME(LO=0.0, SC=0.2, TI=.50, NI=10, UN=SEC) ...
* NG(LO=21000, SC=1000, TI=1.33, NI=6, UN=RPM) ...
* NGD(LO=21000, SC=1000, TI=1.33, NI=6, UN=RPM) ...
* NS(LO=900, SC=100, TI=2.0, NI=4, UN=RPM) ...
* NSD(LO=900, SC=100, TI=2.0, NI=4, UN=RPM) ...
* MEM(LO=80, SC=10., TI=2.0, NI=4, UN=LB/HR) ...
*
* RUN #1 THIS IS FOR THESIS PRESENTATION FIGURES
*
* GRAPH (G2, DE=TEK618) TIME(LO=0.0, SC=0.2, TI=.50, NI=10, UN=SEC) ...
* NSD(LO=900, SC=100, TI=1.6, NI=5, UN=RPM) ...
* NS(LO=900, SC=100, TI=1.6, NI=5, UN=RPM) ...
* NSF(LO=900, SC=100, TI=1.6, NI=5, UN=RPM) ...
* EF(LO=100, SC=10., TI=2., NI=4, UN=LB/HR) ...
* MEM(LO=100, SC=10., TI=2., NI=4, UN=LB/HR) ...
*
* GRAPH (G1, DE=TEK618) TIME(LO=0.0, SC=0.2, TI=.50, NI=10, UN=SEC) ...
* NGD(LO=24000, SC=1000, TI=1.1428, NI=7, UN=RPM) ...
* NG(LO=24000, SC=1000, TI=1.1428, NI=7, UN=RPM) ...
* NGF(LO=24000, SC=1000, TI=1.1428, NI=7, UN=RPM) ...
*
* LABEL (G1) GAS GENERATOR SPEED
* LABEL (G2) DYNAMOMETER SPEED
C
END
STOP
FORTRAN
C
C*****
C SUBROUTINE STEADY(NG, NS, MF, WW)
C*****
C
C THIS PROGRAM PROVIDES THE INITIALIZATION PROCESS FOR THE DYNAMIC
C PROGRAM. SPECIFICALLY, THE USER INPUTS GAS GENERATOR AND DYNO
C SPEEDS, AND THE PROGRAM USES STEADY STATE MAPS (IN EQUATION FORM)
C OF SYSTEM INPUTS/OUTPUTS TO FIND STEADY STATE VALUES.
C
C
C 1 REAL NG, NS, MF, MA, NSO, NGO, MFO, MAFO, MAO, MEDEL, MEU, MEL,
C MF1, ME2, MEMIN, MERR
C
C ESTABLISH THE CONVERGENCE TOLERANCES.
C
C WWERR = 0.05
C MERR = 0.001
C PERR = 0.05
C QERR = 0.01
C

```

```

C FIND AN INITIAL "GOOD GUESS" FOR 'MF' GIVEN 'NG' AND 'NS'.
C
C CALL NGNSMF(NG,NS,MF)
C
C MF1 = MF
C XCOUNT = 0.0
C
C CONVERGE ON 'P2' AND 'P4' FOR THE GIVEN 'MF', 'NG' AND 'NS'.
C
C 5 CALL P2P4(NG,NS,MF,PERR,QPERC,P2G,P4G)
C
C 299 CALL SUBMA(NG,P2G,MA)
C CALL SUBT2(NG,P2G,T2)
C CALL SUBQC(NG,P2G,QC)
C CALL SUBQHT(NG,MA,T2,MF,P4G,QHPT)
C MAF = MA + MF
C CALL SUBT4(NG,MA,T2,MF,P4G,T4)
C CALL SUBOFT(MAF,T4,NS,QEPT)
C QPERC = 100*(QHPT-QC)/QHPT
C
C IF(ABS(QPERC).LT.QERR) GO TO 300
C
C ESTABLISH UPPER AND LOWER BOUNDS ON 'MF'.
C
C XCOUNT = XCOUNT + 1.0
C X1 = 1.0
C XSIGN = -1.0 * SIGN(X1,QPERC)
C MEDEL = 2.0
C IF(XCOUNT.GT.1.5) GO TO 33
C
C XSIGN1 = XSIGN
C ME2 = MF1 + XSIGN * MEDEL
C MF = ME2
C QPERC1 = QPERC
C GO TO 5
C
C 33 IF((XSIGN1*XSIGN).LT.0.5) GO TO 298
C
C ME2 = MF1 + XSIGN1 * MEDEL * XCOUNT
C MF = ME2
C
C GO TO 5
C
C USE THE GOLDEN SECTION METHOD TO FIND THE VALUE OF 'MF' THAT
C WILL LEAD TO ZERO GAS GENERATOR TORQUE MISMATCH.
C

```



```

298      QPERC2 = QPERC
C
C      IF(MF2.LT.MF1) GO TO 34
C
C      MFU = MF2
C      MFL = MF1
C      QU = ABS(QPERC2)
C      QL = ABS(QPERC1)
C
C      MFU = MF1
C      MFL = MF2
C      QU = ABS(QPERC1)
C      QL = ABS(QPERC2)
C
C      TAU = 0.381966
C      XN = -2.078 * ALOG(MERR/100.0) + 3
C      WRITE(6,*) ,XN
C      MF1 = (1.0-TAU)*MFL + TAU*(MFU)
C      CALL P2P4(NG,NS,MF1,PERR,QPERC,P2G,P4G)
C      O1 = ABS(QPERC)
C      MF2 = (1.0-TAU)*MFU + TAU*(MFL)
C      CALL P2P4(NG,NS,MF2,PERR,QPERC,P2G,P4G)
C      Q2 = ABS(QPERC)
C      XK = 3.0
C      XK = XK + 1.0
C      MEMIN = (MF1 + MF2)/2
C      ODIF = (O1 + Q2)/2.0
C      IF(ODIF.LT.QERR) GO TO 92
C      IF(XK.GT.XN) GO TO 92
C      IF(Q1.GT.Q2) GO TO 91
C      MFU = MF2
C      QU = Q2
C      MF2 = MF1
C      Q2 = Q1
C      MF1 = (1.0-TAU)*MFL + TAU*(MFU)
C      CALL P2P4(NG,NS,MF1,PERR,QPERC,P2G,P4G)
C      O1 = ABS(QPERC)
C      GO TO 90
C      MFL = MF1
C      QL = Q1
C      MF1 = MF2
C      O1 = Q2
C      MF2 = (1.0-TAU)*MFU + TAU*(MFL)
C      CALL P2P4(NG,NS,MF2,PERR,QPERC,P2G,P4G)
C      O2 = ABS(QPERC)
C      GO TO 90
C      MF = MEMIN

```

C

```

CALL SUBMA(NG,P2G,MA)
CALL SUBT2(NG,P2G,T2)
CALL SUBOC(NG,P2G,OC)
CALL SUBQHT(NG,MA,T2,ME,P4G,QHPT)
MAF = MA + ME
CALL SUBT4(NG,MA,T2,ME,P4G,T4)
CALL SUBQFT(MAF,T4,NS,QEPT)
QPERC = 100*(QHPT-QC)/QHPT

```

C

EQUATE QD = QEPT FOR STEADY STATE AND SOLVE FOR 'WW' USING NEWTON'S METHOD. NOTE THAT 'WWERR' HALTS THE ITERATION.

"WW1" IS THE INITIAL GUESS FOR DYNO WATER WEIGHT. IT IS NEEDED TO START NEWTON'S SCHEME. THE VALUE IS FAIRLY ARBITRARY BUT DO NOT USE 'WW1 = 0.0'!

```

WW1 = 5.00

```

C

```

GG = QD - QEPT, WHERE QD = FCN(WW1)

```

```

C5 = 1.19294E-5

```

```

C3 = 4.0E-6

```

```

C4 = -20.0 + C3*NS*NS

```

```

OD = C4 + C5*NS*NS*(WW1**1.3)

```

```

QG = QD - OEPT

```

```

GGP = 1.3*C5*NS*NS*(WW1**0.3)

```

```

WW = WW1 - GG/GGP

```

```

WWDIFF = 100.0 * ABS((WW - WW1)/WW1)

```

```

IF(WWDIFF.LT.WWERR) GO TO 300

```

```

WW1 = WW

```

```

GO TO 37

```

C

```

RETURN

```

300

C

```

SUBROUTINE TORQ(NS,ME,WW,DELOG,DELOD)

```

\*\*\*\*\*

THE INPUTS TO THIS SUBROUTINE ARE 'NG', 'NS', AND 'ME', AND 'P2', 'P4', AND 'P4'. FOR THESE INPUTS THE SUBROUTINE CONVERGES ON 'P2' AND 'P4' AND FINDS THE "STEADY STATE" TORQUE DIFFERENTIAL, WHICH IS REPRESENTED AS 'DELOG' AND 'DELOD'.

C

REAL NG, NS, ME, MAF, MA, NSO, NGO, MFO, MAFO, MAO, MEDEL, MFU, MEL

P2G AND P4G ARE NOMINAL VALUES OF COMPRESSOR DISCHARGE AND FPT INLET PRESSURES. THEY PROVIDE AN INITIAL GUESS FOR THE CONVERGENCE ROUTINE. P2ERR AND P4ERR ARE THE MAXIMUM ALLOWABLE DIFFERENCES BETWEEN P2G AND P2 , AND BETWEEN P4G AND P4.

```

P2G = 31.5
P4G = 17.0
P2ERR = 0.05
P4ERR = 0.05
ZS = 50.0
ZX = 0.0

```

COMPUTE COMPRESSOR OUTPUTS.

```

10 ZX = ZX + 1.0

```

```

CALL SUBMA(NG, P2G, MA)
CALL SUBT2(NG, P2G, T2)
CALL SUBQC(NG, P2G, QC)

```

COMPUTE P2 AND CHECK AGAINST P2G.

```

20 CALL SUBP2(NG, MA, T2, ME, P4G, P2)
P2DIFF = 100.0 * ABS(P2 - P2G)/P2
P2G = P2
P2G = P2G + 0.5*(P2-P2G)
IF(ZX.GT.ZS) GO TO 511
IF(P2DIFF.GT.P2ERR) GO TO 10

```

```

511 ZX = 0.0

```

COMPUTE HPT OUTPUTS.

```

MAF = MA + MF
WRITE(6, *) 'MAF = ', MAF

```

```

47 CALL SUBT4(NG, MA, T2, ME, P4G, T4)

```

COMPUTE P4 AND CHECK AGAINST P4G.

```

CALL SUBP4(MAF, T4, NS, P4)
P4DIFF = 100.0 * ABS(P4 - P4G)/P4

```



APPENDIX E  
STATE EQUATION FORMULATION

1. Note that for any variable Y,

$$Y = Y_0 + \Delta Y$$

where Y. = final value

Y<sub>0</sub> = initial value

$\Delta Y$  = change in Y

Assume the initial condition, Y<sub>0</sub>, is known. Then the final state, Y, can be found if  $\Delta Y$  is known.

Applying a Taylor series approximation to Y, where Y is a function of X (i.e. Y = Y(X)) yields,

$$Y - Y_0 = \Delta Y = Y_0 + Y_0'(\Delta X) + Y_0''(\Delta X)^2/2! + \dots + Y_0^{(n)}/n! .$$

For very small changes in X, a linear approximation can be made:

$$Y = dY = Y_0 + Y_0 * dX.$$

As a convenience of notation the following substitution is made:

$$dY = y$$

2. If Y is a function of X (i.e. Y = Y(X)), then (making the linear assumption)

$$\partial Y / \partial X = \partial Y_0 / \partial X + \partial y / \partial X.$$

But  $\partial Y_0 / \partial X = 0$ , since Y<sub>0</sub> is a constant.

Then in general,

$$\partial Y / \partial X = \partial y / \partial X.$$

3. In what follows the state space equation set for the propulsion test facility is derived by using a linear Taylor series approximation for each of the input/output equations used in the nonlinear model.

$$\begin{aligned}
 \dot{N}G &= (QH-QC)/JG \\
 QH &= QH(Ma, T2, E, NG, P4) \\
 QC &= QC(P2, NG) \\
 \dot{n}g &= (\partial QH/\partial Ma)ma + (\partial QH/\partial T2)t2 + (\partial QH/\partial E)e + \\
 &\quad \dots (\partial QH/\partial NG)ng + (\partial QH/\partial P4)p4 - \\
 &\quad \dots (\partial QC/\partial P2)p2 - (\partial QC/\partial NG)ng \\
 \dot{n}g &= a1*ma + a2*t2 + a3*e + a4*p4 + a5*ng - \\
 &\quad \dots a6*p2 - a7*ng \tag{1}
 \end{aligned}$$

$$\begin{aligned}
 Ma &= Ma(P2, NG) \\
 ma &= (\partial Ma/\partial P2)p2 + (\partial Ma/\partial NG)ng \\
 &= b1*p2 + b2*ng \tag{2}
 \end{aligned}$$

$$\begin{aligned}
 P2 &= P2(Ma, T2, E, P4, NG) \\
 p2 &= (\partial P2/\partial Ma)ma + (\partial P2/\partial T2)t2 + (\partial P2/\partial E)e + \\
 &\quad \dots (\partial P2/\partial NG)ng + (\partial P2/\partial P4)p4 \\
 p2 &= e1*ma + e2*t2 + e3*e + e4*p4 + e5*ng \tag{3}
 \end{aligned}$$

$$\begin{aligned}
 T2 &= T2(P2, NG) \\
 t2 &= (\partial T2/\partial P2)p2 + (\partial T2/\partial NG)ng \\
 &= c1*p2 + c2*ng \tag{4}
 \end{aligned}$$

substitute (2), (4) into (3),

$$\begin{aligned}
 p2 &= e1(b1*p2+b2*ng)+e2(c1*p2+c2*ng)+\dots \\
 &\quad e3*e+e4*p4*e5*ng \tag{5}
 \end{aligned}$$

$$\begin{aligned}
 P4 &= P4(Maf, T4, NS) \\
 p4 &= (\partial P4/\partial Maf)maf + (\partial P4/\partial T4)t4 + \dots \\
 &\quad (\partial P4/\partial NS)ns \\
 p4 &= d1*maf + d2*t4 + d3*ns \\
 maf &= ma + e \\
 p4 &= d1*(ma+e) + d2*t4 + d3*ns \tag{6}
 \end{aligned}$$

$$\begin{aligned}
 T4 &= T4(Ma, T2, E, P4, NG) \\
 t4 &= (\partial T4/\partial Ma)ma + (\partial T4/\partial T2)t2 + (\partial T4/\partial E)e + \\
 &\quad \dots (\partial T4/\partial NG)ng + (\partial T4/\partial P4)p4
 \end{aligned}$$



$$t4 = f1*ma + f2*t2 + f3*e + f4*p4 + f5*ng \quad (7)$$

substitute (6) into (7) and solving for t4,

$$t4(1-f4*d2) = ma*(f1+f4*d1) + t2*f2 + \dots e*(t3+f4*d1) + f4*d3*ns + f5*ng \quad (8)$$

let  $g1 = (1-f4*d2)$   
 $g2 = (f1+f4*d1)/g1$   
 $g3 = f2/g1$   
 $g4 = (f3+f4*d1)/g1$   
 $g5 = f4*d3/g1$   
 $g6 = f5/g1$

then  $t4 = g2*ma + g3*t2 + g4*e + g5*ns + g6*ng$

grouping terms in (5),

$$p2(1-e1*b1-e2*c1) = ng(e1*b2+e2*c2+e5) + \dots e*e3 + e4*p4$$

let  $g7 = (1-e1*b1-e2*c1)$   
 $g8 = (e1*b2+e2*c2+e5)/g7$   
 $g9 = e3/g7$   
 $g10 = e4/g7$

then  $p2 = g8*ng + g9*e + g10*p4 \quad (10)$

substitute (2), (4) into (1),

$$ng = a1(b1*p2+b2*ng) + a2(c1*p2+c2*ng) + \dots a3*e + a4*p4 + a5*ng - a6*p2 - a7*ng$$

collecting terms,

$$ng = p2(a1*b1+a2*c1-a6) + ng(a1*b2+a2*c2+a5-a7) \dots a3*e + a4*p4$$

let  $g11 = (a1*b1+a2*c1-a6)$   
 $g12 = (a1*b2+a2*c2+a5-a7)$   
 $g13 = a3$   
 $g14 = a4$

then  $ng = g11*p2 + g12*ng + g13*e + g14*p4 \quad (11)$

substitute (10) into (11) and collecting terms,

$$ng = ng(g11*g8+g12) + e*(g11*g9+g13) + \dots p4*(g11*g10+g14)$$

let  $g15 = (g11*g8+g12)$   
 $g16 = (g11*g9+g13)$

$g_{17} = (g_{11} * g_{10} + g_{14})$   
 then  $\dot{n}g = g_{15} * ng + g_{16} * e + g_{17} * p_4$  (12)  
 substitute (9) into (6) and collect terms,  
 $p_4 = ma(d_1 + d_2 * g_2) + e(d_1 + d_2 * g_4) + t_2 * d_2 * g_3 + \dots$   
 $\quad ns(d_2 * g_5 + d_3) + ng * d_2 * g_6$

let  $g_{18} = (d_1 + d_2 * g_2)$   
 $g_{19} = (d_1 + d_2 * g_4)$   
 $g_{20} = d_2 * g_3$   
 $g_{21} = (d_2 * g_5 + d_3)$   
 $g_{22} = d_2 * g_6$   
 then  $p_4 = g_{18} * ma + g_{19} * e + g_{20} * t_2 + g_{21} * ns \dots$  (13)  
 $\quad + g_{22} * ng$

substitute (2) and (4) into (13) and collect terms,  
 $p_4 = p_2(g_{18} * b_1 + g_{20} * c_1) + ng(g_{18} * b_2 + g_{20} * c_2 + g_{22}) \dots$   
 $\quad \dots + g_{19} * e + g_{21} * ns$

let  $g_{23} = (g_{18} * b_1 + g_{20} * c_1)$   
 $g_{24} = (g_{18} * b_2 + g_{20} * c_2 + g_{22})$   
 $p_4 = g_{23} * p_2 + g_{24} * ng + g_{19} * e + g_{21} * ns$  (14)

substitute (10) into (14) and collect terms,  
 $p_4(1 - g_{23} * g_{10}) = ng(g_{23} * g_8 + g_{24}) + e(g_{23} * g_9 + g_{19}) \dots$   
 $\quad \dots + g_{21} * ns$

let  $g_{25} = (1 - g_{23} * g_{10})$   
 $g_{26} = (g_{23} * g_8 + g_{24}) / g_{25}$   
 $g_{27} = (g_{23} * g_9 + g_{19}) / g_{25}$   
 $g_{28} = g_{21} / g_{25}$   
 $p_4 = g_{26} * ng + g_{27} * e + g_{28} * ns$  (15)

substitute (15) into (12) and collect terms,  
 $\dot{n}g = (g_{15} + g_{17} * g_{26}) + e(g_{16} + g_{17} * g_{27}) + ns * g_{17} * g_{28}$   
 let  $g_{29} = (g_{15} + g_{17} * g_{26})$   
 $g_{30} = (g_{16} + g_{17} * g_{27})$   
 $g_{31} = g_{17} * g_{28}$   
 $\dot{n}g = g_{29} * ng + g_{30} * e + g_{31} * ns$  (16)

$\dot{N}S = (QF - QD) / JD$   
 $QH = QH(NS, Maf, T_4)$

$$\begin{aligned}
Q_D &= Q_D(NS, WW) \\
\dot{n}s &= (\partial Q_F / \partial NS)ns + (\partial Q_F / \partial Maf)maf + (\partial Q_F / \partial T4)t4 - \\
&\quad \dots (\partial Q_D / \partial NS)ns + (\partial Q_D / \partial WW)ww \\
\dot{n}s &= z1*ns + z2*maf + z3*t4 - z4*ns - z5*ww \\
maf &= ma + e \\
\dot{n}s &= z1*ns + z2*ma + z2*e + z3*t4 \dots \quad (19) \\
&\quad - z4*ns - z5*ww
\end{aligned}$$

substitute (9) into (19) and collect terms,

$$\begin{aligned}
\dot{n}s &= ns(z1+z3*g5-z4) + ma(z2+z3*g2) + \dots \\
&\quad e(z2+z3*g4) + t2*z3*g3 + \dots \\
&\quad z3*g6*ng - z5*ww
\end{aligned}$$

$$\begin{aligned}
\text{let} \quad g32 &= (z1+z3*g5-z4) \\
g33 &= (z2+z3*g2) \\
g34 &= (z2+z3*g4) \\
g35 &= t2*z3*g3 \\
g36 &= z3*g6 \\
\dot{n}s &= g32*ns + g33*ma + g34*e + \dots \quad (21) \\
&\quad g35*t2 + g36*ng + g36*ng - z5*ww
\end{aligned}$$

substitute (2) and (4) into (21) and collect terms,

$$\begin{aligned}
\dot{n}s &= ns*g23 + p2(g33*b1+g35*c1) + \dots \\
&\quad ng(g33*b2+g35*c2+g36) + \dots \\
&\quad e*g34 - z5*ww
\end{aligned}$$

$$\begin{aligned}
\text{let} \quad g37 &= (g33*b1+g35*c1) \\
g38 &= (g33*b2+g35*c2+g36) \\
\dot{n}s &= g32*ns + g37*p2 + g38*ng + \dots \quad (22) \\
&\quad g34*e - z5*ww
\end{aligned}$$

substitute (10) into (22) and collect terms,

$$\begin{aligned}
\dot{n}s &= ns*g32 + ng(g37*g8+g38) + e(g37*g9+g34)\dots \\
&\quad + p4*g37*g10 - z5*ww
\end{aligned}$$

$$\begin{aligned}
\text{let} \quad g39 &= (g37*g8+g38) \\
g40 &= (g37*g9+g34) \\
g41 &= p4*g37*g10 \\
\dot{n}s &= g32*ns + g39*ng + g40*e + \dots \quad (23) \\
&\quad g41*p4 - z5*ww
\end{aligned}$$

substitute (15) into (23) and collect terms,

$$\begin{aligned}
 \dot{n}s &= ns(g_{32}+g_{41}g_{28}) + ng(g_{39}+g_{41}g_{26}) \dots \\
 &\quad + e(g_{40}+g_{41}g_{27}) - z_5*ww \\
 \text{let } g_{39} &= (g_{32}+g_{41}g_{28}) \\
 g_{40} &= (g_{39}+g_{41}g_{26}) \\
 g_{41} &= (g_{40}+g_{41}g_{27}) \\
 \dot{n}s &= g_{42}*ns + g_{43}*ng + g_{44}*e - z_5*ww \qquad (24)
 \end{aligned}$$

$$\begin{aligned}
 E &= MF/(tS + 1) \\
 e &= -e/t + mf/t \quad (\dots t = \text{time constant}) \qquad (25)
 \end{aligned}$$

4. Equations (16), (24), and (25) comprise the plant state equations.

## LIST OF REFERENCES

1. Miller, R. J., and Hackney, R. D., F100 Multivariable Control System Engine Models/Design Criteria, AFAPL-TR-76-74, 1976 .
2. Merril, W., Lehtinen, B., Zeller, J., The Role of Modern Control Theory in the Design of Controls for Aircraft Turbine Engines, Journal of Guidance and Control, Vol. 7, pp. 652-659, Nov.-Dec. 1984.
3. Johnson, P. N., Marine Propulsion Load Emulation, M.S. Thesis, Naval Postgraduate School, Monterey, California, June 1986.
4. Szuch, J. R., Models for Jet Engine Systems-pt. 1 Techniques for Jet Engine System Modelling, Control and Dynamic Systems-Advances in Theory and Applications, Vol. 14, edited by C. T. Leondes, Academic Press, 1978.
5. DeHoff, R. L., and Hall, W. E. Jr., Jet Engine Systems Models-pt. 2, State Space Techniques and Modelling for Control, Control and Dynamic Systems-Advances in Theory and Applications, Vol. 14, edited by C. T. Leondes, Academic Press, 1978.
6. Rubis, C. J., and Bodnaruk, A., Acceleration Performance Analysis of a Gas Turbine Destroyer Escort, Journal of Engineering for Power, Jan. 1971.
7. Wylie, C. R., Advanced Engineering Mathematics, McGraw-Hill, 1975.
8. Boeing Airplane Co., Instruction Book for the Boeing Model 502-6a Gas Turbine Engine, Seattle, Washington, 1953.
9. Thompson, W. T., Theory of Vibrations with Applications, Prentice-Hall, 1981.
10. Ogata, K., Modern Control Engineering, Prentice-Hall, 1970.

INITIAL DISTRIBUTION LIST

|   | No. | Copies |
|---|-----|--------|
| 1. Defense Technical Information Center<br>Cameron Station<br>Alexandria, Virginia 22304-6145   | 2   |        |
| 2. Library, Code 0142<br>Naval Postgraduate School<br>Monterey, California 93943-5000   | 2   |        |
| 3. Department Chairman, Code 69<br>Department of Mechanical Engineering<br>Naval Postgraduate School<br>Monterey, California 93943-5000 | 1   |        |
| 4. Prof. D.L. Smith, Code 69Sm<br>Department of Mechanical Engineering<br>Naval Postgraduate School<br>Monterey, California 93943-5000  | 10  |        |
| 5. Prof. R.H. Nunn, Code 69Nn<br>Department of Mechanical Engineering<br>Naval Postgraduate School<br>Monterey, California 93943-5000   | 1   |        |
| 6. LCDR. G.F. Herda, USN (ret.)<br>P.O. Box 116<br>Albany, Minnesota 56307  | 1   |        |
| 7. LT. Vincent J. Herda, USN<br>Long Beach Naval Shipyard<br>Long Beach, California 90822   | 5   |        |
| 8. Mr. M. Resner, Code 56X1<br>Commander, Naval Sea Systems Command<br>Washington, D.C. 20362   | 1   |        |
| 9. Mr. R. Stankey, Code 56Z4<br>Commander, Naval Sea Systems Command<br>Washington, D.C. 20362  | 1   |        |
| 10. Mr. Jim Donnely<br>NAVSES, Phil. NSYD<br>Philadelphia, Pennsylvania 19112-5083  | 1   |        |



*pl*





219259

Thesis  
H48642  
c.1

Herda

Marine gas turbine  
modeling for modern  
control design.

13 APR 68

32838

219259

Thesis  
H48642  
c.1

Herda

Marine gas turbine  
modeling for modern  
control design.

thesH48642

Marine gas turbine modeling for modern c



3 2768 000 67205 9

DUDLEY KNOX LIBRARY