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Design report of hybrid compressor and associated test rig

Vavra, Michael Hans

Monterey, California. Naval Postgraduate School

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NAVAL POSTGRADUATE SCHOOL
Monterey, California

DESIGN REPORT OF HYBRID COMPRESSOR

AND

ASSOCIATED TEST RIG

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by

M. H. Vavra

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NAVAL POSTGRADUATE SCHOOL
Monterey, California

Rear Admiral M. B. Freeman, USN   M. U. Clauser
Superintendent   Provost

ABSTRACT:

    This report presents the aerodynamic calculations and describes the
mechanical features of a test rig that has been designed at the Turbo-
propulsion Laboratory, Department of Aeronautics, for research work on a
special type of centrifugal compressor. This so-called Hybrid compressor
consists of a centrifugal rotor with 180° flow deflection in the meridio-
nal plane followed by an axial flow diffusor. The report establishes a
method to predict the off-design performance of the subject compressor,
which can be applied also to conventional centrifugal compressors.
Extensive use is made of modern programmable calculators, and programs
are presented to show the effectiveness of these tools in engineering
endeavors.

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INTRODUCTION

The idea of arranging an axial diffusor after a special centrifugal compressor rotor that turns the flow by 180° instead of 90°, as in conventional machines, has been conceived by Mr. George Derderian, Naval Air Systems Command, Code AIR-53622B. For this so-called Hybrid compressor concept, he was awarded U. S. Patent 3, 365, 892 dated January 30, 1968.

To verify the conditions that exist after a Hybrid impeller, and to investigate whether it is possible to convert the kinetic energy of the flow after such a rotor into useful pressure rise with acceptable efficiency, a research project was started at the Turbopropulsion Laboratory, NPS, which was funded by the Naval Air Systems Command, under: AIRTASK A3303300/186B/3F41432301.

The present report gives the particulars of the design that led to the manufacture of the test rig which is now operative and being used to carry out the afore-mentioned research work.

The project was supervised by Mr. K. H. Guttmann, AIR-330C, who has been extremely helpful in all phases of the program. The author is deeply grateful to Mr. Guttmann for the patience, understanding and considerateness which he received during a lengthy period of personal misfortune which delayed the research program and the completion of this report.

I. AERODYNAMIC DESIGN

1. Impeller

Because of its peculiar design the rotor of the Hybrid compressor of Fig. 1 is highly stressed. (See Section V.1) Therefore, it must have meridional blades at the discharge to eliminate additional blade bending stresses. Ahead of the rotor the absolute inlet velocity will be axial everywhere. Hence it is possible to establish the rotor dimensions with the method of Ref. 1 which is enclosed as Appendix A. The corresponding dimensions of the Hybrid rotor are shown in Fig. 1.

The symbols used in the following are identical with those listed in Appendix A. For easier reference, the figures and equations of Appendix A are denoted by Fig. A .... and Eq. A .... . Thus, Fig. A(3) is figure 3, and Eq. A II(4) is equation II(14) of Table II of Appendix A.

A parametric study indicated that optimum conditions were obtained for the following design values (see Fig. 1):

$$\beta_{1o} = 55^{\circ}$$

$$\alpha_2 = 65^{\circ}$$

$$R_{1o}/R_2 = 0.55$$

$$R_{1i}/R_2 = 0.18$$

The relatively small angle β_{1o} of 55° is necessary to be able to limit the ratio R_{1o}/R_2 to 0.55 and to obtain a sufficiently high flow rate so that the diffusor blade height b_2 does not become too small. For values of R_{1o}/R_2 larger than 0.55 the meridional flow channel would also have very large curvatures at the blade tip contour of the Hybrid rotor. This would produce large radial velocity gradients at the rotor discharge. The choice of $\alpha_2 = 65^{\circ}$ was predicated by the permissible loading of the axial diffusor blade rows, and the large losses that occur if α_2 is

larger than 65°. A radius ratio $R_{1i}/R_2 = 0.18$ of the hub at the inducer inlet was chosen to be able to arrange 17 rotor blades with a thickness of about 0.125 inches. With smaller ratios R_{1i}/R_2 it is not possible to have 17 blades and it would then be necessary to design the impeller with splitter vanes, a feature which did not seem to be warranted for the present tests.

Preliminary investigation also showed that the peripheral rotor speed U_2 at the mean discharge radius R_2 of Fig. 1 should not exceed about 800 ft/s because of critical speed considerations if the rotor is made of aluminum.

For air with $\gamma = c_p/c_v = 1.4$ and a gas constant $R_G = 53.35$ (ft-lb)/ (lbm, $^\circ$R), the velocity of sound a_0 at an assumed total inlet temperature $T_0 = 520^\circ$R is

$$a_0 = \sqrt{g \, \gamma \, R_G \, T_0} = 1117.85 \text{ ft/s}$$

giving a ratio

$$U_2/a_0 = 0.7156$$

From Eq. A II(4) the Mach number M_{W1} of the relative velocity at the outer radius R_{1o} of the rotor inlet eye is then

$$M_{W1} = \left[\frac{\sin^2 \beta_{1o}}{\left(\frac{R_{1o}}{R_2} \frac{U_2}{a_0} \right)^2} - \frac{\gamma - 1}{2} \cos^2 \beta_{1o} \right]^{-\frac{1}{2}} = 0.4842 \tag{1}$$

For a weight flow rate $\dot{w} = \dot{m} \, g$ (lbm/s) there is from Eq. A II(9)

$$\pi R_2^2 \, k_{B1} = \frac{\dot{w}}{P_0} \sqrt{\frac{R_G \, T_0}{g}} \, (11.7944) \tag{2}$$

Figure A(3a) shows that the so-called slip factor μ depends of the number of rotor blades Z_R, the ratio R_{1o}/R_2, the rotor efficiency η_R, and the flow coefficient φ_2. Minor corrections for μ must be applied if

the tip clearance ratio δ/b_2 differs from 0.05 (see Fig. A(3b)) and if the flow in the rotor is turned by less than 90° in the meridian plane (see Fig. A(3c)). However, no data for μ are available if this turning is 180° as in the present wheel, and for this reason the slip factor is taken as that of a standard centrifugal compressor wheel with $\varepsilon = 90^\circ$.

In accordance with Eq. A II(6) the flow coefficient φ_2 depends on μ. For a chosen value $\mu = 0.86$ there is

$$\varphi_2' = (0.86)(\cot 65^\circ) = 0.401$$

For an assumed rotor efficiency $\eta_R = 0.86$, $Z_R = 17$, and $R_{1o}/R_2 = 0.55$, by extrapolating Fig. A(3a) to higher values of φ_2, there is $\mu = 0.847$. Hence, $\varphi_2 = 0.395$, and the slip factor for this velocity ratio is about 0.85, giving a final value $\varphi_2 = 0.3964$. For $\mu = 0.85$, from Eq. A II(5),

$$\frac{W_2}{W_{1o}} = 0.6312 \tag{3}$$

Appendix A discusses the different possibilities to express the frictional losses in radial wheels. From Eq. A(25)

$$C = 0.7200$$

and from Eq. A(27) the so-called wheel efficiency η_W for $\eta_R = 0.86$ is

$$\eta_W = 0.4999$$

With this value and Eq. 3, the velocity ratio ψ of Eq. A (21) is

$$\psi = \frac{W_2}{W_{2is}} = 0.7548$$

With these data the rotor dimensions at the discharge are obtained from Eq. A II(11)

$$\pi R_2^2 \, \frac{b_2}{R_2} \, k_{B2} = \frac{\dot{w}}{P_0} \sqrt{\frac{R_G \, T_0}{g}} \, (1.2739) \tag{4}$$

Hence, with Eq. 2

$$\frac{b_2}{R_2} \frac{k_{B2}}{k_{B1}} = \frac{1.2739}{11.7944} = 0.1080$$

The restriction factor k_{B1} at the inlet eye due to boundary layer growth is assumed to be 0.98, and $k_{B2} \cong 0.954$,

Thus

$$\frac{b_2}{R_2} = 0.1109 \qquad\qquad (5)$$

In accordance with Fig. A(16) this ratio is acceptable.

The mean radius R_2 is chosen as 5.5 in., primarily to be able to drive the impeller by an available turbine and to mount the compressor to this item. Then the rotative speed N for $U_2 = 800$ ft/s is

$$N = \frac{800}{\frac{\pi}{30} \frac{R_2}{12}} = \frac{(800)(360)}{\pi(5.5)} = 16,666 \text{ rpm}$$

The basic compressor dimensions in inches are then:

$$D_2 = 2\,R_2 = 11.0$$

$$D_{1o} = 2\,R_{1o} = 6.05$$

$$D_{1i} = 2\,R_{1i} = 1.98$$

$$b_2 = 0.61$$

The radial overlaps δ of Fig. 1 at the impeller discharge are chosen to be 0.025 in., so that the blade height b_2' at the wheel discharge equals

$$b_2' = 0.56 \text{ in.}$$

Drawing 2222 of Appendix B shows the design of the Hybrid compressor. Details of the impeller and the inducer are given in Dwgs. 2203 and 2304. The meridional channel of the wheel was laid out by assuming a blade tip contour with the smallest possible curvature changes between R_{1o} and the discharge. Drawings 2203 and 2204 show that such a contour could be

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obtained with a two adjoining circular arcs with radii of 1.666 and 1.02 inches. By assuming that the meridional flow areas, without the restriction due to the blades, change linearly with the distance l along the tip contour from A_1 at the inlet to A_2' at the impeller discharge the meridional channel could be laid out with the method explained in Fig. 2. As shown in Dwgs. 2203 and 2204 the hub contour thus obtained could be approximated by four adjoining circular arcs whose radii decrease from the rotor inlet to the rotor discharge. The clearance between the blade tips and the adjoining casing of Dwg. 2213 is everywhere equal to 0.025 inch.

2. Inducer

Although some designers propose that the leading edges of the inducer blading have to be so arranged that particular incidence angles occur, it is shown in Ref. 2 that the correct incidence angles are obtained if the blockage because of the blade thickness is taken into account in the design. Figure 3 shows the conditions at the inducer entrance where V_1, W_1, β_1 are the flow properties just ahead of the inducer leading edges. In particular, the relative flow angle β_{1o} at the radius R_{1o} is equal to 55°. At an arbitrary radius R_1 the blade spacing is

$$S = \frac{2 \pi R_1}{Z_R} \tag{6}$$

Because of the blade thickness t or its projected thickness t_u in peripheral direction, the axial component V_1' of the flow after entering the inducer is

$$V_1' = V_1 \frac{s}{s - t_u} \tag{7}$$

giving a flow angle β_1' of

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$$\beta_1' = \tan^{-1}\left(\frac{\omega R_1}{V_1'}\right) = \beta_B \qquad (8)$$

If the blade has this angle β_1' at the leading edge there occurs an effective positive incidence angle

$$i = \beta_1 - \beta_1' = \beta_1 - \beta_B \qquad (9)$$

Although in actuality the projected blade width is then $t_u' = t/\cos \beta_1'$ it is sufficiently accurate to take $t_u = t/\cos \beta_1$ because of the small values of i, and because the blade leading edge will actually be profiled as shown by the dotted contours of Fig. 3. For the same reason the thickness t is taken as 0.10 in., although the blade thickness t farther downstream is actually 0.125 in.. With these assumptions the blade angle $\beta_B = \beta_1'$ at the leading edge can be determined from Eqs. 6 to 8, or

$$\tan \beta_B = \frac{\omega R_1}{V_1}\left(1 - \frac{t_u}{s}\right) = \frac{\omega R_1}{V_1}\left(1 - \frac{t \, Z_R}{\cos \beta_1 \, 2 \, \pi R_1}\right)$$

Assuming V_1 to be constant along R_1, and from the condition that at R_{1o}

$$\tan \beta_{1o} = \frac{\omega R_{1o}}{V_1} = \tan 55^{\circ}$$

there is with $R_{1o} = 3.025$ in.

$$\tan \beta_1 = \frac{R_1}{R_{1o}} \tan 55^{\circ} = \frac{R_1}{3.025} \tan 55^{\circ}$$

and

$$\tan \beta_B = \tan \beta_1\left[1 - \frac{(0.1)(17)}{\cos \beta_1 \, 2 \, \pi R_1}\right]$$

Table I gives the angles β_1, β_B and the incidence angles i along the radius R_1 at the inducer inlet.

To be able to machine the impeller with simple means, it is assumed that its blade sufaces consist of generatrices that are everywhere parallel

to the radius at the inducer discharge where the blades must adjoin the radial impeller blades. As shown in Fig. 4, the camber line of the inducer blades can then be specified by a single function $y = f(x)$. At a point P the blade surface has the angle γ, where $\tan \gamma = dy/dx$. This angle, however, is the angle in planes A-A which are perpendicular to the radius at station Q, where the inducer blades line up with the impeller blades. To obtain the actual blade angle β_B at a radius R_1 the blade surface must be intersected with a cylinder of radius R_1. For a point $P(x,y)$ of the blade surface the blade angle β_B at the radius R_1 is from Fig. 4

$$\tan \beta_B = \frac{dy}{\cos \theta \, dx} = \frac{\tan \gamma}{\cos \theta}$$

However

$$\cos \theta = \frac{\sqrt{R_1^2 - y^2}}{R_1}$$

Thus

$$\tan \beta_B = \frac{\tan \gamma}{\sqrt{1 - (y/R_1)^2}} = \frac{dy/dx}{\sqrt{1 - (y/R_1)^2}} \qquad (10)$$

A function $y = f(x)$ for the blade surface will now be established such that the blade angles β_B of Table I can be obtained along the radius R_1 by varying the axial length x of the inducer blades, as indicated in Fig. 3. In particular, the camber line of the inducer blades is chosen to be an ellipse. In accordance with Fig. 5

$$y = b - \frac{b}{a} \sqrt{a^2 - x^2} \qquad (11)$$

where 2a and 2b are the lengths of the major and minor axes of the ellipse, respectively. From Eq. 11

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$$\frac{dy}{dx} = \tan \gamma = \frac{b}{a} \frac{x}{\sqrt{a^2 - x^2}} \qquad (12)$$

Referring to Fig. 3, the values of "a" and "b" will be determined by specifying the conditions at stations C and D at the radii R_{lo} = 3.025 in. and R_{li} = 0.99 in. where, in accordance with Table I, the flow angles β_B must be 50.32°, and 18.08°, respectively. As shown in Fig. 3, it is assumed also that the axial lengths x of the inducer blades are 1.8 in. at C and 1.255 in. at D. These data are sufficient to determine the values of "a" and "b". However if Eqs. 11 and 12 are introduced into Eq. 10, one obtains fourth-order equations which cannot be solved with simple means. For this reason a method of successive approximations is used by assuming values for the angles γ_T and γ_H of Fig. 5 at R_{lo} and R_{li} and calculating the corresponding angles β_B by means of Eq. 10. Let, in accordance with Fig. 5,

$$x_T = 1.8 = \ell$$

$$x_H = 1.255 = \zeta \ell = (0.697) \ell$$

Then, from Eq. 12, with c = b/a,

$$\tan^2 \gamma_T = \frac{c^2}{(a/\ell)^2 - 1}$$

$$\tan^2 \gamma_H = \frac{\zeta^2 c^2}{(a/\ell)^2 - \zeta^2}$$

giving

$$\left(\frac{a}{\ell}\right)^2 = \frac{\zeta^2 (\tan^2 \gamma_T - \tan^2 \gamma_H)}{\zeta^2 \tan^2 \gamma_T - \tan^2 \gamma_H} \qquad (13)$$

$$c^2 = \left(\frac{b/\ell}{a/\ell}\right)^2 = \frac{(1 - \zeta^2) \tan^2 \gamma_T \tan^2 \gamma_H}{\zeta^2 \tan^2 \gamma_T - \tan^2 \gamma_H} \qquad (14)$$

Successive approximations of γ_T and γ_H established the following final values:

$$\gamma_T = 49.964^\circ; \ \tan \gamma_T = 1.1902$$

$$\gamma_H = 17.817^\circ; \ \tan \gamma_H = 0.3214$$

For these angles, from Eqs. 13 and 14,

$$\frac{a}{\ell} = 1.04442; \ a = 1.8799$$

$$\frac{b}{\ell} = 0.37460; \ b = 0.6743$$

and, by Eq. 11

$$\frac{y}{\ell} = 0.37460 - 0.35867 \sqrt{1.09081 - (x/\ell)^2} \tag{15}$$

For $x = \ell$ at $R_{1o} = 3.025$,

$$y = 0.47973$$

and for $x = (0.697)\ell$ at $R = 0.99$,

$$y = 0.1721$$

With these values, from Eq. 10, at $R_{1o} = 3.025$,

$$\tan \beta_{Bo} = \frac{1.1902}{\sqrt{1 - (0.47973/3.025)^2}} = 1.20545$$

and, at $R_{1i} = 0.99$,

$$\tan \beta_{Bi} = \frac{0.3214}{\sqrt{1 - (0.1721/0.99)^2}} = 0.32637$$

Table I shows that these angles coincide very closely with the required blade angles at these radii.

All blade angles β_B of Table I at the different radii R_1 can be obtained with the blade surface that is given by Eq. 15, for a particular change of the distance x of Figs. 3 and 5 with the radius R_1. This

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relationship between x and R_1 must be determined with an iterative method. For chosen values of x there can be determined y and dy/dx from Eqs. 15 and 12. These values introduced into Eq. 10, for the radius R_1 under consideration, give the value of β_B. If the blade angle thus determined differs from the required blade angle of Table I, the distance x must be varied until the correct angle is obtained. Drawing 2204 gives the values of z = 1.8 - x vs. R_1 that were obtained in this manner for the blade surface of Eq. 15 whose coordinates are listed also in Dwg. 2204.

With this design the inducer can be fabricated from a forging by first machining the tip controur of the blades and the surface of revolution of the leading edges that is given by z vs. R. Then the blade passages can be produced by an end-mill that is moved in x and y directions, and along the radius, to produce the hub contour, However, with the described design the axis of the end-mill need not be tilted to produce the correct inlet blade angles.

3. Diffusor

The diffusor is arranged in a cylindrical annulus downstream of the impeller discharge, having the mean radius R_2 = 5.5 in., and a radial height b_2 = 0.61 inches. Ahead of the diffusor at station (2) the flow properties are obtained with the relations of Table A I. From Eq. A I(7), and the data established earlier,

$$\frac{T_2}{T_0} = 1.08402$$

From Eq. A I (8)

$$\frac{T_2'}{T_0} = 1.07013$$

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From Eq. A I (6)

$$\frac{T_{t2}}{T_0} = 1.17411$$

From Eq. A I (20)

$$\frac{P_2}{P_0} = 1.2677$$

and from Eq. A I (19)

$$\frac{P_{t2}}{P_0} = 1.6764$$

The Mach number M_{V2} of the velocity V_2 ahead of the diffusor is from Eq. A II(6)

$$M_{V2} = 0.6446$$

for the chosen flow angle

$$\alpha_2 = 65°$$

A preliminary analysis showed that a minimum of two diffusor blade rows is necessary to produce an acceptable diffusor efficiency. These rows are designed in the same manner as bladings of axial-flow compressors by using the method of Ref. 3. In the following, station (3) is after the first diffusor blade row and station (4) is located after the second diffusor row, as shown in Fig. 1.

Neglecting the change of the through-flow velocity because of the density increase from station (2) to station (3) the diffusion factor D of the first diffusor blade row is

$$D = 1 - \frac{\cos \alpha_2}{\cos \alpha_3} + \frac{(\tan \alpha_2 - \tan \alpha_3)}{2 \sigma} \cos \alpha_2 \qquad (16)$$

where α_3 is the average flow angle at station (3) and σ the cascade solidity defined by

$$\sigma = \frac{\text{blade chord}}{\text{blade spacing}} = \frac{c}{s}$$

For different deflections $\Delta \alpha = \alpha_2 - \alpha_3$ and σ it is possible therefore to evaluate D from Eq. 16. The losses increase with increasing values of D. For the first diffusor blade row these losses can be expressed by the total pressure loss coefficient Y_t defined by

$$Y_t = \frac{\Delta P}{P_{t2} - P_2} = \frac{P_{t2} - P_{t3}}{P_{t2} - P_2} \tag{17}$$

where ΔP is the loss in total pressure in the blade row, and P_{t2}, P_2, the total and static pressure, respectively, ahead of the cascade. Reference 4 shows that Y of a stator blade row with a discharge angle α_3, diffusion factor D, and solidity σ can be calculated from

$$Y = \frac{2 \sigma}{\cos \alpha_3} \left[0.0004 + 0.0639(D + 0.1)^{2.91} + 0.057D^{2.02} (1 - \lambda)^{3.77} \right] \tag{18}$$

The factor λ is defined by

$$\lambda = \frac{R - R_H}{R_T - R_H} \tag{19}$$

where R is the radius at which Y is to be determined, and R_T, R_H are the tip and hub radii, respectively, of the blading. Since $1 - \lambda = 1$ at R_H, and $1 - \lambda = 0$ at R_T, the loss coefficient Y of Eq. 18 is higher at the hub than at the tip, if the other quantities in Eq. 18 do not vary radically along R. Equation 18 may give a realistic description of the loss variation in radial direction if the blade heights are large with respect to their chords, as for instance in axial compressors for jet engines. In such compressors the stator blades are attached at the tip and they usually have a clearance at the hub to prevent rubbing with the rotor assembly. The NASA calculating procedure of Refs. 3 or 4 does not separate the overall blade loss into profile losses, secondary or end losses, and tip clearance

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losses. End and tip clearance losses depend on the ratio of blade height and chord and on the ratio of blade gap to blade height, respectively, and it is evident from Eq. 18 that these quantities do not influence the overall loss coefficient of the NASA design procedure. In the cascades to be determined the blade gap is zero but the ratio of blade height and chord, or b_2/c, is quite small compared with the values in jet engine compressors, and the end losses will be very much larger than those in stator cascades of such machines. It is assumed therefore that Eq. 18 for the mid-span, or for $\lambda = 0.5$, establishes the profile loss coefficients Y_p only, or

$$Y_p = \frac{2 \sigma}{\cos \alpha_3} \left[0.004 + 0.0639(D + 0.1)^{2.91} + 0.0042 D^{2.02} \right] \tag{20}$$

To this profile loss coefficient will be added the so-called secondary loss coefficient Y_S to give the total loss coefficient Y_t, such that

$$Y_t = Y_p + Y_S = \frac{P_{t2} - P_{t3}}{P_{t2} - P_2} \tag{21}$$

Eq. 13(76) of Ref. 5, p. 380, gives the so-called induced drag coefficient C_{Di} of axial-flow cascades where the first part is the drag coefficient C_{DS} due to secondary flow effects, whereas the second part is due to tip clearance losses. This part is taken to be zero because no radial blade gaps δ exist in the present diffusor configuration. Hence

$$C_{DS} = 0.04 \ C_L^2 \ \sigma \ \frac{s}{h} \tag{22}$$

where the blade height h equals b_2. The lift coefficient C_L is equal to (see Eq. 13(14), Ref. 5, p. 337)

$$C_L = \frac{2}{\sigma} (\tan \alpha_2 - \tan \alpha_3) \cos \alpha_\infty \tag{23}$$

The angle α_∞ is obtained from

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$$\tan \alpha_\infty = \frac{\tan \alpha_2 + \tan \alpha_3}{2} \tag{24}$$

Equation 13(11) of Ref. 5 relates the drag coefficient to the total pressure loss coefficient ζ which, in the present application, would be defined by

$$\zeta = \frac{\Delta P}{P_{t3} - P_3}$$

It must be noted that ζ relates the drop in total pressure to the discharge conditions of a cascade. Then, since

$$Y_s \equiv \frac{\Delta P}{P_{t2} - P_2}$$

there is with Eqs. 22, 23, and 24

$$Y_s' = 0.16 \frac{s}{h} \cos^2 \alpha_2 \left[\tan \alpha_2 - \tan \alpha_3 \right]^2 \sqrt{1 + \tfrac{1}{4}[\tan \alpha_2 + \tan \alpha_3]^2} \tag{25}$$

since $1/\cos \alpha_\infty = \sqrt{1 + \tan^2 \alpha_\infty}$ The secondary loss coefficient of Eq. 25 is denoted by Y_s' to distinguish it from a secondary loss coefficient Y_s'' that has been proposed in Ref. 6. In Ref. 6 it is stated that the ratio $Y_s''/(Y_p + Y_s'') = Y_s''/Y_t''$ is a unique function of $\Delta\alpha(c/h)$, where $\Delta\alpha$ is the flow deflection in radians, and c/h the ratio of blade chord and blade height. This relationship is shown in Fig. 6. For known values of Y_p and Y_s''/Y_t'' there are

$$Y_s'' = Y_p \frac{(Y_s''/Y_t'')}{1 - (Y_s''/Y_t'')} \tag{26}$$

and

$$Y_t'' = \frac{Y_p}{1 - (Y_s''/Y_t'')} \tag{27}$$

The losses in the diffusor blade rows will be determined with Eq. 25 as well as with Eq. 26 for purposes of comparison. These two methods are

based on different models and concepts. It can be noted that for given flow angles the secondary losses of Eq. 25 are primarily a function of the ratio of blade spacing and blade height, whereas with the method of Ref. 6, or Eq. 26, they are depending mainly on the ratio of blade chord and blade height. Evidently, if Eq. 25 is used, one obtains different cascade arrangements for a specified total loss than if Eq. 26 is applied, and this situation is indicative of the present state of ignorance about secondary flows in general. A survey of the available analytical methods for the determination of secondary flow effects is given in Ref. 7.

As shown in Dwgs. 2202 and 2210-1, the diffusor blades will have a circular platform with a threaded cylindrical extension to attach them to the blade holders, which are shown as item 1 in Dwg. 2209. This design has been adopted to be able to change the blade stagger angle in the diffusor cascades if, because of the irregular flow conditions at the impeller discharge, the average flow angle α_2 differs from the design value of $65°$. This diffusor blade attachment requires however, that each blade row does not have more than 38 blades. For $Z = 38$, the blade spacing s at the mean radius $R_2 = 5.5$ in. becomes

$$s = \frac{2 \pi R_2}{Z} = 0.9094 \text{ in.}$$

and

$$\frac{s}{h} = \frac{s}{b_2} = \frac{0.9094}{0.61} = 1.4908 \tag{28}$$

For particular values of $\sigma = c/s$,

$$\frac{c}{h} = \sigma \frac{s}{h} = \sigma(1.4908) \tag{29}$$

For $\Delta \alpha$ in degrees, the variable $\Delta \alpha(c/h)$ of Fig. 6 is,

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$$\Delta \alpha (c/h) = \Delta \alpha^{\circ} \frac{\pi}{180} \sigma (1.4908) = \frac{2.602}{100} \sigma \Delta \alpha^{\circ} \qquad (30)$$

Table II shows the diffusion factor D, the profile losses Y_p, and the overall loss coefficients Y_t' and Y_t'' as functions of solidity for flow deflections $\Delta \alpha = 10$, 12 and 14° in the first blade row of the diffusor. The quantities Y_t' and Y_t'' are also plotted in Fig. 7.

Although it is desirable to have the highest possible flow deflection $\Delta \alpha$ in the first diffusor blade row, the general level of the losses as evidenced by Fig. 7, and the non-uniform and non-steady flow conditions at the impeller exit, make it advisable to limit $\Delta \alpha$ to 12°. For this deflection the data of Fig. 7 show that the solidity should be about unity to obtain loss coefficients Y_t that are smaller than about 0.12. Experience with diffusors of centrifugal compressors seems to indicate however that, in spite of the results of Fig. 7, more favorable conditions may be obtained for higher solidities, primarily because of the afore-mentioned irregular flow properties at the rotor discharge. At higher solidities the diffusor blades form channels with better guidance of the flow than if the solidity were low. These channels will act as flow straighteners which can equalize the flow irregularities with smaller flow separations than those which might occur in low-solidity cascades where the diffusion factors and the blade loadings are higher. It is likely then that the performance of the second diffusor blade row, and possibly that of the whole diffusor, is better than if the solidity of the first row is small. In general, the writer is of the opinion that the secondary losses do not increase as radically with the flow deflection $\Delta \alpha$ and the solidity σ as obtained by Ref. 6.

For these reasons it was decided to build two sets of diffusors. In one, denoted by A, the solidity of the first row was chosen as 1.6. In

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another, which is denoted by B, the first row has a solidity of 0.95. The deflections $\Delta \alpha$ have been chosen as 12° for both first rows of A and B. However, since the effects due to the non-steady impeller exit flows cannot be evaluated, the performance of these cascades will be determined with the loss coefficients of Fig. 7. The design criteria of the two first diffusor blade rows are listed in Table III, which also gives the values of the chosen maximum blade thickness.

The flow angle α_3 ahead of the second diffusor blade row is then $65 - 12 = 53^\circ$. Theoretically, the highest pressure recovery would be obtained in the diffusor if this angle could be reduced to zero in the second row. It can be seen, however, that the blade loadings and the losses would become excessive for such deflections. Preliminary investigations showed that the deflections $\Delta \alpha = \alpha_3 - \alpha_4$ cannot exceed about 26° to 38° at reasonable loss coefficients, so that after the diffusor the flow angles α_4 will be between 27° and 15°. Even though the kinetic energy of these whirl components of the discharge flow at station (4) cannot be converted into pressure rise, the overall efficiency of the compressor will be better than the one obtainable if it were tried to reduce the flow angle α_4 to zero.

Because it is intended to orient the blades of the second row in such a manner that they form a so-called tandem foil arrangement with the blades of the first row, the second diffusor row must also have 38 blades. Thus, its geometrical properties are likewise given by Eqs. 28, 29, and 30. The profile losses Y_p of the second row of diffusor blades can be determined by Eq. 20 if α_3 is replaced by α_4. The diffusion factors of these rows are obtained by Eq. 16, replacing α_2 by α_3 and α_3 by α_4. The overall loss coefficient Y_t is, similarly to Eq. 17,

$$Y_t = \frac{P_{t3} - P_{t4}}{P_{t3} - P_3} \qquad (31)$$

The secondary flow loss coefficients Y_s will be determined by Eq. 26, replacing α_2 by α_3, and α_3 by $\alpha_4 = \alpha_3 - \Delta\alpha$, and also with the method proposed in Ref. 6 by using the curve of Fig. 6. The results for different solidities and deflections $\Delta\alpha$ are listed in Table IV and plotted in Fig. 8.

Figure 8 shows that the overall losses increase very radically with solidity if the secondary flow losses are calculated in accordance with Ref. 6. If Eq. 25 is used however to determine Y_s, the overall losses Y_t' are almost constant for different values of σ, in fact they have a minimum for solidities of about unity. The data of Fig. 8 for Y_t''; that is, using Y_s'' of Ref. 6, suggest that with solidities much smaller than unity a diffusor with very low losses could be designed. However, not only would the blade chords be excessively small in such cascades, but the writer also believes that because of the high blade loading the flow would be too severely separated to make possible the small losses that Ref. 6 predicts. If in contrast to this opinion, the method of Ref. 6 should prove to give the correct values of Y_s'', a cascade with solidity of 1.6, which was chosen for blade row A1, would have excessive losses. It was decided, therefore, to design two second row diffusor cascades also. Both rows will have a deflection $\Delta\alpha = \alpha_3 - \alpha_4 = 32^\circ$ to keep the losses within acceptable limits, independent of whether the one or the other prediction method gives the correct loss coefficients. The so-called row A2 will be designed for $\sigma = 1.4$, and for row B2 the solidity is chosen as unity. If Eq. 25 predicts the secondary losses properly, both cascades should have about equal losses. On the other hand, if Ref. 6 gives realistic secondary losses, row A2 would be greatly inferior to row B2. Although it will be

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possible to arrange row A2 or B2 after either of the two first rows A1 or B1, for calculating purposes the so-called diffusor A is supposed to consist of rows A1 and A2 and diffusor B of rows B1 and B2. The design parameters of the second diffusor blade rows are listed in Table V.

The blade profiles and their orientation in the cascade are determined with the method of Ref. 3. The necessary calculating steps are described in paragraph 8 of Ref. 8. The basic thickness distribution of the profiles is shown in Fig. 13 of Ref. 8. Except for slight modifications near the leading edge this distribution corresponds to that of a British C-4 profile. The camber line of the profiles is a circular arc with camber angle ω. For known values of φ and thickness ratios t/c the profile coordinates are obtained with the relations of Fig. 14 of Ref. 8.

Figure 9 shows the attitude of a blade in a diffusor cascade and explains the symbols that are used for the profile calculations in Table VI. By using the method of Ref. 3 one often obtains excessively large incidence angles. As seen from Table VI this situation occurs for row A1 where $i = + 4.312^{\circ}$, for row B1 where $i = - 2.95$, and for row B2 where $i = - 7.002^{\circ}$. For these rows, incidence angles i^* of $+2^{\circ}$, -1°, and -2°, respectively, are chosen, and the corresponding camber angles φ^* and the stagger angles γ^* are calculated with the values of $d\delta/di$ of Fig. 177 of Ref. 3. Table VI also lists the drawings of Appendix B where the different blade profiles and their coordinates are shown. From these drawings the angles $\Delta\gamma$ of Fig. 9 were determined graphically and were used to establish the stagger angles γ' that are necessary for the installation of the blades in the blade holders of Dwg. 2209.

II. DESIGN POINT PERFORMANCE

1. Rotor

For a chosen total temperature $T_0 = 520^{\circ}R$ at the compressor inlet, and for $U_2/a_0 = 0.7156$, $M_{W1} = 0.4842$ (see Eq. 1), the static temperature T_1, and the static pressure p_1 at the inlet eye of the impeller are obtained from Eqs. A I (5) and A I (18), or

$$\frac{T_1}{T_0} = 0.9848$$

$$\frac{p_1}{P_0} = 0.9478$$

The absolute value of the total pressure P_0 at the impeller inlet is as yet unknown because in the test rig the compressor operates as an exhauster. Drawing 2223 shows that the air entering the compressor is expanded in a throttle valve to a pressure below atmospheric pressure. From a plenum chamber (Dwg. 2164-1), where the kinetic energy of the flow through the throttle valve openings is destroyed by a system of adjustable screens, the air enters the suction pipe through a profiled orifice. This suction pipe with an inner diameter of 18 inches has a length of about 18 feet, so that non-uniformities of the flow which have not been removed in the plenum chamber will be equalized ahead of the flow measuring nozzle of Dwg. 2216. This nozzle has a diameter of 5.38 inches, hence its flow area is only about 9 percent of the cross sectional area of the suction pipe. The large acceleration of the flow in the nozzle will produce a uniform flow at its discharge. Drawing 2222 shows the location of the flow nozzle with respect to the compressor inlet. Drawing 2202 shows that provisions have been made in the nozzle casing (Dwg. 2140) to carry out flow surveys ahead of the 7 in. diameter duct ahead of the impeller by

means of Pitot probes.

Drawing 2222 shows that a honeycomb flow straightener is arranged after the diffusor blade rows to remove the whirl components of the flow at this station, and that the air is then discharged into the atmosphere. This arrangement has been adopted for simplicity of the design, since it does not require a scroll or a complicated collector after the compressor from where the flow is discharged into the atmosphere through a throttling valve. Moreover, with this arrangement the driving power of the compressor is lower than with a test set-up where the inlet flow of the compressor is at atmospheric pressure. However, the total inlet pressure P_0, which is equal to the total pressure in the 7 in. diameter inlet duct, depends on the pressure ratio that is produced by the compressor. If, as shown in Fig. 1, the conditions at the exit of the discharge duct, arranged after the annular flow straightener, are denoted by the subscript (6), the static pressure p_6 must be equal to the ambient atmospheric pressure P_{atm}, or

$$P_0 = P_{atm} \frac{1}{(p_6/P_0)} \tag{32}$$

Hence it is necessary to determine the pressure ratio p_6/P_0 to obtain P_0. Evidently, p_6/P_0 depends on the pressure drops in rotor, diffusor and flow straightener which will be evaluated in Section II.3.

The weight flow rate $\dot{w}$ through the compressor can be determined from Eq. 2. For the assumed blockage factor $k_{Bl} = 0.98$, and since $R_2 = 5.5$ inches,

$$\frac{\dot{w}}{P_0} \sqrt{\frac{R_G T_0}{g}} = \frac{\pi R_2^2 k_{Bl}}{11.7944} = 7.8963 \ (in.^2) \tag{33}$$

With $R_G = 53.35$ (ft-lb)/(lbm, $^\circ$R), $g = 32.174$ ft/s^2, $T_0 = 520^\circ$ R,

$$\dot{w} = 0.2689 \quad P_0 \quad (\text{lbm/s}) \tag{34}$$

In Eqs. 33 and 34, P_0 is the absolute total inlet pressure in psia.

In the rotor the total temperature of the fluid is increased from T_0 to T_{t2}. For an adiabatic process the energy increase due to this temperature rise is equal to the energy per unit flow rate that the rotor must transmit to the fluid. Hence, the power HP required to drive the rotor is, exclusive of bearing and other mechanical losses,

$$HP = \dot{w} \, c_p \, (T_{t2} - T_0) \frac{1}{550} \quad (HP) \tag{34a}$$

With

$$c_p = R_G \frac{\gamma}{\gamma - 1} \quad (\text{ft-lb})/(\text{lbm}, \, ^\circ R)$$

and Eq. 33

$$HP = \frac{7.8963}{550} \, \frac{\gamma}{\gamma - 1} \, P_0 \sqrt{g \, R_G \, T_0} \, (\frac{T_{t2}}{T_0} - 1)$$

For $\gamma = 1.4$, and since $T_{t2}/T_0 = 1.17411$,

$$\frac{HP}{P_0 \sqrt{g \, R_G \, T_0}} = \frac{8.7489}{(10^3)} \tag{35}$$

For $T_0 = 520^\circ$ R, $\gamma = 1.4$, $R_G = 53.35$, there is also,

$$HP = 8.2656 \, P_0 \quad (HP) \tag{36}$$

In Eqs. 35 and 36 the pressure P_0 must be in psia.

The following data at the rotor discharge were obtained earlier:

$$\frac{T_2}{T_0} = 1.08402$$

$$\frac{P_2}{P_0} = 1.2677$$

$$\frac{P_{t2}}{P_0} = 1.6764$$

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$$M_{V2} = \frac{V_2}{a_2} = 0.6446$$

With $T_0 = 520^\circ R$, or $a_0 = 1117.85$ ft/s, the velocity of sound a_2 at the rotor discharge is

$$a_2 = a_0 \sqrt{T_2/T_0} = 1163.86 \qquad \text{ft/s}$$

and

$$V_2 = 750.23 \qquad \text{ft/s}$$

This average velocity at the rotor exit has an average flow angle $\alpha_2 = 65^\circ$.

2. Diffusor

The total pressure P_{t3} after the first diffusor blade row is obtained from Eq. 21, or

$$\frac{P_{t3}}{P_0} = (1 - Y_t) \frac{P_{t2}}{P_0} + Y_t \frac{P_2}{P_0} \qquad (37)$$

where the pressure loss coefficients Y_t of the rows A1 and B1 are listed in Table III. At station (3), after the first diffusor row, the velocity V_3 has an average flow angle $\alpha_3 = 53^\circ$. Although the annulur flow areas are equal at the station (2) and (3), the boundary layer growth in the blade row will make the effective flow area smaller at (3) than at (2). At station (2) a restriction factor $k_{B2} = 0.954$ has been assumed earlier to establish the diffusor annulus, or

$$A_2 = k_{B2} A_{geom}$$

where A_{geom} is the cross-sectional area of the annulus. At station (3) it is assumed that the effective flow area A_3 is

$$A_3 = k_{B3} A_{geom}$$

and $k_{B3} = 0.92$ by assumption.

The flow conditions at station (3) must be determined analytically for the flow area A_3, the flow angle α_3, and the total pressure P_{t3}, by using the energy equation, the equation of motion, and the equation of continuity. The energy equation for an assumed adiabatic process of a steady flow gives

$$T_{t3} = T_{t2}$$

In fact, the same total temperature will occur at stations (4), (5) and (6), if the flow processes are adiabatic.

Since the conditions after the second diffusor row at station (4) must be established with the same approach as those at station (3), a calculating procedure will be developed with the symbols of Fig. 10. Figure 10a shows a diffusor cascade in an annulus. The effective flow areas are $A_e = k_{Be} A_{geom}$ and $A_d = k_{Bd} A_{geom}$ at entrance and discharge, respectively. The average axial components V_{ea} and V_{da} that are uniform over A_e and A_d, respectively are

$$V_{ea} = V_e \cos \alpha_e$$

$$V_{da} = V_d \cos \alpha_d$$

A section through the blading of the diffusor row is shown in Fig. 10b, and Fig. 10c depicts the thermodynamic process between entrance and discharge in an entropy diagram. From the equation of motion

$$T_{te} = T_{td} = T_e + \frac{V_e^2}{2 g c_p} = T_d + \frac{V_d^2}{2 g c_p} \tag{38}$$

From the equation of continuity, with $\rho = p/(g R_G T)$

$$A_d V_d \cos \alpha_d \frac{p_d}{R_G T_d} = A_e V_e \cos \alpha_e \frac{p_e}{R_G T_e} \tag{39}$$

With $A_e/A_d = k_{Be}/k_{Bd}$, Eq. 39 can be rewritten as

$$\frac{V_d}{\sqrt{g \, \gamma \, R_G \, T_d}} = \frac{k_{Be}}{k_{Bd}} \frac{\cos \alpha_e}{\cos \alpha_d} \frac{(p_e/P_0)}{\sqrt{(T_e/T_0)}} \frac{V_e}{\sqrt{g \, \gamma \, R_G \, T_e}} \frac{\sqrt{(T_d/T_0)}}{(p_d/P_0)} \tag{40}$$

With the Mach numbers

$$M_d = \frac{V_d}{\sqrt{g \, \gamma \, R_G \, T_d}} \tag{41}$$

$$M_e = \frac{V_e}{\sqrt{g \, \gamma \, R_G \, T_e}} \tag{42}$$

and

$$K = \frac{k_{Be}}{k_{Bd}} \frac{\cos \alpha_e}{\cos \alpha_d} \frac{p_e/P_0}{\sqrt{(T_e/T_0)}} M_e \tag{43}$$

which is a constant for known entrance conditions and area ratios, there is from Eq. 40,

$$M_d = K \frac{\sqrt{(T_d/T_0)}}{(p_d/P_0)} \tag{44}$$

From Fig. 10c at the entropy s_d, from Eq. 38,

$$\frac{T_{td}}{T_d} = \frac{T_{te}}{T_d} = 1 + \frac{\gamma - 1}{2} M_d^2$$

and

$$\frac{P_{td}}{p_d} = \left(1 + \frac{\gamma - 1}{2} M_d^2\right)^{\gamma/(\gamma - 1)}$$

From these relations

$$\frac{T_d}{T_0} = \frac{T_{te}/T_0}{1 + \frac{\gamma - 1}{2} M_d^2} \tag{45}$$

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and

$$\frac{p_d}{P_0} = \frac{P_{td}/P_0}{(1 + \frac{\gamma - 1}{2} M_d^2)^{\gamma/(\gamma - 1)}} \tag{46}$$

where, similar to Eq. 37, with the pressure loss coefficient Y_t of the blade row,

$$\frac{P_{td}}{P_0} = (1 - Y_t) \frac{P_{te}}{P_0} + Y_t \frac{p_e}{P_0} \tag{47}$$

Because of their exponential expressions it is not possible to substitute Eqs. 45 and 46 into Eq. 44 to obtain a closed solution for M_d. It is necessary to choose values of M_d, say M_d^*, to calculate T_d/T_0 and p_d/P_0 from Eqs. 45 and 46. These quantities are then used in Eq. 44 to determine the Mach number M_d. If M_d differs from M_d^*, other values of M_d^* must be chosen until agreement is reached. With the final value of $M_d = M_d^*$ it is possible to calculate the ratios T_d/T_0 and p_d/P_0 with Eqs. 45 and 46, and the velocity V_d is obtained from Eq. 41, or

$$V_d = M_d \, a_0 \, \sqrt{(T_d/T_0)} \tag{48}$$

This iterative calculating process has been carried out for the rows Al and Bl, for both overall loss coefficients Y_t' and Y_t'' that are listed in Table III. In Table VII where the final data are presented, the columns designated by Al' and Al" give the performances of blade row Al for the overall loss coefficients Y_t' and Y_t'', respectively, of Table III. A similar designation is used for the performance of blade row Bl, for the losses Y_t' and Y_t''. With the flow conditions thus determined at (3), the flow properties at station (4), after the second diffusor blade row, can be calculated with the same method. These calculations are also carried out with both loss coefficients Y_t' and Y_t'' of Table V. The

quantity K of Eq. 43 is determined for $k_{Be} = k_{B3} = 0.92$ and $k_{Bd} = k_{B4} = 0.88$. The flow angles α_3 and α_4 are 53° and 21°, respectively, in accordance with Table VI.

The calculations of the flow conditions after the diffusor blade rows are quite lengthy and have to be carried out with great precision. On the other hand they do not warrant the use of a high-speed digital computer for which a rather elaborate program would have to be set up to perform the necessary iterations automatically. For the debugging of such a program several tries would probably be necessary until results could be obtained. However, for evaluations of the type discussed above, in fact for most calculations of this report, modern electronic and programmable display calculators are admirably suited. The Monroe Model 1655 with Card Reader CR-1 used at the Turbo-Propulsion Laboratory has proved to be an extremely valuable tool, and the writer believes that such calculators will completely revolutionize analytical engineering approaches. Libraries of programs for a variety of engineering calculations are already available, and programs for particular tasks can be established with great ease. Since most calculators, specifically the Monroe Model 1655, have provisions to verify and debug programs with a step by step procedure, program errors can be detected and corrected without delay by the programmer himself, without having to go to the trouble of submitting several modified programs as is necessary in most central computer facilities. At present, many high-speed computers are used for programs that do not really need the small access time and the large storage capacity of modern systems, and the use of programmable calculators will make available more time for those calculations that can be solved only by high-speed machines. Conversely the engineer or student is relieved of many routine calculations, without having to worry about inaccuracies and errors, and he obtains

results when needed during the progress of his work. Thus more time is available for creative efforts where the formulation of a problem is more important than the manipulation of numbers that is necessary for its solution.

To show the possibilities that exist in solving engineering problems with the Monroe 1655 calculator, some of the programs used for the calculations for this report are enclosed in Appendix D. Each program consists of a description, an operating instruction, and a listing of the program steps with their codes. The serial numbers of these programs refer to the private program library of the writer. The data of Table VII for the conditions after the two diffusor blade rows have been obtained with Program No. 109.

Appendix D also contains a more elaborate calculating program that requires the use of the Monroe calculator Model 1880 which is an advanced and more expensive machine with larger memory capacity.

The pressure ratios P_{t4}/P_0 of Table VII will be used to determine the so-called total-to-total compressor efficiency η_{t4}. For an isentropic compression from the total inlet pressure P_0 and the total inlet temperature T_0 to the total discharge pressure P_{t4}, the rise in total temperature ΔT_{tis} equals

$$\Delta T_{tis} = T_0 \left[(P_{t4}/P_0)^{(\gamma - 1)/\gamma} - 1 \right]$$

Since this temperature rise is proportional to the theoretical energy input per unit mass flow rate, and because for the actual process the energy per unit mass flow rate necessary to drive the rotor is proportional to $T_{t4} - T_0$, which equals $T_{t2} - T_0$, the compressor efficiency η_{t4} is

$$\eta_{t4} = \frac{(P_{t4}/P_0)^{(\gamma - 1)/\gamma} - 1}{(T_{t2}/T_0) - 1} \tag{49}$$

The compressor efficiencies η_{t4} are given also in Table VII. If the secondary flow losses are calculated in accordance with Eq. 25, an efficiency of 81.5% is obtained for the compressor with diffusor A, whereas if the losses for this configuration are determined with the method of Ref. 6 the efficiency is 78.9% only. The calculated compressor efficiencies with diffusor B are 82.3% and 82.8%, respectively, with the two methods.

It would appear, therefore, that higher efficiencies can be reached with diffusor B than with diffusor A. However, for the reason mentioned earlier, it may be that more favorable conditions can be obtained with the high-solidity diffusor A. Moreover, the performance calculations cannot take account of the radial velocity gradients or the non-steady flow at the rotor discharge, and it is because of these uncertainties that tests must be carried out to verify which diffusor configuration gives the best performance.

3. Flow Straightener and Discharge Duct

The flow conditions in the flow straightener and the discharge duct of Fig. 11a can be determined with approximate methods since the Mach numbers of the flow are small. At station (4), at the diffusor discharge, the velocity V_4 has the angle $\alpha_4 = 21^\circ$ with the axial direction. The peripheral component $V_4 \sin \alpha_4$ will be destroyed as the flow enters the axial flow straightener. This element consists of a honeycomb with hexagonal channels that have a spacing of 0.125 inch, a wall thickness of about 0.002 to 0.003 inch, and an axial length of 1.38 inch. As shown in Dwg. 2212, twelve honeycomb segments are arranged in an annulus between spacers that are 0.25 inches thick. On assuming that the flow leaving the diffusor does not diverge in radial direction, the velocity V_S in the channels of the flow straightener is with the symbols of Fig. 11a, neglecting density

changes,

$$V_4 \; 2 \; \pi \, R_2 \, b_2 = V_S \left[2 \; \pi \, R_2 \, b_2 - (12)(0.25) \, b_2 \right] \left(\frac{0.123}{0.125} \right)$$

where the fraction 0.123/0.125 is the blockage due to the wall thickness
of the honeycomb straightener. With $V_{4a} = V_4 \cos 21^\circ = 0.933 \; V_4$, $R_2 = 5.5$,

$$V_S = V_4 \cos 21^\circ \; \frac{(0.125/0.123)}{1 - \dfrac{(12)(0.25)}{2 \; \pi \; (5.5)}} = 1.039 \; V_4 \qquad\qquad (50)$$

As shown in Fig. 11a, it is supposed that after the honeycomb the flow
will diverge radially to a height $b_5 = 0.65$ in. at station (5). Hence
the velocity V_5 is assumed to be

$$V_5 = \frac{b_2}{b_5} \; V_{4a} = \frac{0.61}{0.65} \; (0.933) \; V_4 = 0.8764 \; V_4 \qquad\qquad (51)$$

Because the discharge duct between stations (5) and (6) is not a properly
designed diffusor it will be assumed that the flow will follow the dash-
dotted boundaries of Fig. 11a. Neglecting the change in density from (5)
to (6), the velocity V_6 is then

$$V_6 = V_5 \; \frac{2 \; \pi \; (5.5)(0.65)}{2 \; \pi \; (6.2)(0.70)} = 0.824 \; V_5 = 0.722 \; V_4$$

Figure 11b shows the flow process between stations (4) and (6) in an
entropy diagram. If the flow is adiabatic the total temperature T_t is
everywhere constant, equal to $T_{t4} = T_{t2}$. From the diffusor discharge at
(4) to the entrance of the honeycomb the velocity V_4 is reduced to V_{4a} at
the constant static pressure p_4. This process is associated with an in-
crease in entropy from s_4 to s_4', reducing the total pressure from P_{t4} to
P_{t4}'. The velocity is then increased from V_{4a} to V_S at station (4')
just inside the entrance to the flow straightener. If this acceleration
is isentropic the pressure p_4 is reduced to p_4'. With the symbols of
Fig. 11b,

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$$T_4^* = T_4 + \frac{V_4^2 - V_{4a}^2}{2 g c_p}$$

Since $C_p = R_G \gamma/(\gamma - 1)$, and $V_{4a} = V_4 \cos \alpha_4$,

$$\frac{T_4^*}{T_0} = \frac{T_4}{T_0} + \frac{\gamma - 1}{2} \left(\frac{V_4 \sin \alpha_4}{a_0}\right)^2 \qquad (53)$$

where $a_0 = 1117.85$ ft/s and $\alpha_4 = 21°$. Further,

$$\frac{P_{t4}'}{P_0} = \frac{P_4}{P_0} \left(\frac{T_{t2}/T_0}{T_4^*/T_0}\right)^{\gamma/(\gamma - 1)} \qquad (54)$$

The velocity increase from V_{4a} to V_S at the entropy s_4' reduces the static temperature from T_4^* to T_4', where

$$T_4' = T_{t2} - \frac{V_S^2}{2 g c_p}$$

or, with Eq. 50,

$$\frac{T_4'}{T_0} = \frac{T_{t2}}{T_0} - \frac{\gamma - 1}{2} \left(\frac{1.039 V_4}{a_0}\right)^2 \qquad (55)$$

Also

$$\frac{P_4'}{P_{t4}'} = \left(\frac{T_4'}{T_{t2}}\right)^{\gamma/(\gamma - 1)}$$

and

$$\frac{P_4'}{P_0} = \frac{P_{t4}'}{P_0} \left(\frac{T_4'/T_0}{T_{t2}/T_0}\right)^{\gamma/(\gamma - 1)} \qquad (56)$$

The loss in total pressure $\Delta P_S = P_{t4}' - P_{t4}''$ in the honeycomb will be determined with the frictional coefficient f of flows in pipes, or

$$\Delta P_S = \left(\frac{L}{d_h}\right) f \frac{\rho}{2} V_S^2 \tag{57}$$

The hydraulic diameter d_h of the flow channels in the honeycomb straightener is 0.123 in., and L = 1.38 in. The factor f depends on the Reynolds number

$$R_e = \frac{V_S d_h}{\nu}$$

Table VII shows that the velocities V_4 do not differ greatly, hence R_e can be determined for an average value V_4 = 330 ft/s. Moreover the average ratio T_4/T_0 is about 1.157, and the pressure p_4 is nearly equal to the atmospheric pressure. For $T_4 = (1.157)(520) = 602°$ R, and $p_4 = 14.7$ psia, there is $\nu = 1.97(10^{-4})$ ft/s^2. Hence, with Eq. 50,

$$R_e = \frac{(1.039)(330)(0.123/12)}{1.97(10^{-4})} = 1.78(10^4)$$

From Ref. 9 for smooth surfaces, f = 0.0265, and by Eq. 57

$$\Delta P_S = \frac{(1.38)}{(0.123)} (0.0265) \frac{\rho}{2} V_S^2 = 0.3 \frac{\rho}{2} V_S^2$$

At the low Mach numbers of the flow, there is approximately

$$\frac{\rho}{2} V_S^2 = P_{t4}' - P_4'$$

or

$$\frac{P_{t4}'}{P_0} = 0.7 \frac{P_{t4}'}{P_0} + 0.3 \frac{P_4'}{P_0} \tag{58}$$

From Fig. 11b, and Eq. 56 the static pressure p_4'' is then obtained from

$$\frac{P_4''}{P_0} = \left(\frac{P_{t4}''/P_0}{P_{t4}'/P_0}\right)\left(\frac{P_4'}{P_0}\right) \tag{59}$$

The reduction of the velocity from V_S to V_5 is supposed to occur at the static pressure p_4'', hence $p_5 = p_4''$, as indicated in Fig. 11b. The static temperature T_5 is with Eq. 51,

$$\frac{T_5}{T_0} = \frac{T_{t2}}{T_0} - \frac{\gamma - 1}{2}\left(\frac{0.8764\ V_4}{a_0}\right)^2 \tag{60}$$

and the pressure ratio P_{t5}/P_0 is

$$\frac{P_{t5}}{P_0} = \frac{p_4''}{P_0}\left(\frac{T_{t2}/T_0}{T_5/T_0}\right)^{\gamma/(\gamma - 1)} \tag{61}$$

The loss in the discharge duct between stations (5) and (6) is assumed to be

$$P_{t6} - P_{t5} = (0.4)(P_{t5} - p_5)$$

Thus, with $p_5 = p_4''$

$$\frac{P_{t6}}{P_0} = 0.6\ \frac{P_{t5}}{P_0} + 0.4\ \frac{p_4''}{P_0} \tag{62}$$

With Eq. 52

$$\frac{T_6}{T_0} = \frac{T_{t2}}{T_0} - \frac{\gamma - 1}{2}\left(\frac{0.722\ V_4}{a_0}\right)^2 \tag{63}$$

and

$$\frac{p_6}{P_0} = \frac{P_{t6}}{P_0}\left(\frac{T_6/T_0}{T_{t2}/T_0}\right)^{\gamma/(\gamma - 1)} \tag{64}$$

For the data at the diffusor discharge (station (4)) of Table VII the conditions of state in the flow straightener and the discharge duct have been calculated with the above relations. The results are summarized in Table VIII. As discussed earlier, the static pressure p_6 at the exit of the duct will equal the atmospheric pressure. If this ambient pressure

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P_{atm} is taken as 14.7 psia, the total pressure P_O at the compressor inlet is obtained from Eq. 32. The last line of Table VIII gives these pressures for diffusors A and B and the two different losses which were taken into account for their performance prediction.

4. Compressor Performance at Design Point

The weight flow rate $\dot{w}$ and the driving power of the compressor can be determined from Eqs. 34 and 36 for the values of P_O from Table VIII. The pressures thus obtained are for a total inlet temperature $T_O = 520^O$ R and a speed of rotation N = 16,666 rpm. Of interest is also the torque M that is necessary to turn the compressor, which equals

$$M = \frac{HP(550)}{\omega} = \frac{HP(550)}{\pi\, N/30} \qquad \text{(ft-lb)} \tag{65}$$

With Eq. 34, and N = 16,666 rpm

$$M = 2.6045\, P_O \qquad \text{(ft-lb)}$$

or

$$M = 31.2554\, P_O \qquad \text{(in-lb)} \tag{65}$$

where P_O must be in psia. In Table IX the compressor performance data for the design point at N = 16,666 rpm and $T_O = 520^O$ R are summarized. Also given are the pressure ratios P_{t4}/P_O and p_6/P_O, and the efficiencies η_{t4} with the two diffusors A and B, for the two methods used for the determination of their secondary flow losses.

It is evident from Appendix A (Ref. 1), and the calculations of this report, that U_2/a_O, $\gamma = c_p/c_v$, and the flow angles are the prime variables that establish the performance of a particular compressor, in fact of all designs which are geometrically similar. Except for possible changes in the loss coefficients which will be discussed later, the pressure ratio P_{t4}/P_O of these machines will be equal if U_2/a_O, γ, and the flow angles

are equal. This situation occurs because the density ratios of the fluid
and the Mach numbers of the flow remain constant at particular stations
in the compressors, which makes it possible to maintain the same flow
angles with respect to the bladings. From Eq. A II(9) it is seen that
the dimensionless mass flow rate $(\dot{m})*$ defined by

$$(\dot{m})* = \frac{(\dot{w}/g) \sqrt{g \, R_g \, T_0}}{\pi \, R_2^2 \, P_0} \tag{66}$$

must be constant at these conditions. From Eq. 35 and Eq. A I(6) it is
apparent that the dimensionless power $(HP)*$, defined by

$$(HP)* = \frac{(HP)(550)}{\pi \, R_2^2 \, P_0 \sqrt{g \, R_G \, T_0}} \tag{67}$$

is invariant also for similar machines that operate at the same values
U_2/a_0 and γ, and produce the same pressure ratio P_{t4}/P_0.

Since $\omega = U_2/R_2$, the moment of Eq. 65 becomes with Eq. 67, and

$$a_0 = \sqrt{\nu \, g \, T_G \, T_0},$$

$$M = \pi R_2^3 \, P_0 \, \frac{(HP)*}{(U_2/a_0) \sqrt{\gamma}} \tag{68}$$

Hence, similar to Eqs. 66 and 67 the so-called dimensionless moment $(M)*$
will be defined as

$$(M)* = \frac{M}{\pi R_2^3 \, P_0} \tag{69}$$

which is constant also for the conditions at which $(\dot{m})*$ and $(HP)*$ do not
change.

Obviously the dimensionless quantities of Eqs. 66, 67, and 69 have
equal magnitudes in any consistent system of units for geometrically

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similar compressors that operate at the same values of U_2/a_0, γ, and P_{t4}/P_0, independent of their size and the magnitudes of P_0 and T_0. However, the losses in these machines do not depend only on the angles and the Mach numbers but also on the Reynolds numbers of the flow. That the Mach numbers remain constant at fixed values U_2/a_0, γ, and flow angles, independent of the magnitudes of T_0 and P_0, is shown by Eqs. A II(4) and A II(6). The flow angles, and therefore the blade incidence angles, remain equal at particular stations because the ratios T/T_0 and P/P_0, which establish the density ratios ρ/ρ_0, are also not affected by T_0 and P_0. The Reynolds number R_e at a particular station, where the velocity V exists at p and T, can be expressed by

$$R_e = \frac{V \, R_2}{\mu_v} \, \rho$$

since, for geometrically similar compressors, the dimensions of all flow channels are constant fractions of the mean compressor radius R_2. If M_V is the Mach number of V, or $V = M_V \sqrt{\gamma \, g \, R_G \, T}$, and, since $\rho = p/(g \, R_G \, T)$, there is also

$$R_e = \left[\frac{P_0 \, R_2}{\mu_v \sqrt{g \, R_G \, T_0}} \right] \left(\frac{(P/P_0) \, M_V \sqrt{\gamma}}{\sqrt{(T/T_0)}} \right) \tag{70}$$

Since the dynamic viscosity μ_v has the dimension $(lb\text{-}s)/ft^2$ in the system of units used in this report, the term in the square bracket is dimensionless. This is necessary because the term in the round bracket and R_e are dimensionless also.

Whereas, for reasons discussed earlier, the expression in the round bracket is constant for all geometrically similar compressors operating at particular values of U_2/a_0, P_{t4}/P_0 and γ, independent of P_0 and T_0, the term in the square bracket depends on the compressor size, the gas properties,

and the magnitudes of P_0 and T_0. Experience has shown, however, that the influence of Reynolds number on losses in turbomachines is quite small, and that large increases of the losses occur only below some critical value of R_e which is usually reached only at very low pressures or with small dimensions. For most gases the dynamic viscosities increase slightly with temperature but the absolute magnitudes of μ_v do not vary greatly for different gases. Most diatomic gases such as N_2, O_2, H_2, CO, and also air, have values of γ of about 1.4 at ambient temperature, and the ratio of the viscosities of the heaviest of these gases (O_2) and the lightest one (H_2) is only about 2. A change in Reynolds number by a factor of two has a very small influence on the losses, except near the above-mentioned critical value of R_e.

This discussion shows that geometrically similar compressors that operate with gases that have the same specific heat ratio will have almost equal values of $(\dot{m})*$, $(HP)*$, and $(M)*$ at particular values of U_2/a_0 and P_{t4}/P_0, if the Reynolds numbers are sufficiently high. Evidently the efficiencies of the compressors at these operating conditions will then also be nearly equal, irrespective of the molecular weight of the gas and the magnitudes of inlet pressure and inlet temperature. The quantities $(\dot{m})*$, $(HP)*$ and $(M)*$ are shown in Table IX for the ratio $U_2/a_0 = 0.7156$.

For a particular compressor operating with a particular gas, the dimensionless quantities of Eqs. 66, 67, and 69 can be simplified by introducing the ratios

$$\theta_C = \frac{T_0}{T_{REF}} \qquad (71)$$

and

$$\delta_C = \frac{P_0}{P_{REF}} \qquad (72)$$

where T_{REF} and P_{REF} are usually taken as 518.4° R and 14.7 psia. The subscript C was introduced to differentiate these ratios from similar ones that later on are used for the performance calculations of the drive turbine.

With Eq. 71, the ratio U_2/a_0 is also

$$\frac{U_2}{a_0} = \frac{(\pi/30) \ N \ R_2}{\sqrt{g \ \gamma \ R_G \ \theta_C \ T_{REF}}},$$

Hence in a compressor that handles a specific gas, equal values of U_2/a_0 are obtained for equal ratios $N/\sqrt{\theta_C}$. Thus,

$$N_{REF} = N/\sqrt{\theta_C} \qquad \text{(rpm)} \qquad\qquad (73)$$

will be called the referred speed of the compressor. Similarly, from Eq. 66, the so-called referred weight flow rate is defined by

$$\dot{w}_{REF} = \frac{\dot{w} \ \sqrt{\theta_C}}{\delta_C} \qquad \text{(lbm/s)} \qquad\qquad (74)$$

From Eq. 67 the referred power is

$$(HP)_{REF} = \frac{HP}{\delta_C \ \sqrt{\theta_C}} \qquad \text{(HP)} \qquad\qquad (75)$$

and from Eq. 69 the so-called referred torque becomes

$$M_{REF} = \frac{M}{\delta_C} \qquad \text{(ft-lb) or (in-lb)} \qquad (76)$$

On the basis of the previous discussion it can be stated that a compressor designed for and operated with a particular fluid will have the same pressure ratio at the same values of N_{REF} and $\dot{w}_{REF}$ independent of the absolute magnitudes of P_0 and T_0, provided that the possible variations of Reynolds number have a minor effect on the losses in the bladings of

the machine. Then the referred power required by the compressor will also be a unique function of $N/\sqrt{\theta_C}$ and $\dot{w}\sqrt{\theta_C}/\delta_C$, indicating that its efficiency is only depending on these two variables also. The main disadvantage of the so-called referred parameters is that they are not dimensionless, and that they cannot be used to compare the operating performance of different machines with each other, as it is possible with the earlier defined non-dimensional quantities.

The referred operating parameters of Eqs. 73 to 76 for the design point are given in Table IX.

III. OFF-DESIGN POINT PERFORMANCE

1. General

Because the Hybrid compressor operates as an exhauster in the test rig it is of interest to know its performance at pressure ratios and speed other than those for the design point. If the pressure ratio is smaller than the design value, the pressure P_0 will be higher and since the weight flow rate, and the driving power are proportional to P_0, it is likely that the maximum power occurs at pressure ratios lower than the values at the design point.

2. Rotor Performance

Prime variables for the rotor performance are the peripheral speed ratio U_2/a_0 and the absolute discharge angle α_2. If particular values of these quantities are chosen and if the slip factor μ and the velocity ratio ψ were known it would be possible to determine the dimensionless mass flow rate through the wheel by means of Eq. A II(11). These calculations can be carried out by means of program 102 of Appendix D, which also establishes the ratios T_2/T_0 and p_2/P_0 for the assumed values of μ and ψ. Actually, program 102 determines the quantities:

$$\frac{\dot{w} \sqrt{(R_G/g) T_0}}{P_0} = (\dot{m})^* \, \pi \, R_2^{\,2} \tag{77}$$

$$\Phi_2 = \frac{\dot{w} \sqrt{(R_G/g) T_0}}{A_2 \, k_{B2} \, P_0} = \frac{\dot{w} \sqrt{(R_G/g) T_0}}{2\pi \, R_2 \, b_2 \, k_{B2} \, P_0} \tag{78}$$

and

$$\Phi_1 = \frac{\dot{w} \sqrt{(R_G/g) T_0}}{A_1 \, k_{B1} \, P_0} = \frac{\dot{w} \sqrt{(R_G/g \, T_0}}{\pi \, (R_{10}^{\,2} - R_{1i}^{\,2}) \, k_{B1} \, P_0} \tag{79}$$

for chosen blockage factors k_{B1} and k_{B2}.

The dimensionless flow function Φ_1 of Eq. 79 can be used to establish the ratio of the static pressure p_1 and P_0, since P_0 is identical with the total pressure P_{t1} at station (1), with the relation

$$\Phi_1 = \sqrt{\frac{2\gamma}{\gamma - 1} \left[(p_1/P_0)^{2/\gamma} - (p_1/P_0)^{(\gamma + 1)/\gamma} \right]} \tag{80}$$

Since for known values of Φ_1 and γ, it is not possible to calculate p_1/P_0 in closed form, the calculating program 103 of Ref. D has been set up to determine p_1/P_0 with an iterative process.

Program 104 of Appendix D can then be used to determine the flow properties at the inducer inlet with the relations of Appendix A which are listed in the program description. This program gives T_1/T_0, V_1/a_0, W_{1o}/a_0, and the quantities M_{W1} and i'. The latter is the incidence angle at the outer inlet radius R_{1o} if blockage due to inducer blade thickness is taken into account.

Appendix C analyzes available test data of losses in centrifugal compressor rotors, and shows that Fig. 24 can be used for the present off-design calculations. From Fig. 24 the rotor efficiencies η_R are obtained as functions of i' and M_{W1}. The efficiency η_R is defined by Eq. A (12). With Eqs. A II(5), A (27), and A (21) it is possible to calculate the velocity ratio $\psi = W_2/W_{2is}$ which is used for the performance calculations with the method of Appendix A. This conversion can be carried out with program 105 of Appendix D. The wheel efficiency η_W of Eq. A (15) and the deceleration ratio W_2/W_{1o} are outputs of this program also. The value of ψ thus obtained should coincide with that initially assumed for use in program 102, and ψ must be iterated by successive approximations till agreement is reached.

For the design point the slip factor $\mu = \mu_d = 0.85$ has been determined from Fig. A (3a) for the given rotor dimensions, the assumed rotor

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efficiency $\eta_R = 0.86$, and the design flow coefficient $\varphi_2 = \varphi_{2d} = 0.3964$.
Experience shows that Fig. A (3a) cannot be used to establish μ at off-design conditions. Most theoretical analyses predict that the slip factor for rotors with radial blades at the discharge remains constant if the flow coefficient and η_R change. As shown in Ref. 13, and by other authors, this condition does not occur in actuality. For the present calculations the conclusion reached in Ref. 13 is applied, namely, that the relative flow angle β_2 of Fig. 1 at the rotor exit remains constant at all operating conditions. Then, by Fig. 1

$$\tan \beta_2 = \frac{U_2 (1 - \mu)}{V_{m2}} = \frac{1 - \mu}{\varphi_2}$$

For the design point with μ_d and φ_{2d}, and for $\beta_2 = \beta_{2d}$

$$\frac{1 - \mu}{\varphi_2} = \frac{1 - \mu_d}{\varphi_{2d}}$$

and, since

$$\varphi_2 = \mu \cot \alpha_2$$

there is

$$\mu = \frac{1}{1 + \dfrac{1 - \mu_d}{\varphi_{2d}} \cot \alpha_2} \tag{81}$$

Then, for $\mu_d = 0.85$ and $\varphi_{2d} = 0.3964$

$$\mu = \frac{1}{1 + (0.3784) \cot \alpha_2} \tag{82}$$

Sheets 1 and 2 of Table X give the final results of the rotor performance for speed ratios $U_2/a_0 = 0.7156$ and $U_2/a_0 = 0.516$, respectively, obtained with the procedure outlined above. As pointed out earlier, a value of $\psi = \psi_j$ has to be assumed (line 7 of Table X) and must be changed until it and the value ψ calculated by program 105 (line 22 of Table X) coincide.

Table X only gives the final value of ψ_j for each chosen angle α_2, the intermediate results of the iterations in ψ have not been listed. The curves of Fig. 25 are identical with those of Fig. 24 which were used to obtain the rotor efficiencies η_R as functions of M_{W1} and i' for the calculations in Table X. In Fig. 25 the rotor efficiencies η_R of Table X are plotted vs. M_{W1} and i' to show the location of the curves $U_1/a_0 =$ 0.7156 and $U_1/a_0 = 0.516$ in relation to the other curves $U_1/a_0 =$ constant which were actually disregarded in establishing η_R for the calculations of Table X. It can be noticed that the two curves $U_1/a_0 =$ constant, that could be drawn through the data points of Table X, are similar to the dashed curves of Figs. 24 and 25 but have somewhat different slopes.

A far more interesting representation of the data of Table X is given in Fig. 26 where the velocity coefficients ψ and the incidence angles i' are shown as function of the deceleration ratio W_2/W_{1o} of the relative velocities in the rotor. As expected, the velocity coefficients ψ decrease with decreasing ratios W_2/W_{1o}, and if W_2/W_{1o} approaches unity the values of ψ seem to reach an asymptotic value which is higher at the lower velocity ratio U_1/a_0 because of the lower Mach number of the flow. Figure 26 also shows that the incidence angles decrease almost linearly with W_2/W_{1o}. In the writer's opinion losses of centrifugal compressors rotors should be presented in the manner of Fig. 26. Data of this nature for different impellers would enable the engineer to arrive at optimum designs and make it possible to establish off-design performance maps with greater accuracy than with the rotor efficiencies η_R.

3. Diffusor Performance

To determine the compressor performance for the rotor data of Table X the conditions in the diffusor must be evaluated also. Experience shows that the pressure loss coefficient Y_t of a decelerating axial

cascade varies with incidence angle and inlet Mach number. Limited information is however available in the literature about these influences. Figure 27 has been established on the basis of Fig. 130 of Ref. 3, but these data are educated guesses at best, although they are representative of observed behavior. In particular, the solid curve will be used for $U_2/a_0 = 0.7156$ and the dashed curve for $U_2/a_0 = 0.516$, for the range of the Mach numbers indicated. Because of the approximate nature of these curves it is sufficient to treat the two diffusor rows together. At the design point the total pressure loss coefficient of rows A_1' and A_2' of diffusor A' is from Table VII

$$Y_t = (Y_t)_{io} \frac{P_{t2}/P_0 - P_{t4}/P_0}{P_{t2}/P_0 - P_2/P_0} = \frac{1.6764 - 1.5910}{1.6764 - 1.2677} = 0.2089$$

This loss coefficient is supposed to occur at the design incidence angle $i = i_0 = + 2°$ of the first diffusor blade row Al in accordance with Table VI. At other incidence angles

$$i = \alpha_2 - 63°$$

the pressure loss coefficients Y_t are taken as

$$Y_t = 0.2089 \left[Y_t/(Y_t)_{io} \right]$$

where the ratio in the square bracket is read from Fig. 27.

Reference 3 shows that the deviation angle δ is almost constant if the incidence angle of the flow of a particular cascade changes. Thus, the discharge flow angle of a cascade is nearly constant. This general phenomenon is evident also from Fig. 14 (7) of Ref. 5. Because of the approximate nature of the present investigation it is permissible, therefore, to assume that the flow angle after the second diffusor row A_2 is

constant, equal to $\alpha_4 = 21°$, irrespective of incidence angle and Mach number of diffusor row A_1 (see Table VI).

The calculating method of program 109 of Appendix D will be used to establish the conditions of state of the fluid after the diffusor for the data of Table X. It is assumed that the blockage factors at inlet and exit of the diffusor are those at the design point, or

$$k_{Be} = k_{B2} = 0.954$$

$$k_{Bd} = k_{B4} = 0.88$$

The quantity K of Eq. D 109(2) is then, with $A_4 = A_2$, $\alpha_4 = 21°$, and $M_2 = M_{V2}$

$$K = 1.161218 \cos \alpha_2 \frac{P_2/P_0}{\sqrt{T_2/T_0}} M_2$$

The Mach number M_4 and the velocity V_4 must be obtained with the iterative procedure outlined in program 109.

The processes in the flow straightener and discharge duct, illustrated in Figs. 11a and 11b, are determined with Eqs. 50 to 64. The objective of this procedure is to obtain the pressure ratio p_6/P_0. Since p_6 is equal to the ambient pressure, or 14.7 psia, these calculations establish the value of the total pressure P_0 ahead of the compressor rotor. It is assumed that the total temperature T_0 equals $520°R$.

4. Compressor Off-Design Performance

From line 8 of Table X there are known the ratios $\dot{w}\sqrt{(R_G/g)T_0}/P_0$. Hence the flow rate $\dot{w}$ in lbm/s is obtained from

$$\dot{w} = 0.034055 \frac{\dot{w}\sqrt{(R_G/g)\,T_0}}{P_0} P_0 \quad (\text{lbm/s}) \tag{83}$$

for $R_G = 53.35$ (lb-ft)/(lbm, $°R$), $g = 32.174$ ft/s^2, and $T_0 = 520°R$, if P_0 is introduced in psia. The drive power of the compressor is, from Eq. 34a,

$$HP = 176.54 \ \dot{w} \left[(T_{t2}/T_0) - 1 \right] \ (HP) \qquad (84)$$

where T_{t2}/T_0 is known from line 23 of Table X.

The total-to-total efficiency η_{t4} of Eq. 49 can be determined for the pressure ratio P_{t4}/P_0 that is obtained by the calculations. For $T_0 = 520\ ^\circ R$, and $R_2 = 5.5$ in., the speed N of the compressor is

$$N = 23290.21 \ (U_2/a_0) \ (rpm) \qquad (85)$$

These calculations have been performed with program 517 on a Monroe Model 1880-22 scientific programmable printing calculator. Program 517 contains the earlier mentioned program 109. With this advanced calculator the whole calculating procedure can be carried out without the need of introducing several programs as would have been necessary with Monroe Model 1556, which is limited to 256 program steps and seven active memory registers. Program 517 which is described in Appendix D requires 557 program steps and 40 data storage registers.

The results of the calculations for the data of Table X are listed in Table XI for the design velocity ratio $U_2/a_0 = 0.7156$ and in Table XII for $U_2/a_0 = 0.516$. The data of these tables are direct print-outs of the Model 1880 calculator.

The data at the design speed of 16,666 rpm and for $\alpha_2 = 65^\circ$ (Table XI) should coincide with the values of Table IX. It can be noted that the agreement is good, hence, it can be concluded that no arithmetic errors were made in the calculations.

Figure 28 is a graph of the data of Tables XI and XII. As expected, the driving power is higher at flow rates larger than that of the design point. It is necessary therefore to run the compressor with a turbine that is capable of producing at least 130 HP at 16,666 rpm, although only about 83 HP are required at the design point conditions. It can also be seen

from Fig. 28 that the calculated optimum compressor efficiencies at 12,018 and 16,666 rpm are nearly equal, namely, 81.35% at the lower and 81.49% at the higher speed. It seems possible, therefore, to obtain a good measure of the maximum compressor efficiency with tests at speeds lower than design, say, at about 13,000 to 14,000 rpm.

The data points in Fig. 28 at the lowest flow rates are for $\alpha_2 = 73^\circ$ at both speeds. As indicated in Fig. 25 these points lie on the curve labeled "surge limit." At $\alpha_2 = 73^\circ$ the diffusor incidence angle i is 10°. By Fig. 27 the ratio $Y_t/(Y_t)_0$ for $i = 10^\circ$ is 1.90 for $U_2/a_0 = 0.7156$ and 1.22 for $U_2/a_0 = 0.516$. A frequently applied rule assumes that an axial blade row stalls if the loss is twice that at the design incidence angle. If this condition were to hold for the tandem row of the present diffuser, it could be stated that compressor surge is due to rotor stall at both speed ratios. The surge limit indicated in Fig. 28 holds for this premise.

IV. DRIVE TURBINE

1. General

An available test stand for investigations of transonic axial compressor wheels is driven by a dual-flow air turbine with 50 percent reaction which is illustrated in Dwg. 2222 of Appendix B. The rotors of this turbine are shown in Dwg. 2108-1 and the guide vanes in Dwg. 2109. The blades of rotor and stator are identical with the profiles of Dwg. 2107, but to avoid wake interferences the stator row has 31 and the rotor 32 blades. The two parallel stages are designed for the following conditions

$$P_{t0}/p_2 = 2.8 \text{ for } p_2 = p_{AMB} = 14.7 \text{ psia}$$

$$T_{t0} = 640 \, ^\circ R$$

$$\dot{w} = 10.85 \text{ lbm/s}$$

$$HP = 485 \text{ HP}$$

$$N = 30,500 \text{ rpm}$$

where P_{t0} and T_{t0} are total inlet pressure and total inlet temperature, respectively, and p_2 the static discharge pressure.

To be determined are the pressure ratio, inlet temperatures, and weight flow rates for turbine powers of 130 HP at 16,666 rpm, and 60 HP at 12,018 rpm.

2. Off-Design Turbine Performance

These calculations were performed by Prof. E. Macchi during his stay as Visiting Professor at NPS. Use was made of the computer program of Ref. 14 which treats the three-dimensional flow in a turbine stage by taking account of streamline curvatures and slopes, as well as energy and entropy gradients. In Ref. 14 it is possible to select one of five loss correlation methods that are included in the program. For the present

investigation the method of Traupel (Ref. 15) has been applied, since it was found to give good performance predictions for 50 percent reaction turbines. The results of these calculations are presented in Fig. 29, showing referred flow rate $\dot{w}\sqrt{\theta_T}/\delta_T$, and referred power $HP/(\delta_T\sqrt{\theta_T})$ as function of the referred speed $N/\sqrt{\theta_T}$ for different turbine pressure ratios. There are:

$$\delta_T = P_{t0}/14.7$$

$$\theta_T = T_{t0}/518.4$$

If the ambient pressure is assumed to be 14.7 psia the turbine pressure ratio P_{t0}/p_2 equals δ_T.

For ease of operation it will be endeavored to run the turbine at the lowest possible inlet temperature T_{t0}. A lower limit is given by the condensation or icing of the water vapor in the operating air which has nearly 100 percent relative humidity. It will therefore be assumed that the static turbine discharge temperature T_2 shall not be less than 45° F or 505° R. The off-design calculations showed that the total-to-static turbine efficiency η_s does not exceed about 81% in the range of operating conditions for the Hybrid compressor. The temperature T_2 is obtained from

$$T_2 = T_{t0}\left\{1 - \eta_s\left[1 - (1/\delta_T)^{(\gamma-1)/\gamma}\right]\right\} \tag{86}$$

For $T_2 = 505^\circ$ R and $\eta_s = 0.81$ the temperature T_{t0} can therefore be determined for different values of δ_T and $\gamma = 1.4$. Thus, the ratios $\theta_T = T_{t0}/518.4$ are known as functions of δ_T. For a particular speed N, or ratio $N/\sqrt{\theta_T}$, the referred turbine parameters are then obtained from Fig. 29 for the three values of δ_T. The results are listed in the following table:

N (rpm)	16,666			12,018		
δ_T	1.4	1.8	2.2	1.4	1.8	2.2
T_{to} (°R) (Eq. 86)	545.5	577.3	603.6	545.5	557.3	603.6
$\theta_T = T_{to}/518.4$	1.05227	1.11360	1.16439	1.05227	1.11360	1.16439
$N/\sqrt{\theta_T}$	16,247	15,793	15,445	11,716	11,388	11,137
$\dfrac{\dot{w}\sqrt{\theta_T}}{\delta_T}$ (Fig. 29)	3.65	4.18	4.30	3.72	4.27	4.36
$\dfrac{HP}{\delta_T\sqrt{\theta_T}}$ (Fig. 29)	48.5	89.1	111.8	46.8	81.0	97.2
$\dot{w}$ (lbm/s)	4.98	7.13	8.77	5.08	7.28	8.89
HP	69.6	169.2	265.4	67.2	153.8	230.7

From the plot of these data in Fig. 30 it can be seen that the turbine is capable of producing 130 HP at 16,666 rpm with a pressure ratio of 1.64 at a flow rate of 6.4 lbm/s. The inlet temperature must be about 105° F. At the lower speed of 12,018 rpm a power of 60 HP is produced at a pressure ratio of 1.37 for a flow rate of 4.85 lbm/s with a turbine inlet temperature of 82° F.

The air supply system of the Turbopropulsion Laboratory is capable of producing these inlet conditions and no difficulty is expected to drive the compressor at all possible operating conditions.

V. MECHANICAL DESIGN

1. Rotor

An investigation of the stresses in the Hybrid rotor has been carried out to determine its maximum operating speed. As evident from Dwg. 2203 of Appendix B the outer rim of the rotor will produce bending stresses which will be reduced, in part, by the restraint of the radial blades. In Ref. 16 the stresses were calculated by ignoring these bending stresses and the support by the blades. Referred to the outer rotor radius $R_o = 5.94$ inch the maximum stress σ_{max} was determined to be

$$\sigma_{max} = 0.53 \; \rho\omega^2 \; R_o^2$$

where ρ is the density of the rotor material.

For aluminum alloy AL-7079 with $\rho = 2.616 \; (10^{-4})$ lb $s^2/in.^4$, there is at $N = 17,000$ rpm

$$\rho\omega^2 \; R_o^2 = 29,252 \text{ psi}$$

and

$$\sigma_{max} = 15,504 \text{ psi}$$

With a correction factor of about 1.25, to allow for the inaccuracies of the model used for the calculation, the design stress σ_d was taken as

$$\sigma_d = 1.25 \; \sigma_{max} = 19,380 \text{ psi}$$

Aluminum alloy Al-7079-T6 was chosen as material. In forged condition this alloy has a 0.2% yield stress of 73 kpsi, and an ultimate stress of 83 kpsi.

During his stay at NPS as Visiting Assistant Professor, Dr. W. Schlachter undertook a more accurate stress analysis with the method of Ref. 17 which is discussed also in Ref. 18. This method takes account of the bending moments that occur in non-symmetrical disks with radial blades. Although the forces and moments produced by the blade elements are evaluated properly, these

effects are later distributed evenly along the periphery to obtain axi-
symmetric conditions. Thus the rotor is supposed to have an infinite
number of blades which have the same effect as the actual number of blades.
Inspite of its complexity the method of Ref. 17 gives doubtful results in
the vicinity of the outer radius of the Hybrid rotor, and finite-element
methods should actually be employed to give more accurate conditions.

Figure 31 shows the dimensionless stresses $\sigma/(\rho\omega^2 R_o^2)$ in the disk in
radial and peripheral directions. In Fig. 31 the shape of the Hybrid rotor is
shown also to indicate that the plotted stress ratios exist on either the
outer or the inner disk contour, which are designated by A and B, respec-
tively. Evidently, high stresses occur at a radius ratio $R/R_o = 0.7$ where
the disk has its smallest thickness. On contour A the disk is in com-
pression and on contour B it is in tension. This is indicative of the
bending moment that must occur at this station.

The highest stress occurs at the radius R_o on the inner contour B of
the rotor but it has the nature of a stress concentration which, in ductile
materials, will be reduced considerably by local plastic deformations if
the yield stress is exceeded. For this reason ductile materials have to
be used for rotors to equalize stress peaks. From Fig. 31 it can be concluded
that a maximum stress of about 0.60 $(\rho\omega^2 R_o^2)$ can be used as a design
criterion for the Hybrid rotor if it is made of a material with good duc-
tility.

This criterion seems to be invalidated by Fig. 32 which shows the
blade stresses at the tip, and at the base where they adjoin the disk.
These stations are designated as contours D and C, respectively, of the
rotor which is shown in Fig. 32, also. However, the high stress ratio at
the blade tips at a radius ratio $R_D/R_o = 0.7$ is clearly a local condition
which will be reduced by plastic yielding if the material has good

ductility. Drawing 2203 of Appendix B shows that the blades of the rotor have a thickness of 0.125 inch. If this thickness were increased to 0.16 inches the blade tip stress ratio could be reduced from 2 to about 1.22 without loss in efficiency. However, the writer believes that even with the thin blades the rotor is capable of operating at 17,000 rpm without danger. For a stress ratio of 0.6, the maximum stress σ_{max} is

$$\sigma_{max} = 17,500 \text{ psi}$$

If a maximum design stress of 55 kpsi is taken for AL-7075-T6, or about 75 percent of its 0.2% yield stress (73 kpsi), the maximum rotor speed could be

$$N_{max} = 17,000 \sqrt{\frac{55,000}{17,500}} = 30,100 \text{ rpm}$$

A design speed of 17,000 rpm was used because of the critical speed of the rotor assembly. For the overhung arrangement of Dwg. 2222, where the shaft is supported by ball bearings with 30 mm bore, and for an aluminum rotor that weighs about 19.5 lb, the critical speeds are:

$$N_{CI} = 21,620 \text{ rpm}$$

and

$$N_{CII} = 66,230 \text{ rpm}$$

These speeds were obtained without taking account of the flexibility of the bearing supports. Thus, the decision was made to limit the operating speed to 17,000 rpm or about 78 percent of the first critical shaft speed.

2. Maximum Obtainable Pressure Ratios

It is of interest to evaluate what pressure ratio could be produced by the Hybrid compressor if it were rotating at 30,100 instead of at 16,666 rpm. The peripheral speed ratio U_2/a_0 for a total inlet temperature $T_0 = 520^\circ$ R could then be increased from 0.7156 to

$$(U_2/a_0)_{max} = 1.2924$$

From Eq. A II(3)

$$\frac{P_{t4}}{P_0} = \left[1 + (\gamma - 1) \; \mu \; \eta_c \; (U_2/a_0)^2 \right]^{\gamma/(\gamma - 1)} \tag{87}$$

For an assumed efficiency $\eta_c = 0.8$, and $\gamma = 1.4$, $\mu = 0.85$,

$$\left(\frac{P_{t4}}{P_0} \right)_{max} = 3.71$$

At this pressure ratio the static temperature T_2 at the rotor exit is from Eq. A I(7), for $T_0 = 520^\circ$ R,

$$(T_2)_{max} = 662.5^\circ \; R = 202.5^\circ \; F$$

This temperature is somewhat high for aluminum alloys since their physical properties are reduced considerably at higher temperatures. At 300° F, for instance, the 0.2% yield strength of AL-7075-T6 is reduced from 73 kpsi (at room temperature) to 22 kpsi.

Titanium alloy 6AL-4V would be a better rotor material for the higher speeds. At a temperature of about 300° F the 0.2% yield strength of a forging with an elongation of 13 percent is about 130 kpsi. For a design stress of 75 percent of this yield strength, or

$$\sigma_{max} = 97,500 \; psi$$

and

$$\sigma_{max} = 0.6 \; (\rho \omega^2 \; R_0^2)$$

there is with

$$\rho = 4.144 \; (10^{-4}) \; lb \; s^2/in.^4$$

$$N_{max} = \frac{30}{\pi} \; \omega = \frac{30}{\pi} \sqrt{\frac{\sigma_{max}}{(0.6) \; \rho \; R_0^2}} = 31,835 \; rpm$$

55

Then

$$U_2/a_0 = 1.3669$$

From Eq. 87 the pressure ratio at this speed ratio is, for $\eta_c = .80$, $\gamma = 1.4$, $\mu = 0.85$,

$$\frac{P_{t4}}{P_0} = 4.213$$

at a temperature T_2 of

$$T_2 = 679.4^\circ \text{ R} = 219.4^\circ \text{ F}$$

These calculations indicate that pressure ratios larger than about 4.2 can be reached only in a Hybrid compressor of the design proposed here, if spin tests show that stress ratios $\sigma_{max}/(\rho \, \omega^2 \, R_0^2)$ higher than 0.6 are permissible, or that the ratio of 75 percent of design and yield stress is too conservative.

3. General Description of Test Rig

Drawing No. 2222 of Appendix B shows that the compressor shaft is supported by two matched pairs of high-precision ball bearings. The rotor assembly is held together by a central tie-bolt which is prevented from turning by prongs in the quill shaft that connects the compressor to the drive turbine. At the compressor end of the assembly, a steel attachment, shown in Dwg. 2103-A, pre-loads the inner races of the ball bearings and serves as support for the aluminum rotor. To ensure that the rotor remains concentric with the shaft, even if it increases its diameter by centrifugal stresses, four matched bushings (part 2103-2) are inserted in holes in the rotor collar and part 2103-1, that are drilled and reamed together. These bushings center the rotor and transmit the torque. The maximum torque is about 605 in.-lb at 160 HP and 16,666 rpm. The cross-sectional area of one bushing (0.25 OD, 0.196 ID) is 0.0189 in.^{2}. The shear force acting at the

diameter of 3.2 in., where the rotor rests on the steel disk (part 2103-1) is 605/(2 x 3.2) = 94.5 lb if all bushings carry equal loads. Thus the shear stress per bushing is 94.5/0.0189 = 5000 psi. The bushings are of Steel AISI 4340, hardened to 360 Brinell, to obtain a yield strength of about 160 kpsi. Hence the allowable shear stress is 80,000 psi and it is possible for one bushing to transmit the whole torque without danger.

The axial thrust exerted by the impeller is eliminated by the rotating balance piston near the quill shaft. The ball bearings at this shaft end are floating but they are supported by flexures which are equipped with strain gages. Calibrations of the assembly with known applied axial forces will indicate how much thrust is acting on the bearings. The read-out of the strain gages is displayed in the control room so that the balance air pressure can be adjusted for minimum thrust acting on the bearings. Because of its symmetrical design the drive turbine will not produce any axial thrust. The bearings are oil-mist lubricated, and the temperature of each outer race of the eight bearings is measured by a thermocouple which can be read in the control room also.

The diffusor blades are attached to blade holders (Part 1 of Dwg. 2209) by nuts and lock washers. Hence their stagger angles can be varied. These blade holders are inserted in a casing (Part 4 of Dwg. 2208). A number of spacer rings (see Dwg. 2209) were manufactured to be able to locate the diffusor blade rows at different distances from the rotor discharge. It is possible also to rotate the blade holders with respect to each other. With this arrangement it is possible to produce different arrangements of tandem blade rows. Part 4 of Dwg. 2208 is bolted to a casing (Part 1 of Dwg. 2207) on one side and to the shroud support of Dwg. 2212 on the other. To this support is attached the rotor shroud (Part 1 of Dwg. 2213) to form the floating stator assembly whose functions

are described in the next paragraph. Honeycomb flow straighteners are arranged between the fins of the shroud support.

At the design point the total temperature of the air passing through the compressor will increase by about 90° R. Hence a temperature error of one degree will result in a change of the calculated efficiency of about 1.2 points. Errors of temperature measurements of one degree easily occur in high speed flows, especially if they are non-steady. It was therefore decided to make arrangements for direct torque measurements. As shown in Dwg. 2222 the so-called floating stator assembly, consisting of the diffusor vanes, the flow straightener, the rotor shroud, and an outer casing, is supported by two special Kaydon ball bearings. The flow ahead of the inducer is in axial direction and the flow straightener after the diffusor will produce an axial discharge velocity. Then, the moment excerted on the rotor must be equal and opposite to the moment acting on the above-mentioned assembly. This moment is measured by flexures with strain gages (Part 4 of Dwg. 2215) which are calibrated against known torques, that are applied with a lever and known weights.

This arrangement requires labyrinth seals at the inner and outer diameters of the shroud of Dwg. 2213. These labyrinths are shown in Dwg. 2215. For radial clearances of 0.015 inch a leakage flow of about 0.012 lbm/s will pass through the inner labyrinth with 6.4 inch ID, from the region inside the shroud to the inducer inlet. This quantity is about 0.4 percent of the design flow rate. Through the outer labyrinth with an OD of 9.48 inch, however, a leakage flow of 0.064 lbm/s will occur from the opening after the flow straightener to the region inside the shroud. To maintain the required pressure between the labyrinths, an air flow of 0.064 - 0.012 = 0.054 lbs/s has to be vented from this region. For this reason the inlet casing, shown in Dwg. 2214-2, is hollow and is connected

by four 1 inch tubes to openings in the 18 inch suction pipe ahead of the flow measuring nozzle.

The measuring nozzle has a diameter of 5.375 inches and is formed of epoxy as shown in Dwg. 2222, with parts of the contour machined in the nozzle frame of Dwg. 2216. The shape of the nozzle conforms to the norms of VDI measuring orifices. A nozzle with a diameter of 5.375 inches will produce a pressure difference of about 20 inches of water for the measuring of the design flow rate of 2.7 lbm/s.

Drawing 2223 shows the general installation of the compressor test rig in Test Cell 2 of the Turbopropulsion Laboratory. Air supplied from a multi-stage axial compressor with a drive power of 1250 HP passes through a remote-controlled butterfly valve to the drive turbine. In case of runaway conditions, which could be caused by a compressor blade failure, the turbine air can be blown directly to the atmosphere through an emergency bypass valve.

The compressor air flow is controlled by the inlet throttle valve of Dwg. 2158. It consists of a fixed and a rotating plate that have the same arrangement of holes. The maximum flow area is 158 in.^{2}, corresponding to the area of a pipe of about 14 inch ID. The rotating plate is supported by ball bearings and can be moved with the oil pressure actuator of Dwg. 2159. This actuator can produce a force of about $1700_{\text{lb}} \pm 1700$ lb for an oil pressure of 400 psi. It is controlled from the control room by a reversible electric motor of less than 1/10 HP. The actuator is inherently stable and maintains the same position irrespective of the force applied to it, provided it is less than about 2000 lb.

After the throttling valve the velocity of the air is destroyed in the plenum chamber of Dwg. 2164-1. It is equipped with six perforated plates, with 43 percent free opening, which can be located at arbitrary positions

along the axis of the plenum. A contoured plastic nozzle guides the flow

into the 18 inch diameter suction pipes, which contain the measuring

nozzle.

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TABLES

TABLE I: Flow, Blade, and Incidence Angles

at Inducer Leading Edge

R_1 (in.)	β_1 ($^\circ$)	β_B ($^\circ$)	$\tan \beta_B$	$i = \beta_1 - \beta_B$ ($^\circ$)
3.025	55	50.32	1.20545	4.68
2.8	52.89	47.99	1.11016	4.90
2.6	50.83	45.71	1.02525	5.12
2.4	48.57	43.23	0.94024	5.34
2.2	46.09	40.51	0.85449	5.58
2.0	43.36	37.54	0.76852	5.82
1.8	40.36	34.30	0.68216	6.06
1.6	37.07	30.76	0.59530	6.31
1.5	35.30	28.88	0.55166	6.42
1.4	33.46	26.92	0.50784	6.54
1.3	31.54	24.88	0.46388	6.66
1.2	29.53	22.77	0.41973	6.76
1.1	27.44	20.57	0.37538	6.87
1.023	25.78	18.83	0.34111	6.95
1.00	25.27	18.30	0.33085	6.97
0.99	25.05	18.08	0.32639	6.97

TABLE II: Loss Coefficients of First Blade Row of Diffusor

$\Delta\alpha$	σ =	0.8	1.0	1.2	1.4	1.6	1.8
10°	D	0.4524	0.4146	0.3893	0.3713	0.3578	0.3473
	Y_P	0.0452	0.0486	0.0527	0.0572	0.0619	0.0668
	$Y_t{'}$	0.0900	0.0934	0.0975	0.1020	0.1067	0.1116
	$Y_t{''}$	0.0680	0.0788	0.0902	0.1031	0.1169	0.1323
12°	D	0.5137	0.4705	0.4417	0.4211	0.4057	0.3937
	Y_P	0.0545	0.0578	0.0620	0.0666	0.0716	0.0768
	$Y_t{'}$	0.1116	0.1148	0.1190	0.1236	0.1286	0.1338
	$Y_t{''}$	0.0873	0.0988	0.1127	0.1289	0.1470	0.1669
14°	D	0.5687	0.5207	0.4886	0.4657	0.4485	0.4352
	Y_P	0.0639	0.0670	0.0711	0.0760	0.0812	0.0857
	$Y_t{'}$	0.1332	0.1362	0.1403	0.1452	0.1504	0.1549
	$Y_t{''}$	0.1069	0.1207	0.1376	0.1569	0.1788	0.2017

$\Delta\alpha = \alpha_2 - \alpha_3 = 65^{\circ} - \alpha_3$ = Flow Deflection

σ = Solidity = (Blade Chord/Blade Spacing)

D = Diffusion Factor (Eq. 16)

Y_P = Profile Loss Coefficient (Eq. 20)

$Y_t{'} = Y_P + Y_s{'}$ = Overall Loss Coefficient

$Y_t{''} = Y_P + Y_s{''}$ = Overall Loss Coefficient (Eq. 27)

$Y_s{'}$ = Secondary Flow Loss Coefficient (Eq. 25)

$Y_s{''}$ = Secondary Flow Loss Coefficient (Eq. 26 with

$Y_s{''}/Y_t{''}$ from Fig. 6)

TABLE III: Design Values of First Blade Rows

of Diffusors A and B

Diffusor	A	B
Diffusor Blade Row Designation	A_1	B_1
Flow Deflection $\triangle\alpha^\circ = \alpha_2 - \alpha_3$	12	12
Number of Blades	38	38
Solidity σ	1.6	0.95
Diffusion Factor D	0.4057	0.4796
Profile Loss Coefficient Y_p	0.0716	0.0569
Total Loss Coefficient Y_t'	0.1286	0.1139
Total Loss Coefficient Y_t''	0.1470	0.0958
Blade Chord c (in.)	1.455	0.864
Maximum Blade Thickness t (in.)	0.090	0.085
Thickness Ratio t/c	0.062	0.098

TABLE IV: Loss Coefficients of Second

Blade Row of Diffusor

$\Delta\alpha$	$\sigma =$	0.8	1.0	1.2	1.4	1.6	1.8
26°	D	0.6321	0.5706	0.5296	0.5003	0.4783	0.4612
	Y_P	0.0565	0.0568	0.0587	0.0613	0.0644	0.0678
	$Y_t{}'$	0.1349	0.1352	0.1371	0.1397	0.1428	0.1462
	$Y_t{}''$	0.1201	0.1354	0.1553	0.1793	0.2077	0.2387
32°	D	0.7101	0.6392	0.5919	0.5581	0.5327	0.5130
	Y_P	0.0698	0.0690	0.0703	0.0726	0.0755	0.0789
	$Y_t{}'$	0.1709	0.1702	0.1714	0.1737	0.1767	0.1801
	$Y_t{}''$	0.1654	0.1856	0.2129	0.2461	0.2906	0.3432
38°	D	0.7753	0.6956	0.6425	0.6046	0.5761	0.5540
	Y_P	0.0826	0.0805	0.0810	0.0829	0.0856	0.0889
	$Y_t{}'$	0.2066	0.2044	0.2049	0.2068	0.2095	0.2128
	$Y_t{}''$	0.2135	0.2439	0.2811	0.3288	0.3926	0.4677

$\Delta\alpha = \alpha_3 - \alpha_4 = 53^{\circ} - \alpha_4 =$ Flow Deflection

σ = Solidity = (Blade Chord/Blade Spacing)

D = Diffusion Factor (Eq. 16 with $\alpha_2 = \alpha_3$, $\alpha_3 = \alpha_4$)

Y_P = Profile Loss Coefficient (Eq. 26 with $\alpha_3 = \alpha_4$)

$Y_t{}'$ = $Y_P + Y_s{}'$ = Overall Loss Coefficient

$Y_t{}''$ = $Y_P + Y_s{}''$ = Overall Loss Coefficient

$Y_s{}'$ = Secondary Flow Loss Coefficient (Eq. 25 with

$\qquad \alpha_2 = \alpha_3$, $\alpha_3 = \alpha_4$)

$Y_s{}''$ = Secondary Flow Loss Coefficient (Eq. 26 with

$\qquad Y_s{}''/Y_t{}''$ from Fig. 6)

TABLE V: Design Values of Second Blade

Rows of Diffusors A and B

Diffusor	A	B
Diffusor Blade Row Designation	A2	B2
Flow Deflection $\triangle\alpha^{\circ} = \alpha_3 - \alpha_4$	32	32
Number of Blades	38	38
Solidity σ	1.4	1.0
Diffusion Factor D	0.5581	0.6392
Profile Loss Coefficient Y_P	0.0726	0.0690
Total Loss Coefficient Y_t'	0.1737	0.1702
Total Loss Coefficient Y_t''	0.2461	0.1856
Blade Chord c (in.)	1.275	0.910
Maximum Blade Thickness t (in.)	0.090	0.085
Thickness Ratio t/c	0.070	0.093

Diffusor Blade Row	A1	B1	A2	B2
$\alpha_e (^\circ)$	65	65	53	53
$\Delta\alpha (^\circ)$	12	12	32	32
$\alpha_d (^\circ)$	53	53	21	21
σ	1.6	0.95	1.4	1.0
t/c	0.062	0.098	0.07	0.093
From Ref. 3 $\begin{cases} (k_i)_{sh} \\ (k_\delta)_{sh} \\ (i_0)_{10} \\ (\delta_0)_{10} \\ m \\ n \\ (k_i)_t \\ (k_\delta)_t \end{cases}$	1.1 1.1 7.85° 3.22° 0.245 -0.197 0.79 0.545	1.1 1.1 4.55° 2.05° 0.338 -0.293 0.99 0.925	1.1 1.1 5.80° 1.40° 0.231 -0.140 0.845 0.630	1.1 1.1 4.10° 1.80° 0.300 -0.195 0.970 0.955
$i_0 = (i_0)_{10}(k_i)_t(k_i)_{sh}$	6.822°	4.955°	5.391°	4.375°
$\delta_0 = (\delta_0)_{10}(k_\delta)_t(k_\delta)_{sh}$	1.930°	2.086°	0.97°	1.891°
$\varphi = (\Delta\alpha - i_0 + \delta_0)/(1 - m + n)$	12.738°	24.74°	43.846°	58.447°
$i = i_0 + n\varphi$	4.312°	-2.95°	-0.747°	-7.022°
$\delta = \delta_0 + m\varphi$	5.051°	10.50°	11.098°	19.425°
$\gamma = \alpha_e - \varphi/2 - i$	54.319	54.922	31.824	30.798
Chosen incidence i*	$+2^\circ$	-1°	$0^\circ 45'$	-2°
From Ref. 3: $(d\delta/di)$	0.04	0.13	--	0.085
$\varphi^* = \varphi - (i^* - i)(1 - d\delta/di)$	14.957	23.613	43.846	53.852
$\gamma^* = \alpha_e - \varphi^*/2 - i^*$	$55^\circ 31'$	$54^\circ 11'$	$31^\circ 50'$	$28^\circ 04'$
Profile coordinates:	Dwg 2210-1	Dwg 2210-3	Dwg 2210-2	Dwg 2210-4
$\Delta\gamma$	$0^\circ 39'$	$1^\circ 09'$	0°	$0^\circ 06'$
$\gamma' = \gamma + \Delta\gamma$ or $\gamma^* + \Delta\gamma$	$56^\circ 10'$	$55^\circ 20'$	$31^\circ 50'$	$28^\circ 10'$

TABLE VII: Flow Properties in Diffusor

Blade Row	A1'	A1"	B1'	B1"
P_{t2}/P_0		1.6764		
$T_{t2}/T_0 = T_{t3}/T_0 = T_{t4}/T_0$		1.17411		
P_2/P_0		1.2677		
T_2/T_0		1.08402		
K (Eq. 43)		0.571523		
Y_t (Table III)	0.1286	0.1470	0.1139	0.0958
P_{t3}/P_0 (Eq. 47)	1.6238	1.6163	1.6298	1.6372
M_3^* (chosen)	0.4240	0.4265	0.4220	0.4196
T_3/T_0 (Eq. 45)	1.13336	1.13290	1.13373	1.13417
P_3/P_0 (Eq. 46)	1.4350	1.4263	1.4419	1.4505
M_3 (Eq. 44)	0.4240	0.4265	0.4220	0.4196
V_3 (ft/s) (Eq. 48)	504.6	507.7	502.3	499.5
Blade Row	A2'	A2"	B2'	B2"
K (Eq. 43)	0.385168	0.385168	0.385132	0.385150
Y_t (Table V)	0.1737	0.2461	0.1702	0.1856
P_{t4}/P_0 (Eq. 47)	1.5910	1.5695	1.5978	1.6025
M_4^* (chosen)	0.2743	0.2784	0.2730	0.2722
T_4/T_0 (Eq. 45)	1.15670	1.15618	1.15686	1.15670
P_4/P_0 (Eq. 46)	1.5100	1.4872	1.5172	1.5221
M_4 (Eq. 44)	0.2743	0.2785	0.2730	0.2722
V_4 (ft/s) (Eq. 48)	329.8	334.7	328.2	327.2
η_{t4} (Eq. 49)	81.5%	78.9%	82.3%	82.8%

TABLE VIII: Flow Conditions in Flow Straightener

and Discharge Duct

(See Fig. 11 for Symbols and Location of Stations)

Diffusor	A'	A''	B'	B''
V_4 (ft/s)	329.8	334.6	328.2	327.2
P_{t4}/P_0 — From Table VII	1.5910	1.5696	1.5979	1.6026
p_4/P_0	1.5100	1.4873	1.5172	1.5222
T_4/T_0	1.15670	1.15619	1.15686	1.15698
$V_4/a_0 = V_4/(1117.85)$	0.2950	0.2993	0.2936	0.2927
T_4^*/T_0 (Eq. 53)	1.15893	1.15849	1.15907	1.15918
P_{t4}'/P_0 (Eq. 54)	1.5803	1.5587	1.5872	1.5919
T_4'/T_0 (Eq. 55)	1.15532	1.15477	1.15550	1.15561
p_4'/P_0 (Eq. 56)	1.4935	1.4706	1.5009	1.5059
P_{t4}''/P_0 (Eq. 58)	1.5543	1.5323	1.5613	1.5661
p_4''/P_0 (Eq. 59)	1.4689	1.4457	1.4764	1.4814
T_5/T_0 (Eq. 60)	1.16074	1.16035	1.16087	1.16095
P_{t5}/P_0 (Eq. 61)	1.5290	1.5066	1.5362	1.5410
P_{t6}/P_0 (Eq. 62)	1.5050	1.4822	1.5123	1.5172
T_6/T_0 (Eq. 63)	1.16503	1.16477	1.16512	1.16518
p_6/P_0 (Eq. 64)	1.4647	1.4414	1.4721	1.4772
$P_0 = \dfrac{14.7}{(p_6/P_0)}$ (psia)	10.036	10.198	9.985	9.951

TABLE IX: Estimated Compressor Performance

at Design Point (N = 16,666 rpm, T_0 = 520°R)

Diffusor	A'	A"	B'	B"
P_{t4}/P_0 (Table VII)	1.5910	1.5696	1.5979	1.6026
η_{t4} (Table VII)	81.5%	78.9%	82.3%	82.8%
P_6/P_0 (Table VIII)	1.4647	1.4414	1.4721	1.4772
P_0 (Table VIII), (psia)	10.036	10.198	9.985	9.951
$\dot{w}$ (Eq. 34), (lbm/s)	2.698	2.742	2.685	2.676
HP (Eq. 36), (HP)	83.0	84.3	82.5	82.2
M (Eq. 65), (in.-lb)	313.7	318.7	312.1	311.0
U_2/a_0	———— 0.7156 ————			
$(\dot{m})*$ (Eq. 66)	———— 0.08309 ————			
$(HP)*$ (Eq. 67)	———— 0.05063 ————			
$(M)*$ (Eq. 69)	———— 0.05980 ————			
θ_c = 520/518.4	———— 1.0031 ————			
δ_c = P_0/14.7	0.6827	0.6937	0.6792	0.6769
N_{REF} (Eq. 73), (rpm)	———— 16,642 ————			
$\dot{w}_{REF}$ (Eq. 74), (lbm/s)	———— 3.9591 ————			
$(HP)_{REF}$ (Eq. 75), (HP)	———— 121.317 ————			
M_{REF} (Eq. 76), (in.-lb)	———— 459.45 ————			

PERFORMANCE OF CENTRIFUGAL COMPRESSOR ROTOR
(MONROE CALCULATOR 1655/6)
ROTOR DIMENSIONS:

γ of Fluid = 1.4 / Group	Symbol	No.	A₂= 21.0801 (in²)		A₁= 25.6685 (in²)		R₁₀/R₂ = 0.55	β_B= 50.32 (°)		k= 0.8599
SELECTED PARAMETERS	U_2/a_0	1	→			0.7156				→
	α_2	2	65	62	58	54	67	69	71	73
	k_{B2}	3	→			0.954				↑
	k_{B1}	4	→			0.980				↑
Eq. 82	μ	5	.85	.8325	.8088	.7844	.8616	.8732	.8847	.8963
ITERATION OF ↓	No.=j	6	DESIGN POINT	FINAL	FINAL	FINAL	FINAL	FINAL	FINAL	FINAL
	ψ_j	7	.7548	.788	.780	.781	.717	.6686	.6116	.548
PROGR.102	$\dot{\omega}\sqrt{(R_G/g)T_0}/P_G$	8	7.892 906	8.717 619	9.622 001	10.461 233	1.307 976	6.705 048	6.088 361	5.462 317
	Φ_2	9	.392 478	.433 488	.478 458	.520 190	.363 393	.333 412	.302 747	.271 616
	Φ_1	10	.313 769	.346 554	.382 506	.415 869	.290 516	.266 548	.242 032	.217 145
PROGR.103	P_1/P_0	11	.947 862	.935 492	.919 985	.903 564	.955 697	.963 010	.969 728	.975 796
	T_1/T_0	12	.984 817	.981 128	.976 454	.971 442	.987 136	.989 289	.991 256	.993 024
	V_1/a_0	13	.275 522	.307 180	.343 120	.377 877	.253 608	.231 421	.209 096	.186 761
	W_{10}/a_0	14	.480 435	.499 264	.522 146	.545 615	.468 212	.456 577	.445 675	.435 643
PROGR.104	β_{10} (°)	15	55.006	52.029	48.918	46.166	57.204	59.545	62.020	64.615
	β_{10}' (°)	16	50.851	47.772	44.606	41.849	53.154	55.636	58.291	61.109
	M_{W1}	17	.4841	.5040	.5284	.5536	.4712	.4590	.4476	.4372
	i° (°)	18	+0.531	-2.548	-5.713	-8.471	+2.834	+5.316	+7.971	+10.789
FIG. 24	η_R	19	.86	.8574	.80	.7396	.8514	.8373	.8187	.7964
PROGR.105	W_2/W_{10}	20	.6312	.6783	.7405	.7991	.5976	.5617	.5229	.4813
	η_J	21	.4999	.4789	.2198	-.1250	.4747	.4300	.3699	.2977
	→	22	.7548	.7878	.7802	.7817	.7170	.6686	.6116	.5480
PROGR.106	T_{t2}/T_0	23	1.174 108	1.170 524	1.165 669	1.160 671	1.176 484	1.178 860	1.181 216	1.183 592
	P_{t2}/P_0	24	1.676 382	1.657 610	1.605 044	1.554 246	1.683 471	1.687 492	1.688 961	1.688 362
	T_2/T_0	25	1.084 022	1.079 476	1.072 513	1.064 392	1.086 156	1.089 263	1.091 551	1.093 625
	P_2/P_0	26	1.267 734	1.248 524	1.199 174	1.147 873	1.275 311	1.279 641	1.281 213	1.280 258
	M_{V2}	27	.6446	.6494	.6590	.6725	.6425	.6413	.6409	.6413

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PERFORMANCE OF CENTRIFUGAL COMPRESSOR ROTOR

(MONROE CALCULATOR 1655/6)
ROTOR DIMENSIONS:

Y of Fluid = 1.4	A_2 = 21.0801		(in²)	A_1 = 25.6685		(in²)	R_{1o}/R_2 = 0.55		B_B = 50.32 (°)		k = 0.8599
		No.	α_2 = 65	62	58	54	50	67	69	71	73
SELECTED PARAMETERS	c_2/a_0	1	↓					↑		↑	↑
	α_2	2	65	62	58	54	50	67	69	71	73
	k_{B2}	3	↓				0.954	↓			↑
	k_{B1}	4	↓				0.98	↓			↑
Ec. 82	u =	5	.85	.8325	.8088	.7844	.7590	.8616	.8732	.8847	.8963
ITERATION OF →	No.=j	6	FINAL	FINAL	FINAL	FINAL	FINAL	FINAL	FINAL	FINAL	FINAL
	ψj	7	.7546	.7955	.8351	.8381	.840	.7111	.665	.612	.554
PROGR.102	$\dot{w}\sqrt{(R_G/g)T_0}/P_C$	8	5.265 458	5.875 178	6.653 236	7.384 474	8.099 555	4.881 731	4.478 169	4.070 451	3.660 138
	Φ_2	9	.262 822	.292 146	.330 835	.367 196	.402 754	.242 746	.222 679	.202 405	.182 002
	Φ_1	10	.210 114	.233 558	.264 488	.293 557	.321 984	.194 065	.178 022	.161 814	.145 503
PROGR.103	P_1/P_0	11	.977 378	.971 878	.963 604	.954 715	.944 912	.980 773	.983 875	.986 719	.989 292
	T_1/T_0	12	.993 483	.991 883	.989 463	.986 846	.983 941	.994 468	.995 366	.996 187	.996 929
	V_1/a_0	13	.180 505	.201 455	.229 532	.256 451	.283 366	.166 305	.152 213	.138 070	.123 921
PROGR.104	W_{1o}/a_0	14	.336 340	.348 033	.365 003	.382 504	.401 047	.328 937	.322 042	.315 604	.309 676
	B_{1o} (°)	15	57.542	54.631	51.035	47.898	45.044	59.630	61.793	64.057	66.411
	B_{1o}' (°)	16	53.511	50.460	46.755	43.519	40.735	55.727	58.047	60.500	63.079
	M_{W1}	17	.3374	.3494	.3669	.3850	.4043	.3298	.3228	.3162	.3101
	i° (°)	18	+3.191	+0.14	-3.565	-6.740	-9.584	+5.407	+7.727	+10.180	+12.159
FIG. 24	η_R	19	.856	.86	.86	.8204	.7680	.8428	.8315	.8164	.8006
PROGR.105	W_2/W_{1o}	20	.6502	.7017	.7639	.8220	.8761	.6134	.5742	.5325	.4882
	η_W	21	.4465	.4371	.3914	.1176	-.3847	.4102	.3813	.3386	.2936
	↓	22	.7547	.7955	.8350	.8381	.8394	.7111	.6655	.6119	.5541
	T_{t2}/T_0	23	1.090 552	1.088 663	1.086 139	1.083 540	1.080 835	1.091 762	1.092 998	1.094 223	1.095 458
	P_{t2}/P_0	24	1.321 777	1.315 198	1.305 222	1.287 029	1.267 233	1.323 813	1.326 128	1.327 759	1.329 071
PROGR.106	T_2/T_0	25	1.043 687	1.041 323	1.037 703	1.033 481	1.028 559	1.045 108	1.046 412	1.047 602	1.048 680
	P_2/P_0	26	1.133 514	1.125 676	1.112 604	1.090 658	1.065 369	1.136 169	1.138 616	1.140 082	1.140 810
	M_{V2}	27	.473 705	.476 767	.483 096	.492 128	.504 107	.472 442	.471 802	.471 713	.472 264

(0.516)

TABLE XI CALCULATED PERFORMANCE OF HYBRID COMPRESSOR AT 16,666 RPM

$$T_0 = 520°R \; ; \; P_0 = 14.7/(p_6/P_0) \quad (psia)$$

U_2/a_0	0.7156	0.7156	0.7156	0.7156
α_2	65.0000	62.0000	58.0000	54.0000
P_{t4}/P_0	1.5910	1.5722	1.5135	1.4235
P_4/P_0	1.5100	1.4708	1.3825	1.2527
T_4/T_0	1.1567	1.1485	1.1359	1.1190
M_{V4}	0.2743	0.3100	0.3620	0.4313
v_4/a_0	0.2951	0.3322	0.3858	0.4562
P_{t4}'/P_0	1.5803	1.5586	1.4958	1.4000
P_4'/P_0	1.4935	1.4504	1.3563	1.2193
P_{t4}''/P_0	1.5543	1.5262	1.4539	1.3458
P_4/P_0	1.4689	1.4202	1.3184	1.1720
P_{t5}/P_0	1.5290	1.4946	1.4131	1.2924
P_{t6}/P_0	1.5050	1.4648	1.3752	1.2443
P_6/P_0	1.4646	1.4151	1.3122	1.1647
P_0 (psia)	10.0367	10.3883	11.2026	12.6209
$\dot{w}$ (lbm/s)	2.6978	3.0841	3.6709	4.4963
HP	82.9226	92.8442	107.3626	127.5371
N (rpm)	16,666.	16,666.	16,666.	16,666.
η_T	0.8149	0.8093	0.7587	0.6607

U_2/a_0	0.7156	0.7156	0.7156	0.7156
α_2	67.0000	69.0000	71.0000	73.0000
P_{t4}/P_0	1.5982	1.5997	1.5816	1.5264
P_4/P_0	1.5295	1.5423	1.5339	1.4867
T_4/T_0	1.1618	1.1666	1.1709	1.1747
M_{V4}	0.2513	0.2292	0.2096	0.1943
v_4/a_0	0.2709	0.2475	0.2268	0.2106
P_{t4}'/P_0	1.5892	1.5922	1.5754	1.5212
P_4'/P_0	1.5155	1.5306	1.5242	1.4786
P_{t4}''/P_0	1.5671	1.5737	1.5600	1.5084
P_4/P_0	1.4944	1.5128	1.5093	1.4661
P_{t5}/P_0	1.5457	1.5558	1.5452	1.4961
P_{t6}/P_0	1.5252	1.5386	1.5308	1.4841
P_6/P_0	1.4907	1.5096	1.5066	1.4639
P_0 (psia)	9.8609	9.7375	9.7569	10.0417
$\dot{w}$ (lbm/s)	2.4541	2.2235	2.0230	1.8680
HP	76.4618	70.2088	64.7194	60.5433
N (rpm)	16,666.	16,666.	16,666.	16,666.
η_T	0.8123	0.8032	0.7723	0.6995

TABLE XII CALCULATED PERFORMANCE OF HYBRID COMPRESSOR AT 12,018 RPM

$$T_0 = 520^\circ R \; ; \; P_0 = 14.7/(p_6/P_0) \quad (psia)$$

U_2/a_0	0.5160	0.5160	0.5160	0.5160	0.516
α_2	65.0000	62.0000	58.0000	54.0000	50.000
P_{t4}/P_0	1.2824	1.2756	1.2642	1.2362	1.193
P_4/P_0	1.2414	1.2243	1.1969	1.1501	1.083
T_4/T_0	1.0805	1.0760	1.0693	1.0614	1.051
M_{V4}	0.2160	0.2429	0.2805	0.3228	0.374
V_4/a_0	0.2245	0.2520	0.2901	0.3326	0.383
P_{t4}'/P_0	1.2771	1.2689	1.2553	1.2246	1.178
P_4'/P_0	1.2330	1.2138	1.1833	1.1327	1.061
P_{t4}''/P_0	1.2639	1.2523	1.2337	1.1971	1.143
P_4''/P_0	1.2203	1.1980	1.1630	1.1072	1.029
P_{t5}/P_0	1.2511	1.2364	1.2127	1.1702	1.108
P_{t6}/P_0	1.2388	1.2210	1.1928	1.1450	1.077
P_6/P_0	1.2180	1.1952	1.1595	1.1029	1.024
P_0(psia)	12.0689	12.2989	12.6784	13.3279	14.346
$\dot{w}$ (lbm/s)	2.1724	2.4608	2.8726	3.3517	3.957
H P	34.7276	38.5173	43.6842	49.4315	56.478
N(rpm)	12,018.	12,018.	12,018.	12,018.	12,018
η_T	0.8135	0.8123	0.8042	0.7475	0.639

U_2/a_0	0.5160	0.5160	0.5160	0.5160	
α_2	67.0000	69.0000	71.0000	73.0000	
P_{t4}/P_0	1.2846	1.2870	1.2870	1.2811	
P_4/P_0	1.2498	1.2579	1.2630	1.2617	
T_4/T_0	1.0832	1.0859	1.0884	1.0907	
M_{V4}	0.1984	0.1810	0.1641	0.1479	
V_4/a_0	0.2065	0.1887	0.1712	0.1544	
P_{t4}'/P_0	1.2801	1.2832	1.2839	1.2786	
P_4'/P_0	1.2427	1.2519	1.2581	1.2577	
P_{t4}''/P_0	1.2689	1.2738	1.2761	1.2723	
P_4''/P_0	1.2318	1.2427	1.2505	1.2515	
P_{t5}/P_0	1.2580	1.2647	1.2687	1.2663	
P_{t6}/P_0	1.2475	1.2559	1.2614	1.2604	
P_6/P_0	1.2299	1.2411	1.2491	1.2504	
P_0(psia)	11.9526	11.8448	11.7683	11.7565	
$\dot{w}$ (lbm/s)	1.9871	1.8064	1.6313	1.4654	
HP	32.1903	29.6570	27.1356	24.6953	
N (rpm)	12,018.	12,018.	12,018.	12,018.	
η_T	0.8084	0.8037	0.7933	0.7683	

FIGURES

FIG. 1 HYBRID COMPRESSOR (SYMBOLS AND STATIONS) (NOT TO SCALE)

VELOCITY DIAGRAM AT RADIUS R_2 OF STATION (2)

VELOCITY DIAGRAM AT RADIUS R_{10} OF STATION (1)

INDUCER

IMPELLER WITH RADIAL BLADES

FIRST DIFFUSOR

SECOND DIFFUSOR

HONEYCOMB FLOW STRAIGHTENER

DISCHARGE DUCT

78
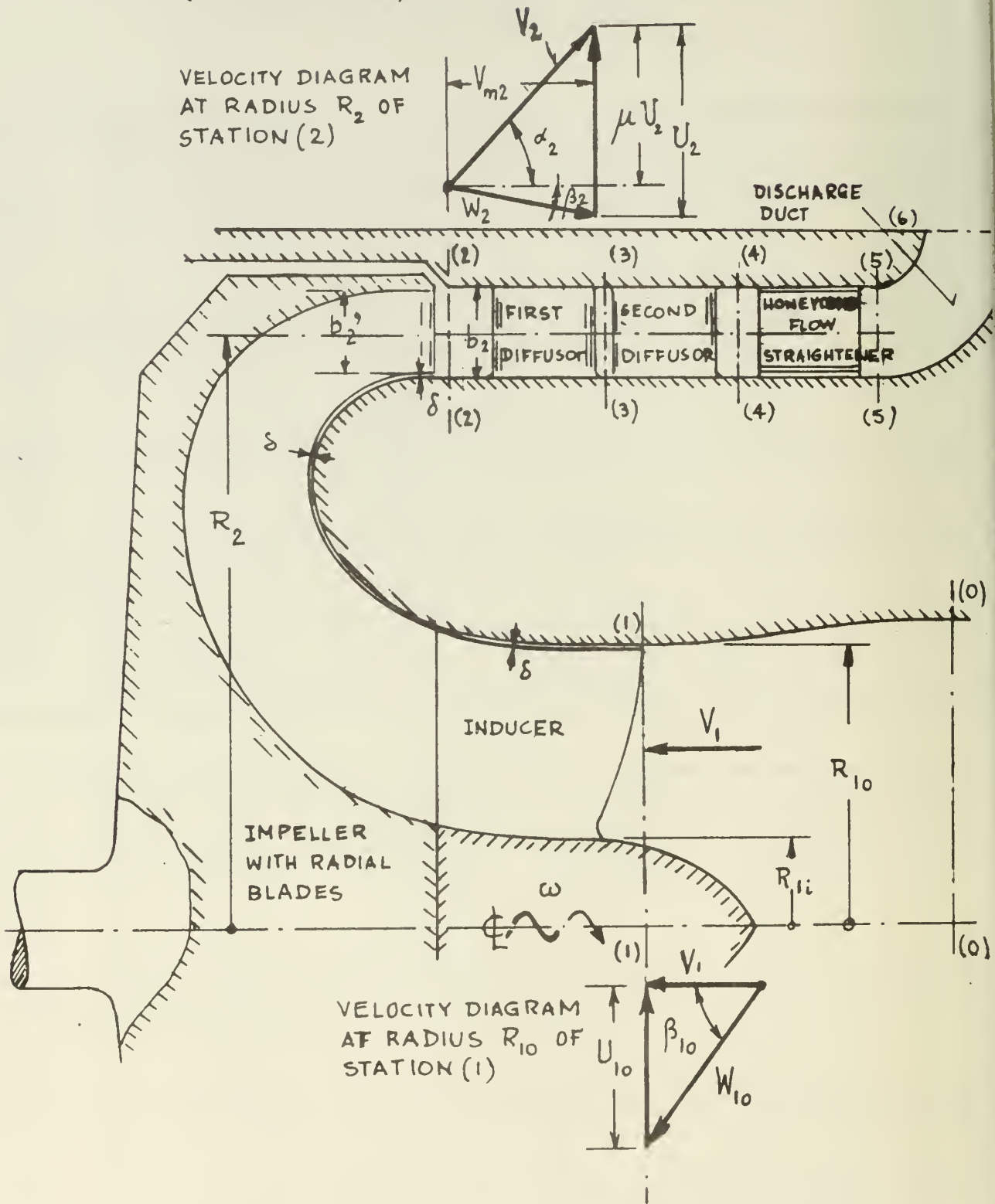
FIG. 2 DETERMINATION OF ROTOR HUB CONTOUR FOR SPECIFIED BLADE TIP CONTOUR
(TO SCALE)
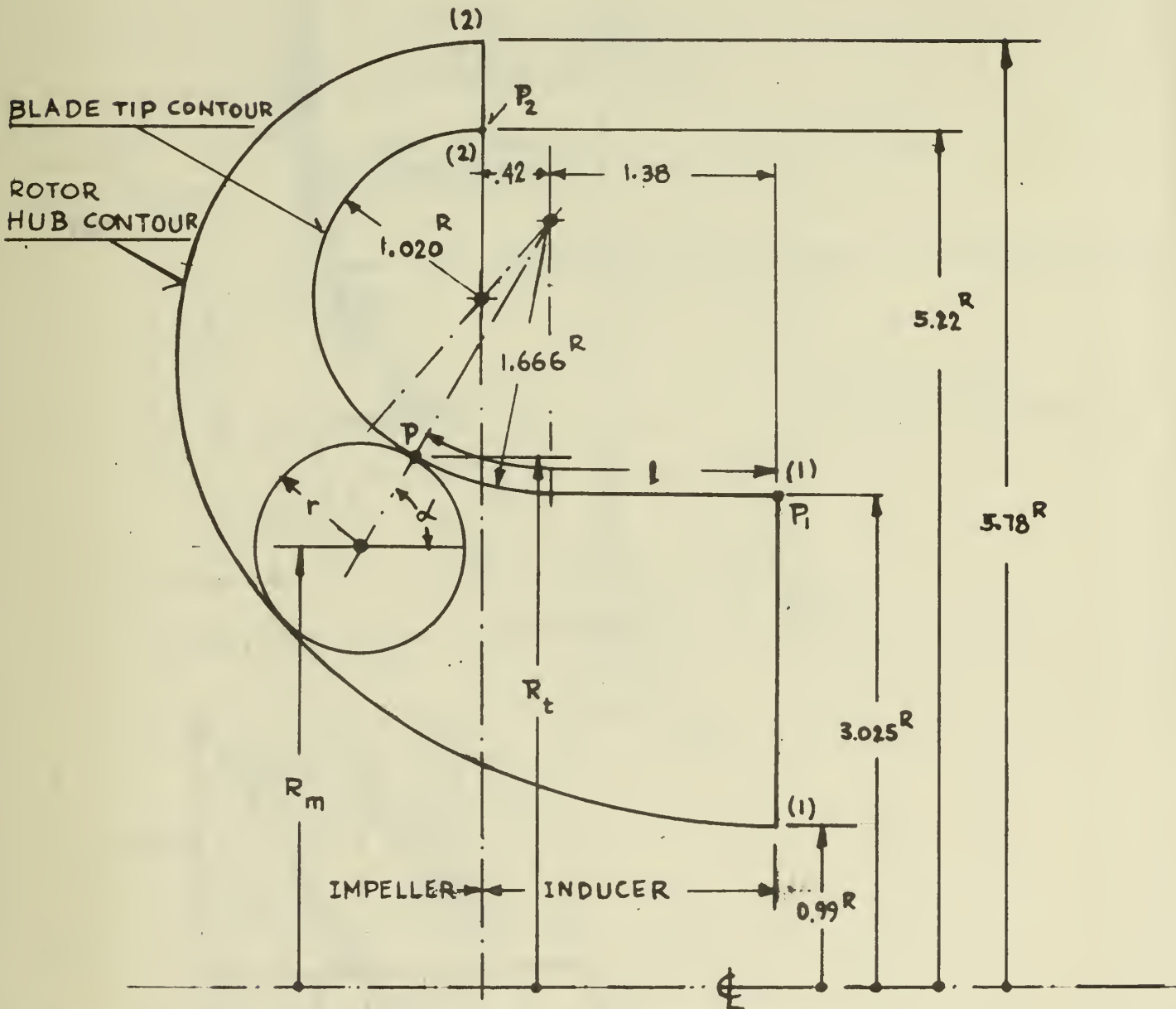
A_1 = ANNULUS AREA AT (1)-(1) ; A_2 = ANNULUS AREA AT (2)-(2)

AT POINT P: l = LENGTH OF TIP CONTOUR FROM P_1 TO P

l_o = LENGTH OF TIP CONTOUR FROM P_1 TO P_2

$$A = 2\pi R_m r = A_1 - (A_1 - A_2)\frac{l}{l_o}$$

$$R_m = R_t - r \sin\alpha$$

$$r = \frac{R_t}{2\sin\alpha} - \sqrt{\left(\frac{R_t}{2\sin\alpha}\right)^2 - \frac{A_1 - (A_1 - A_2)(l/l_o)}{4\pi \sin\alpha}}$$

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FIG. 3 CONDITIONS AT LEADING EDGE OF INDUCER
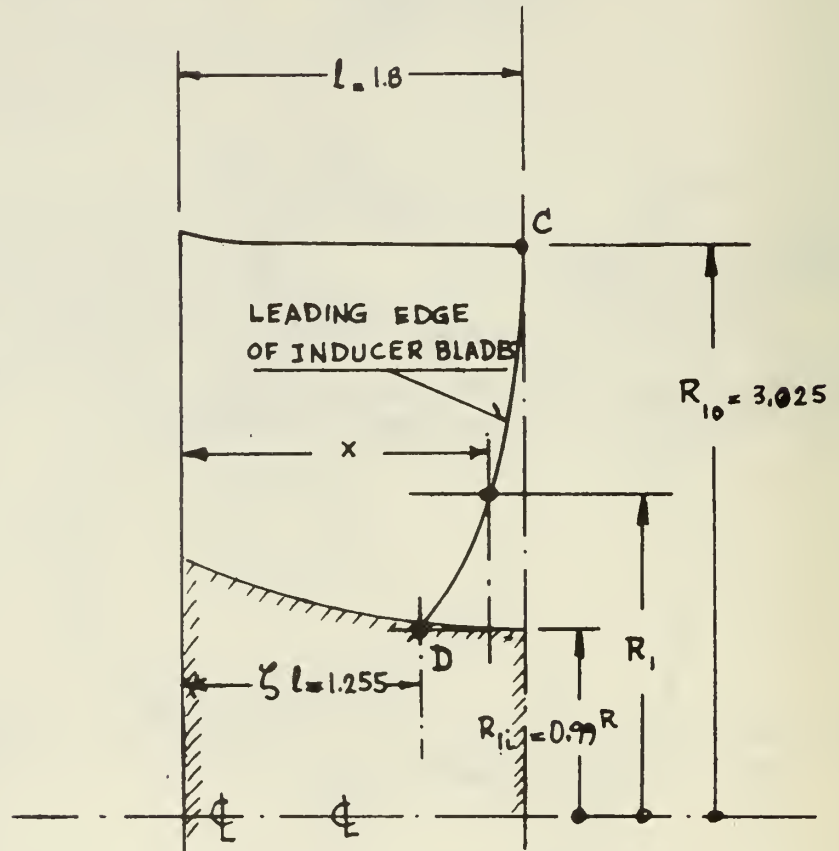
FIG. 3a MERIDIONAL CROSS-SECTION
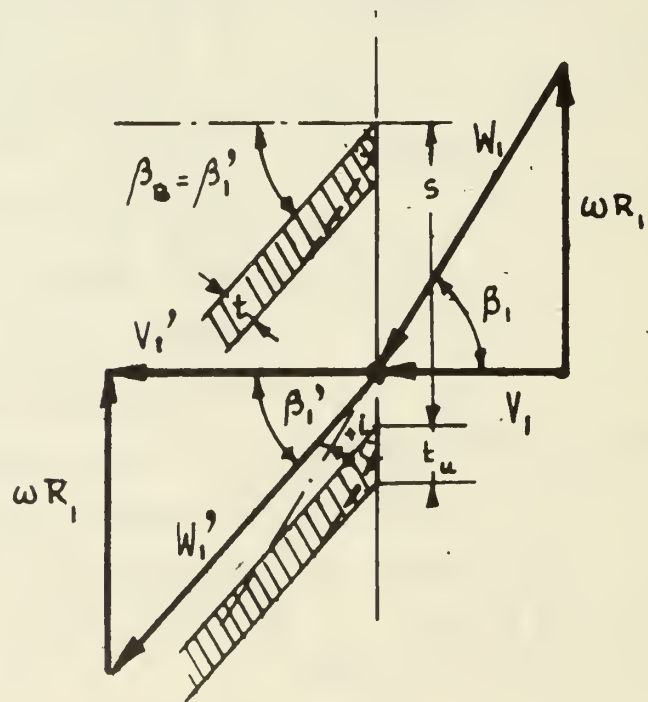
FIG. 3b CONDITIONS AT RADIUS R_1

FIG. 4   BLADE ANGLES OF STRAIGHT INDUCER BLADES

RADIAL IMPELLER BLADE

Q   IMPELLER INLET

INDUCER DISCHARGE

VIEW OF PLANES A-A PERPENDICULAR
TO RADIAL LINE THROUGH Q

STRAIGHT
INDUCER BLADE

BLADE SURFACES CONSISTING OF LINES PARALLEL TO
RADIAL LINES THROUGH Q

VIEW OF TANGENT
PLANE B-B THROUGH P

x

C ———— C

y

dx

dy P'

γ

$\dfrac{dy}{\cos\theta}$

P

β_B P'

dx

B

A

Q

y

P

P'

θ

A

B

$\sqrt{R_1^2 - y^2}$

θ

dy

R_1

BLADE SURFACE

SECTION C-C

81
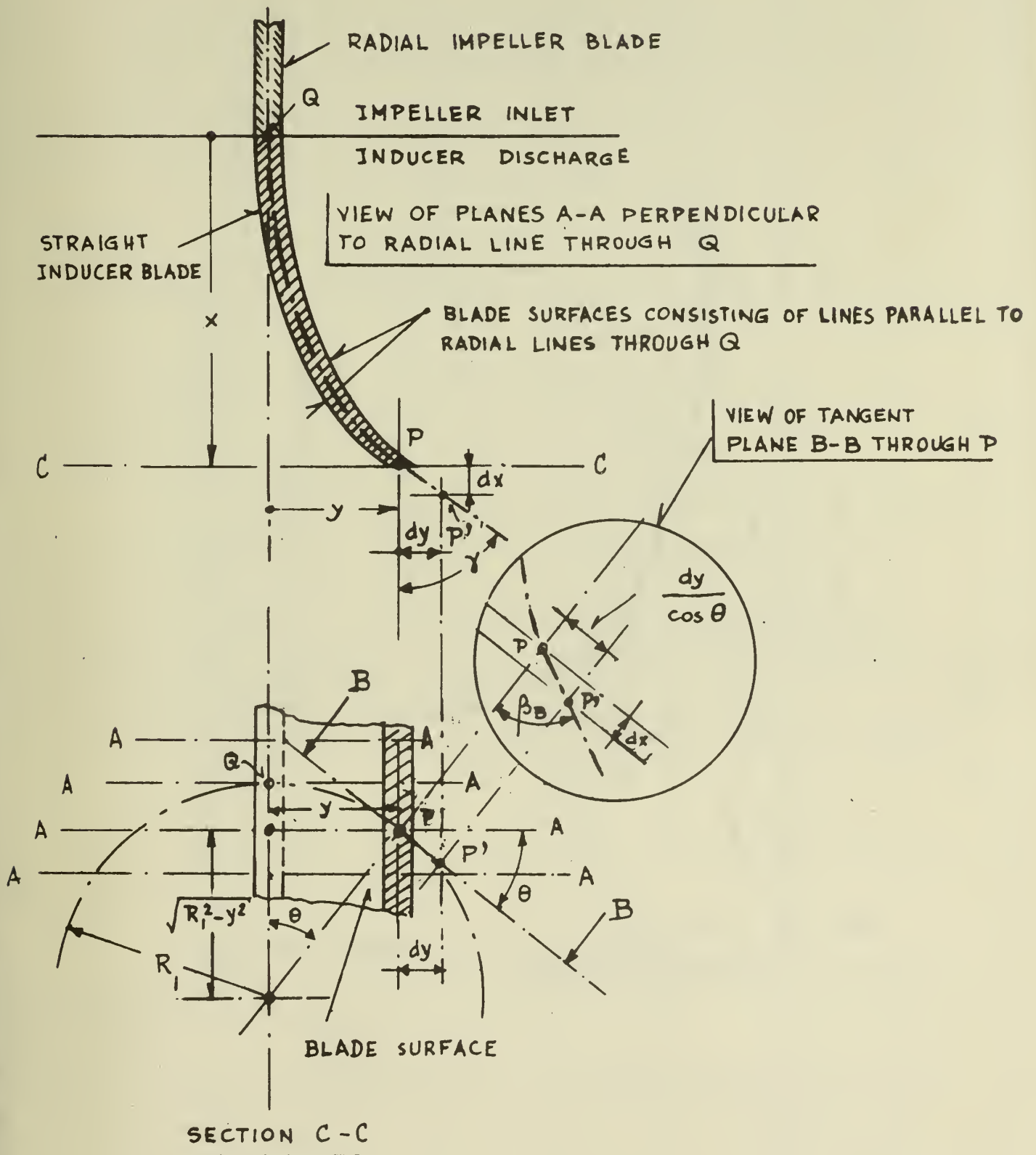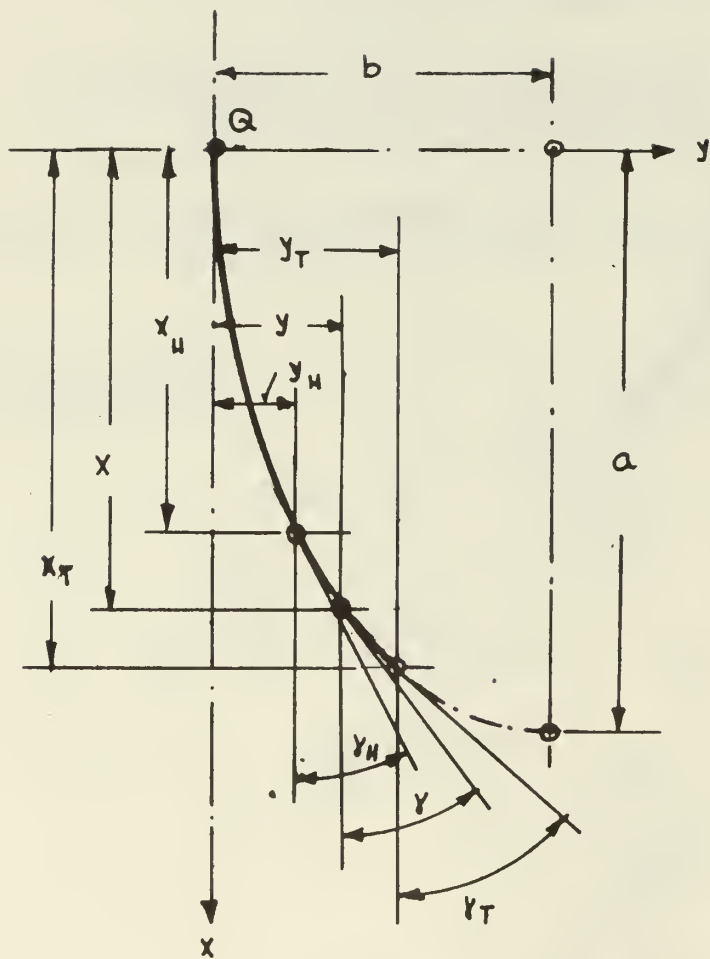
FIG. 5   PROPERTIES OF ELLIPTICAL INDUCER
BLADE SURFACE

FIG. 6 SECONDARY LOSS COEFFICIENT OF REF. 6

Y_s'' = SECONDARY LOSS COEFFICIENT , Y_t'' = TOTAL LOSS COEFFICIENT

$\Delta\alpha$ = FLOW DEFLECTION (RADIANS)

c = BLADE CHORD , h = BLADE HEIGHT

$\Delta\alpha \ (c/h)$

Y_s''/Y_t''

83
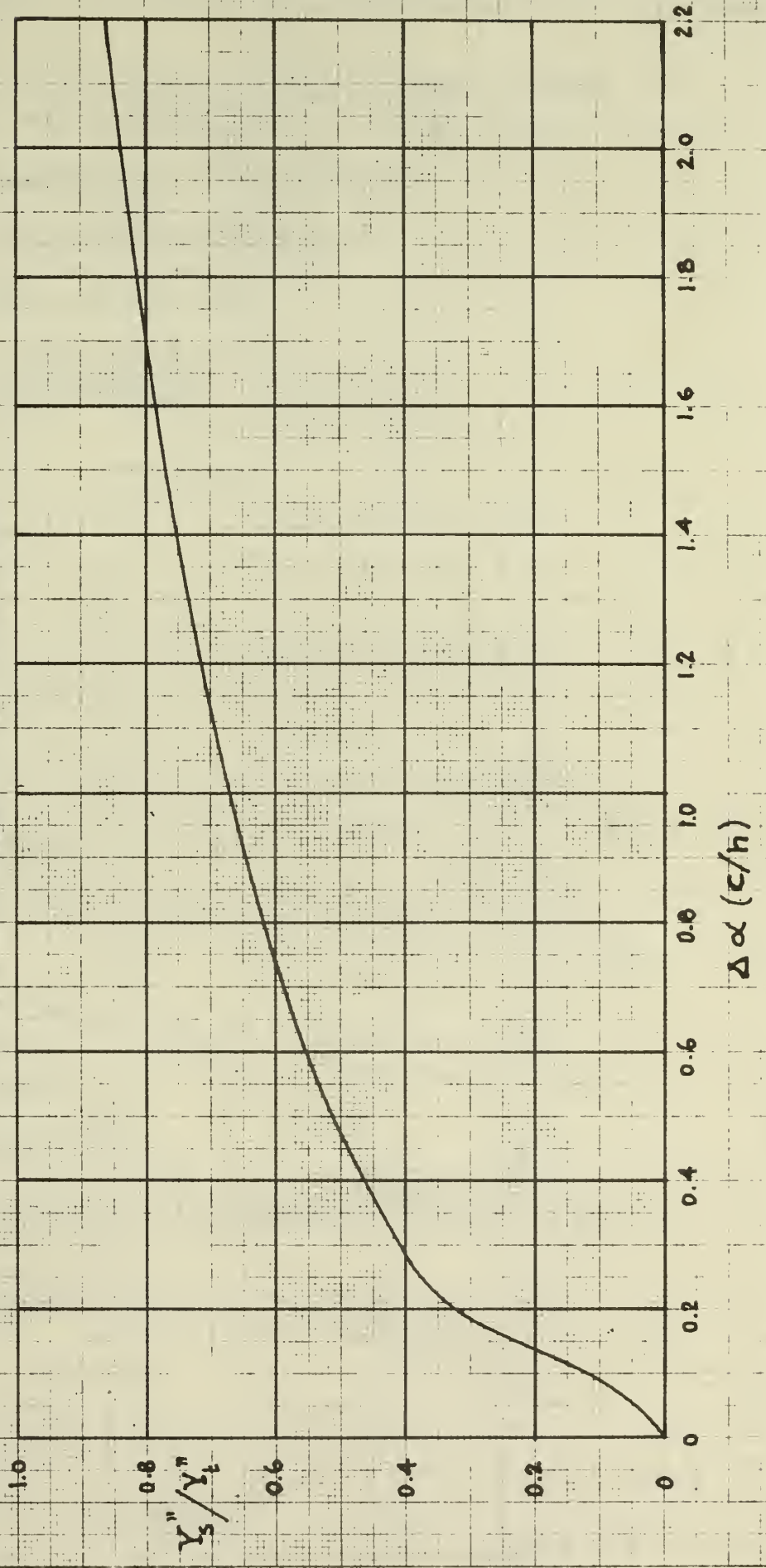
FIG. 7 OVERALL LOSS COEFFICIENTS Y_t', Y_t'' OF FIRST DIFFUSOR ROW

——————— Y_t' WITH SECONDARY FLOW LOSSES OF EQ.26

— — — — Y_t'' WITH SECONDARY FLOW LOSSES FROM FIG.6

$$\Delta\alpha = \alpha_2 - \alpha_3 = 65° - \alpha_3$$

$$\sigma = \frac{\text{BLADE CHORD}}{\text{BLADE SPACING}}$$

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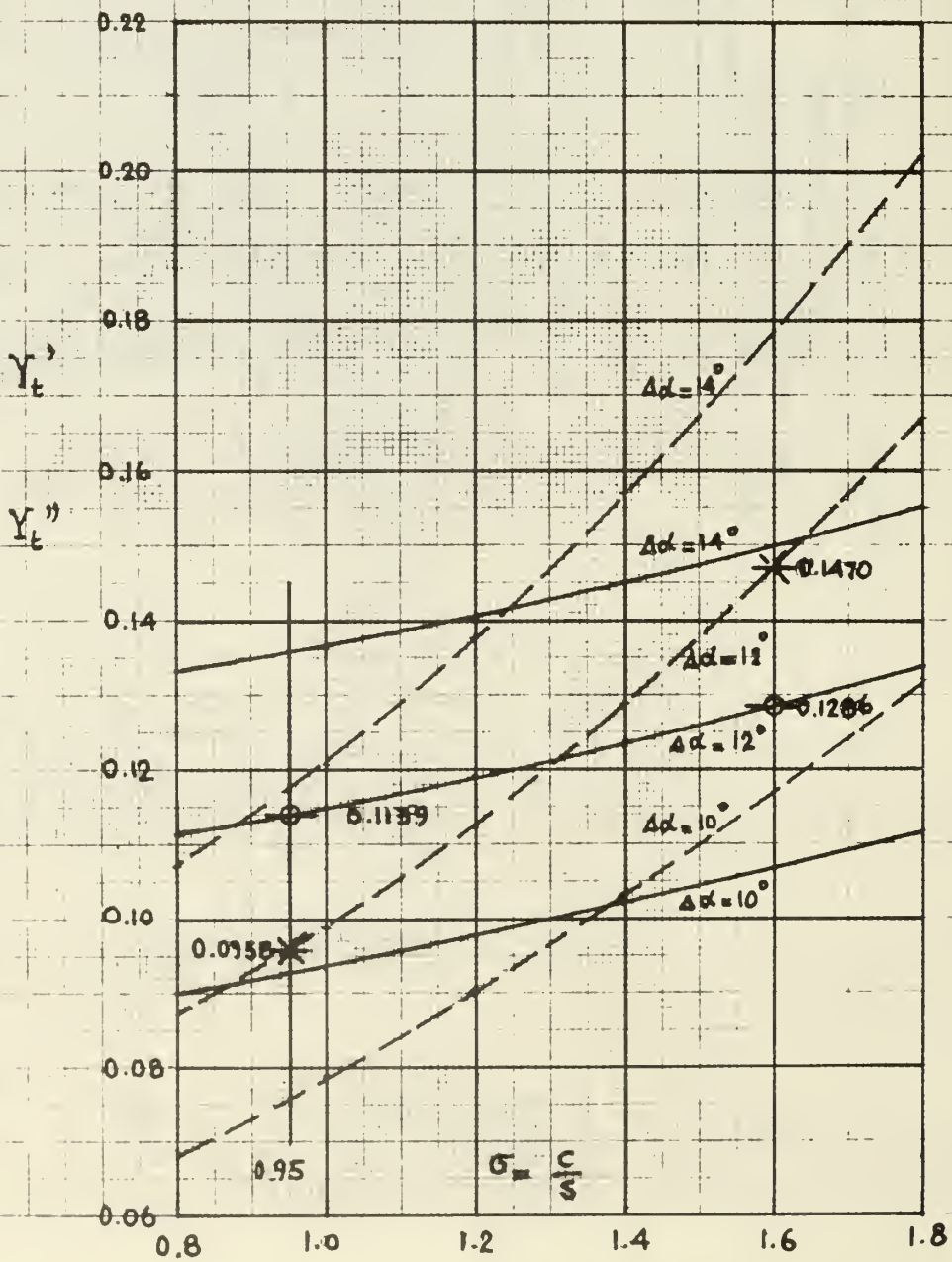
FIG. 8 OVERALL LOSS COEFFICIENTS Y_t', Y_t'' OF SECOND DIFFUSOR ROW

——— Y_t' WITH SECONDARY FLOW LOSSES OF EQ.26

— — — Y_t'' WITH SECONDARY FLOW LOSSES FROM FIG.6

$\Delta\alpha = \alpha_3 - \alpha_4 = 53° - \alpha_4$

$\sigma = \dfrac{\text{BLADE CHORD}}{\text{BLADE SPACING}}$
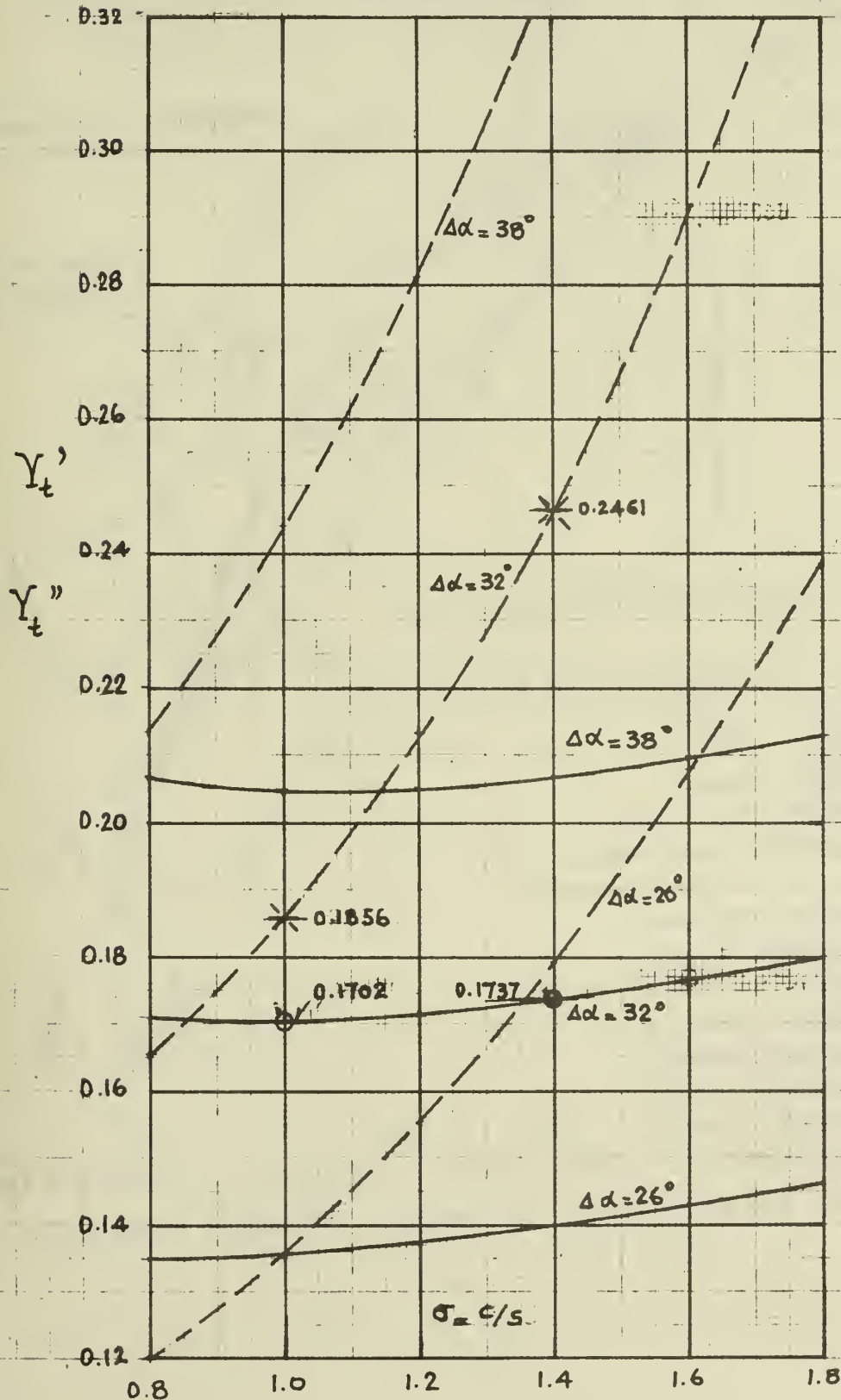
FIG. 9   DIFFUSOR   BLADE   DATA

TANGENT TO CAMBER LINE AT LE

PERIPHERAL DIRECTION

CIRCULAR ARC
CAMBER LINE

TANGENT T
CAMBER LI
AT TE

AXIAL DIRECTION

CHORD LINE FROM LE TO TE

TANGENT TO CONCAVE SIDE OF PROFILE
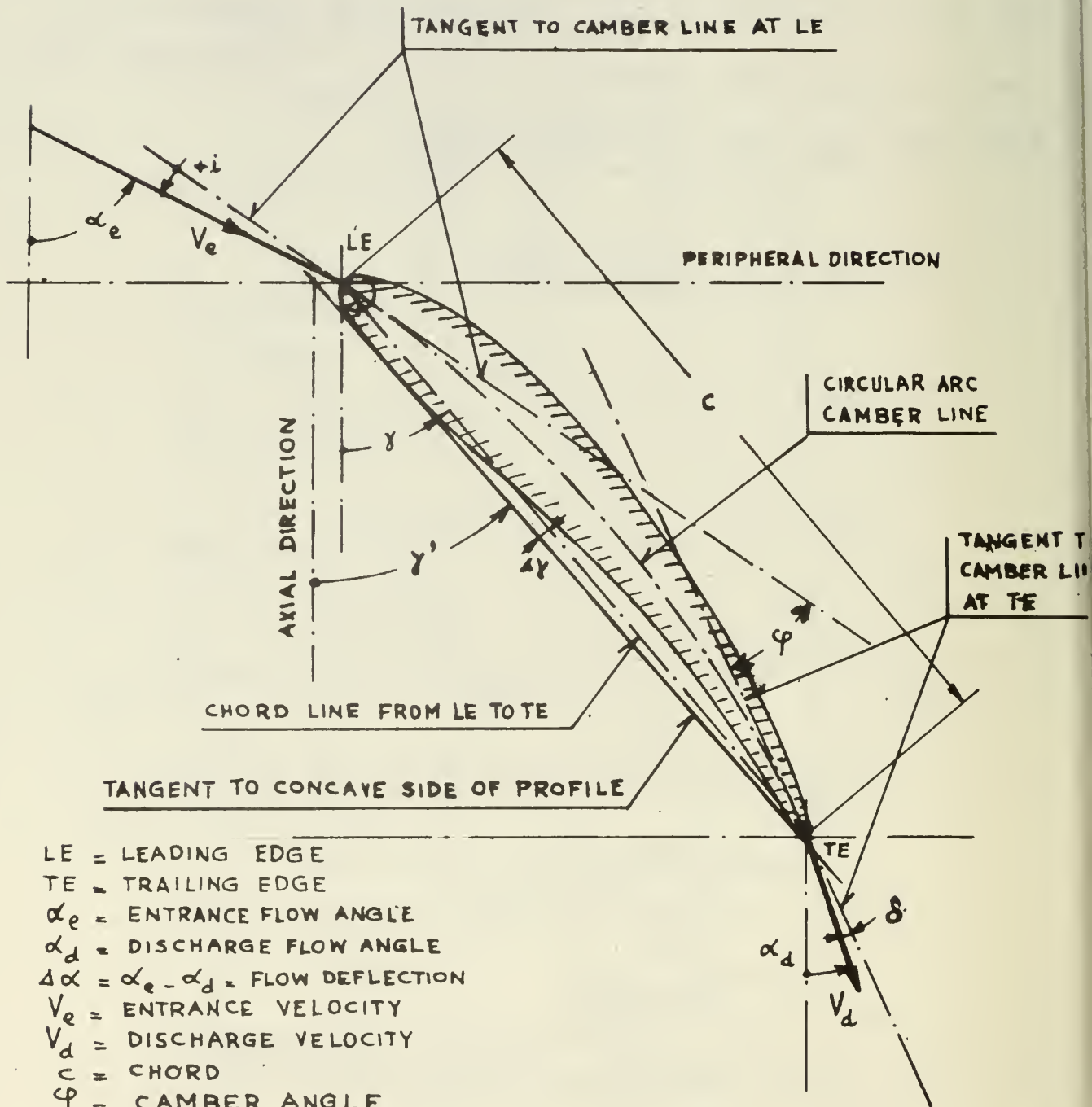
LE = LEADING EDGE
TE = TRAILING EDGE
α_e = ENTRANCE FLOW ANGLE
α_d = DISCHARGE FLOW ANGLE
$\Delta\alpha$ = $\alpha_e - \alpha_d$ = FLOW DEFLECTION
V_e = ENTRANCE VELOCITY
V_d = DISCHARGE VELOCITY
c = CHORD
φ = CAMBER ANGLE
i = INCIDENCE ANGLE
δ = DEVIATION ANGLE
γ = STAGGER ANGLE = $\alpha_e - i - \varphi/2$
$\Delta\gamma$ = ANGLE BETWEEN CHORD LINE AND TANGENT TO CONCAVE PROFILE SIDE
γ' = $\gamma + \Delta\gamma$ = STAGGER ANGLE OF TANGENT TO CONCAVE PROFILE SIDE

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FIG. 10 DETERMINATION OF FLOW CONDITIONS AFTER DIFFUSOR ROW

FIG.10a. MERIDIONAL SECTION

STATION (e) R_2 STATION (d)

FIG. 10b. DEVELOPED CASCADE
AT RADIUS R_2

FIG 10c. PROCESS IN ENTROPY
DIAGRAM

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FIG. 11 CONDITIONS IN FLOW STRAIGHTENER AND DISCHARGE DUCT
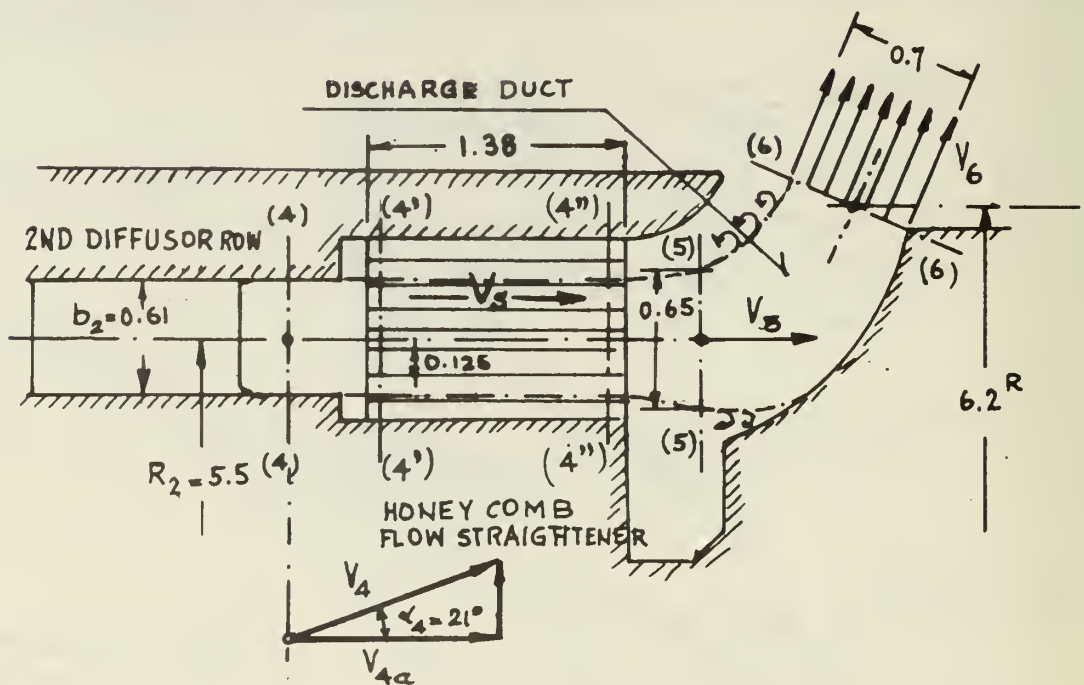
FIG. 11a FLOW STRAIGHTENER AND DISCHARGE DUCT GEOMETRY
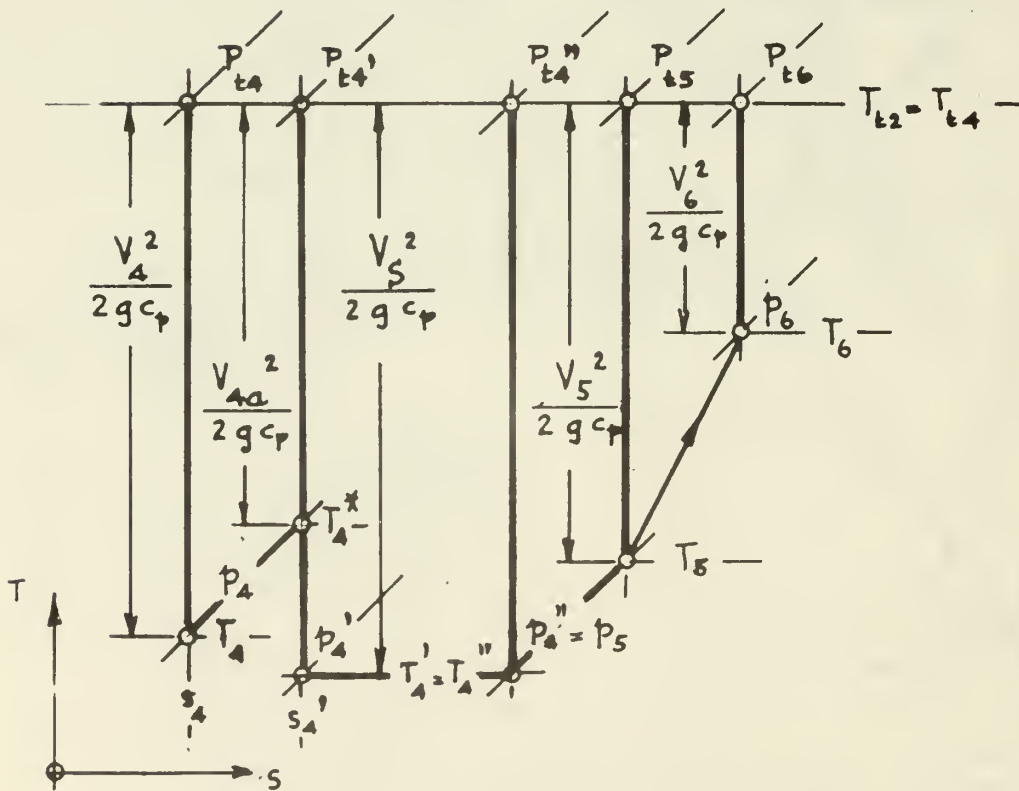
FIG. 11b FLOW PROCESS REPRESENTED IN ENTROPY DIAGRAM

88
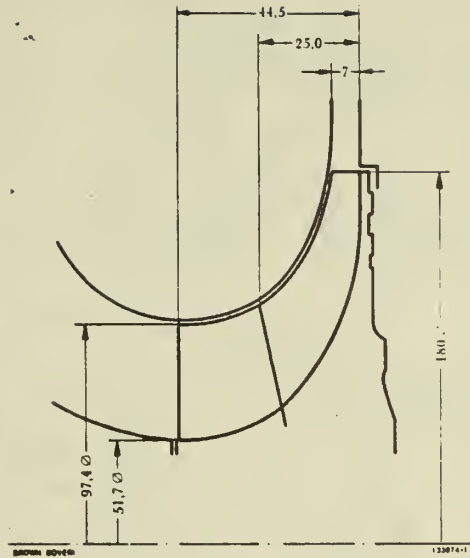
FIG. 12   ROTOR DIMENSIONS

Fig. 12 is identical with Fig. 2 of Ref. 10
(Dimensions are in millimeters)

$$R_{1o}/R_2 = 97.4/180 = 0.541$$

$$R_{1i}/R_2 = 51.7/180 = 0.287$$

$$b_2/R_2 = 7/90 = 0.078$$
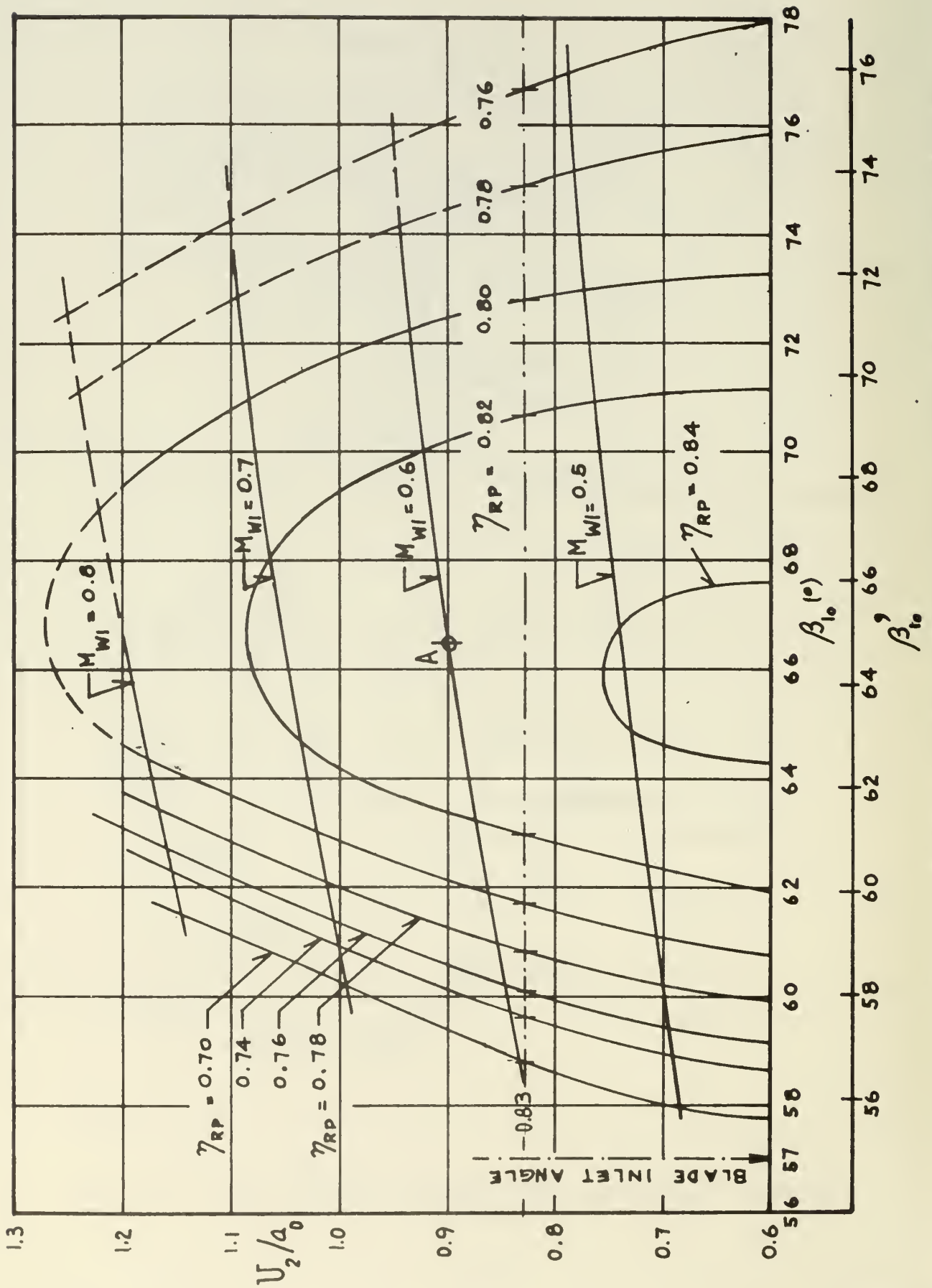
FIG. 13 POLYTROPIC ROTOR EFFICIENCY η_{RP} AS FUNCTION OF FLOW ANGLE β_{1o} AT INDUCER TIP RADIUS AND SPEED RATIO U_2/a_0 (ADAPTED FROM FIG.6 of REF.10)

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FIG. 14. ARC LENGTH OF PARABOLIC MEAN CAMBER LINE OF INDUCER BLADE OF AXIAL LENGTH L AND BLADE ANGLE β_B AT LEADING EDGE LE

PARABOLIC MEAN CAMBER LINE

LINE A-TE = TANGENT TO PARABOLA $y^2 = 2px$ at TE

y-AXIS = TANGENT TO PARABOLA $y^2 = 2px$ at LE
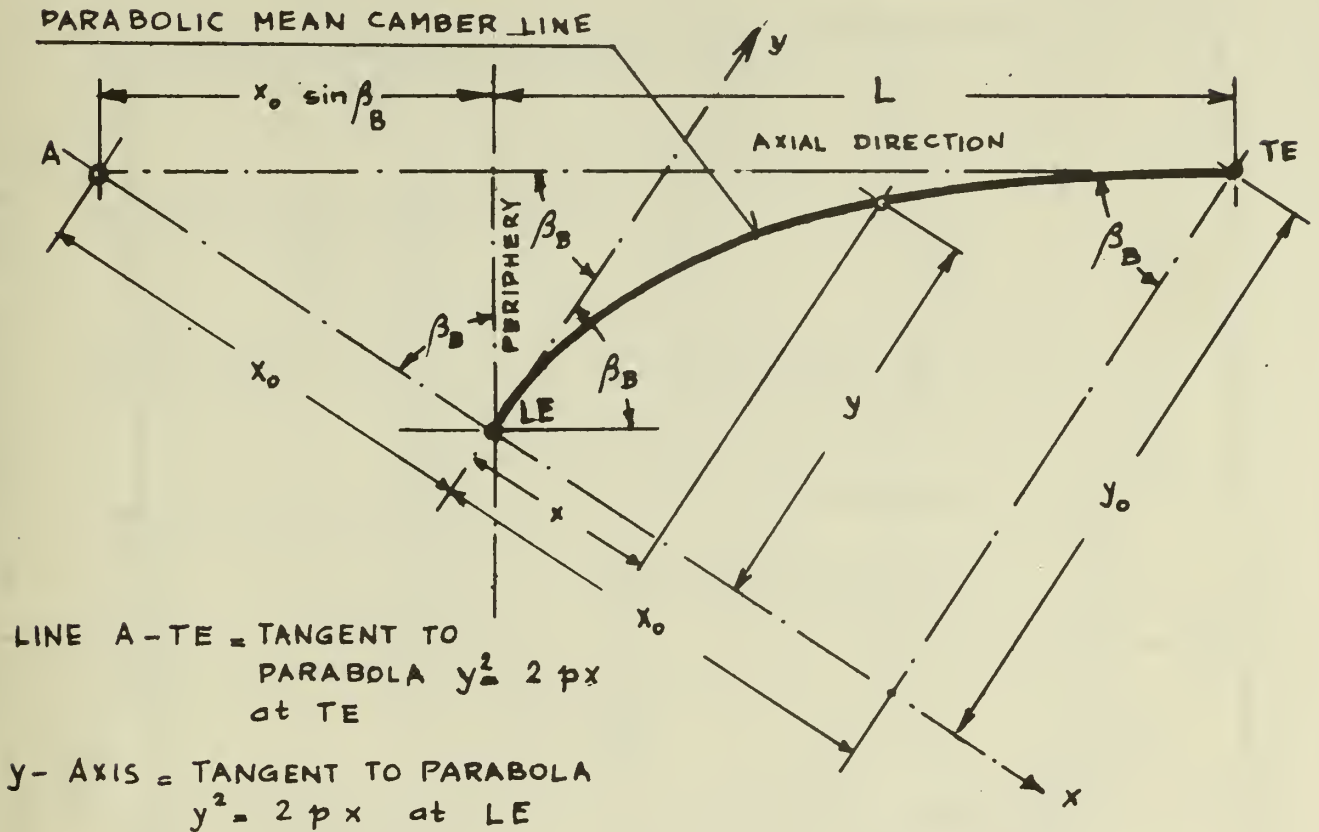
$$\tan \beta_B = \frac{2 x_0}{y_0} \longrightarrow y_0 = 2 x_0 \cot \beta_B$$

$$p = \frac{y_0^2}{2 x_0} = 2 x_0 \cot^2 \beta_B$$

$$(x_0 \sin \beta_B + L) \sin \beta_B = 2 x_0 \longrightarrow x_0 = \frac{L}{(2/\sin \beta_B) - \sin \beta_B}$$

$$p = \frac{2L \cot^2 \beta_B}{(2/\sin \beta_B) - \sin \beta_B}$$

m = ARC LENGTH OF CAMBER LINE FROM LE TO TE

$$m = \frac{p}{2} \left\{ \sqrt{\frac{2 x_0}{p}\left(1 + \frac{2 x_0}{p}\right)} + \ln\left(\sqrt{\frac{2 x_0}{p}} + \sqrt{\left(1 + \frac{2 x_0}{p}\right)}\right) \right\}$$

EXAMPLE : $\beta_B = 57°$, L = 19.5

$x_0 = 12.61$ $y_0 = 16.38$ $p = 10.64$ $m = 21.51$

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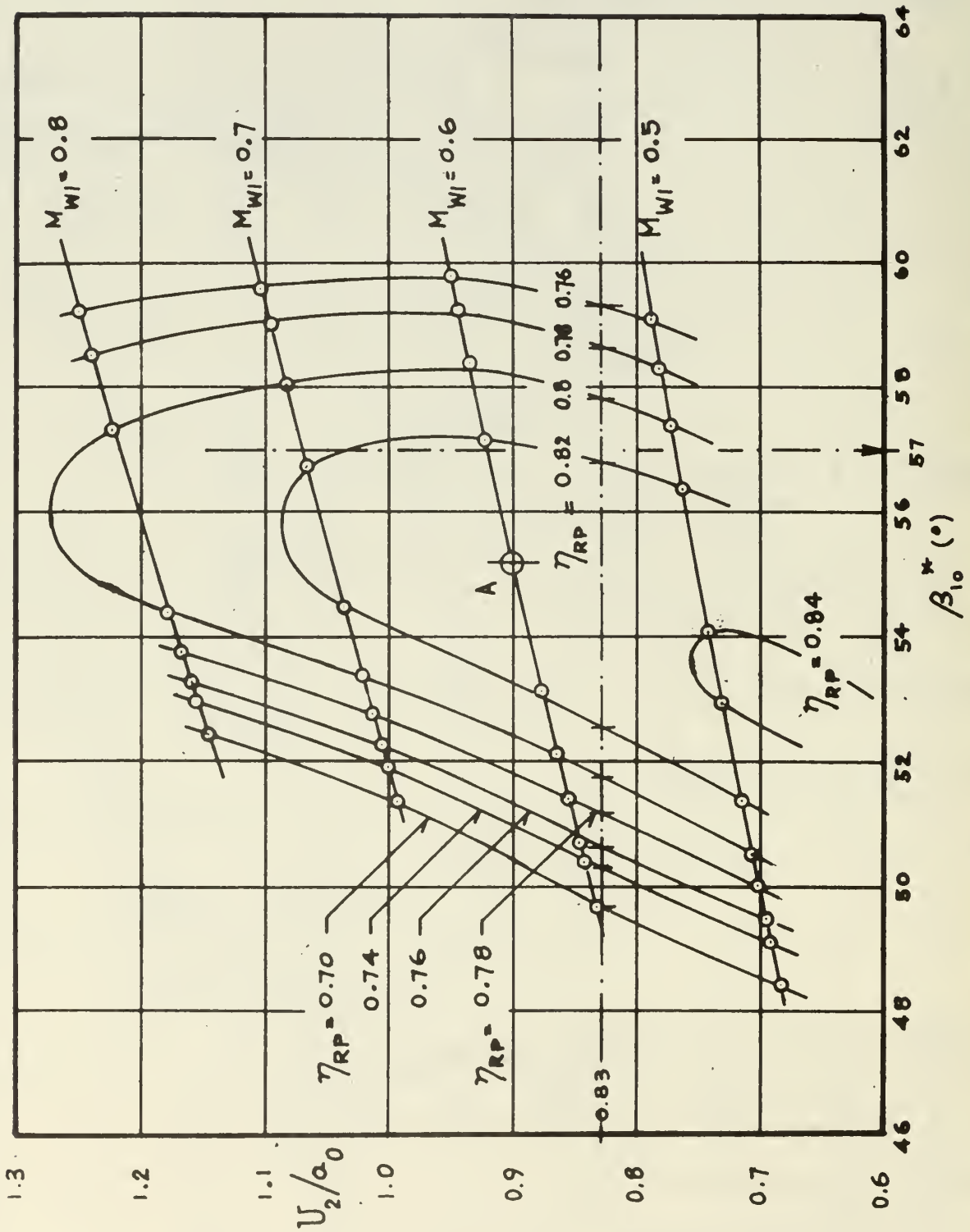
FIG. 15   FLOW ANGLE β_{1o}^* CALCULATED FROM EQ.C(4) FOR VALUES OF U_2/a_0 AND M_{W1}

OF FIG. 13 FOR $R_{1o}/R_2 = 97.4/180 = 0.541$ IN ACCORDANCE WITH FIG. 12

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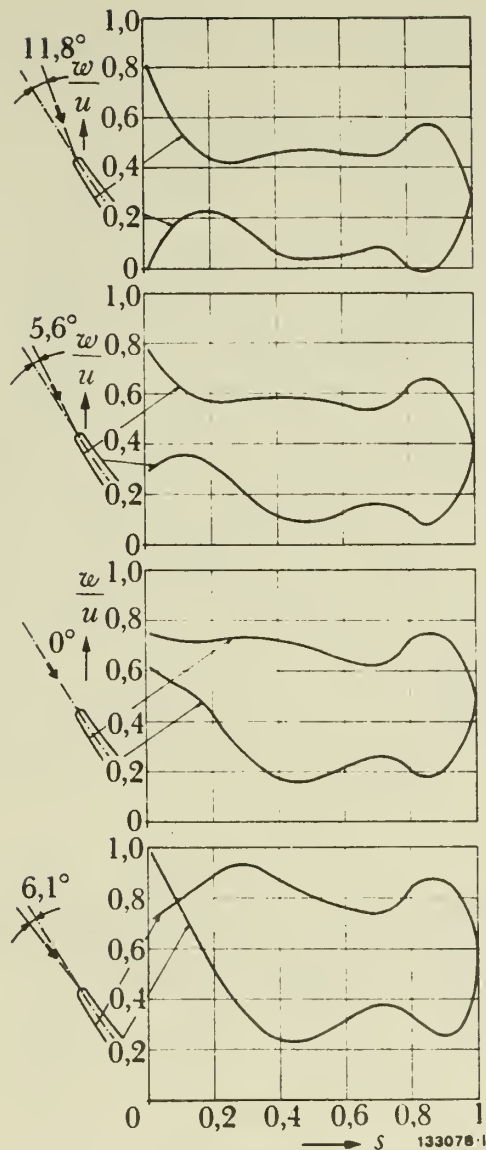
FIG. 16   VELOCITY DISTRIBUTIONS AT INDUCER TIP AT
DIFFERENT INCIDENCE ANGLES

     w = Relative velocity on blade surface

     u = Peripheral speed

     s = Distance along parabolic camber line of inducer

(Fig. 16 is identical with Fig. 5 of Ref. 10 and
presents velocity distributions that are calculated
by ignoring blade thickness, compressibility effects,
and friction)

93
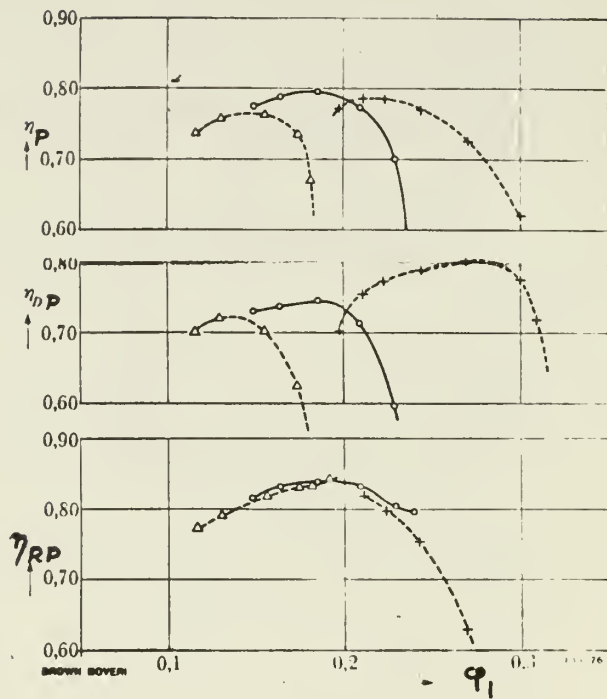
FIG. 17   COMPRESSOR PERFORMANCE AT $U_2/a_0 = 0.83$ OF ROTOR OF
FIG. 12 WITH THREE DIFFERENT DIFFUSORS
(Adapted from Fig. 3 of Ref. 10)

η_{RP} = Polytropic Rotor Efficiency

η_{DP} = Polytropic Diffusor Efficiency

η_P = Polytropic Compressor Efficiency

φ_1 = $Q_1/(U_2\, R_2^2)$

Q_1 = Volume Flow Rate at Inducer Inlet

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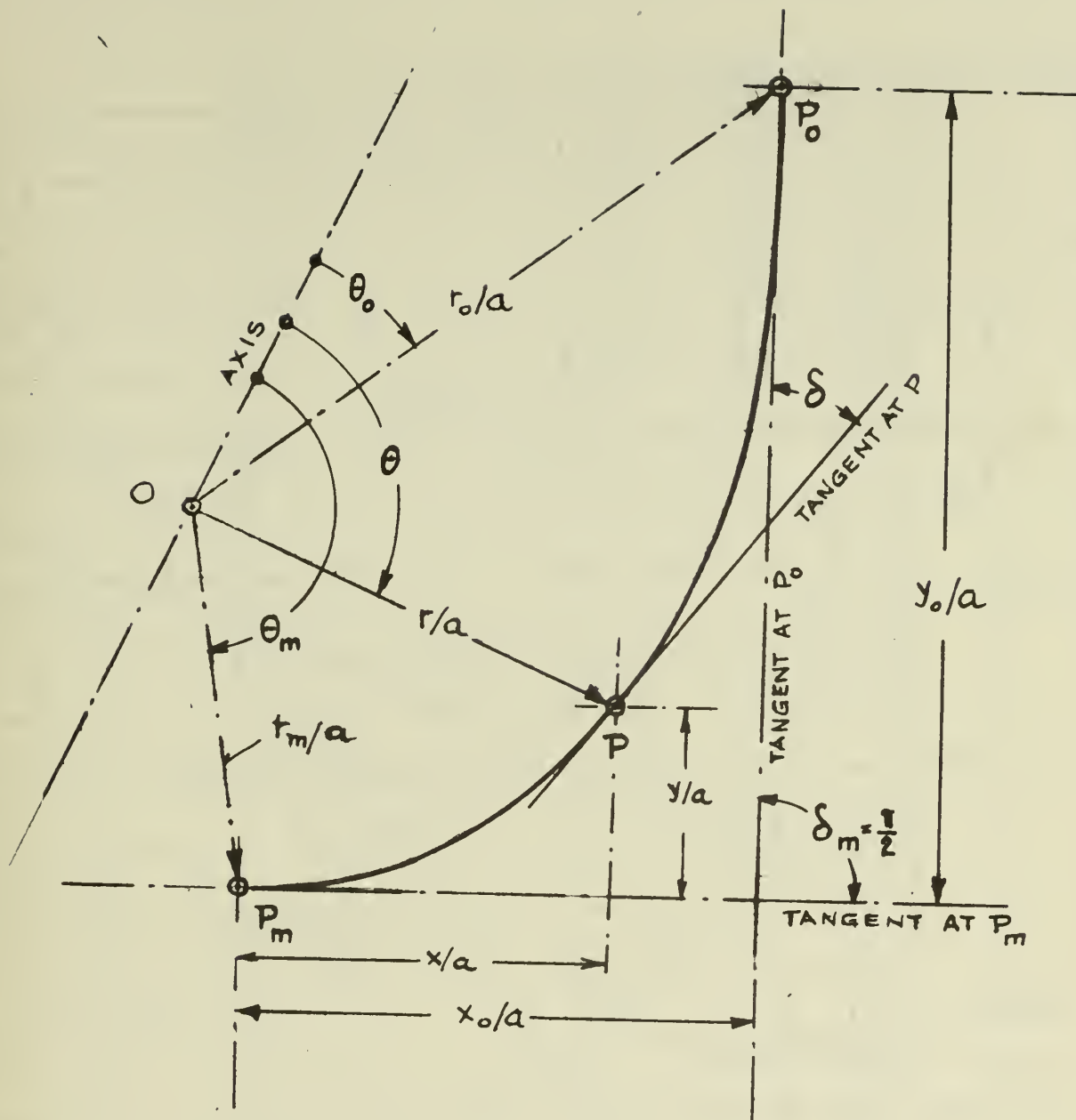
FIG. 18 MERIDIAN CURVE $r/a = \theta^{-b}$ with $\delta_m = \pi/2$

95
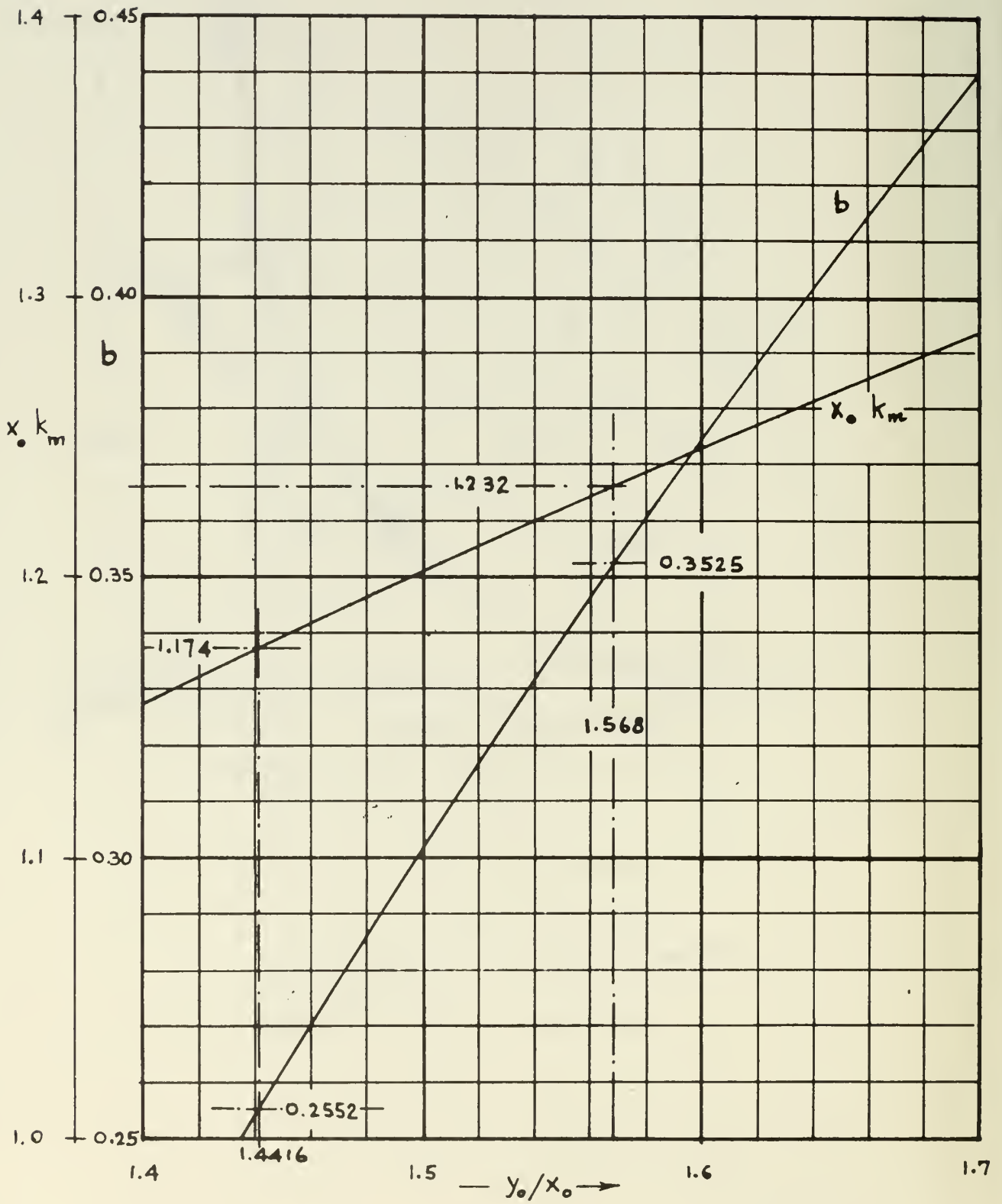
FIG. 19 RELATIONSHIP BETWEEN y_o/x_o, $x_o k_m$ AND y_o/x_o FOR MERIDIAN CURVE
OF FIG. 18 CALCULATED WITH PROGRAM No. 110 OF APPENDIX D
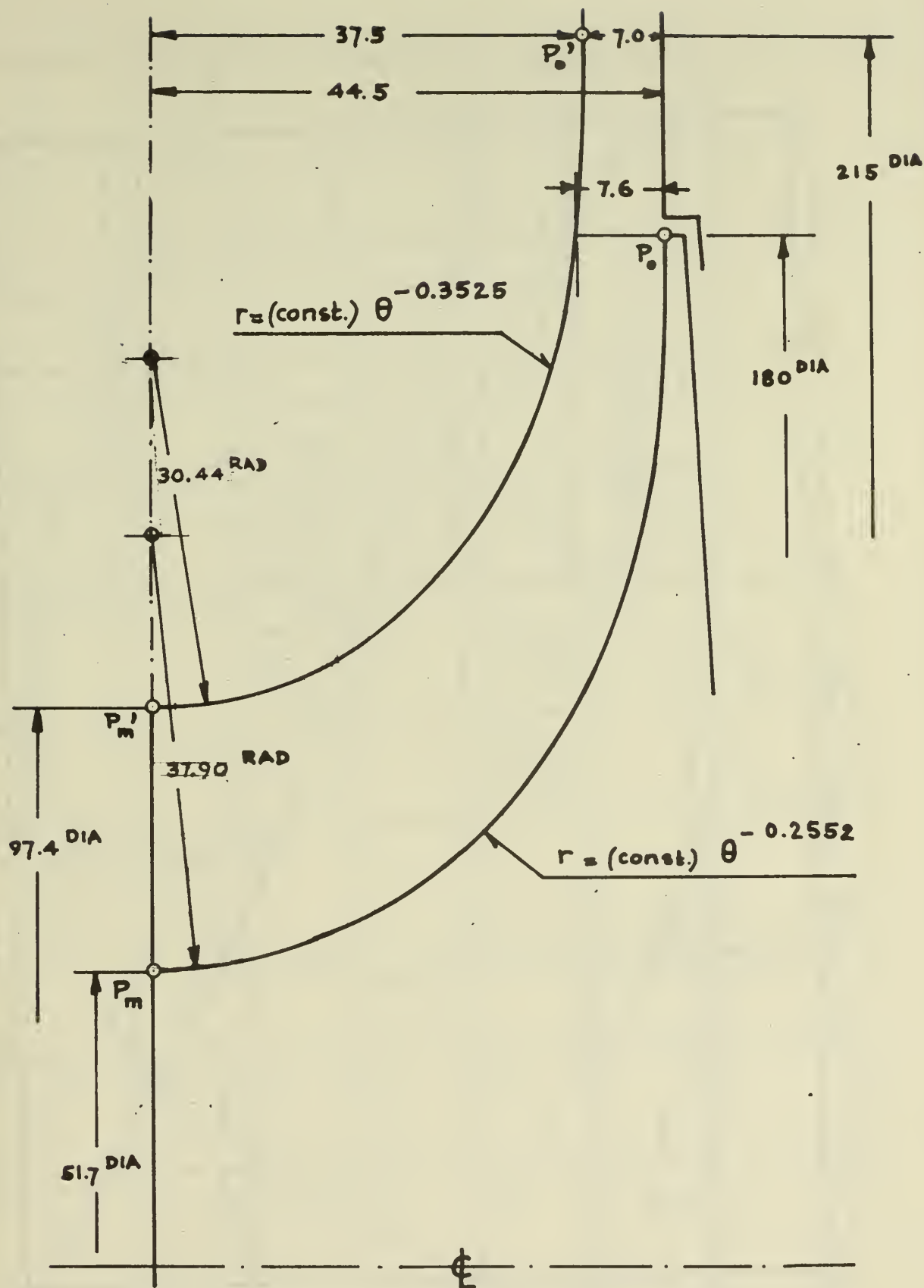
FIG. 20 SCALE DRAWING (2:1) OF MERIDIAN CONTOURS WITH $r/a = \theta^{-b}$ OF IMPELLER
OF FIG. 12 THROUGH POINTS P_o, P_m, P_o', P_m'.
(Dimensions are in Millimeters)

M.H.V. 3/15/72
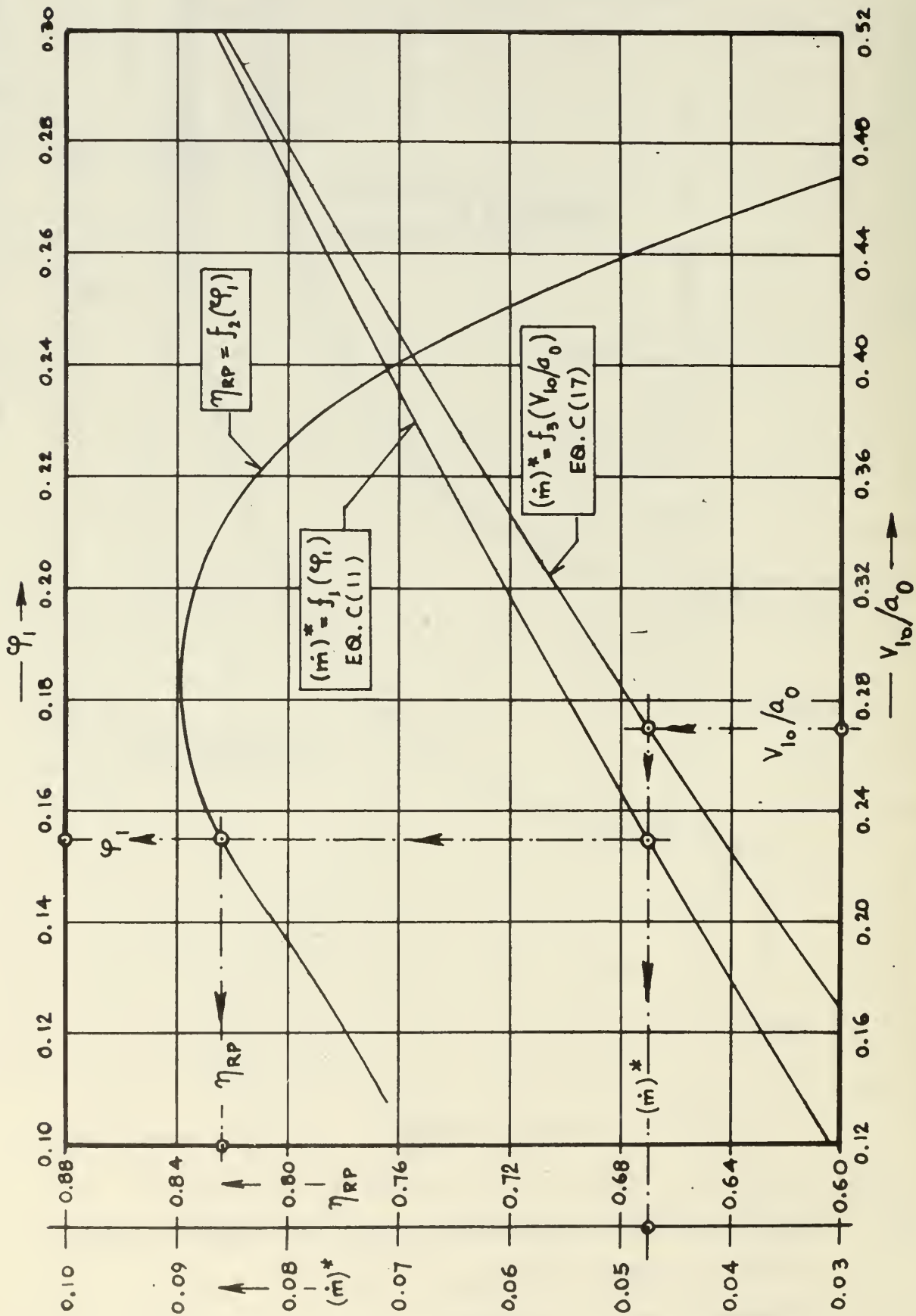
FIG. 21 DIMENSIONLESS MASS FLOW RATE $(\dot{m})^*$ AS FUNCTIONS OF FLOW FUNCTION φ_1 OF FIG. 17, AND V_{1o}/a_0 CALCULATED FROM EQ. C(17), WITH POLYTROPIC ROTOR EFFICIENCY η_{RP} FROM FIG. 17 FOR $U/a_0 = 0.83$.

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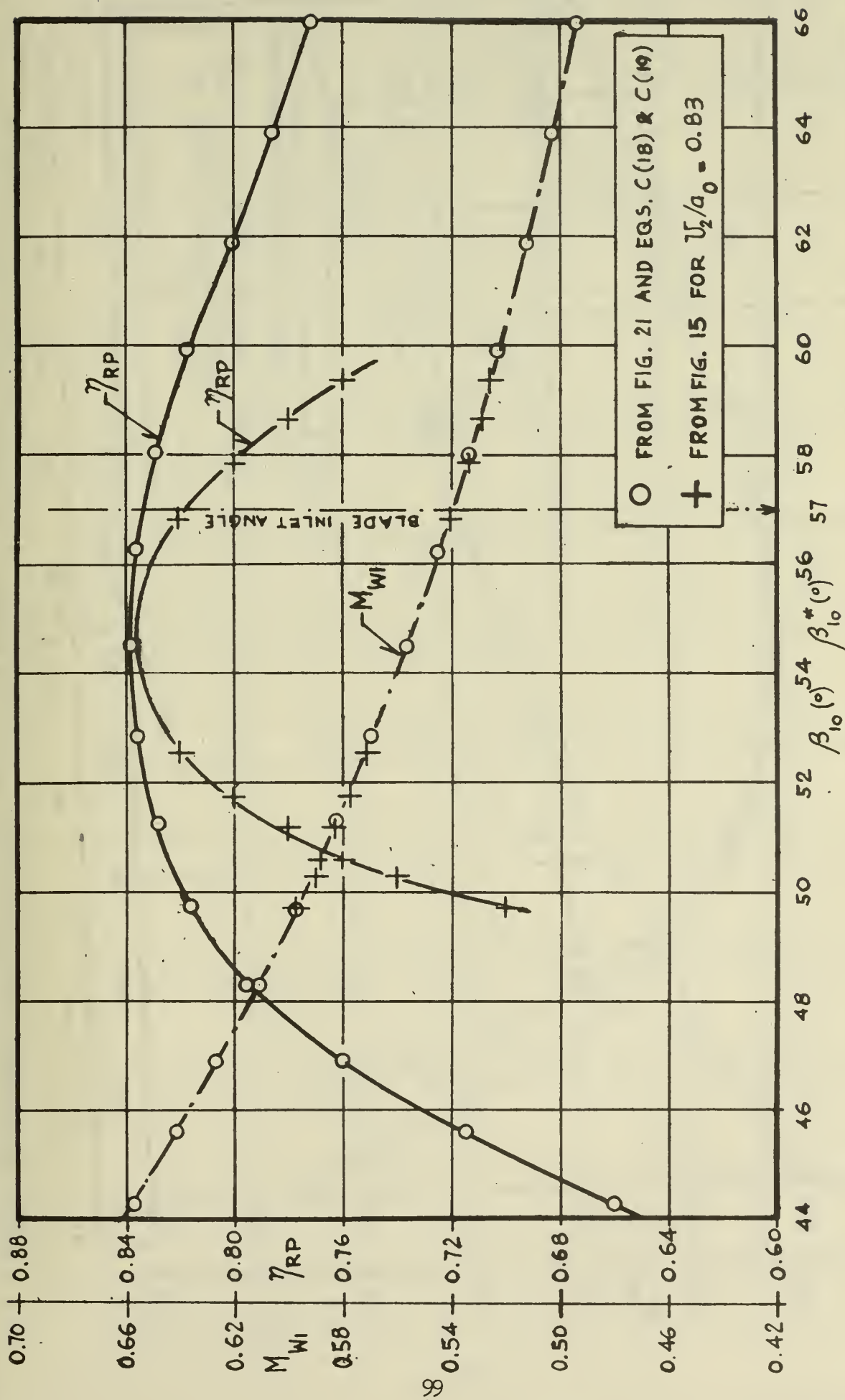
FIG. 22: POLYTROPIC ROTOR EFFICIENCY η_{RP} AND MACH NUMBER M_{W1} FROM FIGS. 21 AND 15, AS FUNCTIONS

OF FLOW ANGLE β_{1o}, FOR $U_2/a_0 = 0.83$
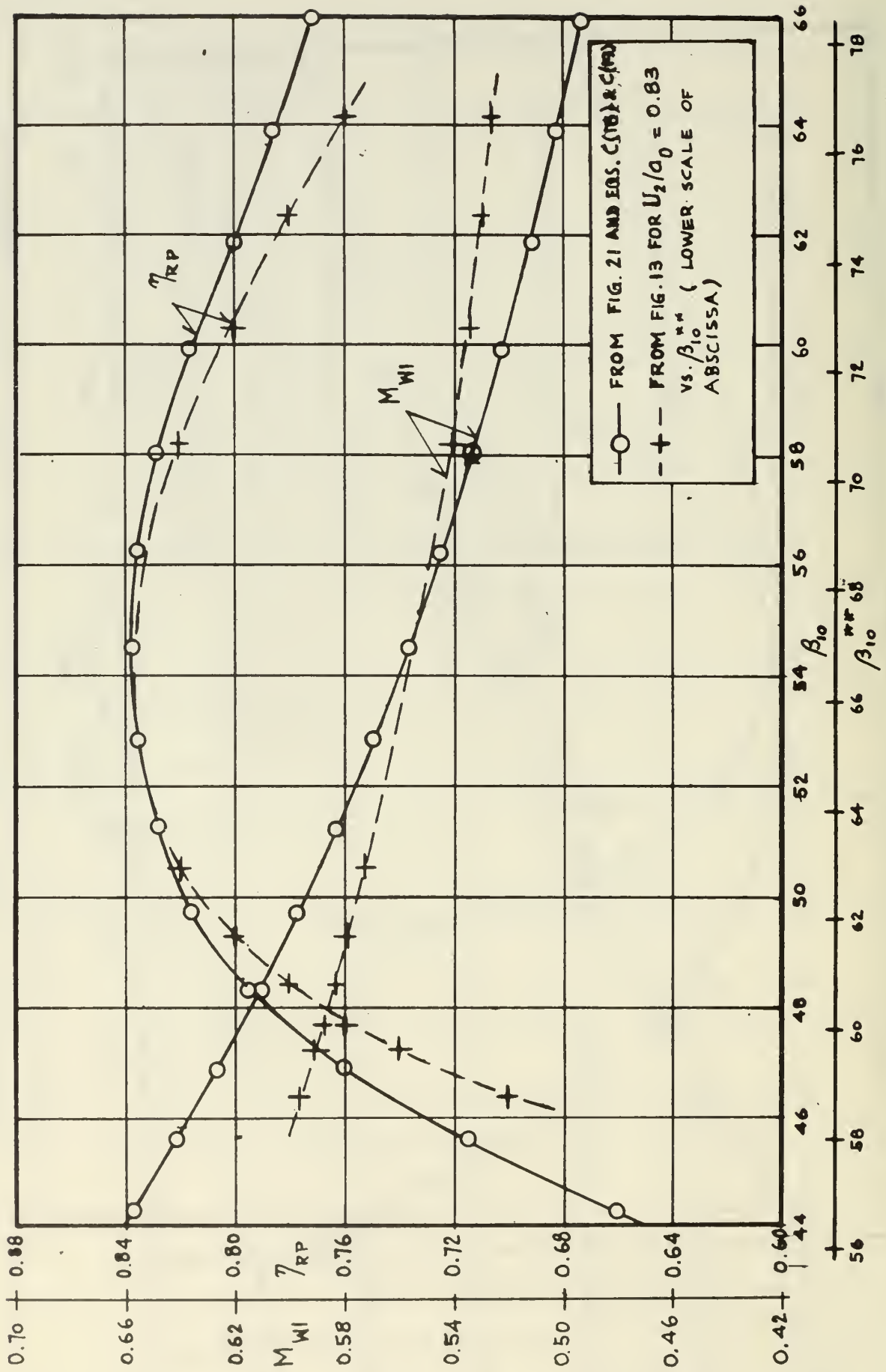
FIG. 23 POLYTROPIC ROTOR EFFICIENCY η_{RP} AND MACH NUMBER M_{W1} AS FUNCTION OF FLOW ANGLE FROM FIG. 21 (UPPER SCALE FOR β_{1o}) AND FIG. 13 FOR $U_2/a_0 = 0.83$ (LOWER SCALE FOR β_{1o}^{**})
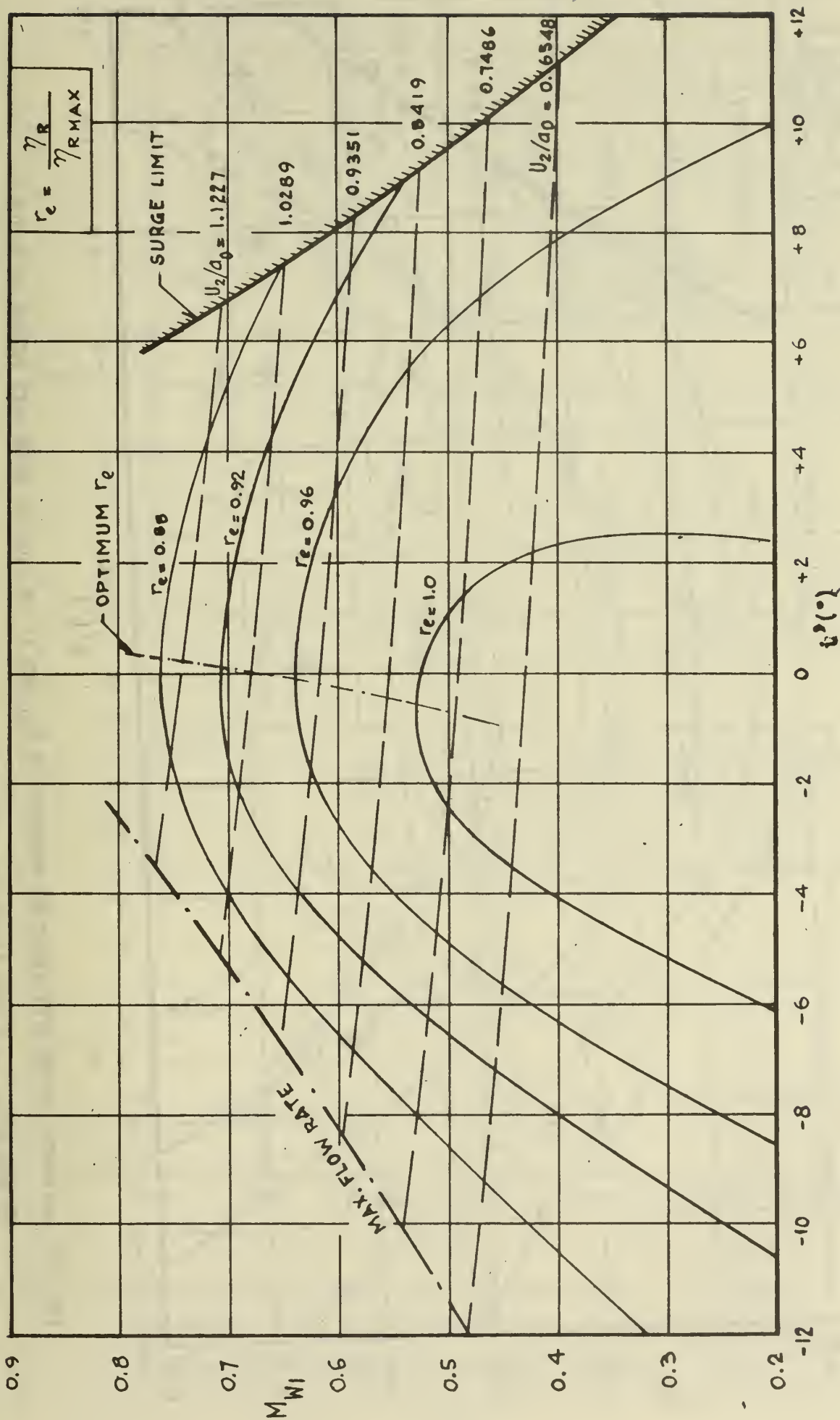
FIG. 24 ADIABATIC ROTOR EFFICIENCY η_R AS FUNCTION OF MACH NUMBER M_{W1}, PERIPHERAL SPEED RATIO U_2/a_0, AND INCIDENCE ANGLE i' (ADAPTED FROM FIG. 23b OF REF. 2)

--- Curves for U_2/a_0 = constant

η_{RMAX} = Maximum Adiabatic Rotor Efficiency

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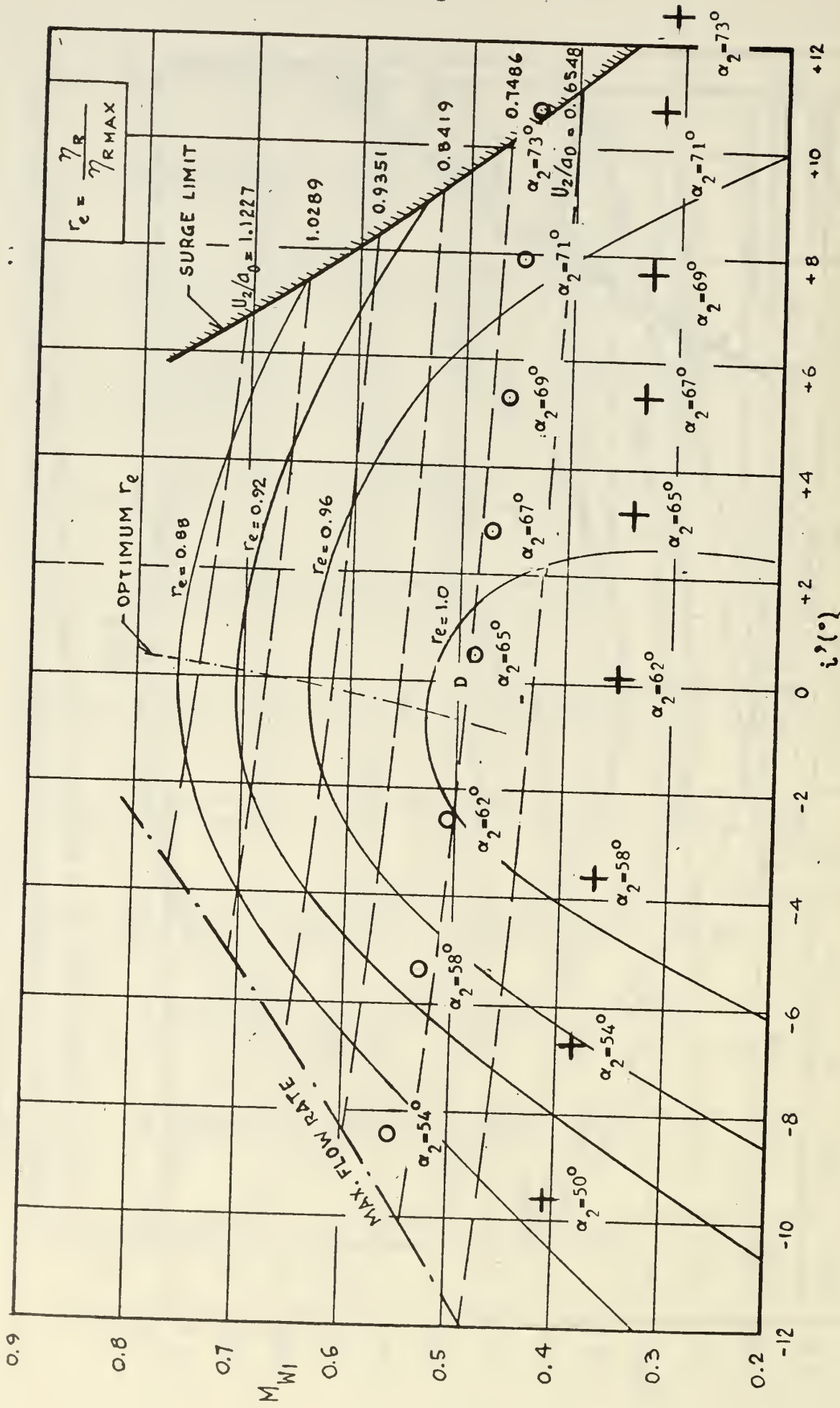
FIG. 25 ADIABATIC ROTOR EFFICIENCY AS FUNCTION OF M_{W1} AND i' OF FIG. 24 WITH DATA POINTS OF TABLE X

⊙ FOR U_2/a_0 = 0.7156 (TABLE X, SHEET 1)

+ FOR U_2/a_0 = 0.516 (TABLE X, SHEET 2)

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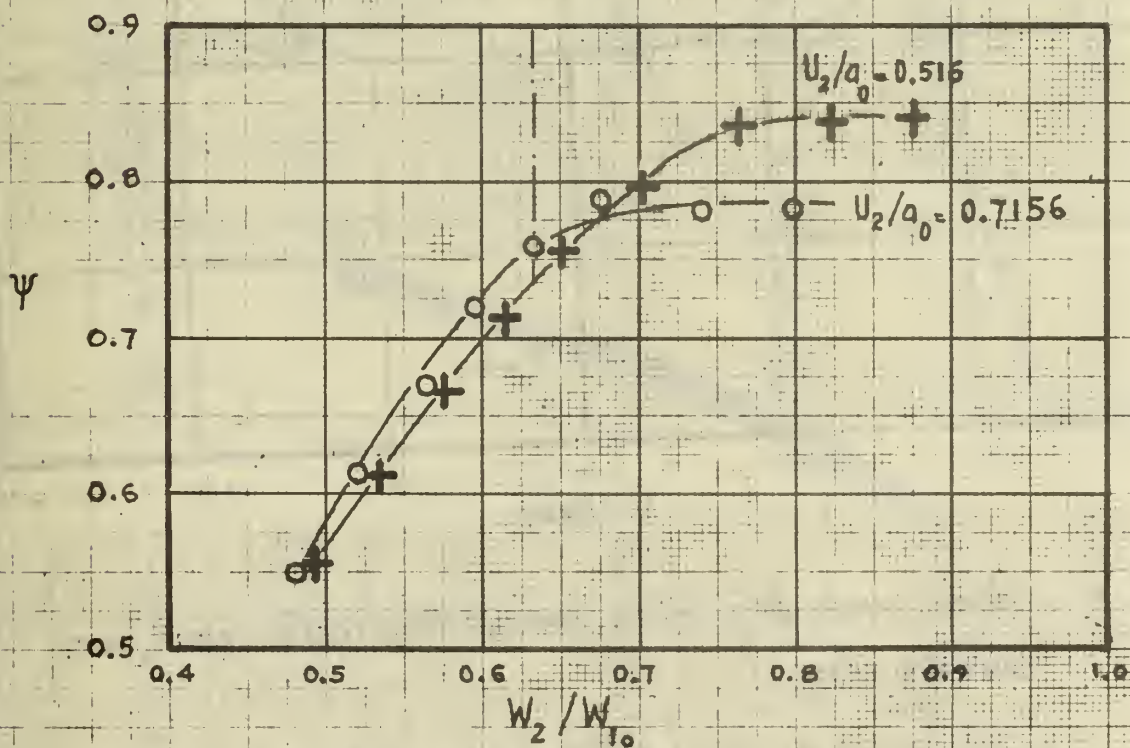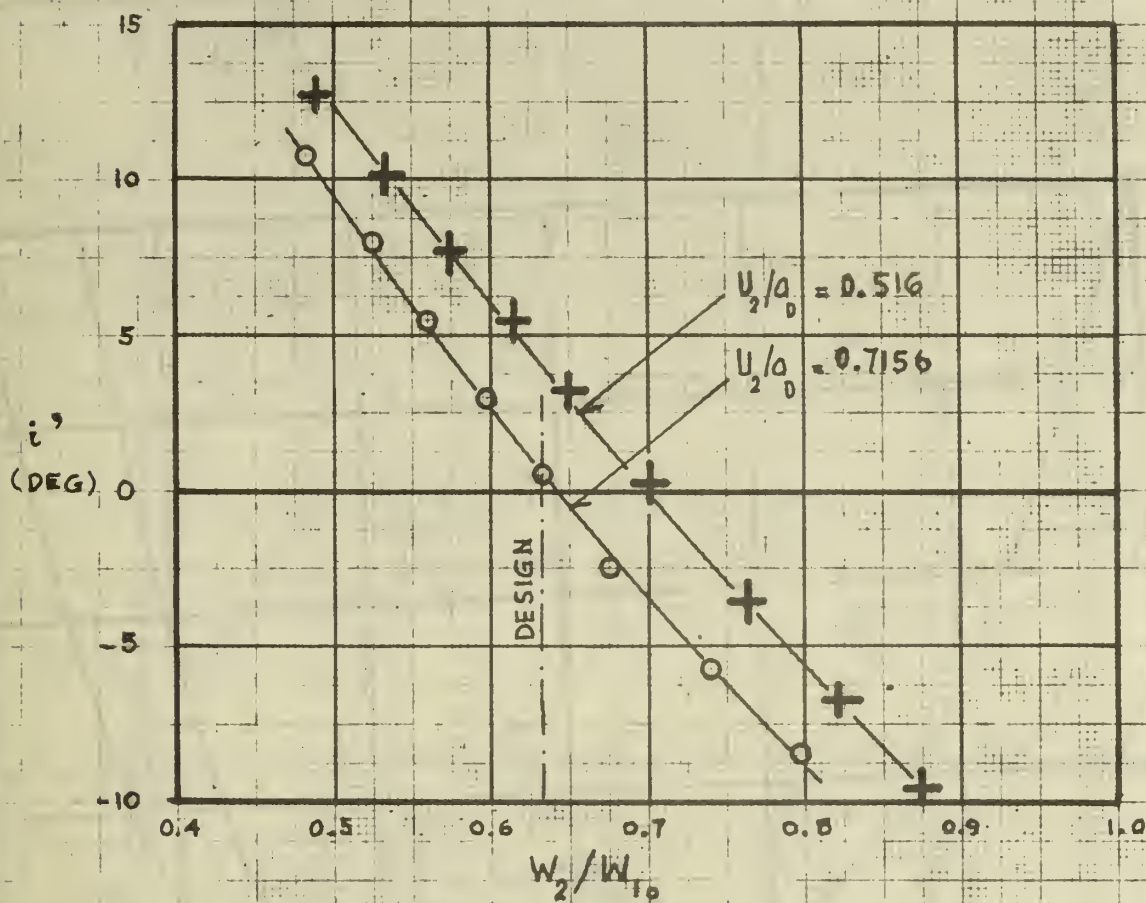
FIG. 26 VELOCITY COEFFICIENT Ψ AND INCIDENCE ANGLE i' OF HYBRID
COMPRESSOR ROTOR AS FUNCTION OF DECELERATION RATIO W_2/W_{T_0}
OF RELATIVE VELOCITIES FROM DATA OF TABLE X
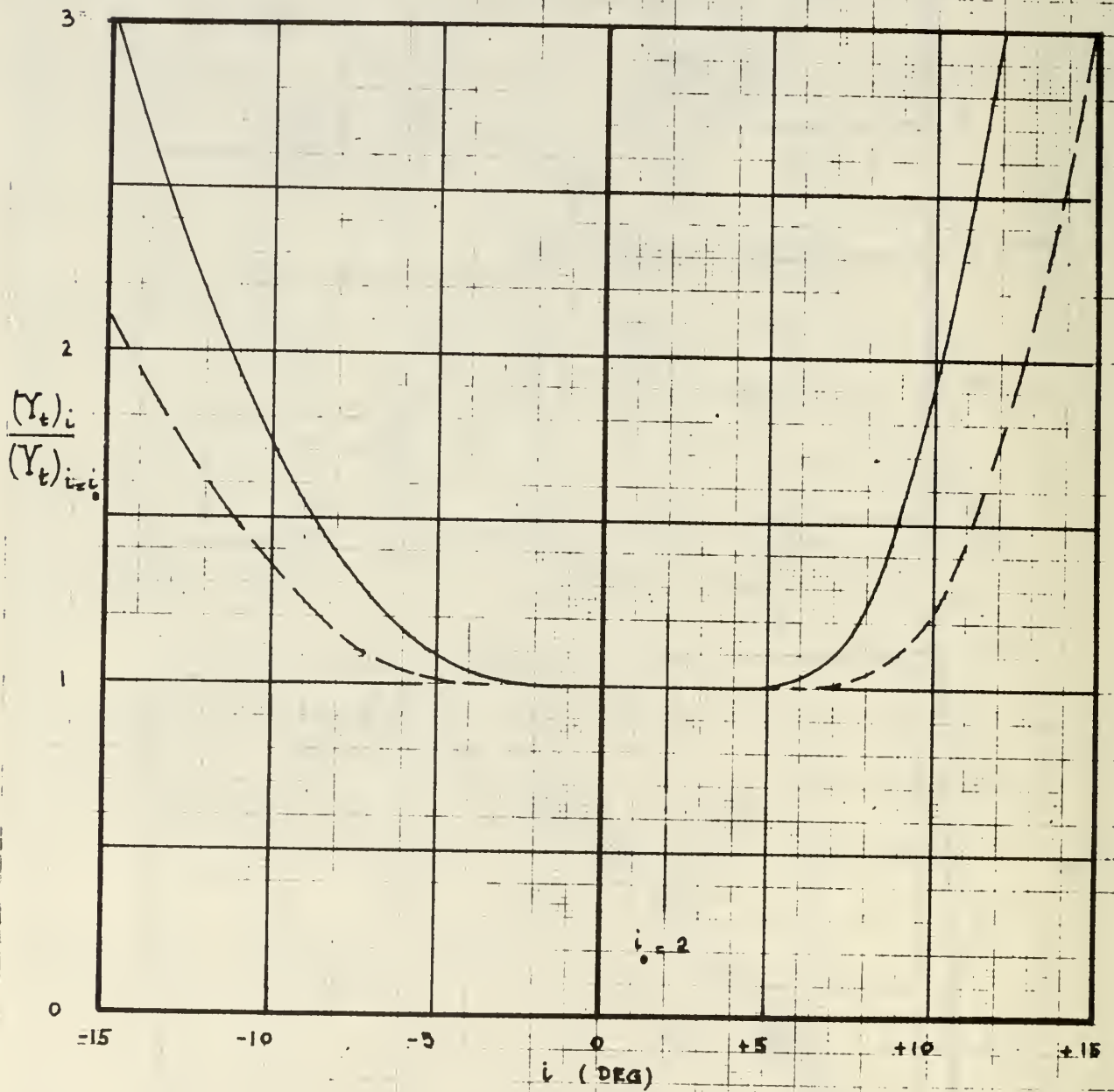
FIG. 27 ASSUMED CHANGE OF DIFFUSOR PRESSURE LOSS COEFFICIENT Y_t WITH INCIDENCE ANGLE i

——— $U_2/a_0 = 0.7156$; $0.641 \leq M_{V2} \leq 0.672$

— · — $U_2/a_0 = 0.516$; $0.472 \leq M_{V2} \leq 0.504$

P_{t4}/P_0 = Pressure Ratio; HP = Drive Power; η_T = Total-Total Efficiency; $\dot{w}$ = Flow Rate; N = Speed

$\dot{w}$ (LBM/S)

YA. 7/5/73

N = 16,666 RPM
N = 12,018 RPM

η_T

η_T

P_{t4}/P_0

HP

$\alpha_2 = 65°$

$\alpha_2 = 65°$

HP

P_{t4}/P_0

SURGE LIMIT

P_{t4}/P_0

η_T

HP

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FIG. 29 PREDICTED PERFORMANCE OF DRIVE TURBINE

HP = Power (HP) δ_T = $P_{to}/14.7$
$\dot{w}$ = Flow Rate (lbm/s) θ_T = $T_{to}/518.4$
N = Speed (rpm)
T_{to} = Turbine Inlet Total Temperature (°R)
P_{to} = Turbine Inlet Total Pressure (psia)
p_2 = Turbine Discharge Static Pressure (psia)
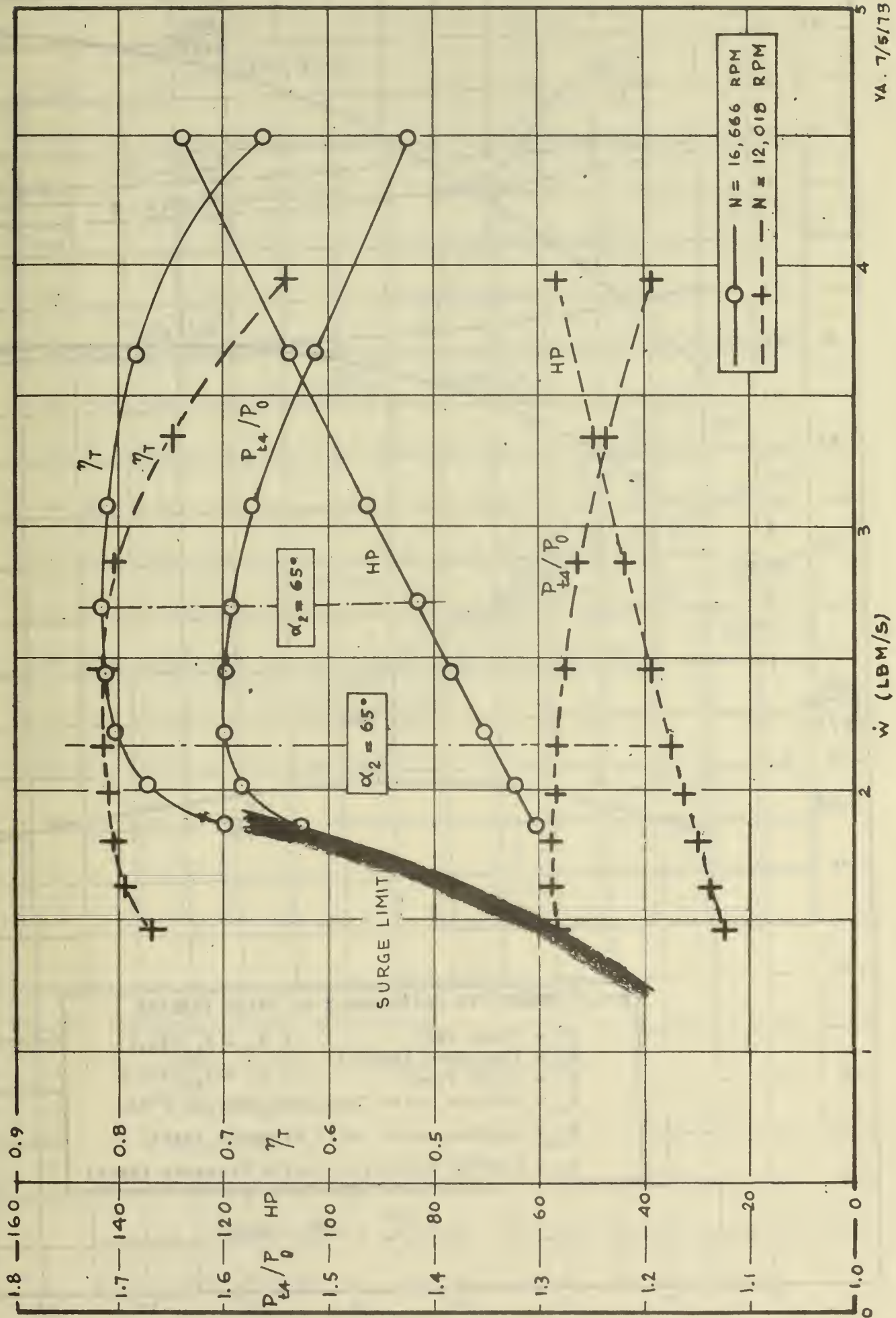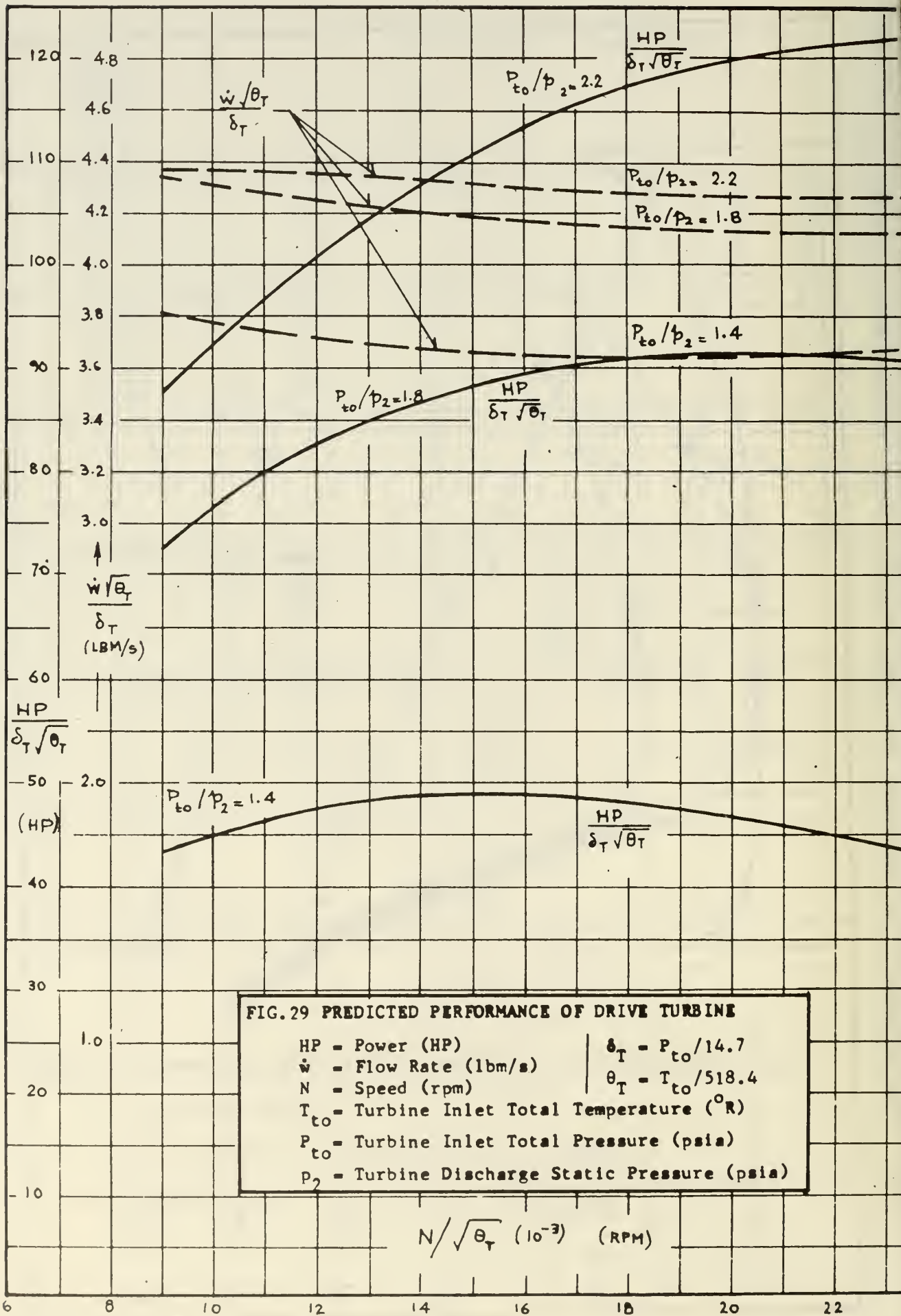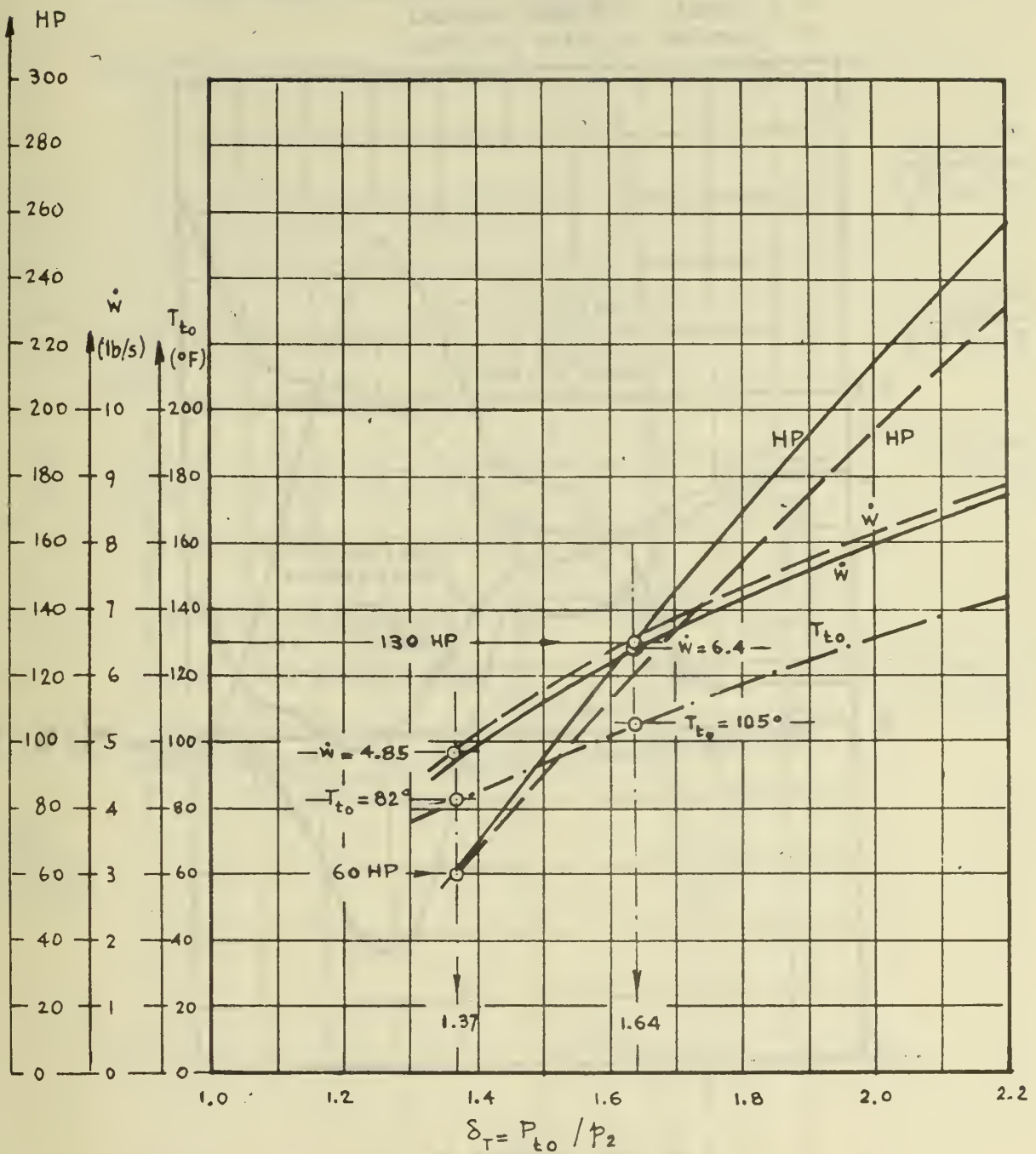
FIG. 30 PREDICTED TURBINE PERFORMANCE

$\delta_T = P_{to}/p_2$ = Total-to-Static Pressure Ratio

$\dot{w}$ = Flow Rate (lbm/s)

HP = Horse Power

T_{to} = Turbine Inlet Temperature ($^\circ$F)

—— N = 16,666 rpm

– – – N = 12,018 rpm

FIG. 31 STRESS DISTRIBUTION IN HYBRID ROTOR
(Method of Schilhansl, Ref. 17)

σ_{RADIAL} = Radial Stress; σ_{HOOP} = Tangential Stress

ρ = Density of Blade Material
ω = Angular Velocity of Rotor
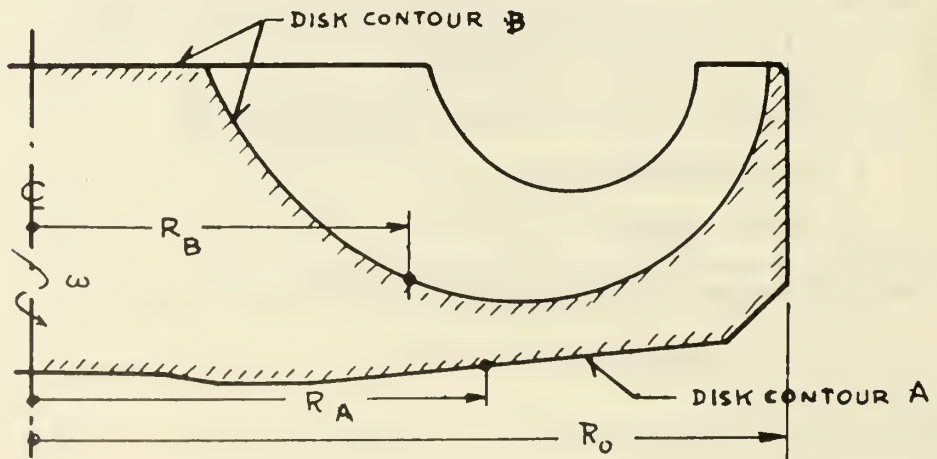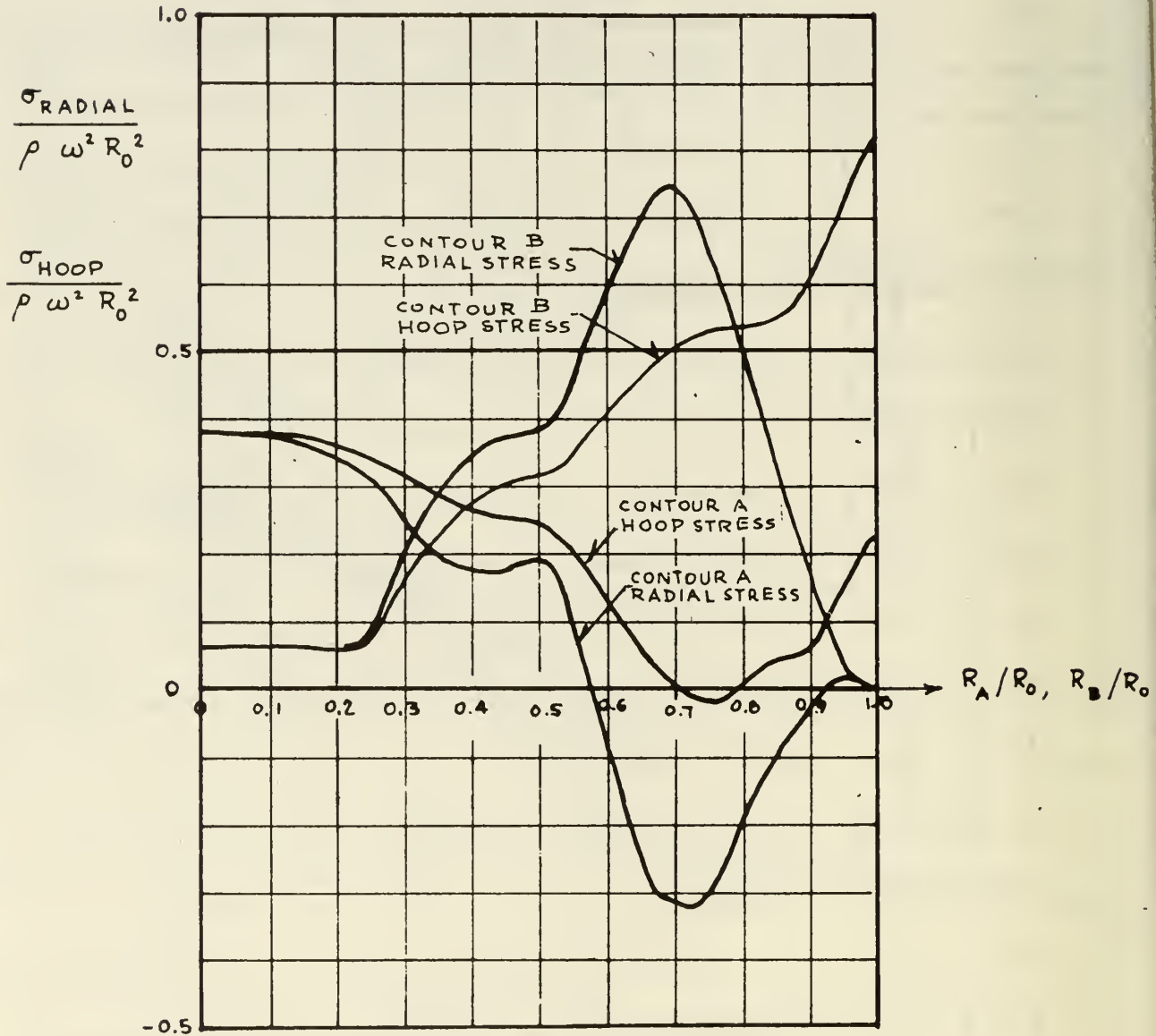
FIG. 32 BLADE STRESSES OF HYBRID ROTOR

(Method of Schilhansl, Ref. 17)

σ_B = Blade Stress

(For other symbols, see Fig. 31)
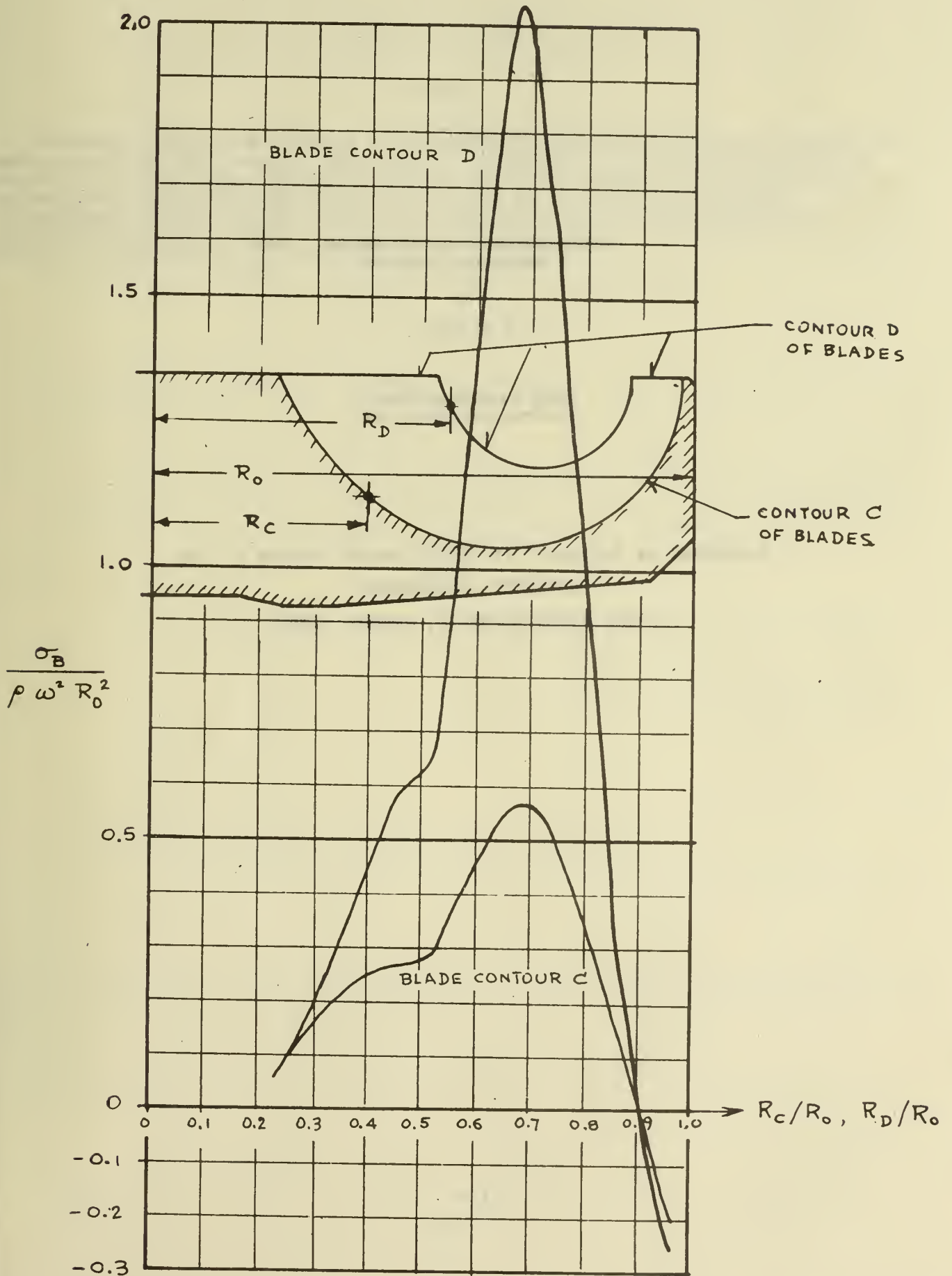
APPENDIX A

BASIC ELEMENTS FOR ADVANCED DESIGNS
OF RADIAL-FLOW COMPRESSORS

by

M. H. Vavra

Naval Postgraduate School
Monterey, California 93940

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SUMMARY

Dimensionless parameters are presented for the design of compressors with axial inlet velocities and radial blades at the rotor discharge. These parameters take account of the compressibility of the flow and hold for arbitrary fluids. They permit to evaluate the effect of changes of the design variables on the conditions of state of the fluid at different locations, and on the geometry of the design. Loss relationships are discussed and their effects on performance are shown. The design parameters are compared with the so-called specific speed criteria to show that the latter do not satisfy the laws of similarity if compressibility effects are taken into account.

BASIC ELEMENTS FOR ADVANCED
DESIGN OF RADIAL-FLOW COMPRESSORS

M. H. Vavra

1. INTRODUCTION

Under consideration are high-speed centrifugal compressors with rotors of the type shown in Fig. 1 that have radial blades at the discharge and where the absolute inlet velocities are in axial direction. With a straight annular inlet duct these inlet velocities will be uniform between the radii R_{1i} and R_{1o} of the impeller eye. For a particular relative flow angle β_{1o} and the relative velocity W_{1o} at R_{1o}, there is then known the peripheral speed U_{1o}, which, for chosen radius ratios R_2/R_{1o}, establishes the peripheral rotor speed U_2 at R_2. The average relative velocity W_2 at the discharge of a rotor with radial blades is not radial, but has an average angle β_2. With the slip factor μ there is

$$\beta_2 = \tan^{-1} \frac{(1-\mu)\ U_2}{V_{m2}} \tag{1}$$

where V_{m2} is the average meridional velocity at the rotor discharge. Equation 1 is a consequence of the definition of the slip factor

$$\mu = \frac{V_{u2}}{U_2} \tag{2}$$

For a simplified analysis of the compressor performance that assumes uniform conditions at the rotor discharge not only in peripheral but also in axial direction, across the blade width b_2, and for axial absolute velocities V_1 at the rotor inlet, the specific work ΔH_w necessary to drive the compressor is from moment of momentum consideration, for an assumed adiabatic process,

$$\Delta H_w = \mu\ U_2^2 \qquad \left(\frac{ft\text{-}lb}{slug}\right) \tag{3}$$

For a perfect gas with $\gamma = c_p/c_v = $ constant, the actual rise in total temperature ΔT_w in the rotor is

$$\Delta T_w = \frac{\Delta H_w}{c_p} = \frac{\mu\ U_2^2}{c_p}$$

With the gas constant R_G there is

$$c_p = R_G\ \frac{\gamma}{\gamma-1} \tag{4}$$

Let

$$a_0 = \sqrt{\gamma\ R_G\ T_{t1}} \quad = \sqrt{\gamma\ R_G\ T_0} \tag{5}$$

be the velocity of sound at the total inlet temperature $T_{t1} = T_0$. Then

$$\frac{\Delta T_w}{T_0} = \mu\ (\gamma-1)\ \left(\frac{U_2}{a_0}\right)^2 \tag{6}$$

For an isentropic compression process from the total inlet pressure $P_0 = P_{t0} = P_{t1}$ to the discharge pressure P_{t4}, the necessary work required would be $c_p\ \Delta T_{is}$, where

$$\Delta T_{is} = T_0 \left[\left(\frac{P_{t4}}{P_0}\right)^{\frac{\gamma-1}{\gamma}} - 1\right] \tag{7}$$

The compressor efficiency η_c is defined by

$$\eta_c = \frac{\Delta T_{is}}{\Delta T_w} = \frac{\left(\frac{P_{t4}}{P_0}\right)^{\frac{\gamma-1}{\gamma}} - 1}{\mu(\gamma-1)\ \left(\frac{U_2}{a_0}\right)^2} \tag{8}$$

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For a particular design the following data are usually prescribed:

$\dot{m}$ — mass flow rate (slug/s)

P_0 — total inlet pressure (psia)

T_0 — total inlet temperature (°R)

P_{t4} — discharge pressure (psia)

γ — ratio of specific heats c_p and c_v

R_G — gas constant $(\frac{ft\text{-}lb}{slug,°R})$

With the indicated units, which are frequently used for engineering purposes, a quantity of mass is in slugs which is derived from the chosen units of force, length, and time. However, the relations which are going to be established hold for any consistent system of units, hence also for one where the primary units are mass, length and time, and where forces are in derived units.

For the given conditions there are to be found the following data for an optimum design:

U_2 — peripheral rotor speed at R_2

b_2/R_2 — $\dfrac{\text{ratio of axial impeller width at discharge}}{\text{outer radius of impeller}}$

R_{1o}/R_2 — $\dfrac{\text{outer radius at rotor inlet}}{\text{outer radius of impeller}}$

R_{1i}/R_{1o} — $\dfrac{\text{inner radius at rotor inlet}}{\text{outer radius at rotor inlet}}$

ω — angular velocity of impeller (radians/s)

β_{1o} — relative flow angle at R_{1o}

α_2 — absolute flow angle at R_2

R_3/R_2 — $\dfrac{\text{radius at inlet lip of diffusor blades}}{\text{outer radius of impeller}}$

R_4/R_2 — $\dfrac{\text{radius at discharge of diffusor}}{\text{outer radius of impeller}}$

Important design criteria are also:

$M_{W1} = \dfrac{W_{1o}}{a_1}$ — Mach number of relative velocity W_{1o} at outer radius R_{1o} at impeller inlet

$M_{V2} = \dfrac{V_2}{a_2}$ — Mach number of absolute velocity V_2 at impeller discharge

Mechanical and fluid dynamics considerations impose design limits of:

a) U_2, because of permissible rotor stresses
b) R_{1o}/R_2, which cannot exceed about 0.70 to 0.75 to obtain an outer rotor contour with acceptably small curvatures in the meridinal plane
c) R_{1i}/R_{1o}, which, if too small, does not permit the arrangement of a sufficiently large number of rotor blades Z_R with reasonable thickness
d) β_{1o}, which cannot be larger than about 70° for manufacturing reasons
e) b_2/R_2, which cannot be smaller than certain limits to obtain good efficiencies
f) α_2, which cannot exceed 70° to 80° because of manufacturing reasons and because of poor diffusor performance, especially if M_{V2} is larger than unity.

2. COMPRESSION PROCESS

Figure 2 is a temperature-entropy diagram showing the thermodynamic process in the compressor of Fig. 1. The temperature differences in Fig. 2 correspond roughly to the velocities of the triangles of Fig. 1 to obtain a realistic representation. Since by Eq. 6 the work input ΔT_w is also $\Delta T_w = \mu (U_2^2/c_p)$, the temperature rise $T_2 - T_1$ in the rotor is roughly one-half of ΔT_w. Later on the so-called degree of reaction $r*$ will be introduced to determine this ratio more precisely.

Station (1) in Fig. 2 corresponds to the static condition at the rotor inlet, given by the static pressure p_1 and the static temperature T_1. The total pressure and total temperature at this station are $P_{t1} = P_0$ and $T_{t1} = T_0$. For the isentropic process between (0) and (1).

$$\frac{T_{t1}}{T_1} = \frac{T_0}{T_1} = 1 + \frac{\gamma-1}{2} M_{V1}^2 \tag{9}$$

and

$$\frac{P_{t1}}{P_1} = \frac{P_0}{P_1} = \left(\frac{T_0}{T_1}\right)^{\frac{\gamma}{\gamma-1}}$$

where

$$M_{V1} = \frac{V_1}{a_1} = \frac{V_1}{[\gamma R_G T_1]^{\frac{1}{2}}}$$

is the Mach number of the absolute velocity V_1 at the rotor inlet.

The conditions of state at all locations can be expressed with the parameters U_2/a_0, R_{1o}/R_2, M_{W1}, β_{1o}, α_2, μ, and loss coefficients that establish the entropy increments between the different stations, if it is assumed that the flow process along the outer contour of the rotor between the radii R_{1o} and R_2 is representative of the rotor flow in general. The later assumption is made because the relative velocity W_1 and the relative flow angle β_1 are higher at R_{1o} than at other radii R_1. Hence along the outer rotor contour from R_{1o} to R_2 there occur the highest deceleration ratio W_{1o}/W_2 and the largest flow deflection $\Delta\beta = \beta_{1o} + \beta_2$. Moreover since the path travelled by a fluid particle along the outer rotor contour is shorter than that travelled by a particle entering at other radii R_1, the conditions along the outer rotor contour will establish design limitations and have a critical influence on the rotor losses.

With the chosen parameters, Eq. 9 can be rewritten

$$\frac{T_1}{T_0} = \frac{1}{1 + \frac{\gamma-1}{2} M_{W1}^2 \cos^2\beta_{1o}}$$

This formula is also given by Eq. I(5) of Table I. This table has been arranged to list the pertinent relations for the determination of the flow properties in the compressor for ready reference. In the following only the main steps will be indicated that led to these formulas without going into the details of their derivations. Some of the equations, for instance Eq. I(6), can be obtained directly from Fig. 2. It can be noted that all temperatures are given as multiples of the total inlet temperature $T_0 = T_{t1}$, and pressures are listed as ratios with respect to $P_0 = P_{t1}$. The static temperature T_2 of the rotor discharge [Eq. I(7)] is equal to the difference of the total temperature T_{t2} at the rotor exit and $V_2^2/2c_p$, where V_2 is given by Eq. I(3). The temperature T_2' is necessary to calculate the pressure ratio p_2/P_0 by Eq. I(20). Evidently T_2' depends on the entropy increase $s_2 - s_1$ in the rotor.

The process between stations (1) and (2) from the rotor inlet to its discharge can be formulated by

$$T_1 - \frac{W_{1o}^2}{2c_p} - \frac{U_{1o}^2}{2c_p} = T_2 + \frac{W_2^2}{2c_p} - \frac{U_2^2}{2c_p} \tag{10}$$

which is a fundamental relation obtained from the energy equation for steady, adiabatic flows along streamlines in rotors, as shown in Art. 7.5 of Ref. 1.

The following discussion uses a relation which is obtained from Eq. 10 for incompressible flows (See Eq. 7(44) of Ref. 1). At a particular radius R along the outer rotor contour where the peripheral and relative velocities are U and W, respectively, the static pressure p is

$$p = p_1 + \frac{\rho}{2}(U^2 - U_{1o}^2) + \frac{\rho}{2}(W_{1o}^2 - W)^2 - \Delta p_f \tag{11}$$

where ρ is the constant mass density of the fluid, and Δp_f the pressure loss due to frictional effects in the rotor. At the rotor inlet, where $U = U_{1o}$ and $W = W_{1o}$, the static pressure is evidently equal to p_1, the static pressure in the absolute flow just ahead of the rotor at R_{1o}. Equation 11 shows that, independently of the values of W and Δp_f, there will always occur a pressure increase $\rho/2(U^2-U_{1o}^2)$ if a fluid particle moves from R_{1o} to R. An additional pressure rise is produced by decelerating the relative velocity from W_{1o} to W. A flow that moves in a direction where the static pressure increases is more susceptible to separations than an accelerated flow, but the frictional pressure loss between neighboring stations is proportional to the dynamic head $(\rho/2) W^2$ in both flows. In view of Eq. 11 however there exist differences between flows that pass through stationary channels and those in rotating impellers. If a relative flow is decelerated in a rotating channel, whose distance from the axis of rotation increases in flow direction, it will not necessarily separate even though it moves against rapidly increasing static pressures, provided these pressure gradients are produced by the centrifugal force field and not by large reductions in relative velocity. If the same static pressure rise would have to be produced in a stationary channel of the same length as the rotating one, the deceleration of the flow per unit length would very likely become excessive and could be associated with considerably increased losses because of flow separations. On the other hand, if it were possible to ignore the effects due to Coriolis accelerations, it could be stated that the pressure losses in a stationary and in a rotating channel of equal length and shape would have to be equal for the same velocity heads and equal flow decelerations, except for influences due to Reynolds number differences. Moreover, for different velocity heads the pressure losses would be directly proportional to the velocity heads at corresponding locations in the two channels. However if the respective performance of the two channels were evaluated by a loss coefficient ζ_R that relates the frictional pressure drop Δp_f to the actual static pressure rise in the channel, its value would be lower for the rotating channel than for the stationary one because of the additional pressure rise $(\rho/2)(U^2 - U_{1o}^2)$. The performance of the channels can be compared only by means of a loss coefficient ζ_W that is defined as the ratio of the pressure drop Δp_f and

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the pressure rise $(\rho/2)(W_{1o}^2 - W_1^2)$ due to the flow deceleration, irrespective of whether additional pressure rise is produced by the centrifugal force field or not.

These elementary considerations have not been presented here to imply that the loss coefficients ζ_W in a rotating and in a stationary channel of the same geometry are equal. In Ref. 1, Art. 8.5, it is shown that flows in stationary and rotating channels have fundamental differences as far as their rotational characteristics are concerned, and consequences of these conditions are described in Arts. 10.5 and 12.2 of Ref. 1. The intent of the above discussion is to draw attention to the fact that frequently used formulations for the efficiency of impellers for centrifugal turbines and compressors cannot serve as a measure for the performance of these rotors, and that some of the separation criteria applied to flows in centrifugal rotors have no physical meaning.

A commonly used definition for the efficiency of a centrifugal compressor rotor is

$$\eta_R = \frac{T_2' - T_1}{T_2 - T_1} \tag{12}$$

The significance of the temperatures is evident from Fig. 2. Equation 12 holds for the compressible flow of fluids with a constant value of $\gamma = c_p/c_v$. Similar to the preceding discussion that delt with incompressible flows, part of the temperature rise in the rotor is due to the increase in peripheral speed from station (1) to station (2). Equation 10, rewritten as

$$T_2 - T_1 = \frac{U_2^2 - U_{1o}^2}{2c_p} + \frac{W_{1o}^2 - W_2^2}{2c_p} = T_u - T_1 + \frac{W_{1o}^2 - W_2^2}{2c_p} \tag{13}$$

shows that the static temperature rise $T_u - T_1$ due to the centrifugal force field is equal to the first term on the right-hand side of Eq. 13. It occurs in rotors with and without flow losses, hence it is independent of the entropy increase $s_2 - s_1$. Thus the compression corresponding to $(U_2^2 - U_{1o}^2)/2 c_p$ occurs along the isentropic line $s_1 = $ constant from T_1 to T_u, from station (1) to station (u) in Fig. 2, producing the static pressure rise $p_u - p_1$, where

$$\frac{p_u}{p_1} = \left(\frac{T_u}{T_1}\right)^{\frac{\gamma}{\gamma-1}} = \left(1 + \frac{(U_2^2 - U_{1o}^2)}{2 c_p T_1}\right)^{\frac{\gamma}{\gamma-1}} = \left(1 + \frac{\gamma-1}{2} \frac{U_2^2 - U_{1o}^2}{\gamma R_G T_1}\right)^{\frac{\gamma}{\gamma-1}}$$

The deceleration of the relative velocity from W_{1o} to W_2 produces the temperature rise

$$T_2 - T_u = \frac{W_{1o}^2 - W_2^2}{2 c_p} \tag{14}$$

with an entropy increase from s_1 to s_2, due to the flow losses, which in turn affect the pressure rise $p_2 - p_u$. The efficiency of the process from (u) to (2) can be defined by the so-called wheel efficiency η_W

$$\eta_W = \frac{T_2' - T_u}{T_2 - T_u} = \frac{T_2' - T_u}{(W_{1o}^2 - W_2^2)/2 c_p} \tag{15}$$

giving

$$\frac{T_2'}{T_u} = \eta_W \frac{T_2}{T_u} + 1 - \eta_W$$

and

$$\frac{p_2}{p_u} = \left(\frac{T_2'}{T_u}\right)^{\frac{\gamma}{\gamma-1}}$$

From a fluid dynamics view point only the efficiency η_W is a measure for the quality of the rotor performance. In particular, low measured values of η_W are indications for the existence of flow separations, although η_W will be affected also by the tip clearance losses, the so-called scrubbing losses produced by the rotating blades in the wall boundary layer at the fixed shroud, and the mixing losses after the rotor. However, low efficiencies η_W are only partly reflected in the rotor efficiency η_R of Eq 12 because of the temperature rise $T_u - T_1$ which is produced without entropy increases. If the entropy diagram of Fig. 2 were to represent the actual conditions in the compressor of Fig. 1, there would be, by measuring the temperature differences in Fig. 2,

$$\eta_R = 0.84$$

and

$$\eta_W = 0.57$$

Although the value of $\eta_R = 0.84$ seems to indicate that the flow in the rotor is reasonably good, the low value of $\eta_W = 0.57$ shows clearly that it should be possible to improve the rotor considerably with a redesign. Such improvement should be undertaken not only to increase the overall efficiency of the compressor by reducing the entropy rise $s_2 - s_1$ in the rotor, but also to produce more uniform flow conditions at the

rotor discharge since it might then be possible to reduce the diffusor losses also.

The process in the rotor that involves the relative velocity changes can be considered also from a different view point. Equation 10 may be written as

$$T_E = T_1 + \frac{W_{1o}^2}{2 \ c_p} + \frac{U_2^2 - U_{1o}^2}{2 \ c_p} = T_u + \frac{W_{1o}^2}{2 \ c_p} = T_2 + \frac{W_2^2}{2 \ c_p} \tag{16}$$

where T_E is the so-called equivalent total temperature of the rotor flow. Equation 16 has the same form as the energy equation for an adiabatic process of an absolute flow if T_E is replaced by the constant absolute total temperature T_t and W_2 by the absolute velocity V. The temperature T_E is constant for a process in a particular rotor having a fixed radius ratio R_{1o}/R_2 and turning at a specified speed. Thus, for given inlet conditions, Eq. 16 can be used also for an isentropic process along s_1 = constant from (u) to (2') to give, in accordance with Fig. 2,

$$T_E = T_2' + \frac{W_{2is}^2}{2 \ c_p} \tag{17}$$

for the same pressure rise $p_2 - p_u$ as produced by the process with friction, and W_{2is} is the theoretical velocity available at the pressure p_2. In turbine calculations it is customary to express the rotor losses by so-called velocity coefficients ψ

$$\psi = \frac{W_2}{W_{2is}} \tag{18}$$

If this formulation is used for compressors also, there is from Eq. 17,

$$T_2' = T_E - \frac{1}{\psi^2} \frac{W_2^2}{2 \ c_p} \tag{19}$$

Introduced into Eq. 15

$$\eta_W = \frac{W_{1o}^2 - W_2^2/\psi^2}{W_{1o}^2 - W_2^2} = \frac{1 - \frac{1}{\psi^2} (\frac{W_2}{W_{1o}})^2}{1 - (\frac{W_2}{W_{1o}})^2} \tag{20}$$

or

$$\psi = \frac{W_2/W_{1o}}{[1 - \eta_W + \eta_W (\frac{W_2}{W_{1o}})^2]^{\frac{1}{2}}} \tag{21}$$

The reason for introducing ψ as an alternate for η_W is that η_W equals $-\infty$ for the special condition where $W_2 = W_{1o}$, or $T_2 = T_u$. In this case, and if W_2 is larger than W_{1o}, the velocity coefficient ψ can however still be applied. On the other hand, for usual designs where W_2 is smaller than W_{1o}, the velocity coefficient is not a good measure for the rotor performance since ψ can be increased by simply making the velocity W_2 smaller, and it is then more appropriate to use the wheel efficiency η_W for the loss evaluation. Since the same difficulties in expressing the losses occur in turbines also, an additional formulation is sometimes used which establishes the drop in total pressure that is associated with the entropy increase $s_2 - s_1$. For radial compressor rotors these formulation are either

$$Y_1 = \frac{P_{E1} - P_{E2}}{P_{E1} - p_u} \tag{22}$$

or

$$Y_2 = \frac{P_{E1} - P_{E2}}{P_{E2} - p_2} \tag{23}$$

depending on whether the pressure drop $P_{E1} - P_{E2}$ is referred to the inlet or the exit conditions. Although these total pressure loss coefficients are useful at small Mach numbers, or for incompressible flows where $P_{E1} - p_u = (\rho/2) W_{1o}^2$ and $P_{E2} - p_2 = (\rho/2)W_2$, it can be shown that the corresponding coefficients which relate the losses to the kinetic energy of the flow (in the same manner as η_W of Eq. 15, or ψ of Eq. 18) become smaller for constant values of Y_1 or Y_2 if the Mach number of the inlet or discharge flow increases.[2] Although the actual energy losses tend to increase with increasing flow Mach numbers, an indiscriminate application of Eqs. 22 or 23 with values of Y from low-speed tests can be used as a wrong argument that the opposite is true.

To simplify the relations for the determination of the conditions of state in the compressor the velocity coefficients ψ will be used in the equations of Table I. To compare two rotors with different radius ratios and different deceleration ratios W_2/W_{1o}, the efficiency η_W of Eq. 15 should be used as a

measure for their performance. Equations 20 and 21 relate ψ and η_W to each other. Paragraph 5 contains a discussion that deals with the magnitudes of η_W. With the formulas of Table I it is possible also to establish a relation for the determination of η_W for known values of η_R of Eq. 12, or vice versa. From

$$\eta_R = \frac{\eta_W \left[\left(\frac{W_{1o}}{U_2}\right)^2 - \left(\frac{W_2}{U_2}\right)^2 \right] + 1 - \left(\frac{R_{1o}}{R_2}\right)^2}{\left(\frac{W_{1o}}{U_2}\right)^2 - \left(\frac{W_2}{U_2}\right)^2 + 1 - \left(\frac{R_{1o}}{R_2}\right)^2} \tag{24}$$

and with

$$C = \frac{1 - \left(\frac{R_{1o}}{R_2}\right)^2}{\left(\frac{R_{1o}}{R_2}\right)^2 \cot^2\beta_{1o} + 2\mu \left(1 - \frac{\mu}{2\sin^2\alpha_2}\right)} \tag{25}$$

there are

$$\eta_R = \eta_W + C(1 - \eta_W) \tag{26}$$

and

$$\eta_W = \frac{\eta_R - C}{1 - C} \tag{27}$$

High performance compressors with high pressure ratios cannot be equipped with diffusors that are circular cascades with airfoil shaped blades. Figure 1 is a realistic sketch of a high speed compressor operating with an average discharge velocity V_2 that is supersonic. To obtain reasonably large axial blade widths b_2 as well as acceptable shapes of the meridinal rotor contours, it is necessary to resort to large angles α_2 at the rotor discharge. At large angles α_2, practical consideration dictate a limited number of diffusor channels, say, about 8 to 10 for angles α_2 of about 75°, and the permissible diffusion in these individual channels produces configurations similar to that depicted in Fig. 1. One of the most critical problem areas is the design of the flow passages from the rotor discharge to the entrance of the diffusor channels proper. The absolute flow leaving the rotor is not only non-uniform but also non-steady, because the relative velocity at the rotor discharge must by necessity vary between the suction and the pressure sides of the rotor blades at R_2. Designs where the radius R_3 is very much larger than the outer rotor radius R_2, or compressors with vaneless diffusor for large angles α_2, were found to be inferior to machines with small radial gaps $R_3 - R_2$, especially for high subsonic or supersonic velocities V_2. If it were not for the excessive noise the diffusor lips would preferably be arranged even closer to R_2 as shown in Fig. 1.

Theoretical attempts were made in Refs. 3 and 4 to evaluate the losses in the space between R_2 and R_3, and in vaneless diffusors, that are due to mixing and frictional effects. The results of these investigations do not agree with reality if M_{V2} and/or α_2 are large. These inconsistencies are due to the assumption that equal flow angles are supposed to occur across the axial width b_2 of the flow channel after the rotor, a condition which is created by assuming that the frictional forces along the walls act equally on all particles between them. In actuality the flow angles α (measured with respect to the radial direction) decrease radically in the wall boundary layers in the direction from the mid-section of the channel toward the wall. The particles inside the boundary layers then move more rapidly to larger radii into zones of higher pressure than those outside of the boundary layers and very easily cause flow separations from the walls, thereby impairing the effectiveness of such diffusors.

In the writer's opinion it is incorrect to state that in efficient diffusors the vanes must not be too close to the impeller, or that the velocity at their entrance must be subsonic in all cases. For the reason mentioned above, it is equally wrong to maintain that vaneless diffusors must be arranged for supersonic absolute velocities at the rotor discharge.

Because of the inability to separate the losses that exist between the radii R_2 and R_4 of Fig. 1 an overall diffusor efficiency η_D will be introduced. With the symbols of Fig. 2

$$\eta_D = \frac{T_4' - T_2}{T_4 - T_2} \tag{28}$$

where

$$T_4 - T_2 = \frac{V_2^2 - V_4^2}{2 c_p} \tag{29}$$

The velocity V_4 exists at the diffusor discharge at the radius R_4, and is taken as

$$V_4 = \lambda V_2 \tag{30}$$

With small values of λ the radius ratios R_4/R_2 become large because of the limited amount of diffusion that is possible per unit length in flow direction to avoid separations in the diffusor channels. Values of λ of about 0.20 to 0.30 are common to limit R_4/R_2 to about 2. With designs of the type shown in Fig. 1 the kinetic energy $V_4/2 c_p$ cannot be converted into pressure rise, since the flow from the individual diffusors is dumped into a receiver surrounding them. As indicated by station (d) in Fig. 2 the total pressure P_{t4} at the compressor discharge is then equal to the static pressure p_4 at the diffusor exit, and

the total temperature at the compressor discharge is $T_{t4} = T_{t2}$ for adiabatic processes. The dumping of the kinetic energy $V_4^2/2\ c_p$ is reflected in the overall diffusor efficiency η_D^* between rotor and compressor discharge

$$\eta_D^* = \eta_D\ (1 - \lambda^2) \tag{40}$$

Diffusor design criteria and approximate methods to evaluate the diffusor losses are given in paragraph 5.

Since

$$T_4 = T_{t2} - \frac{V_4^2}{2\ c_p} = T_{t4} - \lambda^2\ \frac{V_2^2}{2\ c_p}$$

and with Eq. 28 there is then obtained the temperature T_4, as given by Eq. I(11) of Table I. The pressure $p_4 = P_{t4}$ is determined from

$$\frac{p_4}{p_2} = (\frac{T_4'}{T_2})^{\frac{\gamma}{\gamma-1}}$$

for the isentropic process along the line s_2 = constant. Because the isentropic temperature differences between lines of constant pressure are proportional to the initial temperatures of the processes, there is, with the symbols of Fig. 2,

$$\frac{T_4'' - T_2'}{T_4' - T_2} = \frac{T_2'}{T_2}$$

and

$$\frac{T_4''}{T_0} = \frac{(T_4'/T_0)(T_2'/T_0)}{T_2/T_0}$$

As shown in Table I the ratio T_4''/T_0 can be expressed by Eq. I(13) which has the form

$$\frac{T_4''}{T_0} = \frac{1 + A(X_1 + A\ X_2)}{1 + A\ B} \tag{41}$$

where X_1 and X_2 are given by Eqs. I(14) and I(15), and

$$A = (\gamma-1)\ \mu\ (\frac{U_2}{a_0})^2 \tag{42}$$

$$B = 1 - \frac{\mu}{2\ \sin^2\alpha_2} \tag{43}$$

The temperature rise ΔT_{is} for an isentropic compression from the total conditions P_0, T_0 at the compressor inlet, to the discharge pressure P_{t4} is, with Eq. 41,

$$\frac{\Delta T_{is}}{T_0} = \frac{T_4''}{T_0} - 1 = \frac{A[X_1 - B + A\ X_2]}{1 + A\ B} \tag{44}$$

Eq. 44 is identical with Eq. I(16) of Table I.

As shown in Table I the pressures at the different stations can be determined from the established temperatures by using the pressure-temperature relation for isentropic processes of perfect gases.

3. PERFORMANCE AND DESIGN PARAMETERS

The overall compressor efficiency defined by Eq. 8 is, with Eqs. 6, 42, and 44,

$$\eta_c = \frac{\Delta T_{is}}{\Delta T_w} = \frac{X_1 - B + A\ X_2}{1 + A\ B}$$

With Eqs. 42 and 43 the above relation establishes Eq. II(1) of Table II. This table lists the equations necessary to determine the performance and the geometry of the compressor. Only the principal steps that led to the equations of Table II are described in the following, the details of the derivations are omitted. The symbols of Table II are those of Figs. 1 and 2, with additional ones that are defined in this paragraph.

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The degree of reaction r* is defined as the ratio of the isentropic temperature rise $T_2' - T_0$ in the rotor to that corresponding to the pressure ratio P_{t4}/P_0. Equation II(2) of Table II shows that for $\eta_c = 1$ and $\psi = 1$, the degree of reaction is

$$r^* = r_o^* = [1 - \frac{\mu}{2 \sin^2\alpha_2}]$$

For a slip factor $\mu = 0.85$, r_o^* changes from about 0.544 to 0.433 if the angle α_2 is reduced from 75° to 60°. For low degrees of reaction a large part of the overall pressure rise must be produced in the diffusor. Since this energy conversion is associated with greater losses than the pressure rise produced in the rotor, high degrees of reaction are desirable. This condition is used in hydraulic pumps which usually have backward-bent rotor blades to produce most, if not all, of the pressure rise in the rotor. However, if such rotors were employed for light gases, such as air, the pressure rise would be too small for most applications, not only because of the reduced specific work input but also because such rotors would not be able to operate at high speeds on account of the high bending stresses in the blades. In rotors with radial blades it seems beneficial to use large angles α_2 to increase r*. At a fixed peripheral speed U_2 the velocities V_2 decrease if α_2 is increased, but difficulties occur then because of the geometry of the passages from the wheel to the diffusor inlet. The deceleration ratio W_2/W_{1o} becomes smaller also, as shown by Eq. II(5), and the increased losses caused by larger flow decelerations in the rotor may off-set the gain that would be obtained from the increased degree of reaction if other conditions would remain unchanged. The choice of these design parameters to obtain the best possible solution must usually be based on experience because of the interactions between rotor and diffusor that are greatly influenced by their designs.

The slip factor μ appears in most of the equations of Tables I and II. More has been written on this subject than on any other in the field of radial pumps and compressors, primarily because it is of great importance to know exactly how much energy a wheel will absorb. If wrong values of μ are used in a design the desired pressure ratio will not be obtained even though the expected efficiency is reached. Reference 7 is a recent paper where tests obtained with one particular wheel are compared with data obtained from experiments, and with slip factor formulas, by other authors. As is frequently the case in many studies on the subject, test data from a single wheel obtained at off-design conditions are used to establish design point data for other impellers. Moreover, the highest ratio U_2/a_0 was only about 0.51 in the tests of Ref. 7. The bibliography of Ref. 7 fails to mention the investigations of Refs. 5 and 6 which were undertaken at Daimler-Benz A. G. by systematically testing ten high-performance impellers of different shapes up to values of U_2/a_0 of about 1.1. In the writer's opinion, the data published in Refs. 5 and 6 are extremely valuable to the designer and the original curves of the article have been replotted in Fig. 3 to give wider publicity to this important contribution to the state of the art.

With the slip factor known from Fig. 3 the compressor efficiency of a particular design can be determined from Eq. II(1) for known losses. Equation II(3) is plotted in Fig. 4 for $\gamma = 1.4$, and different values of $\mu\eta_c$, to show the magnitudes of U_2/a_0 necessary to produce particular pressure ratios. For advanced gas turbine applications it would be desirable to operate at pressure ratios of between 8 and 10. For $\eta_c = 0.8$ and $\mu = 0.875$, Fig. 3 shows that values of U_2/a_0 of about 1.8 are necessary to reach this goal. Thus, at an inlet temperature of 60°F, where $a_0 = 1120$ ft/s, the rotor of such a compressor has to operate with a peripheral speed U_2 of about 2000 ft/s, requiring special materials and careful rotor designs for the resulting high stresses.

By Eq. I(6) the rise of the total temperature in the compressor is $T_{t2} - T_0 = T_0(\gamma-1)\mu(U_2/a_0)^2 = 590°F$, or about 600°F, for $\mu = 0.875$ and $T_0 = 520°R$. Since the degree of reaction is around 0.5, the static temperature T_2 at the rotor discharge is then about $60 + 600/2 = 360°F$. At this temperature, high-strength aluminum alloys have rupture stresses, and stresses for specified creep rates, which are less than one-half of the allowable stresses at room temperature. Hence it is necessary to use titanium alloys, for instance those with about 6 percent aluminum and 4 percent vanadium. At 360°F the design criterion for these materials is the yield stress since no appreciable creep effects occur even for operating times of 100,000 hours. Their 0.2 percent offset yield strength at 360°F is about 120 kpsi, with an ultimate strength of about 150 kpsi. As shown in chapter C of Ref. 8, the tangential stress in a non-supported ring of small radial thickness rotating with the peripheral speed U_2 is ρU_2^2. For titanium with a specific gravity of 4.43, this value is about 240 kpsi at $U_2 = 2000$ ft/s. Figures C.27 and C.29 of Ref. 8 show the so-called equivalent centrifugal stresses σ_e in rotors with radial blades as multiples of $\rho U_2^2 = \rho \omega^2 R^2$, for a design where the disk extends to the outer tip of the blades at R_2, and another which has so-called scallops between the blades, similar to the rotor design shown in Fig. 1. Not counting the stress peaks at the central bore, which are more of the nature of stress concentrations that will be relieved by plastic deformations, because titanium has high ductility on account of its 20 percent elongation, the maximum stress ratios $\sigma_e/(\rho U_2^2)$ are about 0.25 and 0.16 for the rotors without and with scallops, respectively. Hence the maximum stresses at 2000 ft/s will be about 60 kpsi for one and about 40 kpsi for the other rotor. This discussion shows that compressor rotors operating at tip speeds of 2000 ft/s are feasible and that by arranging scallops, and using 75 percent of the 0.2 percent offset yield stress, or 90 kpsi, as design criterion, the maximum tip speed could be as high as 3000 ft/s or over 900 m/s. The latter speeds would give velocity ratios U_2/a_0 of about 2.68 at $T_0 = 60°F$ and $\gamma = 1.4$. For $U_2/a_0 = 2.68$, $\mu = 0.85$, $\eta_c = 0.80$, pressure ratios P_{t4}/P_0 of about 43 could be reached in a single stage for gases with $\gamma = 1.4$. The extreme difficulties that would be associated with such a design, in particular those arising because of the large volume flow reductions, will not be discussed here. The intent of the fore-going deliberations is to show that pressure ratios in centrifugal compressors for air are not restricted because of rotor stresses.

Important advances are being made in nuclear gas turbines with helium as working fluid, as described in a recent article by Bammert and Bohm[9]. The main difficulties in the design of the turbomachines for this plant are the low pressure ratios that can be produced with helium in a conventional compressor stage, since the molecular weight of helium is only about 4 and $\gamma = 1.659$. At 60°F the velocity of sound in helium is 3275 ft/s. For a rotor with $U_2 = 3000$ ft/s, a speed ratio $U_2/a_0 = 0.916$ would be obtained in a radial compressor. All velocities in the compressor would be subsonic and design point efficiencies of about $\eta_c = 0.85$ seem feasible. For $\mu = 0.90$, $\eta_c = 0.85$, $U_2/a_0 = 0.916$, at $\gamma = 1.659$, the resulting pressure ratio P_{t4}/P_0 would be 2.43 in accordance with Eq. 8.

In Ref. 9 a 25 MW$_e$ closed-cycle helium gas turbine plant is described that operates with a turbine pressure ratio of 2.55. The pressure ratio of the compressors will have to be about 2.7 to overcome the pressure losses in the reactor and heat exchangers, of which no values are given in the paper. Reference 9 shows however that the plant has three axial compressors in series, each consisting of 9 stages. Since intercoolers are arranged between the three compressors each will produce a pressure ratio of about 1.4. If the three axial compressors were replaced by two single-stage radial compressors, of the type described with an intercooler between them, it would be possible to obtain an overall pressure ratio of about six which would be of advantage for the cycle. The writer does not want to minimize the difficulties that would be connected with the development of radial compressors and radial turbines for such applications, in addition to those connected with the bearings, seals and gear drives, but it is felt that they might be the ultimate solution for these highly interesting power plants.

Equation I(1) will be used in an example to show the influence of the diffusor losses on the compressor efficiency at different speed ratios U$_2$a$_0$, for absolute flow angles α_2 of 60° and 75°. The velocity coefficients ψ will be determined by assuming a wheel efficiency η_W of Eq. 15 of 0.7 for both impellers. Equations 21 and 24 were used to establish Fig. 5. The deceleration ratios W$_2$/W$_{1o}$ are 0.68 for $\alpha_2 = 60°$ and 0.366 for $\alpha_2 = 75°$ by Eq. I(5) for the data listed in Fig. 5. This difference makes the choice of equal efficiencies η_W for both cases somewhat dubious. It is seen from Fig. 5 that the rotor efficiencies η_R are 0.89 and 0.855 for $\alpha_2 = 60°$ and $\alpha_2 = 75°$, respectively. The corresponding values of ψ, which will be used in Eq. I(1), are 0.865 and 0.585. It is assumed further that the velocity V$_4$ at the diffusor discharge is 0.2 V$_2$, or $\lambda = 0.2$, so that $\eta_D^* = 0.96 \eta_D$ by Eq. I(12). Figure 6 shows the large effect of the diffusor losses on the compressor efficiency. To obtain $\eta_c = 0.85$, the diffusor efficiency must be about 0.9 for all speed ratios U$_2$/a$_0$. If η_D were 0.7 instead of 0.9, the compressor efficiency would only be 0.75. At U$_2$/a$_0$ = 1.6, this decreased diffusor efficiency would reduce the pressure ratio of the compressor from about 7 to 5.8, which in a gas turbine plant would produce a mismatch between turbine and compressor, with additional adverse effects on the thermal efficiency of the plant. Figure 6 shows also that the diffusor has a larger influence on η_c at the higher flow angle α_2. On the other hand, the Mach number M$_{V2}$ of the rotor discharge velocity will be lower at $\alpha_2 = 75°$ than at $\alpha_2 = 60°$. The respective values can be obtained from Eq. II(6) which has been represented in Fig. 7 for $\gamma = 1.4$. At U$_2$/a$_0$ = 1.6, the values of M$_{V2}$ are 1.16 and 1.24 for α_2 of 75° and 60°, respectively, for the design parameters listed in Fig. 5.

Figure 7 shows that the Mach number M$_{V2}$ becomes unity for values of U$_2$/a$_0$ between 1.1 and 1.3, depending on the choice of α_2. From Fig. 8, which is a representation of Eq. II(4), it can be noted that for a speed ratio U$_2$/a$_0$ = 1.2 and at a radius ratio R$_{1o}$/R$_2$ of about 0.67, which represents an average design value, the relative velocity W$_{1o}$ at the rotor inlet has a Mach number M$_{W1}$ of about 0.9 at an inlet angle β_{1o} of 65°. Figures 8 and 4 show that the Mach number M$_{W1}$ for air compressors will not have to be larger than about 1.3 to produce pressure ratios up to about ten. Some sources state that no efficient inducers can be built for values of M$_{W1}$ larger than 0.8 because of "shock losses". It seems to the writer that such statements are not different from those made some years ago, which predicted that it would be impossible for an airplane to break the "sonic barrier", or others which maintained that an axial compressor has to operate at subsonic velocities to be efficient. Advances in transonic axial-flow compressor stages have shown that human ingenuity can overcome these so-called barriers. Reference 10 is cited as an example, where a transonic boost stage ahead of the inlet of a centrifugal compressor is described, which produces a pressure ratio of 1.43 for air at an efficiency of 90 percent with a tip Mach number of 1.05.

The flow in an inducer of an impeller with radial blades is different from that in an axial-flow rotor. In the latter, particles that have been moving along the suction and the pressure sides of the blades are mixed at essentially constant static pressure after the trailing edges at the discharge, whereas no such mixing occurs in the flow channels where the inducer joins the radial blades of the impeller. Hence the pressure distributions along the walls of the inducer blades must be radically different from those along the surfaces of an axial rotor blade, and separation criteria that are based on the diffusion factor of axial cascades cannot be applied. Similar to the conditions in transonic axial stages the supersonic relative velocity at the tip of an inducer becomes sonic at a particular radius R$_{1c}$, and subsonic at radii R$_{1x}$ smaller than R$_{1c}$. Denoting the Mach number of W$_1$ at R$_{1x}$ by M$_{1x}$, and that at R$_{1o}$ by M$_{W1}$ as previously defined, there is

$$\frac{R_{1x}}{R_{1o}} = \frac{1}{\sin\beta_{1o}}\left[\left(\frac{M_{1x}}{M_{W1}}\right)^2 + \sin^2\beta_{1o} - 1\right]^{\frac{1}{2}} \tag{45}$$

Figure 10 shows the values of R$_{1x}$/R$_{1o}$ obtained from Eq. 45 for M$_{W1}$ = 1.3, at different relative flow angles β_{1o} at the inducer tip, and for particular values of the Mach number M$_{1x}$. This graph is presented to show that it is non-sensical to state that M$_{W1}$ cannot exceed particular values without specifying at what angle β_{1o} and at what ratio R$_{1i}$/R$_{1o}$ this limitation holds. Whereas at $\beta_{1o} = 75°$ a Mach number of unity occurs at R$_{1x}$/R$_{1o}$ = 0.75, the whole inlet annulus will have supersonic relative velocities at $\beta_{10} = 50°$, for the same Mach number M$_{W1}$ = 1.3 at the tip. Moreover, if at $\beta_{1o} = 75°$ the hub/tip ratio R$_{1i}$/R$_{1o}$ of the inlet eye is 0.75 in one machine and, say, 0.3 in another the losses due to compressibility effects will certainly be different. Figure 10 also shows the Mach numbers M$_{V1}$ of the absolute velocity V$_1$ ahead of the impeller which, as indicated earlier, has been assumed to remain constant in radial direction. They have values of 0.336 and 0.919, respectively, for $\beta_{1o} = 75°$ and $\beta_{1o} = 55°$ at M$_{W1}$ = 1.3, and it is inconceivable to the writer that the losses will remain constant independent of M$_{V1}$. Clearly, if M$_{V1}$ becomes larger than unity very special conditions occur since the flow in the annulus becomes choked at M$_{V1} = 1$ as has been discussed in Art. 9.9 of Ref. 1. Some of the peculiarities associated with cascades at supersonic inlet velocities are mentioned in Art. 9.10 of the same reference.

The writer believes that the, by now, almost classical view points of flows through turbomachines have outlived their usefulness. They may even be a hindrance for future developments and if accepted without questioning, may prevent original thinking and could make people believe that all problems have been or will be solved by their use. This classical method assumes that the fluid particles in a turbomachine move on axisymmetric stream surfaces of shapes which are either assumed a priori, or obtained

by simplified theoretical methods. Further, it is assumed that the flow through a turbomachine can be replaced by the flows through a multiplicity of annular channels bounded by neighboring stream surfaces, which are closely spaced between the meridional contours of the flow channel of the machine at hub and tip. The stream surfaces are actually considered to be thin, solid walls that do not create disturbances, and it is assumed that the flows in these individual channels do not interact with each other. In each one of the channels there exists then a so-called quasi two-dimensional flow of the type described in Art. 12 of Ref. 1. The performances of the different cascades, which are now arranged in the various flow channels to produce the specified flow deflection, are taken to be those of two-dimensional cascades obtained either in cascade test rigs or by theoretical methods. With the latter, one can at best attempt a solution for the special relative flows W in rotors that satisfy the condition $\nabla \times \vec{W} = -2\vec{\omega}$; that is, where the curl of the velocity function is a constant, since ω is the angular velocity vector of the rotor. Such flows are isentropic but can be compressible. However, disturbances due to shocks cannot occur. This condition limits the theoretical evaluation to flows where the local Mach numbers must be less than or, at the most, equal to unity. More general solutions of the so-called blade-to-blade problem on axisymmetric stream surfaces have not yet been obtained and are very difficult to formulate.

So-called quasi two-dimensional flows with $\nabla \times \vec{W} = -2\vec{\omega}$ are discussed in Art. 12 of Ref. 1. By introducing a stream function ψ there is obtained a second order partial differential equation of the form (see Eq. 12(9), p. 307, Ref. 1)

$$\frac{1}{R^2} \psi_{,,\theta} + \psi_{,,m} - \frac{1}{R^2} \left[(\ln\rho)_{,\theta} \right] \psi_{,\theta}$$

$$+ \left[(\ln R)_{,m} - [\ln(\Delta h \rho)]_{,m} \right] \psi_{,m} = -2(\Delta h) \, \rho\omega \sin \lambda \tag{46}$$

The commas denote partial differentions with respect to the coordinates listed after them, where θ is the angle in peripheral direction and m the length along the generatrix of the stream surface. The mass density is denoted by ρ, R is the radius from the axis, Δh is the varying distance between neighboring stream surfaces, ω is the angular rotor velocity, and λ is the angle of the tangent to the generatrix with the axis of rotation. For $\lambda = 0$ the particles move on cylindrical stream surfaces, and $\lambda = 90°$ covers flows in radial compressor wheels with stream surfaces that are planes perpendicular to the axis. For the latter case, and for conical stream surfaces, Eq. 46 has been solved by Stanitz for thin blades.[3] For cascades with airfoil-shaped blades, that are arranged on an arbitrary surface of revolution, computer programs are described in Ref. 11 for solutions with relaxation methods that need high-speed computers with large storage capacities. As interesting and useful these theoretical attempts are, one must be critical to evaluate what they really produce in form of results, and whether or how these data will help to improve present designs, and to create the turbomachinery which is to be built in the future.

The mere fact that modern computers can solve differential equations with complicated boundary conditions which, hitherto, could not be tackled by hand calculations is no assurance that the results must be correct from a physical point of view. Computers can only perform mathematical manipulations as they are told to do, and no result is better than the assumptions that were used to formulate the problem that is solved by these apparently sophisticated, but inherently stupid, machines.

Two of the necessary boundary conditions for solving Eq. 46 with the programs of Ref. 11 require that the flows upstream and downstream of the blades are uniform, and that the flow angles at these stations be specified. These conditions imply that the tangential deflection through the cascade is known a priori, whereas in actuality the possible deflection depends on the attitude of the blades in the cascade and the upstream conditions only. Whereas in turbine cascades it is possible to calculate the discharge angle from the geometry of the cascade with approximate methods, such predictions are not possible in axial compressor cascades, in fact one of the major problems is to find out what the discharge angles are for imposed incidence angles. Actually then, Ref. 11 produces pressure distributions about blades for specified locations of the rear stagnation points, and if they have been chosen wrongly the pressure pattern will be wrong also. As in most theoretical cascade flow investigations the effects of upstream or downstream cascades cannot be taken into account; the row investigated constitutes in actuality a disturbance located between two flow fields that extend to infinity far upstream and far downstream without being disturbed by other cascades.

A major drawback of all methods that are based on Eq. 46 is however that the right-hand side of this relation becomes zero if either ω is zero, or if λ is zero. If the angular velocity is zero the cascade is stationary and instead of the pattern of the relative velocity W one deals with the absolute velocity V in a stator whose curl $\nabla \times \vec{V}$ is now zero because of the initial condition that $\nabla \times \vec{W} = -2\vec{\omega}$. The velocities V of such flows must be gradients of a potential function φ, and Eq. 46 can be modified to

$$\nabla^2 \varphi = \frac{\nabla\varphi}{a^2} \cdot \nabla \left(\frac{V^2}{2} \right) \tag{47}$$

where "a" is the variable velocity of sound at the different locations in the flow field. As before it is necessary that $M = V/a$ is everywhere smaller than unity. For incompressible flows, where the velocity of sound "a" is tending toward infinity, Eq. 47 reduces to Laplace's equation $\nabla^2\varphi = 0$. Equation 47 is a partial differential equation of the Poisson type and the term on its right-hand side can be interpreted mathematically to be the result of sources in the flow field. Expressed differently, the curl of $\vec{V}$ is zero, but its divergence $\nabla \cdot \vec{V}$ is not; which means that flow must be generated somewhere in the field, and sources judiciously arranged therein can take care of this situation. Reference 12 develops calculating methods that are based on this idea by using the principles of superposition, but again for assumed axisymmetric stream surfaces, namely, cones in particular.

It can be noticed also, that Eq. 46 changes into Eq. 47 if $\lambda = 0$; that is, if cylindrical stream surfaces are assumed to exist. Thus, as far as axial machines with cylindrical stream surfaces are concerned, the flow through a rotor is not different from the flow through a stator, if the cascades have the same geometries and if the flow angles of the relative and absolute flows are equal. On the other hand it can be proved without a shadow of a doubt, e.g., by Art. 8.5 of Ref. 1, that even isentropic relative flows in rotors must be fundamentally different in character from absolute flows. From Eq. 8(23) of Ref. 1 it can be seen clearly that the simplest relative flow must have $\nabla \times \vec{W} = -2\vec{\omega}$, and if Kelvin's theorem is extended to relative flows (Eq. 8 (22) of Ref. 1), and applied to isentropic conditions, one sees that the change of the circulation Γ_R around a moving fluid curve C in a relative flow is not zero but equal to

$$\frac{D\Gamma_R}{dt} = -2 \oint_{(C)} d\vec{r}_R \cdot \vec{\omega} \times \vec{W} \qquad (48)$$

In an absolute isentropic flow, however, the change of the circulation around a moving fluid is indeed zero. Equation 48 indicates that $D\Gamma_R/dt$ is zero only if the relative flow vectors $\vec{W}$ are everywhere parallel with $\vec{\omega}$, hence parallel with the axis of rotation. Rotors of this type are not capable of changing the energy of fluids and have no practical interest. That the condition $\nabla \times \vec{W} = -2\vec{\omega}$ is not in conflict with Eq. 48 can be proved with simple means.

It can be stated therefore that the stream surfaces in a rotating cascade must differ from those that would occur if the same cascade were stationary. More precisely, the stream surface in a stationary cascade, whose flow satisfies $\nabla \times \vec{V} = 0$, must change to a pattern that satisfies $\nabla \times \vec{W} = -2\omega$, and it is not possible that the relative flow in the rotating cascade has the same stream surfaces as the absolute flow. In particular, the relative stream surfaces cannot be axisymmetric, if those of the absolute have this character. More about these conditions has been described in Art. 10.5 of Ref. 1, but it is evident from the above discussion that results obtained by solving Eqs. 46 and 47 must be of approximate nature even for the idealized flows that are investigated, and they must be interpreted in the proper perspective of their initial assumptions.

Such results, or data from stationary cascade test rigs which basically are obtained with the same assumptions as those of the above-mentioned theories, are now used to establish the blading elements in the individual flow channels between the solid stream surfaces. The classical method consists in designing the actual blade surfaces through the profiles of these blade elements. The "solid" stream surfaces are then, so to say, removed and it is assumed that the originally calculated or assumed stream surfaces will also exist for the flow about these three-dimensional blades. It is quite clear that there are many possibilities of arranging an actual blading with the profile sections that are obtained from the flows through the individual flow channels, depending, for instance, on how the leading edge of the blade is arranged. In the inducer of Fig. 1 the leading edge of the blade could be pulled forward in flow direction to obtain a blade surface that is leaning more away from a meridional plane than if the leading edge were to slant backward, although at the different radii the blade angles would be exactly equal. Without a doubt these two blades would exert different forces on the flow, one could tend to push the flow toward the tip, the other toward the hub, and it is inconceivable that the flow pattern in the meridian channel would remain unchanged. In Ref. 2 (Table C-2, p. 26) an investigation dealing with the blading of an axial-flow machine has been carried out to check whether it is possible to build a rotor with a very large number of thin blades that produces the idealized relative flow with $\nabla \times \vec{W} = -2\omega$ near its cylindrical hub. This flow condition establishes a particular change of the flow angle in radial direction, and requires that the blade surface consists of radial lines. Since for a large number of blades the flow and the blade angles must be identical, the last mentioned requirement establishes the change of the flow angle along the radius by itself. It can be seen that the two values differ, primarily because from $\nabla \times \vec{W} = -2\omega$ the necessary blade angle change depends on the ratio of ω and the axial component of $\vec{W}$, whereas this is not the case for the other. Hence, it is evident that the condition $\nabla \times \vec{W} = -2\omega$ cannot be maintained in a blading with a finite axial length, and that the actual blade shapes as a whole will have an influence on the flow through them. These examples show that the flow patterns in a machine can be influenced by particular arrangements of the profiles in direction of the blade height and that they will have a bearing on the meridional flow. The classical approach, so to say, linearizes the problem, and does not take account of the interactions that occur between the flows through the different elementary channels from the hub to the tip. It further tries to explain all phenomena with a two-dimensional model, at best with one on stream surfaces that are surfaces of revolution, and looses sight of the actual three-dimensional effects that occur in reality. These limiting view points seem to be particularly harmful if supersonic flows occur in a relative flow field where, as discussed earlier in connection with the inducer inlet, the absolute flow is subsonic. Stationary cascade test data cannot give a true picture of the conditions since they replace again the relative flows by an absolute flow between "solid" stream surfaces, where in particular the condition that the flow component perpendicular to the cascade axis, which is in reality the actual absolute flow, has no special significance. In a supersonic cascade test rig it will hardly be possible to determine cascade performance at different incidence angles nor establish design data for blades where only parts of the blades have supersonic velocities. For inducers of radial compressors which are followed by radial blades it does not seem possible to use cascade data with any degree of realism, and only experimental work with actual rotating wheels will show what detrimental effects high relative flow Mach numbers have on the performance.

There seem to exist a number of design variables that should be examined for supersonic inducers. The possibility of influencing the flow pattern near the tip by appropriate blade shapes to produce, say, greater mass flow rates per unit area near the hub, has been mentioned. These designs could be extended to produce swept-wing effects, similar to what has become the standard design of wings for high-speed airplanes. It is well known that in supersonic flows the velocity parallel with the leading edge of a swept-back wing with infinite span cannot produce variations in pressure, hence only the component of velocity perpendicular to the leading edge can create losses that are caused by compressibility effects. Peculiar conditions could however occur at the outer wall, if this principle were applied to the design of the inducer inlet edges, but it might be possible to obtain considerable improvements. The writer is surprised that such designs

have not been tried for axial compressor stages, especially for those with large blade heights. Swept-back blades would not necessarily have greatly increased bending stresses, since the maximum section modulus of an airfoil profile is a large multiple of the minimum modulus about the outer principal axis. If the centers of gravity of the profiles along the blade height were displaced backward along this axis of the hub profile, it should be possible to minimize the stresses that are caused by the additional bending moment about the other principal axis.

The writer believes that it is possible to build inducers at supersonic relative inlet velocities for absolute inlet Mach numbers M_{V1} of about 0.5 to 0.6 with good efficiency and minimum flow disturbances. Converging-diverging passages in the inducer seem unnecessary, especially if only part of the rotating channel has supersonic velocities. Leading edge radii must be as small as possible, but large enough to avoid damage by flutter, and great care must be taken to properly design the suction side of the blade to provide a good transition into the actual blade channel. It is not believed however that the blades must be designed for incidence angles if the proper blockage factor is used for the flow area calculations at the inlet. This statement contradicts the data of Ref. 13, where the optimum rotor efficiency η_R is shown to occur at positive incidence angles of about 10° at R_{1o} for blade angles of 57°. The inlet channel ahead of the eye of the wheel that was tested, has curved meridinal contours, hence the inlet velocity V_1 is not uniform from R_{1i} to R_{1o}. Although it is stated in Ref. 13 that the distribution of V_1 was determined by probes, slight inaccuracies of the measurements, or a location of the probe at some distance forward of the leading edges of the rotor could easily be responsible for these unusually large incidence angles. By means of theoretical methods, which are not described in detail, the velocity distributions along the inducer were determined also in Ref. 13 to verify the test data. However, as shown by Fig. 5 of Ref. 13, the inducer has simply been replaced by a cascade, since at its discharge the velocities on either sides of the blade are shown to be equal, a situation which cannot exist in reality, and which gives questionable value to the argumentation based on it.

Design criteria for the whole rotor passages from the inlet to the discharge are often given in terms of the deceleration ratio W_2/W_{1o} of the relative rotor velocities. From earlier discussions with regard to rotor losses it is evident that not all losses in a rotating impeller depend exclusively on this ratio. They will also be greatly influenced by the performance of the inducer, in particular, on the velocity distribution that exists at the station where the inducer blades join the radial impeller blades. It is necessary to have a good appreciation of the complexities of flows in rotating impellers to avoid over-simplifications and the setting up of design criteria that are based on wrong models. An invaluable contribution to investigating the real flow phenomena in rotating impellers has been made by Fowler[14], who actually measured the velocity distribution in the passages of a large compressor with probes from a platform inside the hub that was rotating with the wheel. Figure 11 has been adapted from a personal communication of Mr. Fowler to the writer. It shows the velocity profiles at seven cross sections of the rotor flow channel of an unshrouded wheel with radial blades at the discharge, when operating at a peripheral speed $U_2 = 17$ ft/s. The meridional flow channel has the smoothly changing contours used for modern designs. Plane 1 of Fig. 11 is at the inlet section of the inducer blades, extending from the leading edge of one blade to the back of a neighboring one, and the blades become radial near plane 3. The zones with reduced velocities at the blade tips that are due to the blade gap and the scrubbing effects along the outside wall, remain almost equal from plane 3 to the discharge plane 7. It is of interest to compare these measured velocity distributions with the theoretical solutions of Eq. 47 for radial blades and incompressible flows. The pattern of the streamlines obtained by Stanitz for a radial impeller with 20 blades is shown in Fig. 3.5.2 of Ref. 3. The velocities are inversely proportional to the distance between neighboring streamlines. The leading surface of a blade will be called the pressure side, the trailing surface of the same blade is its suction side. Hence the direction in a blade channel from the pressure side of one blade to the suction side of the neighboring one, is in direction of rotation of the wheel.

At the outer radius of the wheel (R = 1 in Fig. 3.5.2 of Ref. 3) the theoretical analysis predicts that the velocity in a blade channel increases in direction of rotation, whereas exactly the opposite trend is seen to occur in plane 7 of Fig. 11. However in planes 3 and 4, and to a lesser degree in plane 5, the measured velocity changes agree in the main with the theoretical ones which predict a velocity increase in direction of rotation at all radii. This situation occurs because the theoretical method shows, or is based on the assumption, that at radii smaller than about 70 percent of R_2 the relative velocities are everywhere radial. Then, as determined in Art. 10.6 of Ref. 1, and as shown in Fig. 10(5a), they will increase linearly with the angle along the periphery in direction of rotation. The measured reversal of this behavior, starting from plane 5 to the discharge plane 7, cannot be due to viscous effects only, which are neglected in the theoretical treatment, but must occur because of flow peculiarities that a simplified theory cannot take into account. In his personal communication to the writer, Mr. Fowler also remarked that the directions of the relative velocities at the discharge did not have as large a deviation from the radial direction as Fig. 3.5.3 of Ref. 3 shows. The measured flow distributions suggest that considerable mixing of the different flow strata must occur while they pass through the compressor and it is very unlikely that there exist axisymmetric surfaces. Reference 15 describes tests of single, straight diffusors that were arranged radially and rotated in the test rig of Ref. 14, to examine the effects of centrifugal and Coriolis forces on decelerated flows that move radially outward. Diffusors with different divergence angles where investigated, first while stationary and then while rotating. It was found that considerable differences occur if a diffusor is rotated. Static tests with a two-dimensional diffusor with an included angle of 10° showed the well-known peaked velocity distributions that occur for these angles. If rotating, the peaks flatten out and the flow becomes more stable. These results agree with the conclusions reached earlier about the beneficial effects of a centrifugal force field on decelerated flows, but they show also that boundary layers along rotating walls, where the fluid particles are also affected by Coriolis forces, exhibit different characteristics than those along stationary walls. Similar results have been obtained in Ref. 16 which describes tests of flows through a channel with constant cross section that is rotated about an axis. Because of these conditions, different separation criteria for boundary layers must be applied if they occur on stationary walls or on surfaces that rotate about an axis.

For this reason it is not possible to use conventional boundary layer theories as a means to find permissible deceleration ratio W_2/W_{1o} for the relative flows in impellers, nor can attempts be successful that try to relate this ratio to the NASA diffusion factor, which has proved to be a satisfactory separation criterion for axial compressor bladings which have small flow deflections, hence, where the changes of the

Coriolis forces are small if the blading rotates. Much more fundamental work dealing with boundary layers on rotating walls and investigations with modern flow visualization methods must be carried out before it is possible to establish satisfactory design limits for flows in radial impellers. Recent endeavors that use holography with Pulse-Lasers for investigations of flows in rotating wheels might open entirely new ways to study actual flows in high-speed machines where the effects of centrifugal and Coriolos forces are large.

If the above-mentioned peculiarities of rotor flows are not taken into account one might come to the conclusion, as some sources do, that flow separations will occur in an impeller if W_2/W_{1o} equals 0.6, and that a ratio of 0.62 should be used for design purposes to avoid excessive losses. Such values are obtained from analogies with stationary diffusors or oversimplified boundary layer considerations for, say, linearly changing velocities along a surface, as is the case on the suction side of a blade in an axial compressor cascade. Figure 9 is a diagram for the determination of the deceleration ratio W_2/W_{1o} in accordance with Eq. II(5) of Table II. If, for instance, the limit for this ratio were set at 0.65, the discharge angle α_2 could not be larger than about 60° for a radius ratio R_{1o}/R_2 of 0.7 and $\beta_{1o} = 60°$. For larger discharge angle α_2 the radius ratio R_{1o}/R_2 would have to be decreased. Figure 12 is presented to show these conditions more precisely if the lower limit of W_2/W_{1o} is assumed to equal 0.6 and if the slip factor μ is 0.85. For these conditions and at $\alpha_2 = 75°$, the maximum radius ratio R_{1o}/R_2 could not exceed 0.42 at a relative flow angle $\beta_{1o} = 70°$. Experience with high performance compressors shows however that impellers with radius ratio in accordance with the dashed curve have operated successfully. At $\alpha_2 = 75°$, for instance, and at a radius ratio R_{1o}/R_2 of 0.68 the deceleration ratio is of the order of 0.35 to 0.3, depending on β_{1o}, as shown in Fig. 9 by following path "b" in the diagram. Therefore, if the deceleration ratio W_2/W_{1o} is used as a preliminary design criterion it is permissible to apply minimum values of about 0.3 or even somewhat lower, say, about 0.26. A unique relationship between W_2/W_{1o} and the wheel efficiency η_W cannot be established because of lack of test data but in Paragraph 5 some test results are plotted to show the order of magnitude of η_W. A correlation between W_2/W_{1o} and η_W can probably never be obtained because of the additional rotor losses that depend on a number of additional factors.

For known values of M_{W1}, β_{1o}, and U_2/a_0 it is possible to calculate the wheel radius R_2 with Eq. II(9) of Table II, if the ratio R_{1i}/R_{1o} were known. The quantity k_{B1} is a blockage factor which is primarily depending on the number of inducer blades and their thickness at the inlet throat, although excessively thick boundary layers on the walls of the inlet annulus can affect k_{B1} also. Evidently if U_2/a_0 is known the angular velocity ω is known also, if R_2 has been determined. However ω can be determined directly by Eq. II(10) of Table II, for known or chosen quantities M_{W1} and β_{1o}. Eq. II(10) is useful to establish the necessary rotative speed to handle particular flow rates. If ω is given, because of the prime mover that drives the compressor, Eq. II(10) makes it possible to verify whether a particular flow rate can be handled at this speed. The ratio of axial blade width b_2 and R_2 is obtained by Eq. II(11). The blockage factor k_{B2} is the ratio of the actual flow area at the wheel discharge and the area $2\pi R_2 b_2$, multiplied by an experience factor that depends on the boundary layer thickness on the side walls.

The necessary diffusor exit area A_4 at the radius R_4 is obtained from Eq. II(14) for specified values $\lambda = V_4/V_2$ and known efficiencies η_c. A blockage factor k_{B4} takes account of the displacement thickness of the boundary layers which reduce the actual flow area at the discharge of the diffusor. Section x-x of Fig. 1 is taken to be either the throat of the diffusor where the flow is choked if the absolute velocity V_2 after the rotor is supersonic, or the entrance section of the actual diffusor if V_2 is subsonic. The necessary total flow area of all diffusor channels is denoted by A_x, and k_{Bx} is again an area blockage factor. The area A_x can be determined for both cases if the ratio of the total pressures P_{tx} at station x and P_{t2} at the rotor discharge is known. Although P_{t2}/P_0 could be expressed by Eq. I(19) of Table I and then introduced into Eqs. II(13) and II(14), it is better to use these relations as listed, since it is possible to judge approximately what values the ratio P_{tx}/P_{t2} will have for particular diffusor designs. If V_2 is supersonic the throat area is obtained with the dimensionless critical flow function ϕ_c of Eq. II(14) which has a value $\phi_c = 0.6847$ for $\gamma = 1.4$. For subsonic velocities V_2 the diffusor inlet area can be determined only if the velocity V_x at station x is specified, by assuming a value $\zeta = V_x/V_2$. Usually this ratio is taken to be about 1.02 to 1.05 because a slight acceleration between stations (2) and (x) will produce more uniform flow conditions at the diffusor inlet. For a chosen number of diffusor flow channels, usually arranged between parallel walls, the diffusor widths at inlet and discharge can be determined from A_x and A_4, and the methods described in Paragraph 5 establish the necessary length of the diffusor channels. With this length and the chosen diffusor arrangement it is possible to establish the outer radius R_4 of the diffusor.

4. SIMILARITY CONSIDERATIONS

If effects due to gravity, surface tension, and heat conductivity can be ignored, which is permissible for most flows in turbomachines, the laws of dynamic similarity establish that flow processes of perfect gases in geometrically similar channels are equal in performance if the Reynolds numbers R_e and the velocity ratios $V/\sqrt{R_G T}$ are respectively equal at corresponding stations in the channels. As derived for instance by Ackeret et. al., in Ref. 17, the latter condition can be expressed in terms of equal Mach numbers M, with the additional requirement that the fluids passing through the geometrically similar channels have equal specific heat ratios γ. Reference 17 shows also that the effects of different values of γ are small only if the Mach numbers are less than about 0.6. The reason is that gases with different heat ratios γ produce different relative changes in density if passing through a channel with particular area ratios. Hence the values $V/\sqrt{R_G T}$ cannot remain equal in geometrically similar channels.

Assuming then that gases with equal values of γ are considered only, and that the Reynolds numbers of the flows in the compressors to be compared are in a range where they can vary considerably without largely changing the frictional coefficients; that is, if they are moderately large and if the flow surfaces are rough, dynamic similarity is achieved in geometrically similar machines at equal Mach numbers.

In hydraulic machines, similarity considerations that are based on the so-called specific speed have been used with success and it will now be examined whether it is possible to apply this method also to the compressors considered here that operate at high speed ratios U_2/a_0. Attempts to obtain design limits and to establish the optimum operating range of radial compressors with this means are described in Refs.

18 and 19. In both reference there is used the specific speed N_S (see Eq. III(1) of Table III)

$$N_S = \frac{N\ Q^{\frac{1}{2}}}{H_{is}^{3/4}}$$

similar to the practice in hydraulic pump design. In the latter application, Q, which is the volume flow rate through the machine, is everywhere constant. In a compressor for gases however, where the volume flow rate will change considerably from inlet to discharge, a choice must be made whether Q at station (1), or at, say, station (2) is to be used in Eq. 50. In both references the quantity Q is taken to be the inlet flow rate Q_1 without giving reasons for this choice. As in Refs. 18 and 19, and as shown in Table III by Eq. III(1), the value of N_S depends on the system of units which is used. In the two cited references N_S has the dimension rpm $ft^{3/4}$ $sec^{-1/2}$, which is awkward for purposes of comparison with similar coefficients in other systems of units, and such formulations are not in keeping with the general and very desirable tendency to use dimensionless quantities throughout. For this reason it is more appropriate to use the dimensionless speed n_S, with units as defined by Eq. III(3) of Table III, which for particular conditions has the same value in all consistent systems of units. The quantity n_S is obtained by dividing the value of N_S in the given English units by 129.

Whereas Ref. 18 (Fig. 2.8) simply presents a graph showing a direct correlation of the efficiency of different compressor types with N_S, Ref. 19 uses the so-called specific diameter D_S as an additional parameter, which is defined by (see Eq. III(2) of Table III)

$$D_S = \frac{D\ H_{is}^{1/4}}{Q_1^{1/2}}$$

This quantity is also not dimensionless. However Eq. III(4) defines a dimensionless specific diameter d_S that is obtained from D_S in English units by division with 0.42.

The coefficient ξ_1 of Eq. III(5) represents the ratio of the area of the flow annulus at the compressor inlet and the area $\pi\ R_{1o}^2$, where R_{1o} is the outer radius of the rotor inlet eye. As shown in Table III the quantities n_S and d_S can be expressed also with the chosen parameters of Tables I and II, to obtain Eqs. III(6) and III(7). Both contain ξ_1, so that this ratio can be obtained from either of these relations as shown by Eqs. III(8) and III(9). By equating these expressions there is obtained Eq. III(10), or

$$n_S\ d_S = \frac{2}{(\mu\ \eta_c)^{1/2}}$$

where μ is the slip factor and η_c the compressor efficiency. Since μ is a known quantity for a particular compressor design, and because η_c can be determined with Eq. II(1), the specific diameter d_S is directly related to n_S and there is no reason why both n_S and d_S should be specified for a design with radial blades. Equation III(11) shows that by specifying n_S there can be obtained the radius ratio R_{1i}/R_{1o} for particular values of β_{1o} and R_{1o}/R_2 which are usually chosen on the basis of other considerations, as explained earlier, Equations II(9) and II(10) of Table II, with the known ratios R_{1i}/R_{1o}, would then give directly the necessary radius R_2 or the angular velocity ω for given operating conditions. If the optimum efficiency of a compressor were a unique function of n_S, and if R_{1i}/R_{1o} and/or the other parameters could be adjusted to meet the optimum value, the designer would have a simple criterion for the optimization of compressors.

From Ref. 18 (Fig. 2.8, p. 38) it appears that radial compressors should have the best efficiency for values of N_S between 75 and 85, or for n_S between 0.58 and 0.66. Table III gives an example for design parameters that have been used successfully. In one case, a radius ratio R_{1o}/R_2 of 0.56, in another a ratio $R_{1o}/R_2 = 0.7$ was chosen. For the smaller value of R_{1o}/R_2 it is not possible to design for $N_S = 80$, since the hub/tip ratio at the inlet becomes zero at $N_S = 71$. In an actual design of a compressor that had efficiencies higher than 80 percent, the hub/tip ratio at the inlet was about 0.46 for $R_{1o}/R_2 = 0.56$, hence it operated at $N_S = 60$ and did not have the much lower efficiency predicted by Ref. 18. For the example in Table III with the higher ratio $R_{1o}/R_2 = 0.7$ the ratio R_{1i}/R_{1o} becomes zero at $N_S = 99.4$, and an actual high-performance machine is known to the writer that has an inlet hub/tip ratio of 0.34, hence it operates at $n_S = 0.725$ or $N_S = 93.5$. Thus, the sharp optimum for N_S in Ref. 18 does not occur in reality and $N_S = 80$ or $n_S = 0.62$ is not a design criterion.

It is obvious from Eq. III(6) that all radial compressors have values of N_S between, say, 60 and 110. Lower and higher values would lead to impossible designs which would never be built anyway. The only merit of the specific speed is to find out whether a radial compressor can be built at all for given values of N, Q_1, and H_{is}. If N_S is outside the range of 60 to 110, and if the above-mentioned design conditions cannot be changed, another type of compressor has to be chosen. However, if the relations of Table II were applied, the same conclusions would also be reached immediately even if the specific speed concept had never been invented. In fact its use can also be dangerous if, as might be the case for the example of Table III with $R_{1o}/R_2 = 0.56$, the designer would try to reach the highest possible N_S by making the radius ratio R_{1o}/R_o excessively small or choosing too high a value of R_{1i}/R_{1o} to reduce N_S for $R_{1o}/R_2 = 0.7$. The example also shows that large changes of R_{1i}/R_{1o} have a small influence of N_S except, near the maximum possible value of N_S where R_{1i}/R_o tends toward zero. Further, if $N_S = 80$ would be considered necessary, a large number of high-performance radial compressors would never have been built, much to the detriment of the development of these promising machines, where a better physical understanding of the complicated flow phenomena can still lead to considerably improved performance.

Unfortunately there always exists the tendency in engineering to try to set up simple rules or criteria which make it possible to judge whether or not a design is feasible, without having to go through the strenuous mental processes to try to understand the phenomena that actually occur and to relate them to the fundamental laws of nature. If our only task were to build the same machines over and over again, sometimes

a little smaller, all would be well with this kind of handbook engineering. However, if an engineer believes that improvements are possible, aand if he reflects on what has happened during the past years he cannot doubt that this will be the case, he must not accept the barriers that have been set up by past experience, and be impressed by the achievements that have been made. With a critical mind he has to evaluate what is true and what is false with accepted methods, and his aim must be to try to understand, to search, and to improve. Too often engineers are handlers of formulas or recipes, and there is the tendency to accept their results as correct without much questioning, especially if they are ground out by a computer, without finding out what sort of basic principles and assumptions led to the numbers. In the near future our modern computers may well be the biggest obstacle to imaginative original thinking and the use of new concepts, since for every problem there will very soon exist some sort of a program that can show that everything is known, and that nothing new needs to be added. All one has to know is the necessary format for the input to obtain the desired result, in print, in graphs, even in drawings. The inventive and critical engineer however must take the trouble to find out how the program was established and what basic principles and assumption were made, and must then evaluate the obtained numbers in the light of these conditions.

The biggest objection to the specific speed criteria is however that they do not satisfy the laws of dynamic similarity, even not for the limiting conditions that were assumed earlier. Equation III(6) shows that n_S is independent of the pressure ratio that is produced by a compressor. If all factors in Eq. III(6) are equal for two compressors, they can have different values of U_2/a_0 and therefore widely different blade width b_2 at the rotor discharge. One compressor could operate with subsonic, the other with supersonic velocities at the diffusor inlet. Figure 13 is an adaptation of Fig. 4 of Ref. 19. The curves of constant efficiency $\eta_c = 0.7$ and $\eta_c = 0.8$ and the curves labeled $N_{W1} = 1.0$ and $N_{W1} = 1.2$ for P_{t4}/P_0 were taken from Ref. 19 and redrawn in a bigger scale. Although labeled as lines of constant Mach number in Ref. 19 the curves for N_{W1} = constant are for constant ratios of relative inlet and critical velocity for the total inlet temperature. Equation III(14) of Table III shows how these ratios are related to the actual Mach numbers M_{W1}. Although the differences between N_{W1} and M_{W1} are small at low Mach numbers, the values of M_{W1} vary from 0.94 to 1.01 for $N_{w1} = 1.0$ if β_{1o} changes from 50° to 75°. According to the author of Ref. 19 the curves for $N_{W1} = 1.0$ and 1.2 represent design limits for higher pressure ratios. It is stated that maximum efficiencies will occur for impellers with backward bent blades operating at specific speeds N_S between 90 and 130, and specific diameters D_S between 1.3 and 1.7. The straight lines labeled $\mu\eta_c$ = constant which the present writer drew into the original diagram of Ref. 19 represent Eq. III(10), and relate D_S to N_S for wheels with radial blades at the discharge. Average values for $\mu\eta_c$ for such impellers are 0.7, hence all radial compressor of this type must lie in the vicinity of this curve for $\mu\eta_c$ in Fig. 13. The points labeled (1) to (7) in Fig. 13 represent design points for some actual compressors known to the writer, operating with U_2/a_0 of about unity, and inlet Mach numbers of 0.9 and higher. It is of interest to note that all these points lie on the curve $\eta_c = 0.70$ of Ref. 19 whereas all compressors, even those having N_S-values between 60 and 70, have efficiencies of 80 percent and higher. This situation shows again that the specific speed concept is a highly unsatisfactory design criterion, especially for radially-bladed compressor wheels, since it is impossible to design such machines with operating points that fall inside the closed curve, labeled $\eta = 0.8$ in Fig. 13. It is pointed out in Ref. 19 that the data presented in its Fig. 4 were calculated on the basis of loss considerations. It can be concluded therefore that this loss evaluation is in error or unsuitable for compressors with rotors that have radial blades at the discharge.

What seems more crucial to the writer is the fact that on the basis of Fig. 4 of Ref. 19 (or Fig. 13 of the present article) one might come to the conclusion that it is not possible to build high-speed compressors of the type discussed here with high efficiencies, for instance, as required for gas turbines, and that further developments of these machines might not be undertaken because of "proof" that improvements are not possible. This is again a case which shows that an analysis is no better than its assumption. Since the specific speed has no real physical meaning, unlike the actual similarity parameters such as Reynolds number, Mach number and others, the writer deplores the tendency to express everything in flow machines with N_S, also phenomena on which N_S has really no primary influence. Because of the definition of N_S it is always possible to do so because either rotative speeds and flow velocities, or lengths, can be related to it, and since in all these expressions there then appears N_S in one form or another, depending on what simplifying assumptions were made, the reader is given to believe that N_S has a governing influence on the performance, and that manipulating N_S is all that needs to be done to create an optimum design. Everyone who has observed actual flows in turbomachines in test rigs, and has tried to understand the complexities of these processes will agree that nature just is not so simple that it can be explained by a set of convenient numbers.

5. LOSSES IN RADIAL COMPRESSORS

It has been stated earlier that the wheel efficiency η_W of Eq. 15 is the best measure for the quality of a rotor wheel. As indicated, a number of factors influence η_W, but it will be examined now whether the deceleration ratio W_2/W_{1o} has an overriding effect on η_W, as has been suggested by some sources which state that W_2/W_{1o} should not be smaller than about 0.6 to avoid flow separations. It has already been shown in Fig. 12 that such a limit cannot be used for compressors that operate at high speed ratios U_2/a_0 because the radius ratios R_{1o}/R_2 become too small, and it is then not possible to handle the large changes in volume flow rate from rotor inlet to rotor discharge, that occur at high pressure ratios, with acceptable ratios of axial blade width b_2 and R_2. The example of paragraph 6 demonstrates this condition clearly. If $W_2/W_{1o} \geqq 0.6$ were a realistic criterion, the losses in rotors with high speed ratios would be large and it would be difficult to obtain high efficiencies. Figure 14 is presented to show that many compressors have deceleration ratios that are smaller than 0.6 without a drastic decrease in η_W. The circles in Fig. 14 represent design point data of some of the compressors of Ref. 6, and others that are known to the writer. The points indicated by x and + were calculated from the data given in Ref. 13, and the curves drawn through them represent the change of η_W with operating conditions of a particular wheel at values of U_2/a_0 of 0.83 and 1.02, respectively. All data points are for impellers with radial blades at the rotor discharge, and all compressors operate at high speed ratios, having overall efficiencies in excess of 80 percent.

In contrast to the expected trend that η_W decreases with decreasing values of W_2/W_{1o}, the opposite

could be deduced from Fig. 14, since wheel No. 1 with $W_2/W_{1o} = 0.265$ has the highest efficiency $\eta_W = 0.77$. For each data point in Fig. 14 are also given the ratios R_{1o}/R_2, R_{1i}/R_{1o}, b_2/R_2 and $\Delta x/\Delta R$ of the rotor. The latter ratio establishes the general shape of the meridional channel and the values show that the contours of the meridional flow paths of all compressors must have small curvatures with the exception, maybe, of wheel No. 11. Definite reasons for the higher values of η_W in some designs cannot be given, probably because of the effect of the design of the inducers on the wheel performance. However, it is recognizable from Fig. 14 that high efficiencies η_W are reached either for high ratios R_{1i}/R_{1o} or high values of b_2/R_2. The influence of R_{1o}/R_2 seems small, although most good wheels have values of R_{1o}/R_2 between 0.6 and 0.7. Large ratios R_{1i}/R_{1o} require high relative Mach numbers M_{W1} to pass the flow rate through the eye of the impeller, and high ratios b_2/R_2 are obtained if the absolute flow angles α_2 are large. For high values of M_{W1} the inducer becomes critical, and with large angles α_2 the design of the diffusor, especially the transition between wheel and diffusor throat, becomes a difficult task. It is felt that high performance compressors can be developed if more attention is given to these two problem areas.

From the curves in Fig. 14 it is quite evident that the range in which η_W remains constant for off-design operation becomes smaller the higher the speed ratio U_2/a_0 is, a condition which is, at least in part, responsible for the steeper characteristics of compressors operating at high speed ratios.

The ratio of b_2/R_2 also has an effect on the disk friction loss of an impeller. Assuming that the disk extends to the outer radius R_2; that is, if no scallops are arranged, a frictional moment M_{DF} acts on the back side of the impeller which can be determined by [20]

$$M_{DF} = c_M \, \rho_2 \, D_2^{\,3} \, U_2^{\,2} \tag{49}$$

where c_M depends on the Reynolds number

$$Re = \frac{U_2 \, D_2}{\nu} \tag{50}$$

and the axial gap δ_a between the rotating disk and the stationary wall. The influence of the ratio δ_a/R_2, and the effect of disk roughness, which have been investigated by Refs. 21, 22, 23, and 24 are discussed in Ref. 8. Figure 15 has been established from the results of the quoted references, but experience has shown that the values of c_M can be a multiple of those of Fig. 15 if the flow in the region between the disk and the wall has radial velocity components pointing away from or toward the axis of the impeller. For compressors pumping ambient air the Reynolds number of Eq. 50 varies between about (10^6) and $3(10^7)$ for peripheral speeds between 1000 and 1600 ft/s, and rotor diameters between 3 and 20 inches. Although the average value of c_M from Fig. 15 is then about $1.5 \, (10^{-4})$, it has been shown by experience that $c_M = 2.5(10^{-4})$ is more realistic for actual compressor wheels. For a mass flow rate $\dot{m}$ the power absorbed by an impeller is $\dot{m} \, \mu \, U_2^{\,2}$ in accordance with Eq. 3, which is also equal to $M\omega$, where M is the driving moment, and

$$M = \frac{\dot{m} \, \mu \, U_2^{\,2}}{\omega} = \dot{m} \, R_2 \, \mu \, U_2$$

However

$$\dot{m} = 2 \, \pi \, R_2 \, b_2 \, k_{B2} \, V_{m2} \, \rho_2$$

and, with the relations of Table I,

$$M = 2\pi \, R_2^{\,3} \, \left(\frac{b_2}{R_2}\right) k_{B2} \, \mu^2 \, U_2^{\,3} \, \rho_2 \, \cot\alpha_2 \tag{51}$$

The total moment which has to be overcome by the driving source is then $M + M_{DF}$ and if the efficiency of the compressor is η_c, without taking the disk friction moment into account, the actual compressor efficiency η of the machine is $\xi_{DF} \, \eta_c$, and

$$\xi_{DF} = \frac{M}{M + M_{DF}} = \frac{1}{1 + (M_{DF}/M)}$$

Then by Eqs. 49 and 51

$$\xi_{DF} = \frac{1}{1 + \dfrac{(4/\pi) \, c_M \, \tan\alpha_2}{(b_2/R_2) \, \mu^2 \, k_{B2}}} \tag{52}$$

It can be noted that ξ_{DF} is independent of the mass density ρ_2 and R_2 since both M and M_{DF} are proportional to these quantities. Hence Eq. 51 holds for all impellers with radial blades the outer radius R_2. Equation

52 is plotted in Fig. 16. This figure shows that with small ratios b_2/R_2 there can occur a considerable reduction in efficiency, which is the greater the larger the angle α_2 is. For $\alpha_2 = 75°$ the ratio (b_2/R_2) k_{B2} μ^2 should not be less than about 0.06 to limit ξ_{DF} to 0.98. Then, with $k_{B2} = 0.95$ and $\mu = 0.90$, the ratio of b_2/R_2 must not be smaller than 0.08 to avoid efficiency reductions because of disk friction moments.

Although the above limit for b_2/R_2 has been obtained by considering the frictional moment at the back side of the impeller, it is very probably that the so-called scrubbing loss of the blade tips at the outer contour of the meridional flow path produces frictional moments which are of similar nature and of the same order of magnitude as the disk friction moments. Moreover, as shown in Fig. 15 for the latter, these moments will also not be greatly influenced by the ratio of tip clearance and R_2 if it is of the order of 0.05, which constitutes a normal to lower limit for most designs. The scrubbing loss is similar to the loss due to disk friction because the boundary layer along the stationary outer wall is rotated by the blade tips. If the losses at the blade tip would be taken to be those due to the flow of the fluid from the pressure side to the pressure side of the blade across the blade clearance, it would be inconceivable that the reductions in compressor efficiency with increased tip clearance are as small as shown by the measurements of Ref. 25. The same behavior has been found in radial turbines[8] where an increase of the ratio of tip clearance and axial blade width b from 4 percent to 10 percent produced practically no drop in efficiency, but if 10 percent was exceeded there occured a radical efficiency reduction. The sudden drop beyond the 10 percent clearance ratio could occur because of massively increased leakage flows across the blade tips once they are outside the wall boundary layer.

Experience has also shown that the ratio of blade width b_2/R_2 should not be less than 8 percent. The value of c_M in Eq. 51 for the representation in Fig. 16 has actually been increased from the average value for disk friction (~ 1.5 (10^{-4})) to $2.5(10^{-4})$ to demonstrate that this limit is very likely due to the combined effects of disk friction and scrubbing loss. For this ratio of b_2/R_2 and for properly designed inducer sections of an impeller, with meridional contours having small and smoothly changing curvatures, it should be possible to obtain wheel efficiencies η_W of between 0.75 and 0.80 for $b_2/R_2 = 0.08$ if the ratios R_{1i}/R_{1o} are not less than about 0.5.

A large portion of the total losses in radial compressors occurs between the discharge of the wheel and the diffusor throat. The non-uniform distribution of the relative velocities at the rotor discharge produces a non-steady and greatly irregular absolute flow at this station which must be directed toward the diffusor inlet, preferably in a manner that provides uniform flow conditions at this station. If this uniformity is not achieved it is very unlikely that the diffusor proper can perform its function with minimum losses. Very limited data are available for the design of and the losses in these transition sections. Figure 17 shows a typical distribution of the static pressures along the side walls of such a diffusor inlet for a machine that has a value of M_{V2} of about 1.18. Firstly it is clear that the absolute flow is irregular, judging from the change of the pressures in peripheral direction at the wheel discharge. Secondly, the design of the diffusor inlet is not as good as it is desirable because fluid particles undergo compressions and expansions before they reach the diffusor throat. Moreover, Fig. 17 also shows the futility of trying to apply simplified calculating method for this part of the process in the compressor.

Of particular importance is the design of the leading edge of the diffusor blade since the slightest misorientation will produce major disturbances usually with the effect that the flow rate at which the compressor surges is too close to its design flow rate. This condition occurs if the mean angle of the lip section with respect to the radial direction is too large or too small, and since the optimum angle depends on the performance of the rotor, it is not possible to indicate exactly how the transition section must be designed. Experiences have made it obvious, however, that theoretical methods which prescribe a logarithmic spiral or other shapes for the curved part of the transition section overlook the fact that the flows to be handled are so far from being uniform that is almost impossible to obtain optimum solutions without extensive experimental work that investigate the performance of different shapes, not only with respect to optimum efficiency but also to obtain the necessary surge margin. One of the major problems with experiments however is the accurate measurement of the static pressures in these irregular flows. In most cases it is found that Pitot-static pressure probes with even the smallest possible tube diameters are sufficient to change the flow pattern, in fact they usually throw the compressor into surge if it is operating near the design point, so that one has to rely on static wall pressure taps to investigate the effectiveness of different designs. Schlieren pictures for supersonic conditions do also not give information that can be interpreted with ease because of the three-dimensional character of the flow, not to mention the difficulties associated with the arrangement of the necessary optical system. It is therefore quite difficult to measure the true average static pressure after a compressor wheel, and because of the uncertainties that arise if the average static wall pressures at R_2 is identified with it, the separation of the losses into those originating in the wheel, and those occuring in the transition section to the diffusor, is equally difficult. For this reason the evaluation of the actual wheel efficiency η_W may be associated with errors and this could be the reason why it is often impossible to correlate experimental data from different sources. Laser systems were mentioned earlier as an experimental tool to investigate flows in turbomachines, and if the so-called velocimeter, using two laser beams for the determination of the actual magnitude and direction of the velocity in the vicinity of a particular station has been perfected, this instrumentation would be the best possible means to observe the true flow patterns in machines, not only qualitatively but also quantitatively.

In accordance with a limited amount of test data with a compressor operating at $U_2/a_0 = 1.4$, with $M_{V2} = 1.18$, the approximate ratio of the total pressure P_{t2} at the rotor discharge and P_{tx} at the throat of the diffusor was found to be about 1.14, giving an efficiency of the transition section of 0.63. This efficiency is defined as the ratio of the actual static temperature rise to obtain sonic velocity at the throat to that of an isentropic compression for the same pressure ratio. The average discharge flow angle α_2 was about 75°. It seems however that the transition section of the compressor in question could be improved, so that the numbers given above represent only orders of magnitude and not values that cannot improved.

Although a large number of tests have been carried out with subsonic diffusors by many sources, these data cannot be applied directly to the diffusors of compressors with high speed ratios, especially if the

Mach numbers at the diffusor inlet are close to unity. Moreover, it has almost become standard procedure to apply the so-called equivalent cone angle of straight, round diffusors to decelerating flow channels with other cross sections. This procedure converts the inlet and discharge flow areas of a diffusor with arbitrary cross sections into circular ones, either with equal areas or by means of the hydraulic diameter, and then determines the equivalent cone angle with these diameters and the actual length of the diffusor. Either of the two methods for the determination of the equivalent cone angle breaks down for particular designs, or gives results that are in disagreement with actual test data.

An attempt to establish a more rigorous calculating method for arbitrary channels has been made by Traupel[26], primarily for incompressible flows and approximations for the compressible case, but it is then suggested that the equivalent cone angle be used again as a criterion for the permissible deceleration. A different approach is possible, however, which has a minimum of simplifying assumption and has proved to be valid for diffusors of arbitrary geometry, even axisymmetric ones with curved meridian channels and annular cross sections, for instance those arranged after turbomachines to deflect the flow from the axial to the radial direction. The derivation and the use of the equations are given in Table IV. From the laws of conservation of momentum, mass, and energy, combined with the first law of thermodynamics, there is obtained Eq. IV(10) which relates the frictional heat $T ds$ to the work necessary to overcome the action of the shear stresses along the channel walls. With the so-called referred mass flow rate $\dot{m}_{r3}$ at the diffusor inlet, which is a dimensionless quantity defined by Eq. IV(14), there is then obtained the principal equation IV(15). This equation is of the form $dX_1 = dX_2$, where dX_1 contains the properties of state ρ, p, and s, at the stations along the channel length, and dX_2 is depending only on the channel geometry and the skin friction coefficient c_f. Actually, for a given diffusor the variables in dX_1 are not independent of the changes of the channel geometry along its length L that occur in dX_2. However, if one were to adjust the flow areas A and the wetted perimeter C of the sections between the inlet and the exit in such a manner that the thermodynamic process of the fluid in the channel would follow a polytropic law, it would be possible to integrate dX_1 independently from dX_2 since s, and ρ are then unique functions of the pressure p for a constant polytropic efficiency η_p or a constant loss coefficient $\zeta = 1 - \eta_p$. Conversely, if an average skin friction coefficient $\bar{c}_f$ is introduced, the value of X_2 is obtained by integrating the quantity $d\Omega$ from diffusor inlet to diffusor discharge, establishing the so-called diffusor shape factor Ω which is identical with the value Φ of Ref. 26. The diffusor shape factor is a dimensionless quantity which depends only on the area and perimeter changes along the length L of the diffusor.

From the integration of dX_1 there is obtained the quantity X_1 as a unique function of the static pressure ratio in the diffusor, γ, and the polytropic loss coefficient ζ. For $\gamma = 1.4$ the function X_1 is plotted in Fig. 18 for different values of ζ, as function of the pressure ratio p_4/p_3. Obviously the conditions of state change monotonously during the polytropic process from p_3 to p_4 in Fig. IV(2), and the function X_1 only holds for such changes. Hence if the area changes in the diffusor would be such that compressions in one part would be followed by expansions in another part, the function X_1 could not take care of the situation, since for an expansion the polytropic law established by Eq. IV(7) would produce an entropy decrease in violation of the second law of thermodynamics. However, even for smoothly changing areas in the diffusor, which it will have in any case, the thermodynamic process in the T-s diagram of Fig. IV(2) might not follow the isentropic line which is shown there, but one which curves either upward or downward from it. It must be recognized however that the value of the function X_1 will not be greatly changed by different distribution of p along L, similar to the integral of Tds which is about equal to $(T_3 + T_4)$ $(s_4 - s_3)/2$ almost independent of how the process proceeds from station (3) to station (4), provided it goes along a smooth and fairly regular curve in the T-s diagram.

Moreover, the polytropic loss coefficient ζ is not assumed a priori, but adjusted to satisfy the equation of continuity at the diffusor discharge for a specified average skin friction coefficient. The necessary iteration to solve this problem is explained in Table IV. The method employs the dimensionless flow function Φ which is plotted in Fig. 18 also, with the ratio of total and static pressure that correspond to an isentropic process as variable. Blockage factors for the diffusor areas are introduced to take account of the boundary layer thickness.

For small pressure ratios p_4/p_3; that is, for low Mach numbers at the diffusor inlet, the method leads to relations that are identical with those commonly applied for the loss evaluation for incompressible diffusor flows. In particular, the average skin friction coefficient is equal to

$$\bar{c}_f = \frac{C_{PRi} - C_{PR}}{\Omega} \tag{53}$$

where C_{PRi} and C_{PR} are the so-called ideal and actual recovery factors, which express the increase in static pressure as percentage of the kinetic energy of the flow at the diffusor inlet. The quantity Ω is the diffusor shape factor defined by Eq. IV(19).

Figure 19 shows the skin friction coefficients $\bar{c}_f$ obtained with Eq. 53 from the experimental data of Ref. 27 for two-dimensional diffusors. Except for the diffusor with $L_0/a_i = 48$, which is unduly long, the data lie within a relatively small band, with the test data for a thin displacement thickness of the boundary layer at the inlet near its lower boundary. It is of interest to note that for large values of Ω the skin friction coefficients are very nearly equal to those of fully developed turbulent flows along moderately rough surfaces in pipes or along plates, as shown by Ref. 20 (p. 587, and p. 611). The results of Ref. 28 which were obtained, in part, at high subsonic speeds give values of $\bar{c}_f$ that lie in the same band as in Fig. 19, indicating that the skin friction coefficients $\bar{c}_f$ are directly related to Ω for different types of cross sections, and at speeds where compressibility effects cannot be disregarded.

From Eq. IV(18) of Table IV it is seen that X_2 is directly proportional to $\bar{c}_f \Omega$ for the same data points of Ref. 27 as plotted in Fig. 19. Hence it appears that a diffusor with a shape factor Ω equal to 10 represents an optimum solution. If Ω is smaller the efficiency decreases radically and for values of Ω larger than 10 a diffusor does not make full use of the possible adverse pressure gradient that a boundary layer can sustain without flow separations. The criterion $\Omega = 10$ has been used by the writer with

This product is shown in Fig 20

success for a number of diffusor designs, and a variety of different diffusor shapes is now being tested at NPGS to verify the validity of the criterion at high inlet velocities and with inlet flow distortions.

As shown also in Ref. 26, the shape factor of a round conical diffusor with inlet radius R_i, length L, and the half-angle ϵ of its divergence is

$$\Omega = \frac{1}{2 \tan \epsilon} \left[1 - \frac{1}{(1 + 2(L/R_i) \tan \epsilon)^4} \right] \tag{54}$$

For conical diffusors where L is large with respect to R_i, Eq. 54 gives a divergence angle of $2\epsilon = 5°45'$. The influence of the ratio L/R_i is small if L/R_i is larger than about 10. Two-dimensional straight diffusors with constant depth b, and widths a_i at the inlet and a_d at the discharge, determined by $a_d = a_i + 2 L \tan \epsilon$, where ϵ is again the half-angle of the channel, have shape factors

$$\Omega = \frac{L/a_i}{1 + 2(L/a_i) \tan \epsilon} \left[1 + \frac{1}{1 + 2(L/a_i) \tan \epsilon} + \frac{2 \, a_i}{b} \right] \tag{55}$$

If the diffusor of Fig. 17 had a ratio $a_i/b = 2.4$, the value of Ω for $\epsilon = 5°$ and $L/a_i = 10$, is about equal 22.4, which appears to be excessive. Hence the diffusor should have a divergence perpendicular to the plane of drawing also to increase b_i at the inlet to b_d at the discharge. For shapes of this type the expression of Eq. IV(19) for Ω leads to complicated integrals. However with a simple graphical integration for a half-angle of divergence of about $2°$ that produces a ratio $b_d/b_i = 2.4$ with the widths a_i and a_d remaining unchanged, the diffusor form factor is reduced to about 11.2. A diffusor channel for this value of Ω for compressors is very likely very close to the optimum possible solution because of then non-uniform flow conditions that exist at its inlet.

Because of these disturbances, the values of $\Omega \, \overline{c_f}$ presented in Fig. 20 should also be increased, say, from 0.10 to about 0.15, or 0.20, for Ω of about 10. How these values affect the diffusor efficiency will be shown with a simplified approach of the diffusor design method of Table IV. It is assumed that the Mach number M_{V3} at the throat is unity, but the method is not restricted to this value. The flow function Φ_3 of Eq. IV(22) is then equal to 0.6847 in accordance with Fig. 18, and $P_{t3}/p_3 = 1.8929$. From Eq. IV(28) for for $M_{V3} = 1$, $\gamma = 1.4$,

$$\dot{m}_{r3} = (0.6847) (1.2)^3 = 1.1832$$

From Eq. IV(18)

$$X_2 = \frac{1.1832^2}{2} \, \overline{c_f} \, \Omega = 0.7 \, \overline{c_f} \, \Omega$$

Hence, $X_2 = 0.07$ for $\overline{c_f} \, \Omega = 0.1$, $X_2 = 0.14$ for $\overline{c_f} \, \Omega = 0.2$, and these values are equal to the values of the function X_1 which is plotted in Fig. 18. It will now be assumed that the area ratio A_3/A_4 of the diffusor is $1/6.6 = 0.151$ as is the case for the design of Fig. 17 with a half-angle of divergence of $2°$ to increase the depth b also. With blockage factors $k_{B3} = 0.96$ and $k_{B4} = 0.90$, by Eq. IV(29)

$$\Phi_4 = (0.6847) (0.151) (0.96/0.9) (P_{t3}/P_{t4}) = 0.11 \, (P_{t3}/P_{t4})$$

Assuming that P_{t3}/P_{t4} is about 1.05, the value of Φ_4 is 0.115. From the plot of Φ vs P_t/p_t it can be seen that for $\Phi_4 = 0.115$, or slight changes of it on account of a wrongly chosen value of P_{t3}/P_{t4}, the value of P_{t4}/p_4 will not be higher than 1.02 because of the large change of Φ with P_t/p_t close to unity. Then,

$$\frac{p_4}{p_3} = \frac{P_{t3}/p_3}{P_{t4}/p_4} \frac{P_{t4}}{P_{t3}} = \frac{1.8929}{1.02} \left(\frac{1}{1.05} \right) = 1.77$$

The approximate values of ζ can then be read from Fig. 18 at the intersection of the lines for the known values of X_1 and for $p_4/p_3 = 1.77$. For $\overline{c_f} \, \Omega = 0.1$, or $X_1 = 0.07$, there is $\zeta = 0.070$, and for $\overline{c_f} \, \Omega = 0.2$, or $X_1 = 0.14$, one finds $\zeta = 0.130$, giving approximate values of the diffusor efficiency of 0.93 and 0.87, respectively, without taking account of the reheat effects that are reflected in Eq. IV(35). The values of ζ thus obtained can then be used to determine the pressure ratio p_4/p_3 more precisely, by taking the pressure ratio P_{t3}/P_{t4} to be that obtained from Eq. IV(33) with the approximate pressure ratio $p_4/p_3 = 1.77$.

6. SAMPLE CALCULATIONS

To demonstrate the effectiveness of the developed performance parameters, and the help of the figures, the dimensions of an impeller for an air compressor with a pressure ratio of eight will be established for the following conditions:

$$\dot{m} = 2.5 \text{ lbm/s} = (2.5/32.174) \text{ slug/s}$$

$$P_0 = 14.7 \text{ psia}; \ T_0 = 520°R$$

$$P_{t4}/P_0 = 8$$
$$R_G = 1716.48 \frac{\text{ft-lb}}{\text{slug, } {}^\circ R} \; ; \; \gamma = 1.4$$

From Eq. 5

$$a_0 = 1117.8 \text{ ft/s}$$

Assuming $\mu = 0.9$; $\eta_c = 0.82$, from Eq. II(3), or Fig. 4,

$$U_2/a_0 = 1.658$$

hence

$$U_2 = 1853.4 \text{ ft/s}$$

Figure 8 clearly shows that for this U_2/a_0 and reasonable ratios R_{1o}/R_2 the relative inlet velocity M_{W1} must be supersonic. For $M_{W1} = 1.15$ and $\beta_{1o} = 70^\circ$ there is from Fig. 8, or Eq. II(4),

$$\frac{R_{1o}}{R_2} = 0.642$$

Judging from Fig. 4 it is necessary to choose $\alpha_2 = 74^\circ$ to obtain a value of W_2/W_{1o} of about 0.4. More precisely from Eq. II(5)

$$\frac{W_2}{W_{1o}} = 0.405$$

For a chosen value of the wheel efficiency η_W of 0.7, there are from Eq. 21

$$\Psi = 0.629; \; \Psi^2 = 0.394$$

and the usual rotor efficiency η_R defined by Eq. 12, in accordance with Eq. 24, is

$$\eta_R = 0.88$$

With these values by Eq. II(9)

$$[1 - (\frac{R_{1i}}{R_{1o}})^2] \, k_{B1} = \frac{\dot{m}\sqrt{R_G \, T_0}}{\pi \, R_2^2 \, P_0} \quad (5.7138)$$

and from Eq. II(11)

$$\frac{b_2}{R_2} \, k_{B2} = \frac{\dot{m}\sqrt{R_G \, T_0}}{\pi \, R_2^2 \, P_0} \quad (0.4127)$$

and, for approximate values $k_{B1} = 0.85$, $k_{B2} = 0.95$, by division of two above-listed relations,

$$\frac{b_2/R_2}{1 - (R_{1i}/R_{1o})^2} = 0.0646$$

Evidently this ratio holds for all compressors for the chosen conditions, irrespective of the flow rate and the inlet pressure. For chosen radius ratios R_{1i}/R_{1o} there are:

$$R_{1i}/R_{1o} = \quad 0.2 \quad 0.3 \quad 0.4 \quad 0.5$$
$$b_2/R_2 = \quad 0.062 \quad 0.059 \quad 0.054 \quad 0.048$$

All these ratios are too small to obtain the desired efficiency. They were obtained because R_{1o}/R_2 was chosen too small and the angle β_{1o} is too large, and both these values were taken to maintain a low Mach number M_{W1}. For a second try, let:

$$R_{1o}/R_2 = 0.7; \; \beta_{1o} = 60^\circ; \; \alpha_2 = 75^\circ$$

Then, from the inverse of Eq. II(4), expressing M_{W1} as function of R_{1o}/R_2 and β_{1o},

$$M_{W1} = 1.3198$$

From Eq. II(5)

$$\frac{W_2}{W_{1o}} = 0.360$$

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Radial Impeller

Inducer

View from A
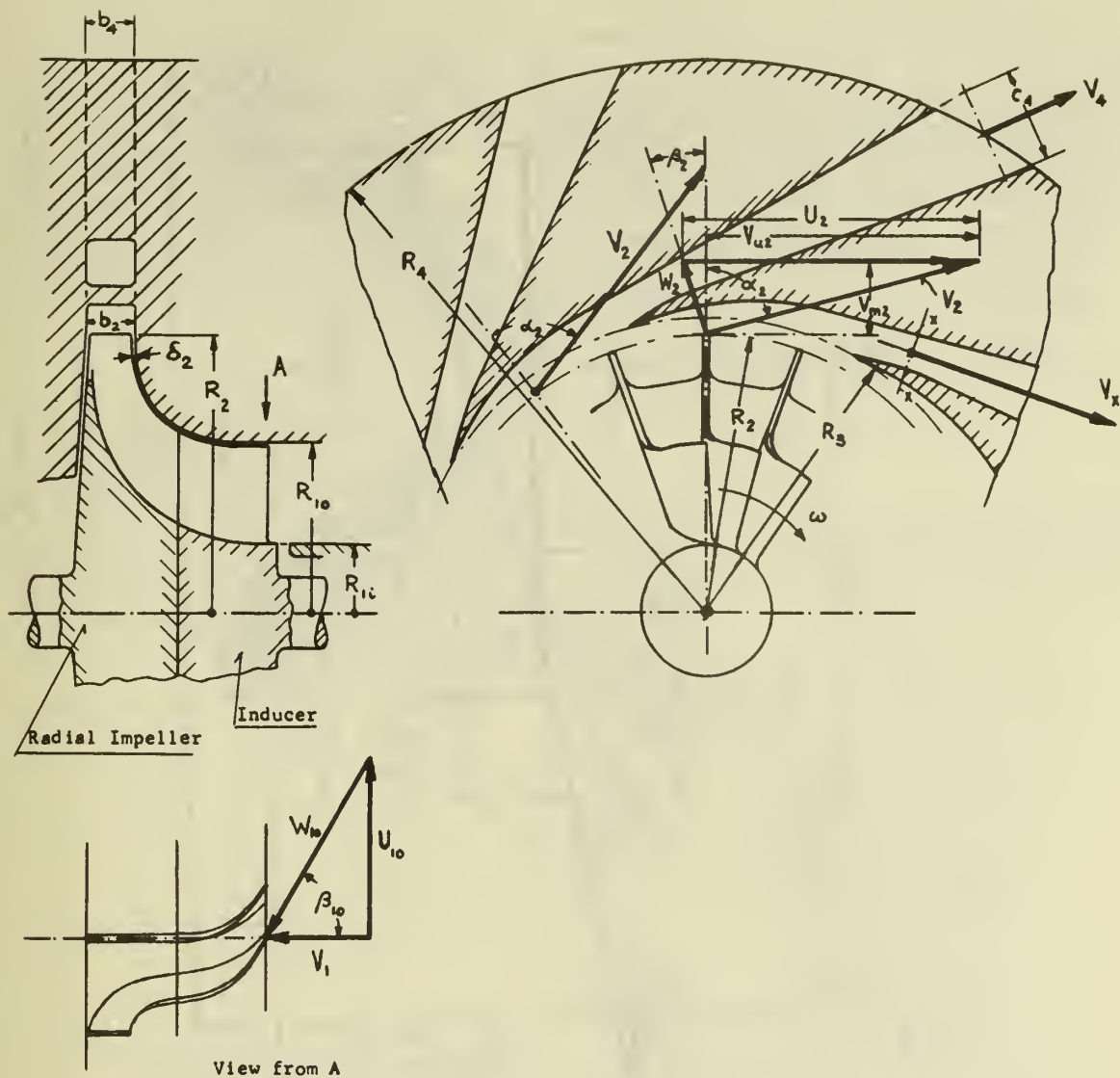
FIG. 1 RADIAL - FLOW COMPRESSOR

    R - Radius
    V - Absolute Velocity
    W - Relative Velocity
    U - Peripheral Speed
    α - Absolute Flow Angle
    β - Relative Flow Angle
    b - Axial Channel Width
    c - Height of Diffusor Channel

Subscripts:
    1 - refers to rotor inlet
    2 - refers to rotor discharge
    3 - refers to inlet lip of diffusor blades
    x - refers to throat of diffusor channel
    4 - refers to discharge of diffusor channel

    m - refers to meridional direction
    u - refers to peripheral direction
    i - refers to inner radius at compressor inlet
    o - refers to outer radius at compressor inlet

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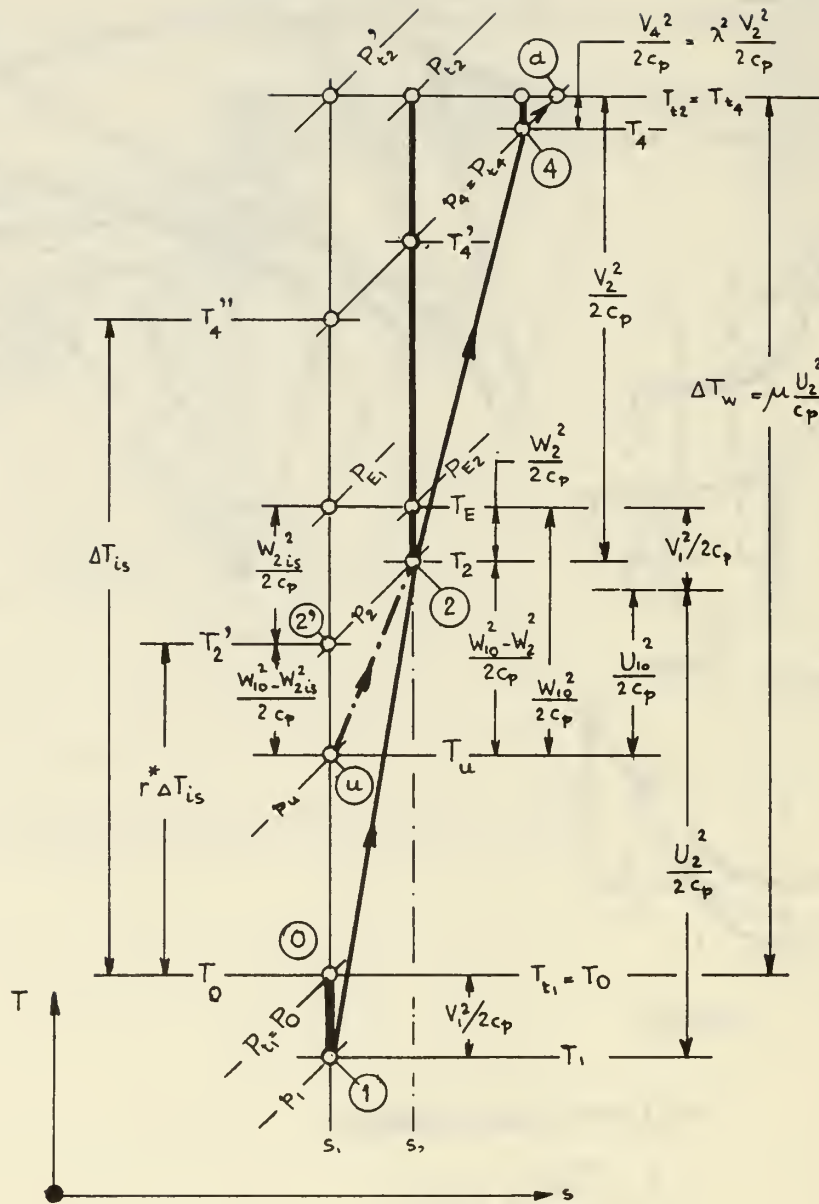
FIG.2 TEMPERATURE-ENTROPY DIAGRAM OF COMPRESSION PROCESS
IN COMPRESSOR OF FIG. 1

c_p - Specific Heat at constant Pressure

p - Static Pressure

P_t - Total Pressure

T - Static Temperature

T_t - Total Temperature

s - Entropy

λ - V_4 / V_2

(For other symbols and station designation see Fig.1)

FIG. 3a   SLIP FACTOR μ FOR δ_2/b_2 = 0.05 AND $\varepsilon = 90°$

$\frac{\mu}{\mu_{0.05}}$
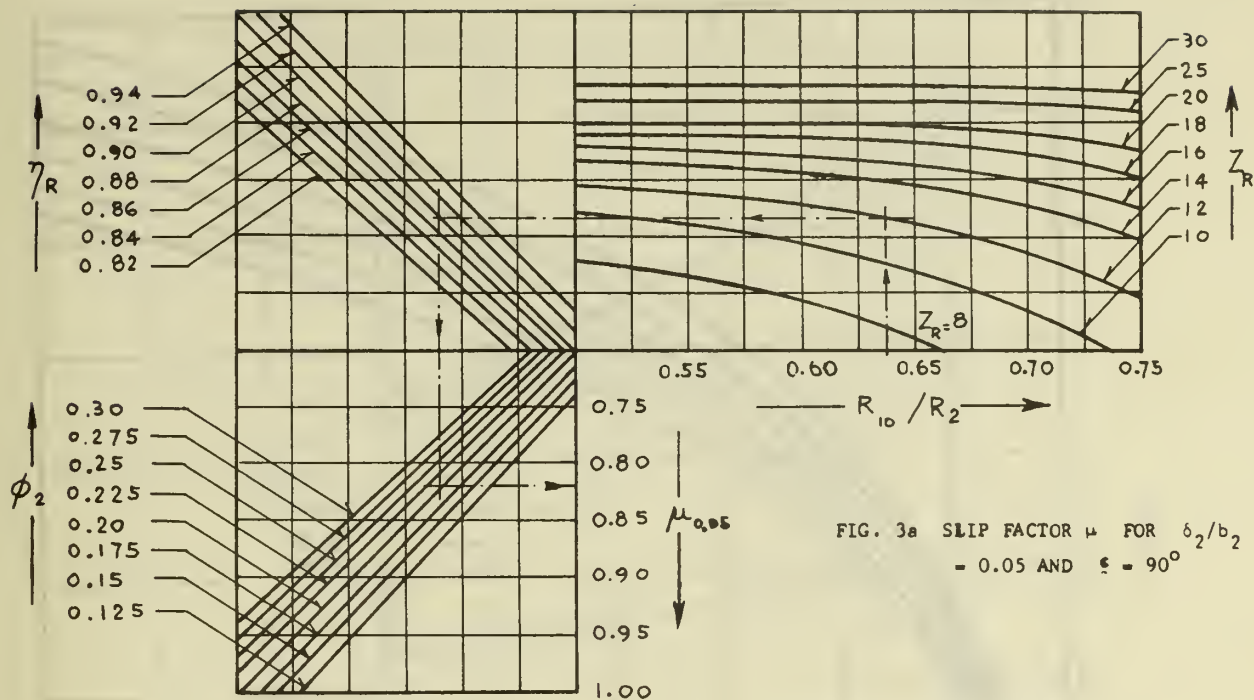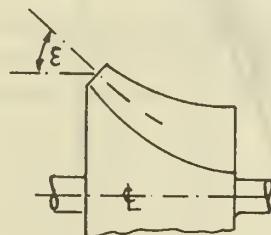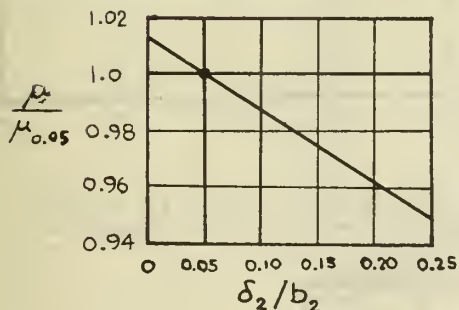
FIG. 3b   CORRECTION FACTOR FOR RATIOS
OF TIP CLEARANCE δ_2 AND AXIAL
BLADE WIDTH b_2 DIFFERENT FROM 0.05
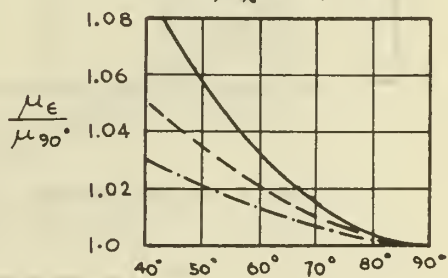
FIG. 3c   CORRECTION FACTOR FOR
MIXED-FLOW IMPELLERS

FIG. 3   SLIP FACTOR FOR RADIAL COMPRESSOR IMPELLERS WITH
RADIAL BLADES AT DISCHARGE

(Figures were adapted from Refs. 5 and 6)

ϕ_2 - $\dfrac{V_{m2}}{U_2}$ (see Eq. II(8) of Table II)

η_R - Rotor Efficiency (see Eq. 12)

Z_R - Number of Rotor Blades

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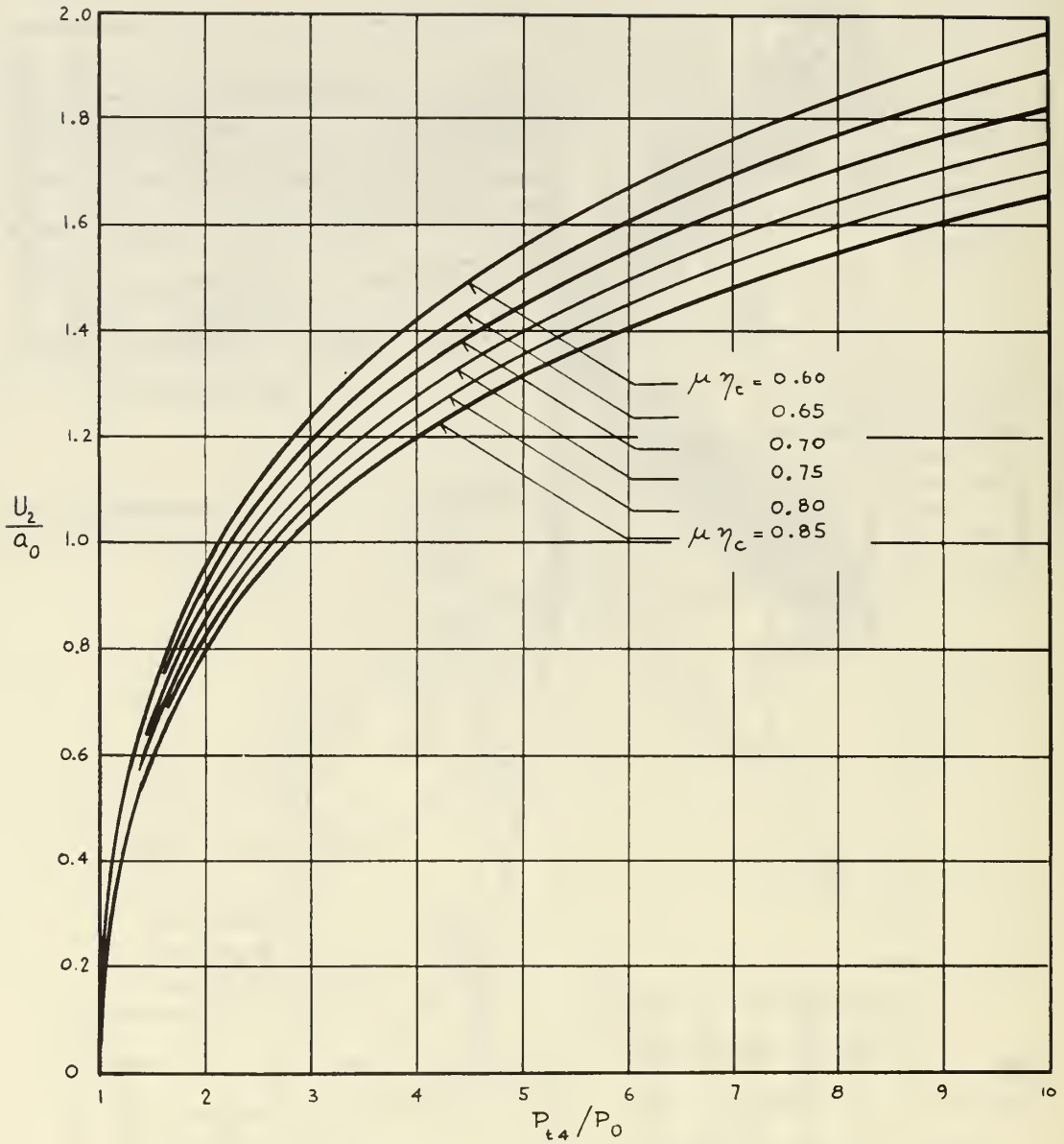
FIG. 4 RELATION BETWEEN PRESSURE RATIO AND U_2/a_0 FOR $\nu = 1.4$ (Eq. II(3))
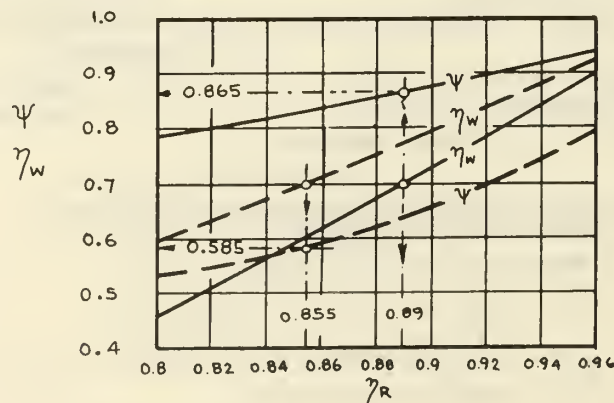
FIG. 5 RELATION BETWEEN ROTOR LOSS FORMULATIONS WITH η_R, η_W AND Ψ (Eqs. 22 and 24)

————— $\alpha_2 = 60°$
— — — $\alpha_2 = 75°$ } $\beta_{10} = 70°$, $R_{10}/R_2 = 0.7$, $\mu = 0.85$

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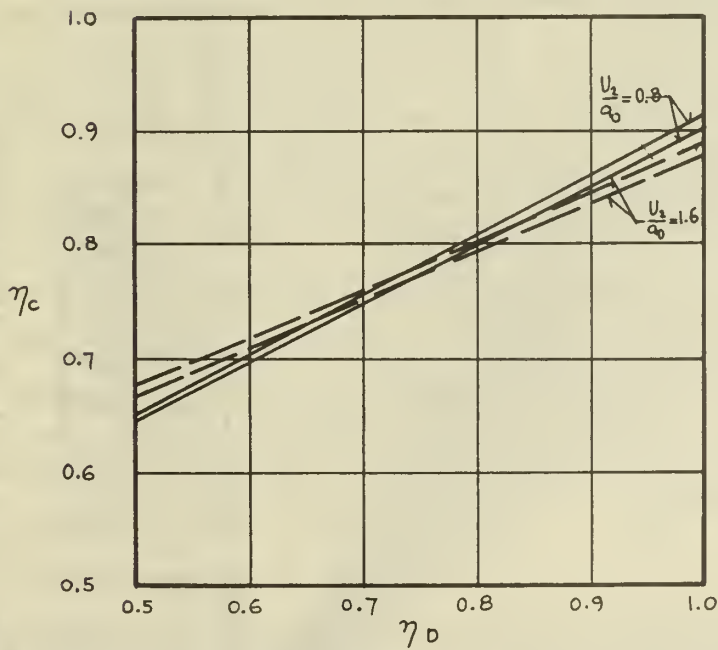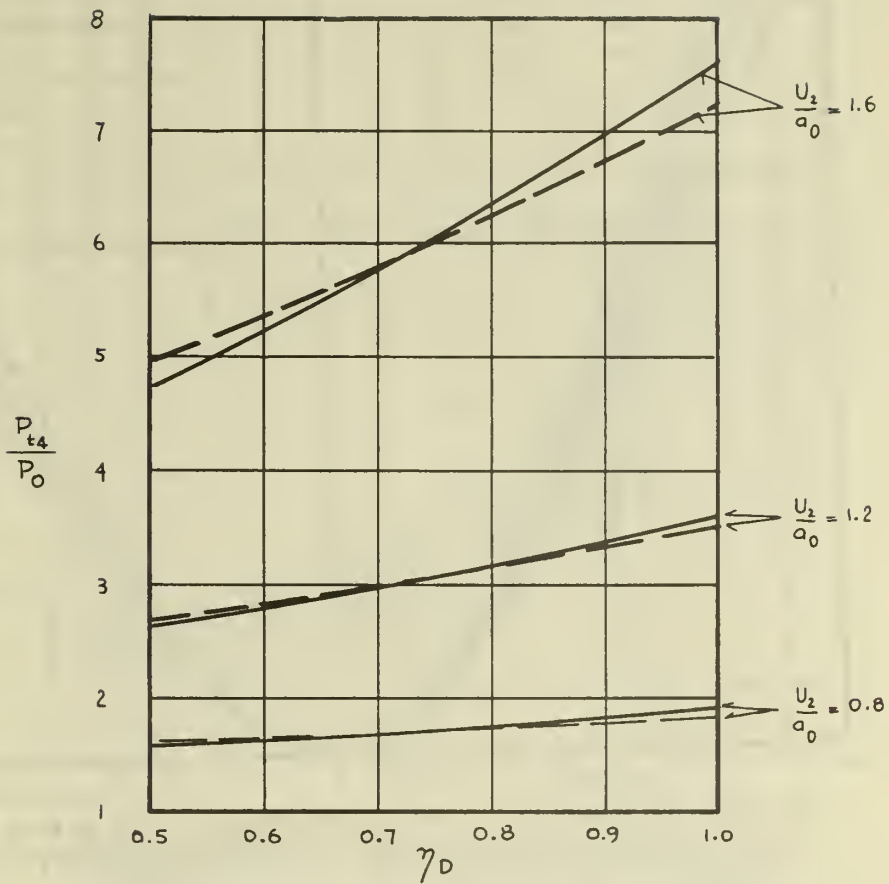
FIG.6 INFLUENCE OF DIFFUSOR EFFICIENCY η_D ON EFFICIENCY η_c AND

PRESSURE RATIO P_{t4}/P_0 OF COMPRESSORS AT DIFFERENT SPEED RATIOS U_2/a_0

$\beta_{1o} = 70^o$; $R_{1o}/R_2 = 0.7$; $\lambda = V_4/V_2 = 0.2$

——— $\alpha_2 = 60^o$; $\eta_W = 0.7$; $\eta_R = 0.89$; $\psi = 0.865$

— — — $\alpha_2 = 75^o$; $\eta_W = 0.7$; $\eta_R = 0.855$; $\psi = 0.585$

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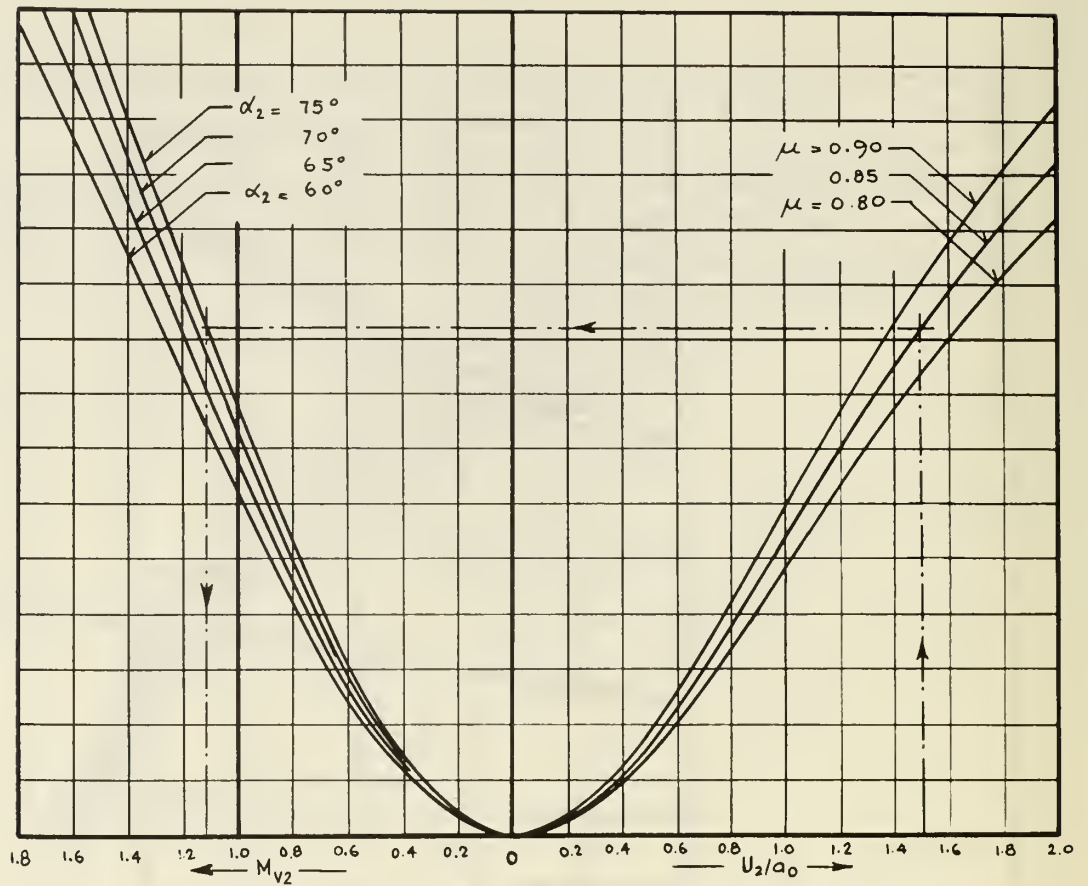
FIG.7 RELATION BETWEEN MACH NUMBER M_{V2} OF ABSOLUTE VELOCITY AT ROTOR DISCHARGE AND SPEED RATIO U_2/a_0 , FOR $\gamma = 1.4$ (Eq. II(6) of Table II)
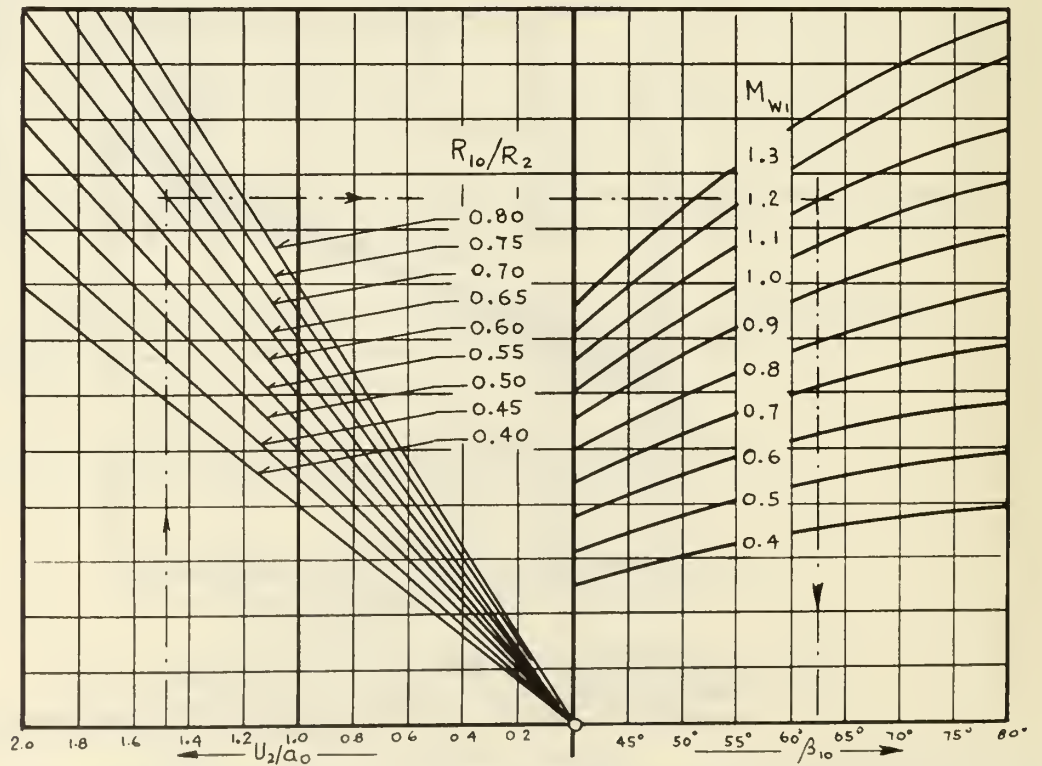
FIG.8 RELATION BETWEEN SPEED RATIO U_2/a_0 ,RADIUS RATIO R_{10}/R_2, VS. MACH NUMBER $M_{W1} = W_{10}/a_1$ AND RELATIVE FLOW ANGLE β_{10} AT OUTER RADIUS R_{10} OF COMPRESSOR INLET, FOR $\gamma = 1.4$.
(Eq. II(4) ot Table II)

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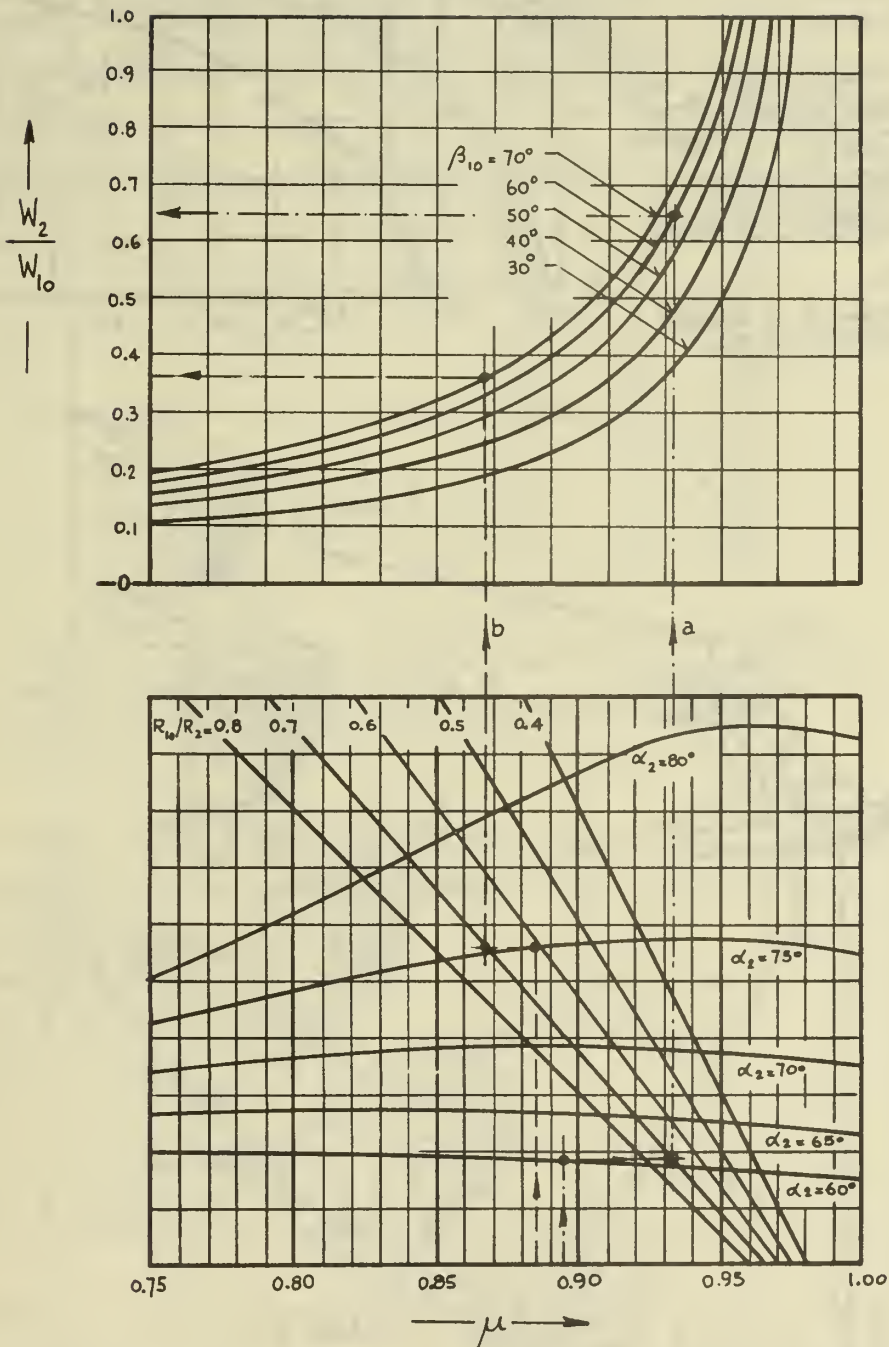
FIG.9 DIAGRAM REPRESENTING EQUATION II(5) OF TABLE II, SHOWING RELATIONSHIP
BETWEEN DECELERATION RATIO W_2/W_{1o} OF RELATIVE ROTOR VELOCITIES,
RADIUS RATIO R_{1o}/R_2, RELATIVE INLET FLOW ANGLE β_{1o}, ABSOLUTE
ROTOR DISCHARGE ANGLE α_2, AND SLIP FACTOR μ.

FIG. 10 MACH NUMBER M_{1x} OF
RELATIVE INLET VELOCITY AT
RADIUS R_{1x} FOR $M_{W1} = 1.3$ AT
OUTER RADIUS R_{1o} OF WHEEL
INLET, AT DIFFERENT FLOW ANGLES
β_{1o} AT R_{1o}

M_{V1} = Mach number of Absolute
Velocity V_1 at Inlet

PLANE 1

PLANE 2

PLANE 3

PLANE 4

PLANE 5

PLANE 6

PLANE 7
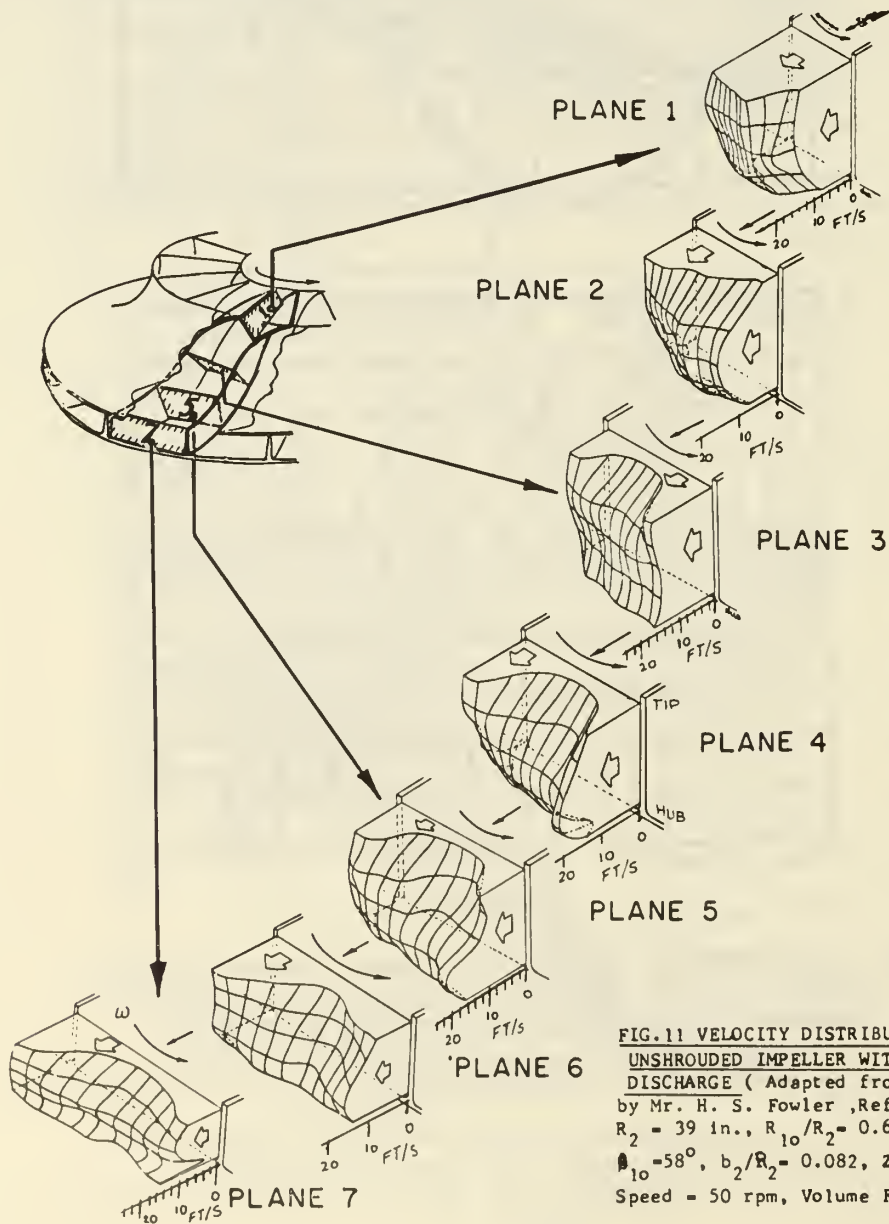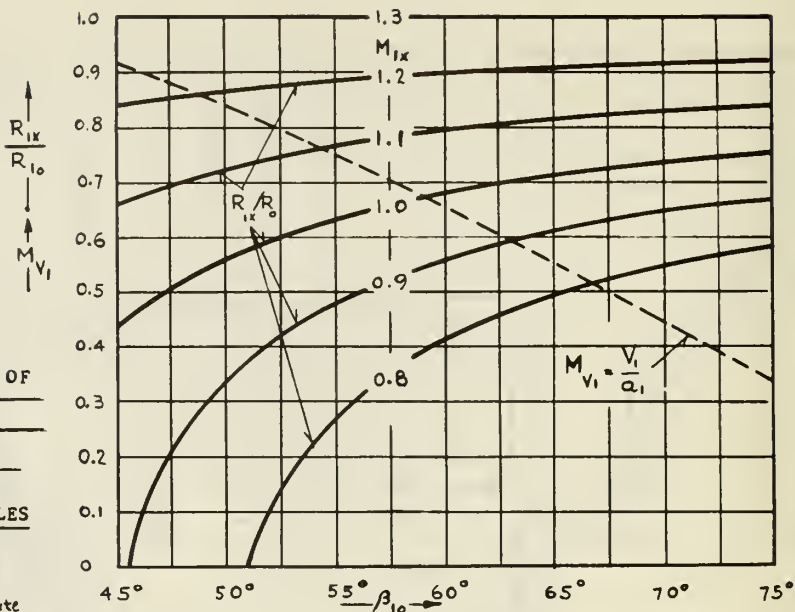
FIG. 11 VELOCITY DISTRIBUTIONS MEASURED IN
UNSHROUDED IMPELLER WITH RADIAL BLADES AT THE
DISCHARGE (Adapted from Personal Communication
by Mr. H. S. Fowler ,Refs.14 and 15)
R_2 = 39 in., R_{1o}/R_2 = 0.629, R_{11}/R_{1o} = 0.752
β_{1o} = 58°, b_2/R_2 = 0.082, z_R = 26, δ_2/R_2 = 0.005
Speed = 50 rpm, Volume Flow = 64.2 ft^3/s

$(R_{10}/R_2)_{MAX}$ for $(W_2/W_{10}) = 0.6$

1.0
0.9
0.8
0.7
0.6
0.5
0.4
0.3
0.2

$\beta_{10} = 70°$
$\beta_{10} = 60°$
$\beta_{10} = 50°$

UPPER LIMIT OF ACTUAL DESIGNS

50°   55°   60°   65° α_2 70°   75°   80°
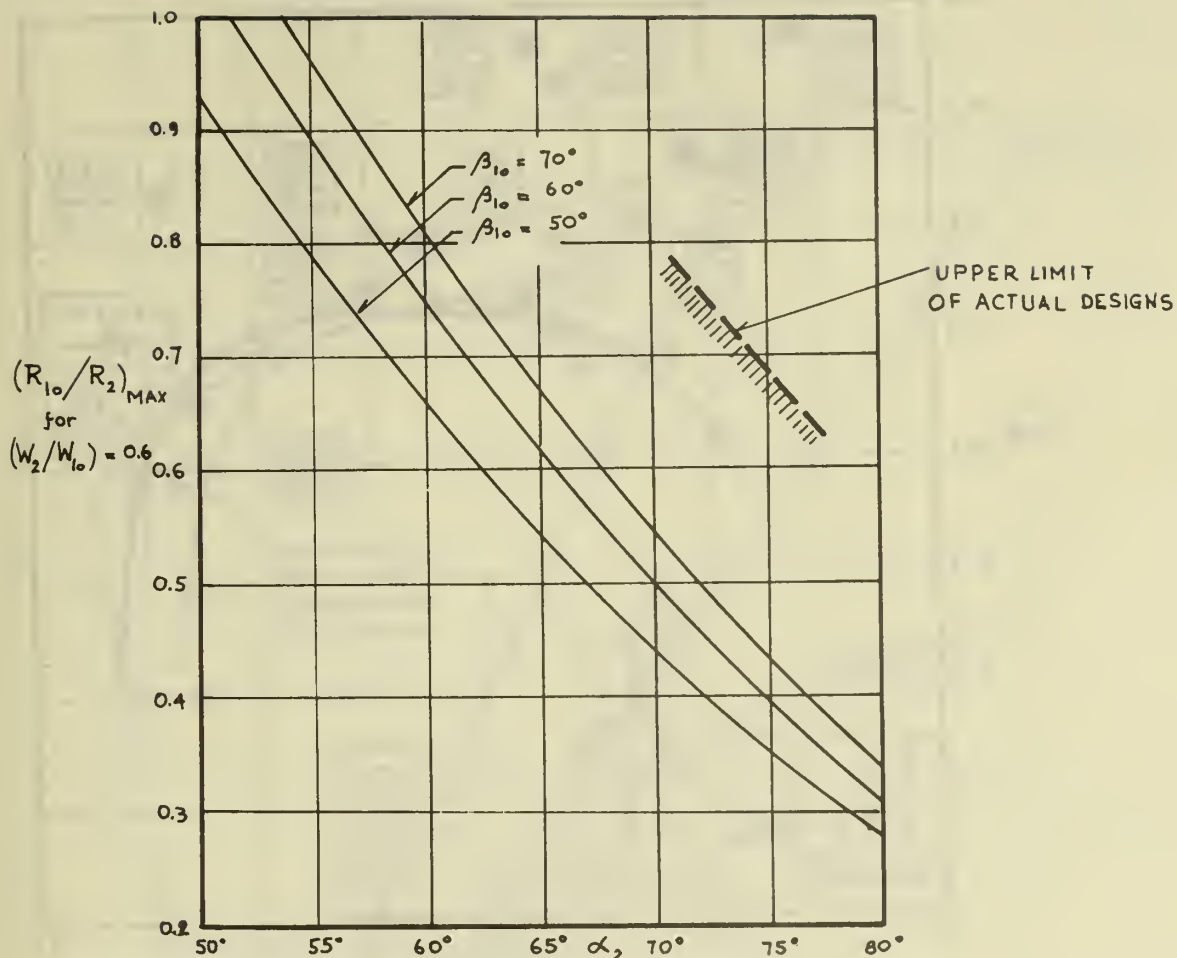
FIG.12   MAXIMUM POSSIBLE RADIUS RATIOS R_{10}/R_2 FOR A DECELERATION RATIO

$W_2/W_{10} = 0.6$ FOR A SLIP FACTOR $\mu = 0.85$

n_S

0.310   0.387   0.465   0.543   0.62   0.698   0.775   0.93   1.085   1.55

3.0   7.143
2.8
2.6   6.190
2.4
2.2   5.238
2.0
1.8   4.286
1.6
1.5   3.807
1.4   3.333
1.2   2.857
1.0   2.381

$4\eta_c$
0.5
0.6
0.7
0.8

$P_{t4}/P_0 = 3$
$\eta_c = 0.7$
$\eta_c = 0.8$

$P_{t4}/P_0 = 4$

$N_{W1} = 1.2$
$N_{W1} = 1.0$

D_S d_S

1   2   3   4   5   6   7

40   50   60   70   80   90 N_S 100   120   140   160   180   200
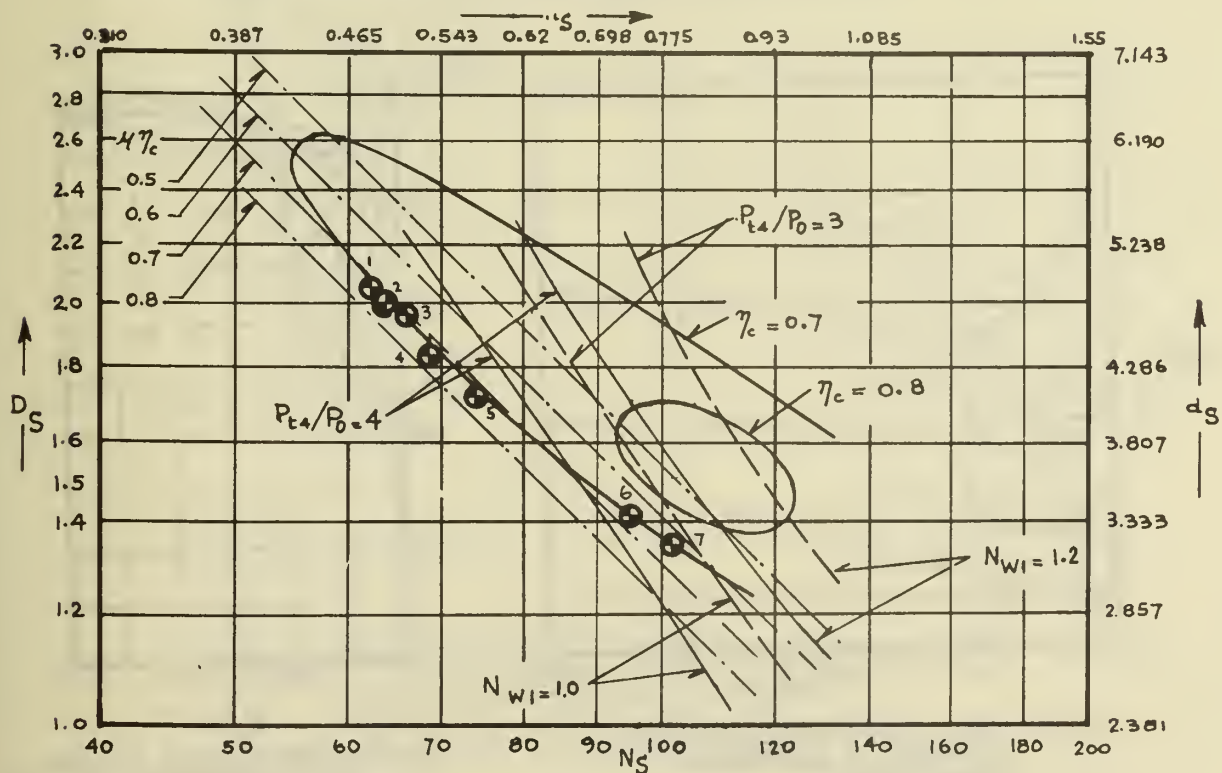
FIG.13   REPRESENTATION OF EQUATION $n_S d_S = 2/(\mu \eta_c)^{\frac{1}{2}}$ OF EQ. III(10) WITH

DESIGN DATA POINTS OF ACTUAL COMPRESSORS

(Other Curves adapted from Fig. 4 of Ref. 19)
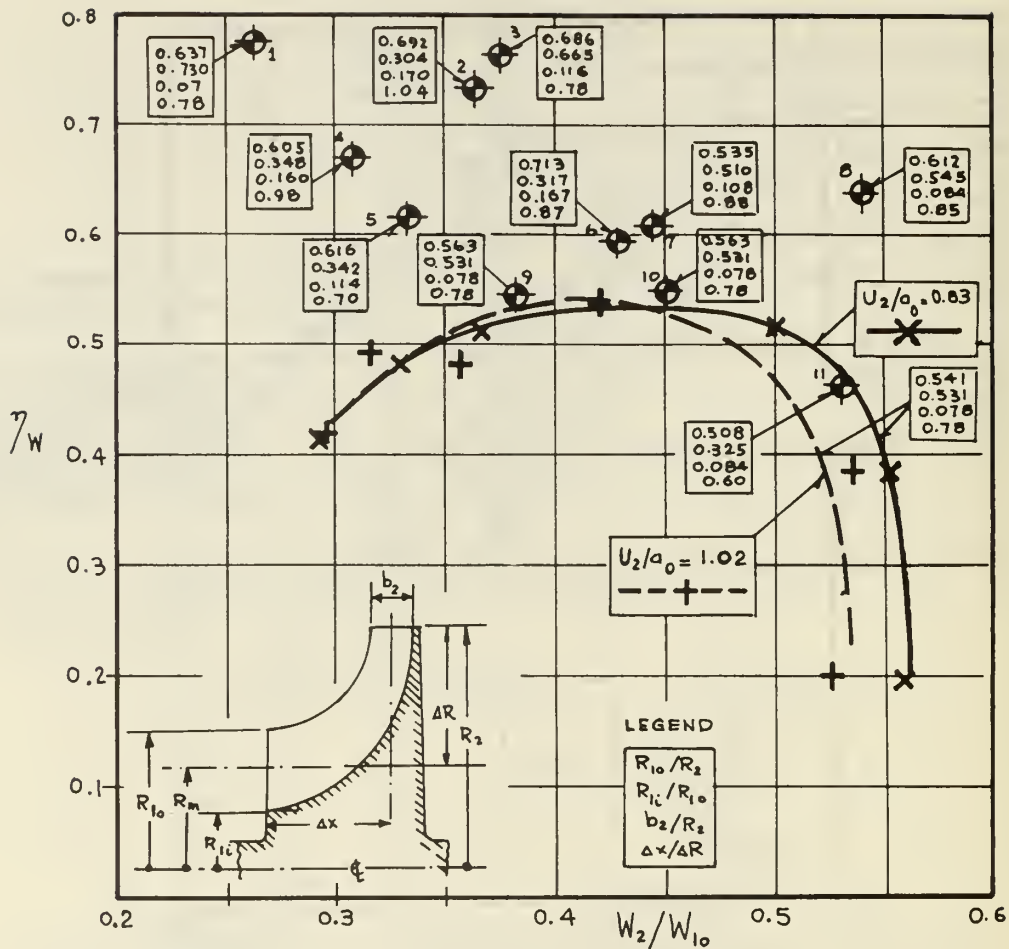
FIG. 14 WHEEL EFFICIENY η_w AS FUNCTION OF THE DECELERATION RATIO W_2/W_{10}
OF DIFFERENT RADIAL IMPELLERS
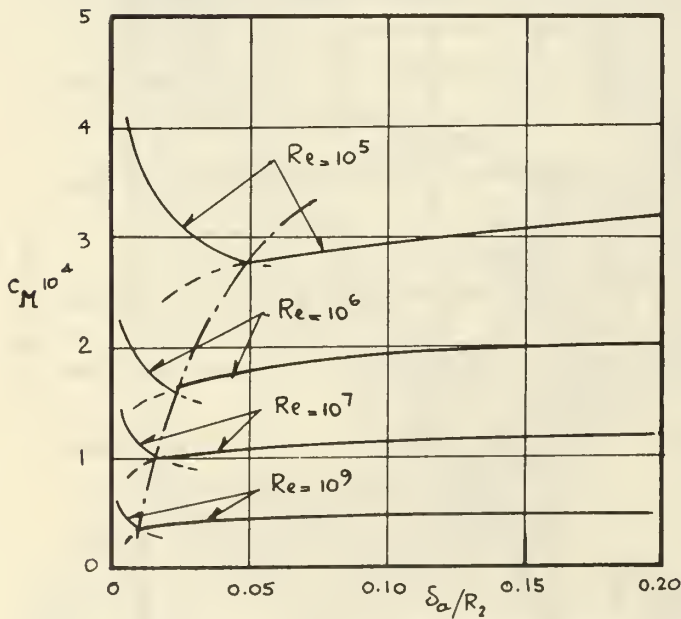
FIG. 15 DISK FRICTION MOMENT COEFFICIENT
AS FUNCTION OF CLEARANCE AND
REYNOLDS NUMBER
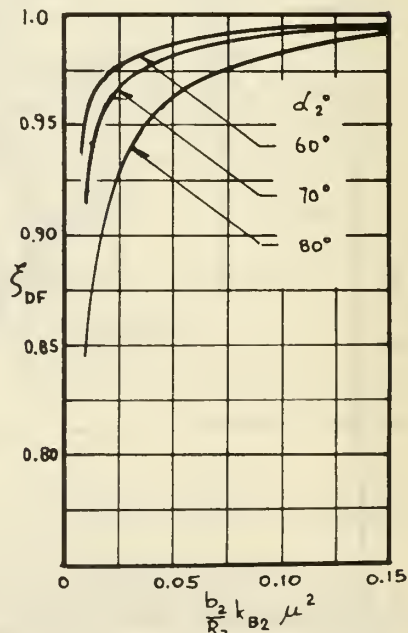
FIG. 16 INFLUENCE OF DISK FRICTION
MOMENT ON COMPRESSOR EFFICIENCY

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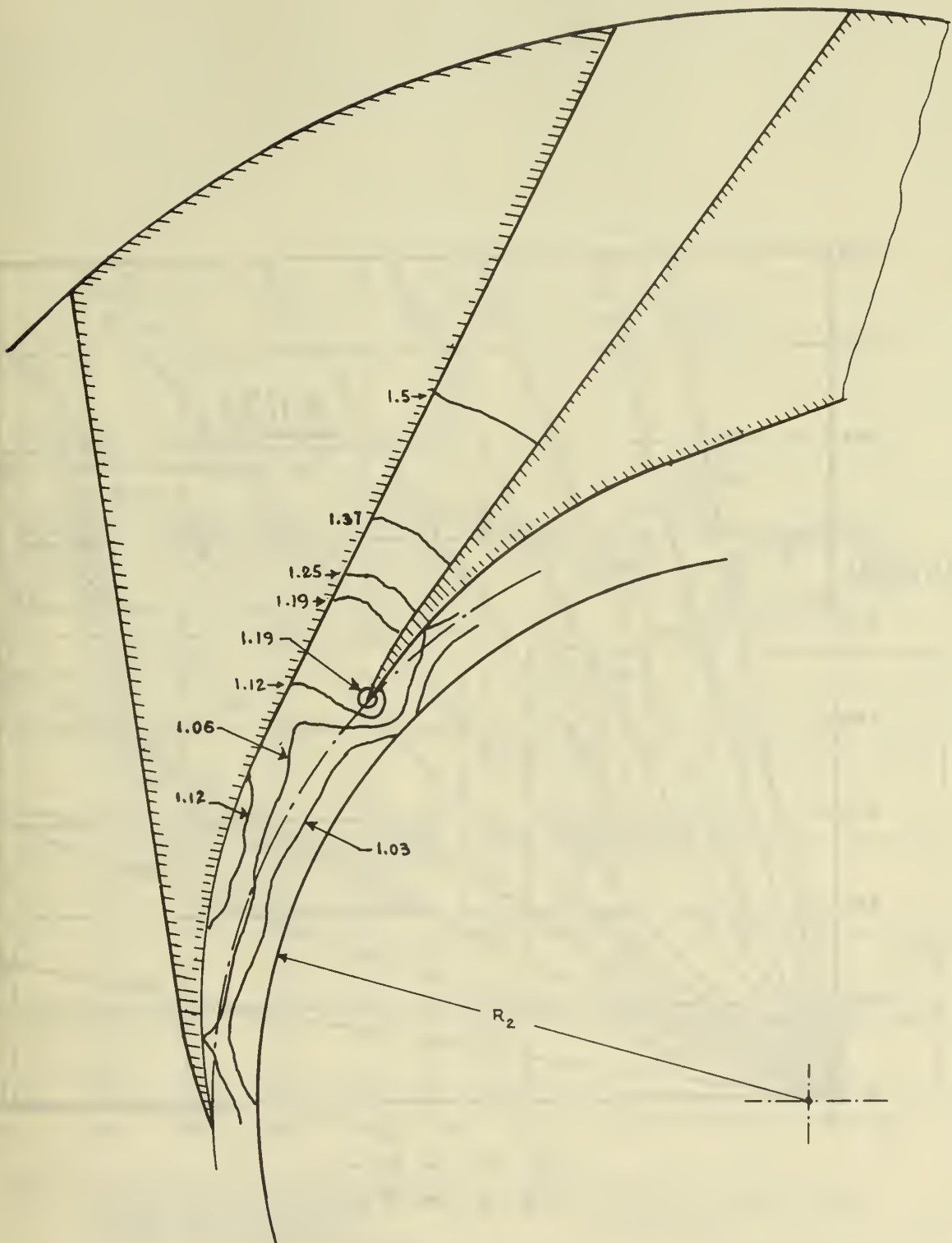
FIG. 17 TYPICAL DISTRIBUTION OF STATIC PRESSURES IN TRANSITION

SECTION AND DIFFUSOR OF HIGH SPEED COMPRESSOR

(Numbers represent approximate ratios of static
pressures and average pressure p_2)
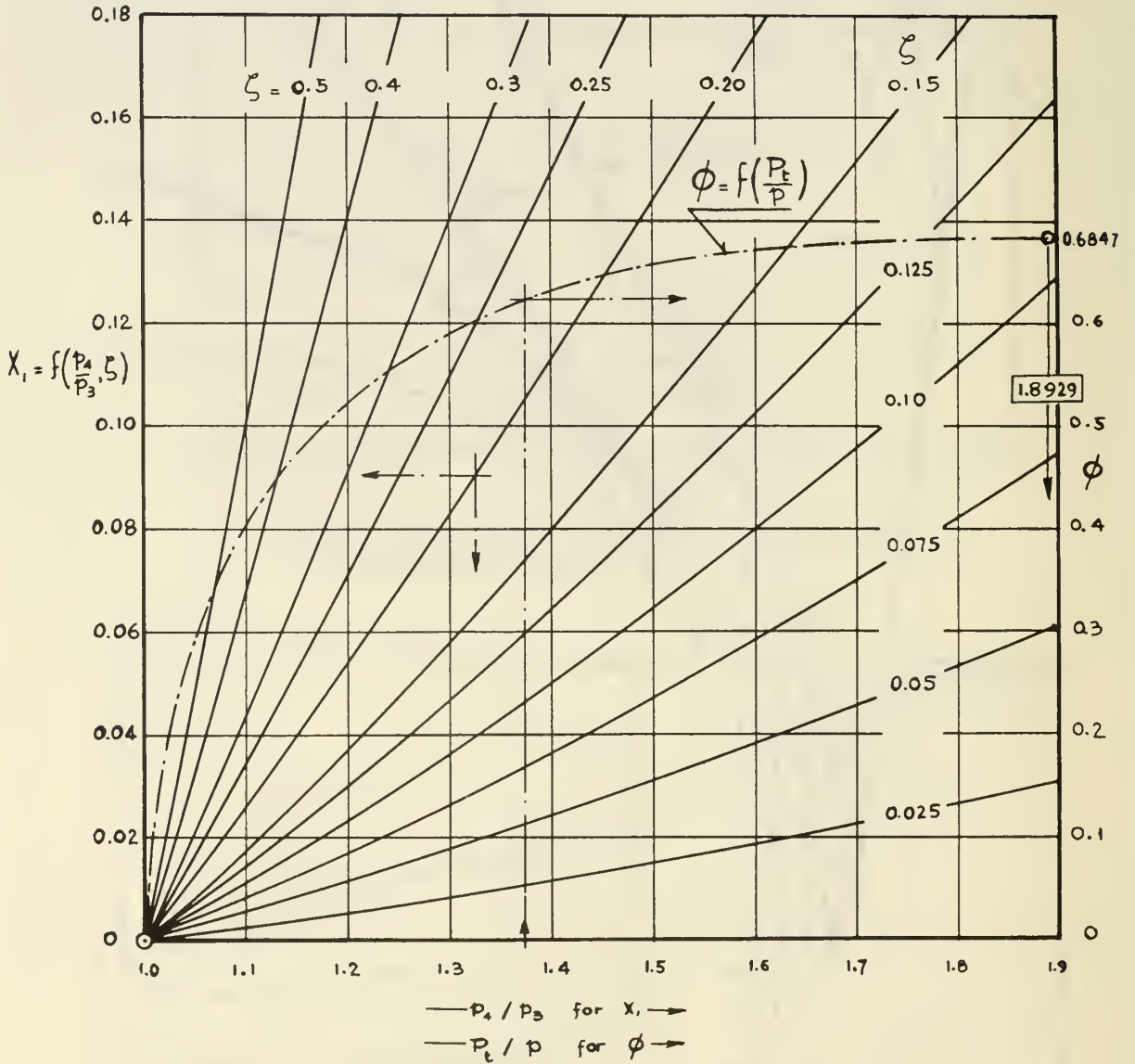
FIG.18 FUNCTION X₁ OF EQ. IV(16) OF TABLE IV FOR DIFFUSOR CALCULATION
AND DIMENSIONLESS FLOW FUNCTION OF EQ. IV(22) AND IV(29) OF TABLE IV

$(\gamma = 1.4)$

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TABLE I   FLOW PROPERTIES IN COMPRESSOR

(For Symbols see Figs. 1 and 2)

VELOCITIES

$$\frac{V_1}{U_2} = \frac{R_{10}}{R_2} \cot\beta_{10} \quad I(1)$$

$$\frac{W_{10}}{U_2} = \frac{R_{10}}{R_2} \frac{1}{\sin\beta_{10}} \quad I(2)$$

$$\frac{V_2}{U_2} = \frac{\mu}{\sin\alpha_2} \quad I(3)$$

$$\frac{W_2}{U_2} = \left[1 - 2\mu\left(1 - \frac{\mu}{2\sin^2\alpha_2}\right)\right]^{\frac{1}{2}} \quad I(4)$$

$$\frac{V_{u2}}{U_2} = \mu$$

$$\frac{W_{u2}}{U_2} = 1 - \mu$$

$$\frac{V_{m2}}{U_2} = \mu \cot\alpha_2$$

$$V_4 = \lambda V_2 \qquad W_2 = \psi W_{2is}$$

TEMPERATURES

$$\frac{T_{t1}}{T_0} = 1$$

$$\frac{T_1}{T_0} = \frac{1}{1 + \frac{\gamma-1}{2} M_{w1}^2 \cos^2\beta_{10}} = \frac{1 + \frac{\gamma-1}{2}\left(\frac{U_2}{a_0}\right)^2\left(\frac{R_{10}}{R_2}\right)^2}{1 + \frac{\gamma-1}{2} M_{w1}^2} \quad I(5)$$

$$\frac{T_{t2}}{T_0} = 1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2 \quad I(6)$$

$$\frac{T_2}{T_0} = 1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left[1 - \frac{\mu}{2\sin^2\alpha_2}\right] \quad I(7)$$

$$\frac{T_{t4}}{T_0} = \frac{T_{t2}}{T_0}$$

$$\frac{T_2'}{T_0} = 1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left[\frac{1}{\psi^2}\left(1 - \frac{\mu}{2\sin^2\alpha_2}\right) - \frac{1}{2\mu}\left(\frac{1}{\psi^2} - 1\right)\right] \quad I(8)$$

$$a_0 = \left[\gamma R_G T_0\right]^{\frac{1}{2}}$$

$$\frac{T_4}{T_0} = 1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left[1 - \frac{\lambda^2\mu}{2\sin^2\alpha_2}\right] \quad I(9)$$

$$\frac{T_E}{T_0} = 1 + \frac{\gamma-1}{2}\left(\frac{U_2}{a_0}\right)^2 \quad I(10)$$

$$\frac{T_4'}{T_0} = 1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left[1 - \frac{\mu}{2\sin^2\alpha_2}\left(1 - \eta_D^*\right)\right] \quad I(11)$$

$$\eta_D^* = \eta_D\left(1 - \lambda^2\right) \quad I(12)$$

$$\frac{T_4''}{T_0} = \frac{(T_4'/T_0)(T_2'/T_0)}{T_2/T_0} = \frac{1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left[X_1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2 X_2\right]}{1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left[1 - \frac{\mu}{2\sin^2\alpha_2}\right]} \quad I(13)$$

$$X_1 = \eta_D^* - \frac{1}{2\mu}\left(\frac{1}{\psi^2} - 1\right) + \left(1 - \frac{\mu}{2\sin^2\alpha_2}\right)\left(1 + \frac{1}{\psi^2} - \eta_D^*\right) \quad I(14)$$

$$X_2 = \frac{\eta_D^*}{2\mu}\left(1 - \frac{1}{\psi^2}\right) + \left(1 - \frac{\mu}{2\sin^2\alpha_2}\right)\left(\frac{\eta_D^*}{\psi^2} - \frac{[1 - \eta_D^*]}{2\mu}\left[\frac{1}{\psi^2} - 1\right]\right) + \left(1 - \frac{\mu}{2\sin^2\alpha_2}\right)\left(\frac{1 - \eta_D^*}{\psi^2}\right) \quad I(15)$$

$$\frac{\Delta T_{is}}{T_0} = \frac{T_4'' - T_0}{T_0} = \frac{(\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left[X_1 - \left(1 - \frac{\mu}{2\sin^2\alpha_2}\right) + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2 X_2\right]}{1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left[1 - \frac{\mu}{2\sin^2\alpha_2}\right]} \quad I(16)$$

PRESSURES

$$\frac{P_{t2}'}{P_0} = \left(T_{t2}/T_0\right)^{\frac{\gamma}{\gamma-1}} \quad I(17)$$

$$\frac{P_1}{P_0} = \left(T_1/T_0\right)^{\frac{\gamma}{\gamma-1}} \quad I(18)$$

$$\frac{P_{t2}}{P_0} = \frac{P_2}{P_0}\frac{P_{t2}}{P_2} = \left[\frac{(T_2'/T_0)(T_{t2}/T_0)}{T_2/T_0}\right]^{\frac{\gamma}{\gamma-1}} \quad I(19)$$

$$\frac{P_2}{P_0} = \left(T_2'/T_0\right)^{\frac{\gamma}{\gamma-1}} \quad I(20)$$

$$\frac{P_{t4}}{P_0} = \frac{P_4}{P_0} = \left(T_4''/T_0\right)^{\frac{\gamma}{\gamma-1}} \quad I(21)$$

$$\frac{P_4}{P_2} = \left(T_4'/T_2\right)^{\frac{\gamma}{\gamma-1}} = \left(\frac{T_4'/T_0}{T_2/T_0}\right)^{\frac{\gamma}{\gamma-1}} \quad I(22)$$

$$\frac{P_{E1}}{P_0} = \left(T_E/T_0\right)^{\frac{\gamma}{\gamma-1}} \quad I(23)$$

$$\frac{P_{E2}}{P_0} = \frac{P_2}{P_0}\frac{P_{E2}}{P_2} = \left[\frac{(T_2'/T_0)(T_E/T_0)}{T_2/T_0}\right]^{\frac{\gamma}{\gamma-1}} \quad I(24)$$

TABLE II PERFORMANCE AND DESIGN PARAMETERS

$$\eta_c = \frac{\Delta T_{is}}{\Delta T_w} = \frac{X_1 - \left(1 - \frac{\mu}{2\sin^2\alpha_2}\right) + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2 X_2}{1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left[1 - \frac{\mu}{2\sin^2\alpha_2}\right]} \qquad \text{II}(1)$$

(X_1 and X_2 are given by Eqs. I(14) and I(15) of Table I)

$$r^* = \frac{T_2' - T_0}{\Delta T_{is}} = \frac{\frac{1}{\gamma^2}\left(1 - \frac{\mu}{2\sin^2\alpha_2}\right) - \frac{1}{2\mu}\left(\frac{1}{\gamma^2} - 1\right)}{\eta_c} \qquad \text{II}(2)$$

$$\frac{U_2}{a_0} = \left[\frac{\left(P_{t4}/P_0\right)^{\frac{\gamma-1}{\gamma}} - 1}{(\gamma-1)\mu\,\eta_c}\right]^{\frac{1}{2}} \qquad \text{II}(3)$$

$$\frac{R_{10}}{R_2} = \frac{M_{w1}\,\sin\beta_{10}}{\frac{U_2}{a_0}\left[1 + \frac{\gamma-1}{2}M_{w1}^2\cos^2\beta_{10}\right]^{\frac{1}{2}}} \qquad \text{II}(4)$$

$$\frac{W_2}{W_{10}} = \frac{\left[1 - 2\mu\left(1 - \frac{\mu}{2\sin^2\alpha_2}\right)\right]^{\frac{1}{2}}\sin\beta_{10}}{(R_{10}/R_2)} \qquad \text{II}(5)$$

$$M_{V2} = \frac{V_2}{a_2} = \frac{\mu\frac{U_2}{a_0}}{\sin\alpha_2\left[1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left(1 - \frac{\mu}{2\sin^2\alpha_2}\right)\right]^{\frac{1}{2}}} \qquad \text{II}(6)$$

$$\phi_1 = \frac{V_1}{U_2} = \frac{M_{w1}\cos\beta_{10}}{\frac{U_2}{a_0}\left[1 + \frac{\gamma-1}{2}M_{w1}^2\cos^2\beta_{10}\right]^{\frac{1}{2}}} \qquad \text{II}(7)$$

$$\phi_2 = \frac{V_{m2}}{U_2} = \mu\,\cot\alpha_2 \qquad \text{II}(8)$$

$$\pi R_2^2\left[1 - \left(\frac{R_{1i}}{R_{10}}\right)^2\right]k_{B1} = \left(\frac{\dot{m}\sqrt{R_G T_0}}{P_0}\right)\left(\frac{U_2}{a_0}\right)^2\frac{\left[1 + \frac{\gamma-1}{2}M_{w1}^2\cos^2\beta_{10}\right]^{\frac{3\gamma-1}{2(\gamma-1)}}}{\sqrt{\gamma}\,M_{w1}^3\,\cos\beta_{10}\,\sin^2\beta_{10}} \qquad \text{II}(9)$$

$$\frac{\omega}{\left[1 - \left(\frac{R_{1i}}{R_{10}}\right)^2\right]k_{B1}} = \left[\frac{a_0\,P_0}{\dot{m}}\right]^{\frac{1}{2}}\frac{\sin\beta_{10}\left[\pi\,\gamma\,\cos\beta_{10}\right]^{\frac{1}{2}}}{\left[1 + \frac{\gamma-1}{2}M_{w1}^2\cos^2\beta_{10}\right]^{\frac{3\gamma-1}{4(\gamma-1)}}} \qquad \text{II}(10)$$

$$\left(\frac{b_2}{R_2}\right)k_{B2} = \left(\frac{\dot{m}\sqrt{R_G T_0}}{\pi R_2^2 P_0}\right)\frac{1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left(1 - \frac{\mu}{2\sin^2\alpha_2}\right)}{2\mu\sqrt{\gamma}\,\cot\alpha_2\left(\frac{U_2}{a_0}\right)\left\{1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left[\frac{1}{\gamma^2}\left(1 - \frac{\mu}{2\sin^2\alpha_2}\right) - \frac{1}{2\mu}\left(\frac{1}{\gamma^2} - 1\right)\right]\right\}^{\frac{\gamma}{\gamma-1}}} \qquad \text{II}(11)$$

Diffusor Exit Area A_4:

$$A_4\,k_{B4} = \left(\frac{\dot{m}\sqrt{R_G T_0}}{P_0}\right)\frac{\sin\alpha_2}{\lambda\mu\sqrt{\gamma}\left(\frac{U_2}{a_0}\right)}\frac{\left[1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left(1 - \frac{\lambda^2\mu}{2\sin^2\alpha_2}\right)\right]}{\left[1 + \eta_c(\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\right]^{\frac{\gamma}{\gamma-1}}} \qquad \text{II}(12)$$

Diffusor Throat Area A_x if $M_{V2} > 1$:

$$A_x\,k_{Bx} = \frac{\left(\frac{\dot{m}\sqrt{R_G T_0}}{P_0}\right)}{\phi_c\left(\frac{P_{tx}}{P_{t2}}\right)\left[1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\right]^{\frac{\gamma+1}{2(\gamma-1)}}}\,Y^{\frac{\gamma}{\gamma-1}} \qquad \text{II}(13)$$

where

$$\phi_c = \left\{\frac{2\gamma}{\gamma-1}\left[\left(\frac{2}{\gamma+1}\right)^{\frac{2}{\gamma-1}} - \left(\frac{2}{\gamma+1}\right)^{\frac{\gamma+1}{\gamma-1}}\right]\right\}^{\frac{1}{2}} \qquad \text{II}(14)$$

and

$$Y = \frac{T_2/T_0}{T_2'/T_0} = \frac{1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left[1 - \frac{\mu}{2\sin^2\alpha_2}\right]}{1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left[\frac{1}{\gamma^2}\left(1 - \frac{\mu}{2\sin^2\alpha_2}\right) - \frac{1}{2\mu}\left(\frac{1}{\gamma^2} - 1\right)\right]} \qquad \text{II}(15)$$

Diffusor Throat Area A_x if $M_{V2} \leq 1$, and $V_x = \xi V_2$:

$$A_x\,k_{Bx} = \frac{\sin\alpha_2\left(\frac{\dot{m}\sqrt{R_G T_0}}{P_0}\right)}{\xi\mu\sqrt{\gamma}\left(\frac{U_2}{a_0}\right)\left(\frac{P_{tx}}{P_{t2}}\right)\left[1 + (\gamma-1)\mu\left(\frac{U_2}{a_0}\right)^2\left(1 - \frac{\xi^2\mu}{2\sin^2\alpha_2}\right)\right]^{\frac{1}{\gamma-1}}}\,Y^{\frac{\gamma}{\gamma-1}} \qquad \text{II}(16)$$

TABLE III   SPECIFIC SPEED RELATIONS

DEFINITIONS WITH ENGLISCH UNITS

(see Refs. 18 and 19)

SPECIFIC SPEED

$$N_S = \frac{N \; Q_1^{\frac{1}{2}}}{H_{is}^{3/4}} \qquad \text{III(1)}$$

SPECIFIC DIAMETER

$$D_S = \frac{D \; H_{is}^{\frac{1}{4}}}{Q_1^{\frac{1}{2}}} \qquad \text{III(2)}$$

DEFINITIONS IN DIMENSIONLESS FORM

$$n_S = \frac{N_S}{129} = \frac{\omega \; Q_1^{\frac{1}{2}}}{(c_p \; \Delta T_{is})^{3/4}} \qquad \text{III(3)}$$

$$d_S = \frac{D_S}{0.42} = \frac{D \; (c_p \; \Delta T_{is})^{\frac{1}{4}}}{Q_1^{\frac{1}{2}}} \qquad \text{III(4)}$$

N - Rotative Speed (rpm)
ω - Angular Velocity (radians/s)
Q_1 - Inlet Volume Flow Rate (cuft/s)
$H_{is} = g_o \, c_p \, \Delta T_{is}$ - Isentropic Head (ft-lb/lbm)
g_o - Gravitational Constant = 32.174 ft/s^2
c_p - Specific Heat at Constant Pressure $\left(\dfrac{ft\text{-}lb}{slug, \; deg.R} \right)$
ΔT_{is}- Isentropic Temperature Rise in Compressor (deg. R)
D - Rotor Diameter (ft)

RELATIONS WITH SYMBOLS OF TABLES I AND II

$$\xi_1 = 1 - \left(\frac{R_{1i}^2}{R_{1o}^2} \right) \qquad \text{III(5)}$$

$$Q_1 = \pi R_{1o}^2 \; \xi_1 \; k_{B1} \; V_1$$
$$V_1 = U_{1o} \cot \beta_{1o}$$
$$c_p \Delta T_{is} = \mu \; \eta_c \; U_2^2$$
$$\omega = U_2/R_2$$
$$D = 2 R_2 = 2 U_2/\omega$$

$$n_S^2 = \pi \left(\frac{R_{1o}}{R_2} \right)^3 k_{B1} \frac{\cot \beta_{1o} \; \xi_1}{(\mu \; \eta_c)^{3/2}} \qquad \text{III(6)}$$

$$d_S^2 = \frac{4}{\pi} \frac{(\mu \; \eta_c)^{1/2}}{(R_{1o}/R_2)^3 \; k_{B1} \cot \beta_{1o} \; \xi_1} \qquad \text{III(7)}$$

and

$$\xi_1 = \frac{n_S^2}{\pi} \frac{(\mu \; \eta_c)^{3/2} \tan \beta_{1o}}{k_{B1} \; (R_{1o}/R_2)^3} \qquad \text{III(8)}$$

$$\xi_1 = \frac{4}{\pi d_S^2} \frac{(\mu \; \eta_c)^{1/2} \tan \beta_{1o}}{k_{B1} \; (R_{1o}/R_2)^3} \qquad \text{III(9)}$$

Equating Eqs. 8 and 9:

$$n_S \, d_S = \frac{2}{(\mu \; \eta_c)^{\frac{1}{2}}} \qquad \text{III(10)}$$

From Eq.8

$$\frac{R_{1i}}{R_{1o}} = \left[1 - \frac{n_S^2}{\pi} \frac{(\mu \; \eta_c)^{3/2} \tan \beta_{1o}}{k_{B1} \; (R_{1o}/R_2)^3} \right]^{\frac{1}{2}} \qquad \text{III(11)}$$

EXAMPLE: For $\mu = 0.88$, $\eta_c = 0.83$, $k_{B1} = 0.85$, and $\beta_{1o} = 68°$, find R_{11}/R_{1o} for different values of N_S for the two radius ratios $R_{1o}/R_2 = 0.56$ and $R_{1o}/R_2 = 0.70$

For $R_{1o}/R_2 = 0.56$; from Eq.11

$$\frac{R_{11}}{R_{1o}} = \left[1 - n_S^2 (3.288) \right]^{\frac{1}{2}} \qquad \text{III(12)}$$

R_{11}/R_{1o} is zero for $n_{S \; max} = 0.552$, or $N_{Smax} = 71$
For values of N_S lower than 71:

N_S	60	65	70
n_S	0.465	0.504	0.543
R_{11}/R_{1o}	0.537	0.406	0.178

For $R_{1o}/R_2 = 0.70$; from Eq.11

$$\frac{R_{11}}{R_{1o}} = \left[1 - n_S^2 (1.683) \right]^{\frac{1}{2}} \qquad \text{III(13)}$$

R_{11}/R_{1o} is zero for $n_{Smax} = 0.771$, or $N_{Smax} = 99.4$
For values of N_S lower than 99.4:

N_S	70	80	90	98
n_S	0.543	0.620	0.698	0.760
R_{11}/R_{1o}	0.710	0.594	0.424	0.169

Relation between so-called Mach Number $N_{W1} = W_{1o} / \sqrt{\dfrac{2\gamma}{\gamma + 1} R_G T_0}$ and actual Mach Number $M_{W1} = W_{1o}/a_1$:

$$N_{W1}^2 = \left[\frac{\gamma + 1}{2} M_{W1}^2 \right] \Big/ \left[1 + \frac{\gamma - 1}{2} M_{W1}^2 \cos^2 \beta_{1o} \right] \qquad \text{III(14)}$$

TABLE IV   ANALYSIS OF FLOWS IN DIFFUSORS

ONE-DIMENSIONAL FLOW IN CHANNEL
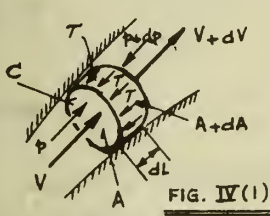
A - Flow Area
C - Wetted Perimeter
L - Channel Length
$\dot{m}$ - Mass Flow Rate
p - Static Pressure
τ - Wall Shear Stresses
ρ - Mass Density

FIG. IV(1)

From Momentum Theorem:

$$\frac{1}{\rho}\,dp + d\left(\frac{V^2}{2}\right) = -\frac{\tau}{\rho}\frac{C}{A}\,dL \qquad \text{IV (1)}$$

From Equation of Continuity:

$$\dot{m} = A\,\rho\,V \qquad \text{IV (2)}$$

Derivation:

Eq. IV(4) into Eq. IV(1)

$$c_p\,dT - T\,ds + d\left(\frac{V^2}{2}\right) = -\frac{\tau}{\rho}\frac{C}{A}\,dL$$

$$d\left(c_p\,dT + \frac{V^2}{2}\right) - T\,ds = -\frac{\tau}{\rho}\frac{C}{A}\,dL$$

From Eq. 3

$$dT_t = 0 = d\left(T + \frac{V^2}{2c_p}\right)$$

$$T\,ds = \frac{\tau}{\rho}\frac{C}{A}\,dL \qquad \text{IV (10)}$$

From Frictional Law with Eq. 2:

$$\tau = c_f\frac{\rho}{2}V^2 = \frac{c_f}{2}\frac{\dot{m}^2}{\rho A^2} \qquad \text{IV (12)}$$

Into Eq. 10

$$T\,ds = \frac{c_f}{2}\frac{\dot{m}^2}{\rho^2 A^3}C\,dL \qquad \text{IV (13)}$$

THERMODYNAMIC CONDITIONS
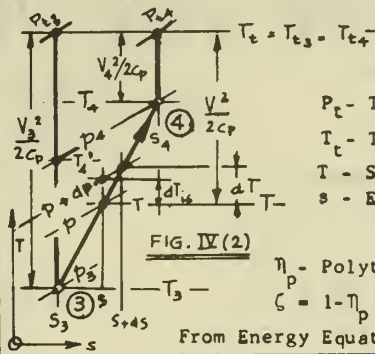
$$T_t = T_{t_3} = T_{t_4}$$

P_t - Total Pressure
T_t - Total Temperature
T - Static Temperature
s - Entropy

FIG. IV(2)

η_p - Polytropic Efficiency
$\zeta = 1 - \eta_p$ - Loss Coefficient

From Energy Equation:

$$T_t = T_{t_3} = T_{t_4} = T + \frac{V^2}{2c_p} = T_3 + \frac{V_3^2}{2c_p} = T_4 + \frac{V_4^2}{2c_p} \qquad \text{IV (3)}$$

From First Law of Thermodynamics:

$$T\,ds = c_p\,dT - \frac{1}{\rho}\,dp = R_G\frac{\gamma}{\gamma-1}\,dT - \frac{1}{\rho}\,dp \qquad \text{IV (4)}$$

$$ds = R_G\left[\frac{\gamma}{\gamma-1}\frac{dT}{T} - \frac{dp}{p}\right] \qquad \text{IV (5)}$$

For Adiabatic Polytropic Process

$$\eta_p = \frac{dT_{is}}{dT} = \frac{T\left[\left(\frac{p+dp}{p}\right)^{\frac{\gamma-1}{\gamma}} - \right]}{dT} = \frac{T}{dT}\frac{\gamma-1}{\gamma}\frac{dp}{p} \qquad \text{IV (6)}$$

$$\frac{dT}{T} = \frac{\gamma-1}{\eta_p\gamma}\frac{dp}{p} \qquad \text{IV (7)}$$

$$T = \text{constant} \quad p^{\frac{\gamma-1}{\eta_p\gamma}} \qquad \text{IV (8)}$$

$$\rho = \text{constant} \quad p^{1-\frac{\gamma-1}{\eta_p\gamma}} \qquad \text{IV (9)}$$

From Eqs. 5 and 7

$$\frac{ds}{R_G} = \left(\frac{1}{\eta_p} - 1\right)\frac{dp}{p} = \frac{\zeta}{1-\zeta}\frac{dp}{p} \qquad \text{IV (11)}$$

Dimensionless Referred Mass Flow Rate

$$\dot{m}_{r3} = \frac{\dot{m}\sqrt{R_G T_3}}{P_3 A_3} \qquad \text{IV (14)}$$

PRINCIPAL EQUATION obtained from Eqs. 13 and 14, and $\rho = \dfrac{p}{R_G T}$

$$dX_1 = \frac{\rho}{\rho_3}\frac{p}{p_3}\,d\left(\frac{s}{R_G}\right) = \frac{c_f}{2}\left(\dot{m}_{r3}\right)^2\left(\frac{A_3}{A}\right)^3\frac{C\,dL}{A_3} = \frac{c_f}{2}\left(\dot{m}_{r3}\right)^2\,d\Omega = dX_2 \qquad \text{IV (15)}$$

$$X_1 = \int_3^4 dX_1 = \int_3^4 \frac{\rho}{\rho_3}\frac{p}{p_3}\,d\left(\frac{s}{R_G}\right) \qquad \text{IV (16)}$$

With Eqs. 11 and 9

$$dX_1 = \left(\frac{1}{\eta_p} - 1\right)\frac{\rho}{\rho_3}\frac{p}{p_3}\frac{dp}{p} = \left(\frac{1}{\eta_p} - 1\right)\frac{\rho}{\rho_3}\,d\left(\frac{p}{p_3}\right)$$

$$dX_1 = \left(\frac{1}{\eta_p} - 1\right)\left(\frac{p}{p_3}\right)^{1-\frac{\gamma-1}{\eta_p\gamma}}\,d\left(\frac{p}{p_3}\right)$$

$$X_1 = \int_1^{(p_3/p_4)} dX_1 = \frac{\frac{1}{\eta_p} - 1}{2 - \frac{\gamma-1}{\eta_p\gamma}}\left[\left(\frac{p_4}{p_3}\right)^{2-\frac{\gamma-1}{\eta_p\gamma}} - 1\right]$$

and

$$X_1 = \frac{\zeta\gamma}{\gamma + 1 - 2\zeta\gamma}\left[\left(\frac{p_4}{p_3}\right)^{\frac{\gamma+1-2\zeta\gamma}{(1-\zeta)\gamma}} - 1\right] \qquad \text{IV (20)}$$

$$X_2 = \frac{1}{2}\left(\dot{m}_{r3}\right)^2\int_0^L c_f\,d\Omega = \frac{\bar{c_f}}{2}\left(\dot{m}_{r3}\right)^2\int_0^L d\Omega \qquad \text{IV(17)}$$

$$X_2 = \frac{\bar{c_f}}{2}\left(\dot{m}_{r3}\right)^2\,\Omega \qquad \text{IV (18)}$$

$$\Omega = \int_0^L \left(\frac{A_3}{A}\right)^3\frac{C\,dL}{A_3} \qquad \text{IV (19)}$$

Ω will be denoted as Diffusor Shape Factor

From Eq. 20

$$\frac{p_4}{p_3} = \left[\frac{X_1(\gamma+1-2\zeta\gamma)}{\zeta\gamma} + 1\right]^{\frac{(1-\zeta)\gamma}{\gamma+1-2\zeta\gamma}} \qquad \text{IV (21)}$$

TABLE IV (CONTD.)   METHODS OF SOLUTION

For Effective Flow Area $A_3^* = k_{B3} A_3$ (k_{B3} =Blockage Factor, A_3=Actual Area at Diffusor Inlet)

$$\frac{\dot{m}\sqrt{R_G T_{t3}}}{A_3^* P_{t3}} = \sqrt{\frac{2\gamma}{\gamma-1}\left[\left(\frac{p_3}{P_{t3}}\right)^{\frac{2}{\gamma}} - \left(\frac{p_3}{P_{t3}}\right)^{\frac{\gamma+1}{\gamma}}\right]} = \phi_3 = f\left(\frac{P_{t3}}{p_3}, \gamma\right) \qquad \text{IV}(22)$$

From Eq.14

$$\dot{m}_{r3} = \frac{\dot{m}\sqrt{R_G T_3}}{A_3^* p_3} = \phi_3 \frac{\sqrt{(T_3/T_{t3})}}{p_3/P_{t3}} \qquad \text{IV}(23)$$

If p_3 is known,

$$\frac{T_3}{T_{t3}} = \left(\frac{p_3}{P_{t3}}\right)^{\frac{\gamma-1}{\gamma}} \qquad \text{IV}(25)$$

Into Eq.23

$$\dot{m}_{r3} = \phi_3 \left(\frac{P_{t3}}{p_3}\right)^{\frac{\gamma+1}{2\gamma}} \qquad \text{IV}(27)$$

If $M_{V3} = V_3/\sqrt{\gamma R_G T_3}$ is known, with $c_p = R_G \frac{\gamma}{\gamma-1}$,

$$\frac{T_{t3}}{T_3} = 1 + \frac{V_3^2}{2 c_p T_3} = 1 + \frac{\gamma-1}{2}\frac{V_3^2}{\gamma R_G T_3} = 1 + \frac{\gamma-1}{2} M_{V3}^2 \qquad \text{IV}(24)$$

$$\frac{P_{t3}}{p_3} = \left[1 + \frac{\gamma-1}{2} M_{V3}^2\right]^{\frac{\gamma}{\gamma-1}} \qquad \text{IV}(26)$$

Into Eq.23

$$\dot{m}_{r3} = \phi_3 \left[1 + \frac{\gamma-1}{2} M_{V3}^2\right]^{\frac{\gamma+1}{2(\gamma-1)}} \qquad \text{IV}(28)$$

For known Ω and $\bar{c}_f$, i.e. X_2 from Eq.18, and $X_1 = \lambda_2$, the Loss Coefficient ζ must be obtained with an iteration to satisfy the Equation of Continuity at Diffusor Discharge. For Effective Flow Area $A_4^* = k_{B4} A_4$ (k_{B4} = Blockage Factor, A_4 = Actual Diffusor Discharge Area), since $T_{t4} = T_{t3}$,

$$\frac{\dot{m}\sqrt{R_G T_{t3}}}{A_4^* P_{t4}} = \sqrt{\frac{2\gamma}{\gamma-1}\left[\left(\frac{p_4}{P_{t4}}\right)^{\frac{2}{\gamma}} - \left(\frac{p_4}{P_{t4}}\right)^{\frac{\gamma+1}{\gamma}}\right]} = \phi_4 = f\left(\frac{P_{t4}}{p_4}, \gamma\right) = \phi_3 \frac{A_3^*}{A_4^*} \frac{P_{t3}}{P_{t4}} \qquad \text{IV}(29)$$

Since P_{t3}/P_{t4} is as yet unknown, it is not possible to determine $P_{t4}/p4$ from function ϕ_4 to obtain $p_4/p_3 = (P_{t3}/p_3)/(P_{t4}/p_4)$. Additional relation is obtained by calculating entropy increase $\Delta s = s_4 - s_3$ for polytropic process from p_3 to p_4 with Eq.11, and for T_t = constant from P_{t3} to P_{t4} with Eq.5.

For Polytropic Process:

$$\frac{\Delta s}{R_G} = \frac{\zeta}{1-\zeta} \ln\left(\frac{p_4}{p_3}\right) = \ln\left[\left(\frac{p_4}{p_3}\right)^{\frac{\zeta}{1-\zeta}}\right] \qquad \text{IV}(30)$$

Along Line $T_{t3} = T_{t4}$ = Constant:

$$\frac{\Delta s}{R_G} = -\ln\left[\frac{P_{t4}}{P_{t3}}\right] = \ln\left[\frac{P_{t3}}{P_{t4}}\right] \qquad \text{IV}(31)$$

Equating Eqs.30 and 31

$$\frac{p_4}{p_3} = \left(\frac{P_{t3}}{P_{t4}}\right)^{\frac{1-\zeta}{\zeta}} \qquad \text{IV}(32)$$

$$\frac{P_{t3}}{P_{t4}} = \left(\frac{p_4}{p_3}\right)^{\frac{\zeta}{1-\zeta}} \qquad \text{IV}(33)$$

With Eq.33

$$\frac{P_{t4}}{p_4} = \left(\frac{P_{t4}}{P_{t3}}\right)\left(\frac{P_{t3}}{p_3}\right)\left(\frac{p_3}{p_4}\right) = \frac{(P_{t3}/p_3)}{(P_{t3}/P_{t4})(p_4/p_3)} = \frac{(P_{t3}/p_3)}{\left(\frac{p_4}{p_3}\right)^{\frac{1}{1-\zeta}}} \qquad \text{IV}(34)$$

ITERATION PROCEDURE

(1) For given values of Ω and $\bar{c}_f$ calculate X_2 from Eq.18 with Eq.27 or 28. $X_1 = X_2$

(2) Choose initial value of ζ

(3) Calculate $p_4/p_3 = p_4'/p_3$ by Eq.21 for X_1 and ζ

(4) Calculate $P_{t3}/P_{t4} = P_{t3}/P_{t4}'$ from Eq.33 for p_4'/p_3

(5) Calculate $\phi_4' = \phi_3(A_3^*/A_4^*)(P_{t3}/P_{t4}')$ (Eq.29)

(6) Calculate P_{t4}'/P_4' from Eq.34 for p_4'/p_3

.7) Calculate $\phi_4 = \phi_4''$ from Flow Function (Eq.29) for $P_{t4}/p_4 = P_{t4}'/p_4'$

Change Value of ζ ← No ← $\phi_4'' = \phi_4'$? → Yes → ζ ;$(p_4/p_3) = (p_4'/p_3)$;$(P_{t4}/P_{t3} = P_{t4}'/P_{t3})$
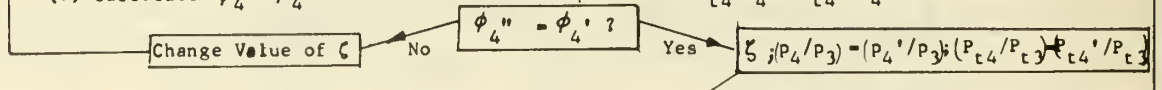
Diffusor Efficiency η_{D3-4} between Stations (3) and (4)

$$\eta_{D3-4} = \frac{T_4' - T_3}{T_4 - T_3} = \frac{T_4'/T_3 - 1}{T_4/T_3 - 1} = \frac{(p_4/p_3)^{\frac{\gamma-1}{\gamma}} - 1}{T_4/T_3 - 1}$$

With Eq.8

$$\eta_{D3-4} = \frac{(p_4/p_3)^{\frac{\gamma-1}{\gamma}} - 1}{(p_4/p_3)^{\frac{\gamma-1}{\gamma(1-\zeta)}} - 1} < (1 - \zeta) \qquad \text{IV}(35)$$

APPENDIX B: MANUFACTURING DRAWINGS

TURBINE BLADE PROFILE

TRANSONIC COMPRESSOR TEST RIG

2107

NAVAL POSTGRADUATE SCHOOL
DEPT. OF AERONAUTICS, TURBO PROPULSION LABORATORY

A — BLADING OF ROTOR PART 2108-1 WITH 32 BLADES, AND BLADING OF STATOR PART 2107-2 WITH 31 BLADES. BLADE DIMENSIONS ARE IDENTICAL WITH THOSE GIVEN BELOW LEFT

B — BLADING OF ROTOR PART 2108-2 WITH 32 BLADES, AND BLADING OF STATOR PART 2109-1 WITH 31 BLADES

(PROFILE CONSISTS OF CIRCULAR ARCS BETWEEN POINTS MARKED ⊕)

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NOTE 1) BOTH STATORS ARE IDENTICAL EXCEPT FOR THE ORIENTATION OF
THE BLADES
2) BLADE PROFILES ARE THE SAME FROM HUB TO TIP AND HAVE NO TWIST
3) PROFILE IS THE SAME FOR STATORS 1 AND 2 BUT ORIENTATION
IS REVERSED

DRILL #9 (.196 DIA)
12 HOLES THRU
EQ SPACED ON 4.50 B.C.

DRILL #25 (.1495)
12 HOLES THRU
EQ SPACED ON
3.90 B.C.

31 BLADES EQ. SPACED

SECTION A-A

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(

BODINE ELECTRIC MOTOR
TYPE KCI-23A2A1
115V, 15WATT, 67 RPM

SECTION B-B

PACKING .03 THICK

SECTION A-A

NAVAL POSTGRADUATE SCHOOL
DEPT. OF AERONAUTICS, TURBO PROPULSION LABORATORY

DRAWN M H VAVRA 5/14/70

USED ON 2158

SHEET 1 OF 1

SCALE FULL

TRANSONIC COMPRESSOR TEST RIG
CONTROL VALVE ACTUATOR

DWG NO 2159

SECTION C-C

SECTION D-D

SECTION B-B

VIEW FROM A

DETAIL II (FULL SCALE)

DETAIL I (FULL SCALE)

24 HOLES 3/16 EQ SPACED
ON 34 1/2 B.C., USE
PART 16 AS TEMPLATE

24 HOLES 9/16 EQ. SPACED
ON 34 1/2 B.C., USE
PART 17 AS TEMPLATE

DRILL 5/16 THRU
TAP 3/8-16 UNC
18 PLACES AT 2" CENTERS
IN EACH ITEM 5

8 HOLES 7/16 DIA
EQ. SPACED
ON 7 1/2 B.C.

DRILL 27/64 THRU
TAP 1/2-13 UNC THRU
4 PLACES IN EACH PART 8

8 HOLES 7/16 DIA EQ.
SPACED ON 7 1/2 B.C.
USE PART 12 AS TEMPLATE

MINIMUM CLEARANCE SO
THAT ITEMS 3 CAN BE
LOCATED EVERYWHERE
ALONG ITEMS 5

DRILL 7/16 THRU

DRILL 3/4 DIA THRU
TAP 3/8-18 NPT

FOR NOTES AND PARTS LIST SEE SHEET 2

161   D8

.06×45°

.88 BC

A

45°   .359   .20

$\frac{5}{16}$-24-UNF 2A

$\frac{1}{4}$-28-UNF 2A

.25

1.375
1.374

.20

.03×45°

.06R   .06R   .06R

DRILL #5 (.206 DIA) THRU
COUNTERBORE .359 DIA
.20 DEEP
4 PLACES EQ. SPACED
ON .88 B.C
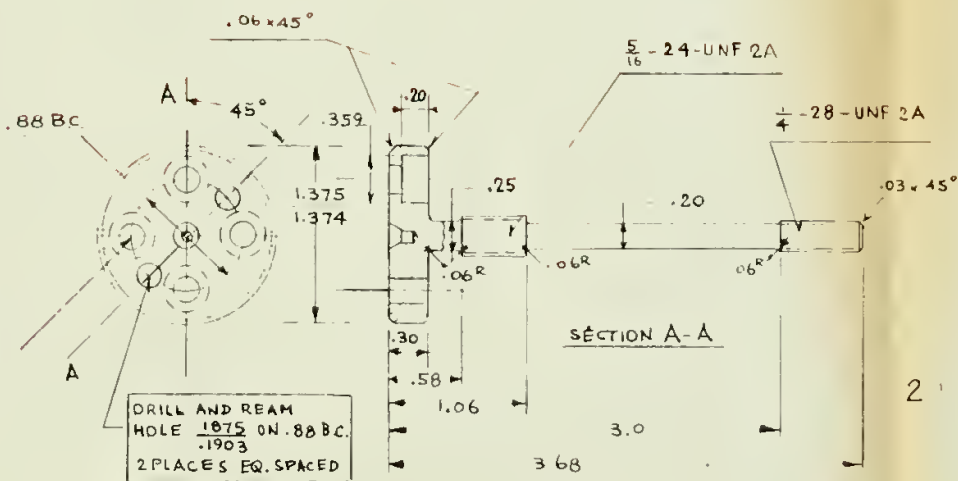
SECTION A-A

.30
.58
1.06

DRILL AND REAM
HOLE $\frac{.1875}{.1903}$ ON .88 B.C.
2 PLACES EQ. SPACED

3.0

3.68

2

1.62
1.16
.50
.25
.02×45°
3°45
1.7506
1.7496
1.44
2.005
2.000
1.69
.12R
.12R
15°
DRILL F
.287 .44 .75
1.39
1.98
1.75
2.0R
1.006
35°
.03R
.06
.12
.30
.187
.168

(1)

.03×45°
30°
.50
HEX
1.12
.50
.50 DIA
.03R
.12
.42
.25
30°
.88

DRILL 23 (.154 DIA) THRU
2 PLACES

DRILL I (.272 DIA) THRU
TAP $\frac{5}{16}$-24-UNF 2B

(3)

164   D 11
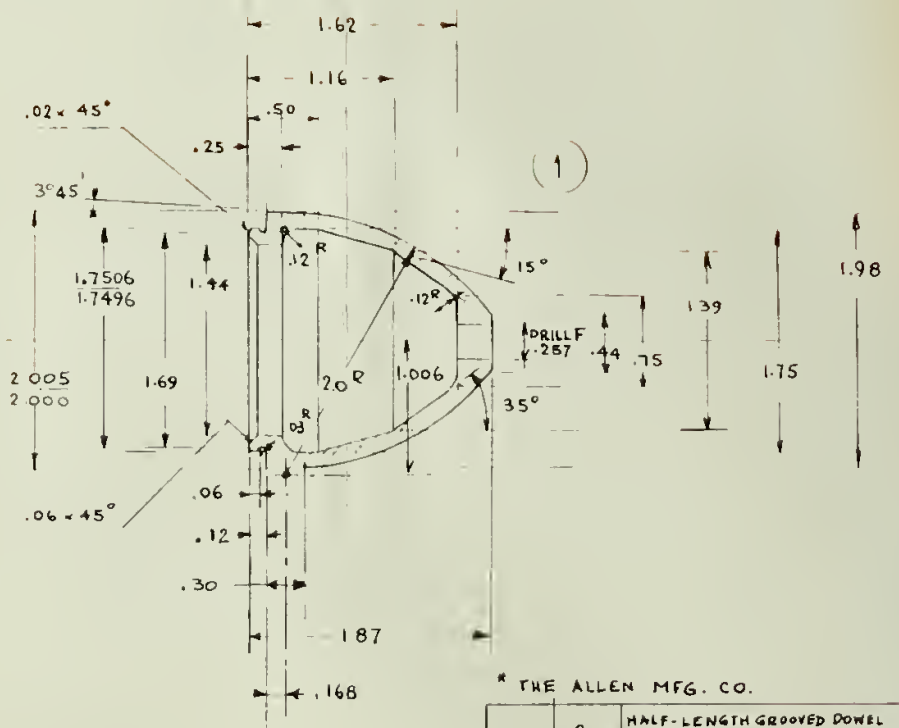
* THE ALLEN MFG. CO.

6	2	HALF-LENGTH GROOVED DOWEL PIN $\frac{3}{16}$ DIA × $\frac{3}{8}$ LG, TYPE B (ASA B.5.20-1958)	STEEL
5	2	CROSS-DRILLED SOCK. HEAD CAP SCREWS #6-32× $\frac{3}{8}$ LG.	ALLENOY ST. *
4	4	SOCK. HEAD CAP SCREWS #10-24× $\frac{3}{8}$ LG.	ALLENOY ST. *
3	1	NUT	ST. AISI 4140
2	1	SUPPORT	ST. AISI 4140
1	1	HUB SPINNER	MAKE FROM AL. ROD 2024-T4
			MATERIAL

NAVAL POSTGRADUATE SCHOOL
DEPT. OF AERONAUTICS, TURBO PROPULSION LABORATORY

DRAWN M.H. VAVRA   11/5/70

TOLERANCES
FRACTIONS ± F
DECIMALS .XX = ± .02
.XX = ± .01
.XXX = ± .005
ANGLES = ± °
BREAK SHARP EDGES .005R
DO NOT SCALE DRAWING

SHEET 1 OF 1
SCALE FULL

WHEEL ATTACHMENTS
HYBRID COMPRESSOR

DWG NO.
2205

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PROFILE COORDINATES

CONVEX SIDE	X1 Y1																				

CONCAVE SIDE	X2 Y2	0 0																			

NOTES:

1. COORDINATE Y2 AS SHOWN IN FIGURE IS NEGATIVE
2. DISTANCES .045" AND .45° ARE NOT CRITICAL BUT SHOULD BE EQUAL FOR ALL BLADES
3. FOR MISSING DIMENSIONS SEE DWG 2210-1
4. FOR 0.12" FILLETS BETWEEN BASE AND PROFILE SEE NOTE 5 OF DWG 2210-1
5. VIEW FROM "A" IS A VIEW FROM THE BLADE TIP TO THE BASE WITH 81/80 DIA
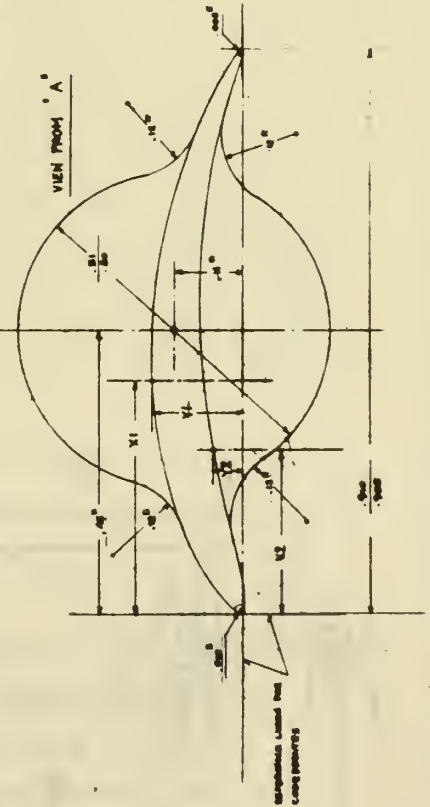
VIEW FROM "A"

REFERENCE LINES FOR COORDINATES

172

INLET CASING | 2214-2

NAVAL POSTGRADUATE SCHOOL
DEPT OF AERONAUTICS TURBO PROPULSION LABORATORY

NOTES:
1. MACHINE AFTER NORMALIZING
2. SURFACE FINISH ∇ EXCEPT WHERE SPECIFIED
3. SURFACES Ⓧ MUST BE CONCENTRIC WITHIN .002 T I R
4. ALL SECTIONS A-A HAVE THE HOLE, CHAMFEROOK AND TAPS AS SHOWN IN SECTION C-C
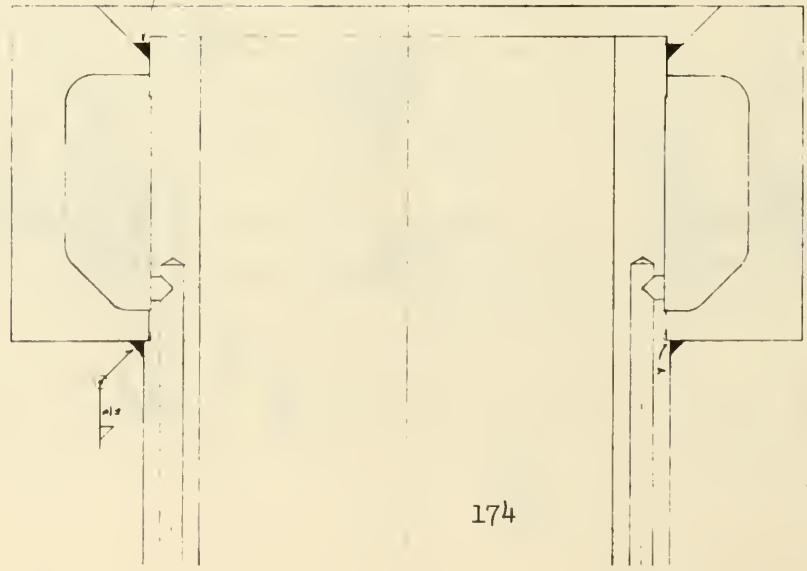
NOTE
1. PARTS 1 AND 2 MUST TOUCH AT STATION Y BEFORE WELDING
2. NORMALIZE AFTER WELDING (HEAT TO 1700°F AND COOL IN STILL AIR AT ROOM TEMPERATURE)

174

DRILL .531 DIA THRU
16 HOLES EQ SPACED
WITHIN .010 ON
22.00 B.C.

SECTION C-C
DRILL X (.397 DIA) THRU
C'BORE .68 DIA, .44 DEEP
4 PLACES ON 22.00 B.C
AT SECTIONS C-C

8 FINS EQ. SPACED
WELD BOTH SIDES
2 PLACES AT
EACH FIN

22.00 BC

DRILL R (.339 DIA) .44 DEEP
DRILL .062 DIA THRU
TAP 1/8-27 NPTF
4 PLACES EQ. SPACED

SECTION A-A

6.625
OD OF 6"
XX ST.
PIPE

NOTES
1. WELDED TYPE CONSTRUCTION WITH THRU
   WELDS AS INDICATED.
2. BEFORE MACHINING SURFACES WITH √
   NORMALIZE WELDMENT (HEAT TO 1700°F
   AND COOL IN STILL AIR AT ROOM TEMPERATURE
3. SURFACES MARKED (X) MUST BE CON-
   CENTRIC WITHIN .010 T.I.R. AND SQUARE
   WITH SURFACE (Y)
4. BORE WITH 5.375/5.380 MUST HAVE
   MINIMUM POSSIBLE TAPER

DETAIL
FULL SCALE

SHARP CORNERS

FULL RAD

SHARP CORNER

SMOOTH TRANSITION

.12 FULL RAD

176   D 23
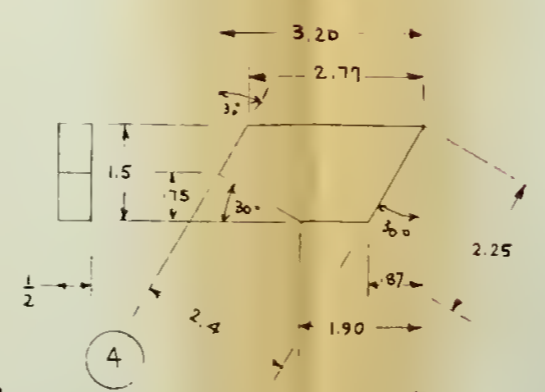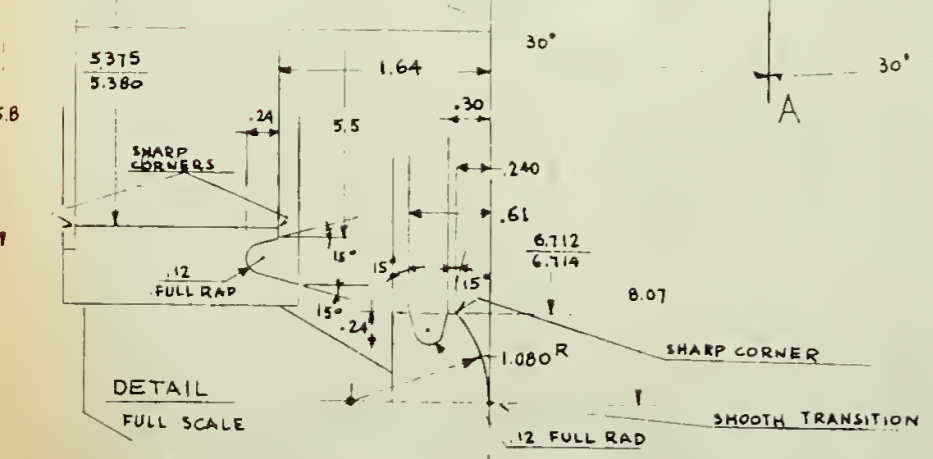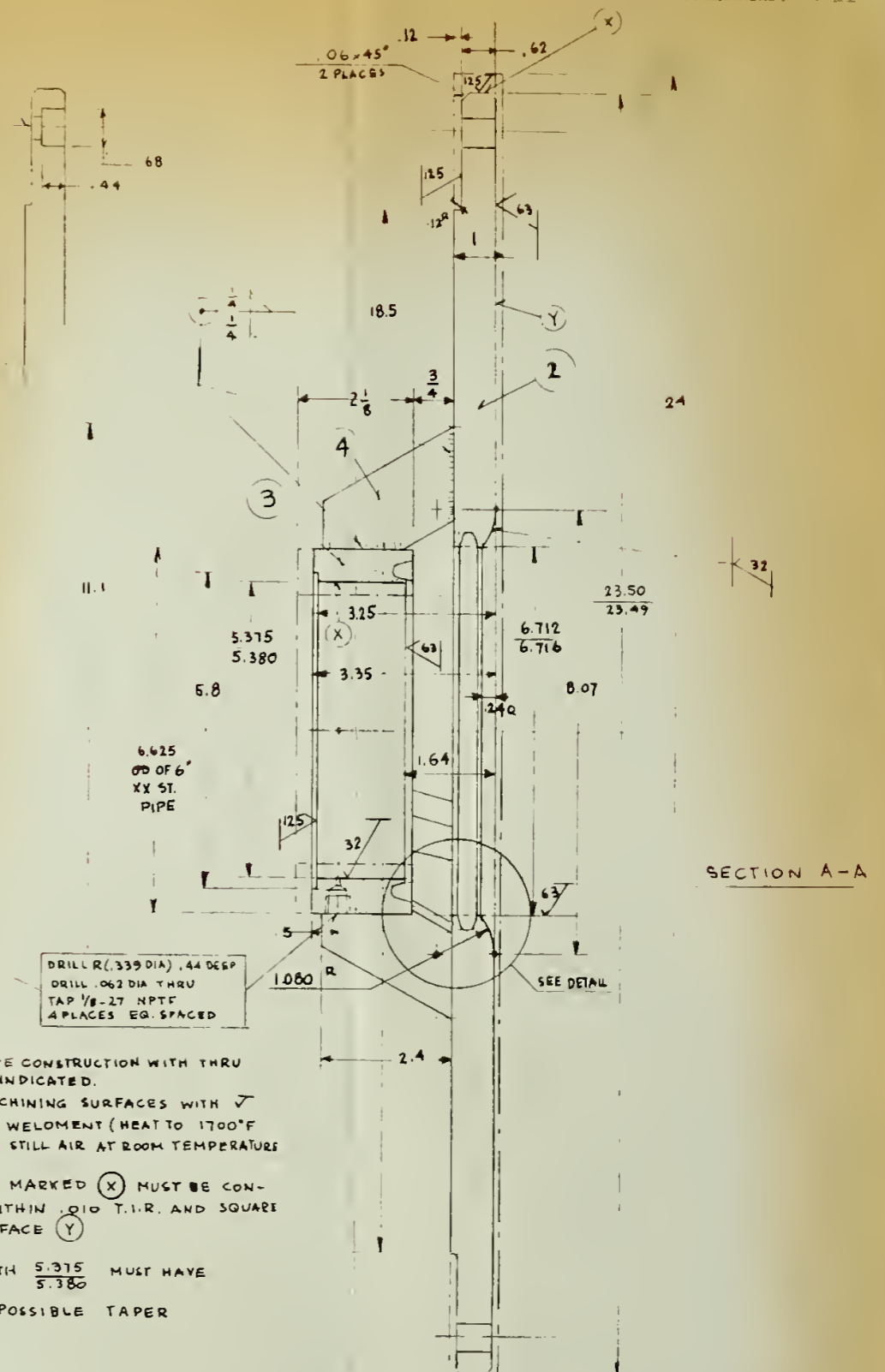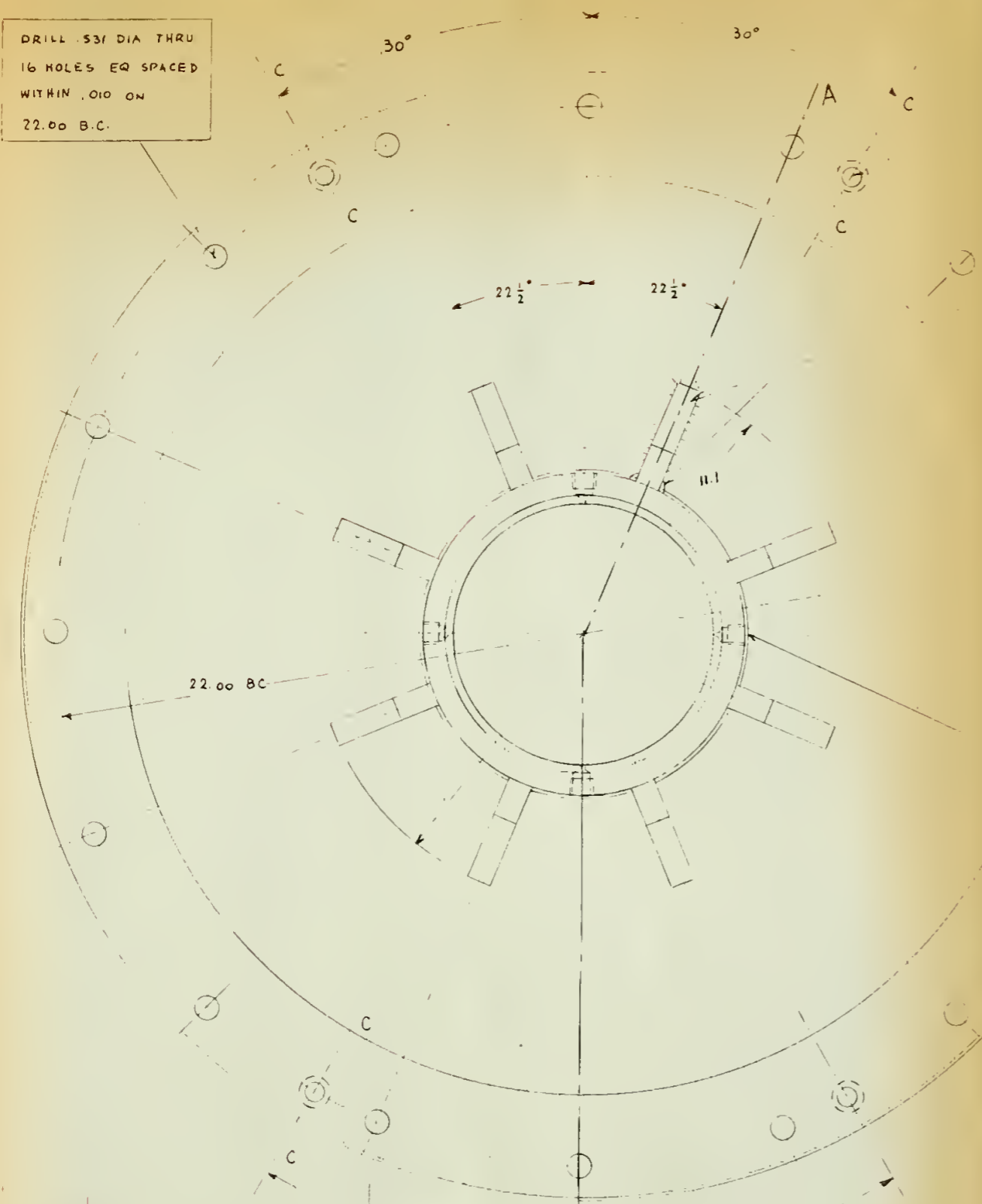
4	8	FINS 1/2 × 1/2 THICK × 3.20 LG	H.R. STEEL FLAT M 1020
3	1	SEAMLESS STEEL PIPE, 6" NOM. DOUBLE EXTRA STRONG, 6.625 OD × .864 WALL × 2 7/8 LG.	ASTM - A 53
2	1	PLATE 24 OD × 1" THICK	ASTM - A 36
1	1	NOZZLE (MACHINE FROM WELD-MENT OF ITEMS 2,3 AND 4)	
ITEM NO	REQ'D		MATERIAL

NAVAL POSTGRADUATE SCHOOL
DEPT. OF AERONAUTICS, TURBO PROPULSION LABORATORY

DRAWN M.H. VAVRA	11/15/70	REV	USED ON
CHECKED			SHEET 1 OF 1
APPD			SCALE HALF OR AS NOTED

FRACTIONS = ± 1/32
DECIMALS .x = ± .03
.xx = ± .01
.xxx = ± .005
ANGLES = ±
BREAK SHARP EDGES .005R
DO NOT SCALE DRAWING

NOZZLE FRAME

DWG NO
2216
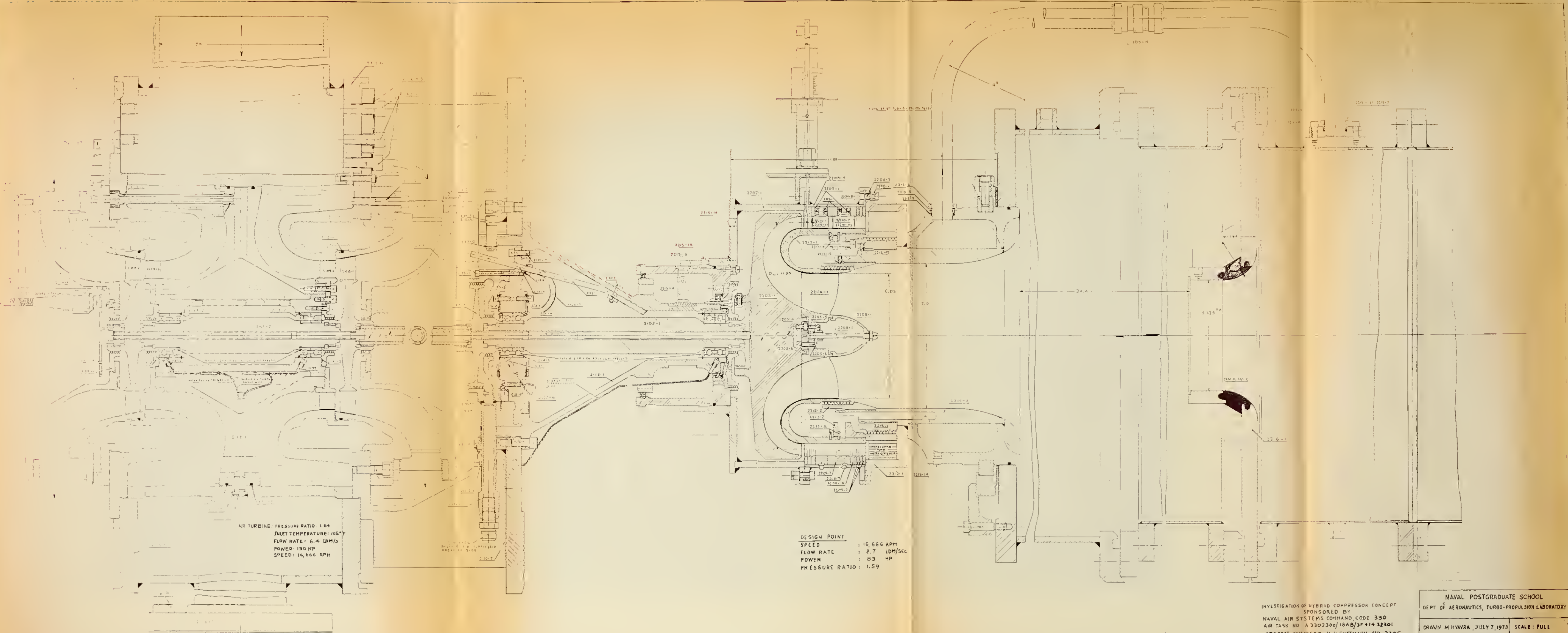
AIR TURBINE: PRESSURE RATIO: 1.64
INLET TEMPERATURE: 105°F
FLOW RATE: 6.4 LBM/s
POWER: 130 HP
SPEED: 16,666 RPM

DESIGN POINT
SPEED   : 16,666 RPM
FLOW RATE   : 2.7 LBM/SEC
POWER   : 83 HP
PRESSURE RATIO : 1.59

NAVAL POSTGRADUATE SCHOOL
DEPT OF AERONAUTICS, TURBO-PROPULSION LABORATORY

| DRAWN M H YAVRA JULY 7, 1973 | SCALE: FULL |
| TEST COMPRESSOR ASSEMBLY | DWG NO. 2222 |

ROTATING
THROTTLE VALVE (DWG 2-381)

AMBIENT AIR

INLET PLENUM (DWG 2164-1)

REMOTE CONTROLLED
BUTTERFLY VALVE

TURBINE INLET PIPE
(DWG 2136)

BLAST SHIELD

FOUNDATION (DWG 2155)

TURBINE EXHAUST

REMOTE CONTROLLED
BUTTERFLY VALVE

EMERGENCY BYPASS VALVE
(DWG 2146)

TO ATMOSPHERE

REMOTE CONTROLLED
BUTTERFLY VALVE
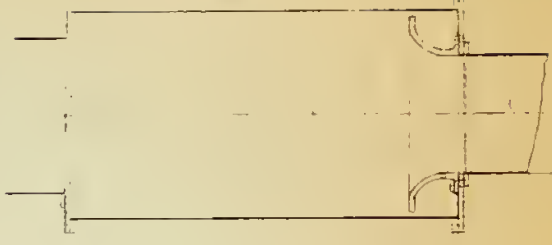
INVESTIGATION OF HYBRID COMPRESSOR CONCEPT
SPONSORED BY
NAVAL AIR SYSTEMS COMMAND
AIR TASK A330330 0/1868/3F41432301
PROJECT ENGINEER K H GUTTMANN, AIR-330C

NAVAL POSTGRADUATE SCHOOL	
TURBO-PROPULSION LAB, DEPT OF AERONAUTICS	
DRAWN. M H VAVRA, JULY 9, 1973	SCALE. 1:10
INSTALLATION OF HYBRID COMPRESSOR TEST RIG IN CELL 2 OF TURBO-PROPULSION LAB	DWG 2223

22½"
(MIN)

12'-4"
(MAX)

84"

15'-0"

28'-0"

HYBRID COMPRESSOR (DWG 2222)

FLOW NOZZLE

84"

74"

THROTTLE
ACTUATOR
(DWG 2-59)

ELECTRIC SERVO MOTOR

36"

DWG 2223

APPENDIX C

LOSSES IN RADIAL COMPRESSOR WHEELS

The flows in rotors of radial machines are greatly influenced by Coriolis and centripetal accelerations and are difficult to analyze even if viscous effects are ignored. The prediction of the losses in radial impellers constitutes an even more difficult task because of the complex three-dimensional nature of the real flow through such wheels which makes it impossible to apply conventional boundary layer theories or to use loss data for stationary channels or diffusors. At off-design operating conditions the prediction of the flow losses with theoretical means is nearly impossible because of local flow separations that occur in the wheels.

A more detailed discussion on losses in impellers of centrifugal compressors is given in paragraph 5 of Appendix A which also emphasizes the need for more and better experimental data. At present only a limited amount of such data is available in the open literature, for instance in Ref. 2 and Ref. 10. Although not directly applicable to the special rotor of the Hybrid compressor the test data of these references are evaluated in the following to obtain indications how the rotor losses are influenced by the different design parameters.

Reference 10 will be discussed first because it gives the losses in a particular rotor with specified dimensions which is shown in Fig. 12. Hence its pertinent geometrical characteristics are:

$$R_{1o}/R_2 = 0.541$$
$$R_{1i}/R_2 = 0.287$$
$$b_2/R_2 = 0.078$$

The blade angle at R_{1o} is given as 57°.

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Figure 13 shows the so-called polytropic impeller efficiency η_{RP} , which is defined in Ref. 11, as a function of β_{1o}, U_2/a_0 and the Mach number M_{W1} of the relative velocity W_{1o} at the inducer tip radius R_{1o}. Figure 13 is an exact reproduction of Fig. 4 of Ref. 10, but with the symbols of this report. The dashed parts of the curves for η_{RP} = constant are extrapolations by the writer. It is noticeable from Fig. 13 that the best rotor performance is obtained for positive incidence angles of about 9° if blockage because of the blade thickness is ignored. Reference 10 states that the inducer blades have a parabolic mean camber line and that their thickness is about 3% of the arc length of the camber line. Figure 14 gives the relations to determine the arc length m of a parabolic blade with axial length L and inlet blade angle β_B. From Fig. 12 there is L = 19.5 mm, and for $\beta_B = 57^o$, m = 21.51 mm. Hence the blade thickness t is equal to (0.03) (21.51) = 0.64 mm. In accordance with Eqs. 7 and 8, the flow angle β_{1o}' of Fig. 3b is

$$\tan \beta_{1o}' = \tan \beta_{1o} \left(\frac{s}{s - t/\cos \beta_B} \right) \qquad C(1)$$

For 20 rotor blades, and with the dimensions of Fig. 12,

$$s = \pi(97.4)/20 = 15.30 \text{ mm}$$

and for $\qquad t = 0.64$ mm, $\beta_B = 57^o$,

$$\tan \beta_{1o}' = \tan \beta_{1o} (0.923)$$

In Fig. 13 the angles β_{1o}' of this relation are shown on a special horizontal scale that is labeled β_{1o}'. Hence if the blockage due to the thickness of the blades is taken into account, the optimum incidence angle i' defined by Fig. 3b is still about $+7^o$, which is at variance with

the findings of Ref. 2 (see Fig. 24) where it is shown that incidence

angles of about zero at the inducer inlet give the best rotor performance.

The same conclusion is made in Ref. 12 on the basis of past experience.

The parametric curves M_{W1} = constant of Fig. 13 were transposed

from Fig. 4 of Ref. 10 also. In the following it will be shown that

these curves give data that are redundant since M_{W1} is known if U_2/a_0 ,

β_{1o}, and R_{1o}/R_2 are known. Reference 10 defines M_{W1} as the Mach number

of the relative velocity W_{1o} at R_{1o}. Independent of whether the absolute

velocity V_1 at the inducer inlet is constant or changing along the

radius R_1 ,

$$M_{W1} = \frac{W_{1o}}{a_1} = \frac{\omega \; R_{1o}}{\sin \; \beta_{1o}} = \frac{U_2}{R_2} \; R_{1o} \; \frac{1}{\sin \; \beta_{1o}} \qquad\qquad C(2)$$

The quantity a_1 is the velocity of sound of the flow at R_{1o} where the

static temperature is T_{1o}. Now, with

$$M_{V1} = \frac{V_{1o}}{a_1} = \frac{W_{1o} \; \cos \; \beta_{1o}}{a_1} = M_{W1} \; \cos \; \beta_{1o}$$

and

$$\frac{a_0}{a_1} = \sqrt{\frac{T_0}{T_{1o}}} = \left[1 + \frac{\gamma - 1}{2} \; M_{V1}^{\;2} \right]^{\frac{1}{2}}$$

there is

$$M_{W1} = \frac{U_2}{a_0} \; \frac{R_{1o}}{R_2} \; \frac{1}{\sin \; \beta_{1o}} \left[1 + \frac{\gamma - 1}{2} \; M_{W1}^{\;2} \; \cos^2 \; \beta_{1o} \right]^{\frac{1}{2}}$$

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and

$$M_{W1} = \frac{(U_2/a_0)\,(R_{1o}/R_2)}{\left[\sin^2 \beta_{1o} - \dfrac{\gamma-1}{2} \cos^2 \beta_{1o}\,(U_2/a_0)^2\,(R_{1o}/R_2)^2\right]^{\frac{1}{2}}} \qquad C(3)$$

This relation could have been derived directly from Eq. A II(4) but it has been developed here to show that it holds for arbitrary distributions of V_1 vs. R_1 and not only for uniform inlet velocities ahead of the rotor. Equation C(3) can be modified to obtain the angle β_{1o} as a function of U_2/a_0 and M_{W1}, or

$$\sin \beta_{1o} = (U_2/a_0)\,(R_{1o}/R_2)\sqrt{\frac{1/M_{W1}^2 + \dfrac{\gamma-1}{2}}{1 + \dfrac{\gamma-1}{2}\,(U_2/a_0)^2\,(R_{1o}/R_2)^2}} \qquad C(4)$$

At point A of Fig. 13 the curve $M_{W1} = 0.6$ intersects the line $U_2/a_0 = 0.9$ at an angle β_{1o} of $66.5°$, giving i = 66.5 - 57 = $9.5°$. However for $R_{1o}/R_2 = 0.541$ of the rotor of Fig. 12, $U_2/a_0 = 0.9$, $M_{W1} = 0.6$, and $\gamma = 1.4$, Eq. C(4) gives a flow angle

$$\beta_{1o} = 55.2°$$

so that the incidence angle without blockage is $-1.8°$ instead of $+9.5°$. Figure 15 has been obtained by calculating the angles $\beta_{1o} = \beta_{1o}*$ from Eq. C(4) with the values of U_2/a_0 along the curves M_{W1} = constant of Fig. 13 that pertain to particular efficiencies η_{RP}. Through the points thus obtained, which are marked by circles in Fig. 15, a new set of curves η_{RP} = constant has been drawn. In Eq. C(4) the value of R_{1o}/R_2 has been taken as 0.541 in accordance with the rotor dimensions of Fig. 12.

Figure 15 shows that the incidence angles are greatly reduced and that their values for optimum efficiencies become smaller with increasing ratios U_2/a_0 .

If Fig. 15 is correct; that is, if the relationship between M_{W1} , U_2/a_0, and η_{RP} in Fig. 13 is valid, but if the flow angles β_{1o} given in this figure are in error, the resulting incidence angles are more in line with experience. Then the argumentation in Ref. 10 based on its Fig. 5, which is presented as Fig. 16 in this report, namely, that positive incidence angles are necessary to obtain favorable velocity distributions along the inducer blades, would be without substance. The curves of Fig. 16 were obtained theoretically by neglecting blade thickness, compressibility and friction. It is very doubtful, however, whether velocity distributions similar to those shown in Fig. 16 occur along the actual inducer blades, not only because effects of blade thickness and leading edge shape were ignored, but primarily because the inducer was treated as a stationary cascade whose flow is not influenced by the impeller downstream of it. Hence no account is taken of Coriolis and centripetal accelerations and the fact that the inducer and impeller blades adjoin at the inducer discharge and form continuous blade surfaces from rotor inlet to rotor discharge. Hence at the station where the inducer and impeller blades join, the velocities on either side of a blade will differ and not be equal as Fig. 16 shows.

It will be tried to support the relationship presented in Fig. 15 by additional data of Ref. 10, namely, those given by its Fig. 3 which are presented here in Fig. 17. This figure shows the polytropic efficiency of the rotor of Fig. 12 at $U_2/a_0 = 0.83$ for three different diffusors.

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It is evident from Fig. 18 that the rotor performance is almost independent of the diffusor configurations, although the latter influences the range of operation of the compressor.

The rotor efficiencies of Fig. 17 are given as functions of the flow coefficient φ_1 , defined by

$$\varphi_1 = \frac{Q_1}{U_2 R_2^2} \qquad\qquad C(5)$$

where Q_1 is the volume flow rate at the inducer inlet. Because of the curved walls of the inlet duct ahead of the inducer of Fig. 12 the absolute velocity V_1 will vary from the inner radius R_{1i} to the outer radius R_{1o} of the inlet eye. Let $\overline{V}_1$ be the average velocity at the inducer inlet such that

$$Q_1 = A_1 \, k_{B1} \, \overline{V}_1 \qquad\qquad C(6)$$

where

$$A_1 = \pi \, R_{1o}^2 \left[1 - \left(\frac{R_{1i}}{R_{1o}} \right)^2 \right]$$

k_{B1} is the blockage factor at station (1). Then, from Eqs. C(5) and C(6)

$$\frac{\overline{V}_1}{a_0} = \frac{\varphi_1}{k_{B1}} \left(\frac{U_2}{a_0} \right) \left(\frac{R_2}{R_{1o}} \right)^2 \frac{1}{\pi \left[1 - (R_{1i}/R_{1o})^2 \right]} \qquad\qquad C(7)$$

The weight flow rate $\dot{w}$ through the compressor is

$$\dot{w} = Q_1 \frac{\overline{p}_1}{R_G \overline{T}_1} = \varphi_1 \, U_2 \, R_2^2 \frac{(\overline{p}_1/P_0) \, P_0}{R_G \, (\overline{T}_1/T_0)T_0} \qquad\qquad C(8)$$

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$\overline{p}_1$, $\overline{T}_1$ are the flow properties at the radius $\overline{R}_1$ where the velocity $\overline{V}_1$ occurs. Then, for an isentropic process from P_0, T_0 to $\overline{p}_1$, $\overline{T}_1$,

$$\frac{\overline{p}_1/P_0}{\overline{T}_1/T_0} = (\overline{T}_1/T_0)^{1/(\gamma-1)} \qquad\qquad C(9)$$

and, since

$$\overline{V}_1^2 = 2 g c_p (T_0 - \overline{T}_1) = \frac{2}{\gamma-1} a_0^2 \left[1 - \frac{\overline{T}_1}{T_0} \right]$$

or

$$\frac{\overline{T}_1}{T_0} = 1 - \frac{\gamma-1}{2} \left(\frac{\overline{V}_1}{a_0} \right)^2 \qquad\qquad C(10)$$

the dimensionless mass flow rate $(\dot{m})*$ of Eq. 66 becomes

$$(\dot{m})* = \frac{(\dot{w}/g)\sqrt{g R_G T_0}}{\pi R_2^2 P_0} = \frac{\varphi_1}{\pi}\left(\frac{U_2}{a_0}\right)\sqrt{\gamma}\left[1 - \frac{\gamma-1}{2}\left(\frac{\overline{V}_1}{a_0}\right)^2 \right]^{1/(\gamma-1)} \qquad C(11)$$

Since by Eq. C(7) the ratio $(\overline{V}_1/a_0)$ is a function of φ_1 and (U_2/a_0) for known impeller dimensions, the dimensionless mass flow rate $(\dot{m})*$ can be determined for assumed blockage factors k_{B1}.

The change of V_1 along R_1 can be determined approximately by assuming that the curvatures k_m of the generatrices of the axisymmetric stream surfaces at the inducer inlet vary linearly from k_{mi} at R_{1i} to k_{mo} at R_{1o}, where k_{mi} and k_{mo} are the curvatures of the meridional contours at these radii. In accordance with Eq. 11 (122) of Ref. 5

$$V_1 = V_{1i}\, e^{-\int_0^n k_m\, dn} \qquad\qquad C(12)$$

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where $n = R_1 - R_{li}$, and V_{li} is the velocity at R_{li}. As shown in Art. 3.3 of Ref. 5 the curvatures k_m in Eq. C(12) for the channel of Fig. 12 must be introduced as negative values. The assumed linear variation of k_m is given by

$$k_m = k_{mi} + \frac{k_{mo} - k_{mi}}{R_{lo} - R_{li}} (R_1 - R_{li})$$

C(13)

and the integral of Eq. C(12) becomes

$$-\int_0^n k_m \, dn = R_2 \, k_{mi} \left(\frac{R_1}{R_2} - \frac{R_{li}}{R_2} \right) + \frac{R_2 \, k_{mo} - R_2 \, k_{mi}}{2\left(\frac{R_{lo}}{R_2} - \frac{R_{li}}{R_2} \right)} \left(\frac{R_1}{R_2} - \frac{R_{li}}{R_2} \right)^2$$

C(14)

On examining Fig. 12 it can be noticed that the rotor drawing presented in Ref. 10 is not to scale. From the measured distances of the figure the radius ratios R_{lo}/R_2 and R_{li}/R_2 are about 0.59 and 0.275, instead of 0.541 and 0.287 in accordance with the dimensions of Fig. 12. Because of this situation it is not possible to determine the radii of curvature of the meridian contours at R_{li} and R_{lo} from Fig. 12 with graphical means. Although the approach explained in the following is speculative it is believed that it gives a sufficiently good approximation for k_{mi} and k_{mo}. It is based on the assumption that the meridian contours of the rotor are curves with the equation $r/a = \theta^{-b}$ in polar coordinates. As shown in Fig. 18 and explained in Program No. 110 of Appendix D, such curves have zero curvature at a point P_0 given by r_0/a and θ_0 for any value of b between zero and unity. For angles θ larger than θ_0 the curvatures increase smoothly to reach a maximum value of k_m at point P_m where the tangent to the curve is perpendicular to that at P_0.

The writer has investigated a large number of curves and believes that those with $r/a = \theta^{-b}$ have the smallest curvature k_m at P_m for a given ratio y_0/x_0 of the coordinates of Fig. 18. Three-dimensional flow analyses indicate that smoothly changing curvatures k of the meridian contours of a channel and small values of k produce small changes of the velocities across the width of the channel and along the flow paths. In addition to satisfying these conditions it is seen from Fig. 20 also that contours with $r/a = \theta^{-b}$ establish flow channels that look very much like those of high-performance radial impellers. The inner or hub contour is supposed to be located between station P_0 and P_m of Fig. 20. For this curve

$$y_0/x_0 = \frac{180 - 51.7}{2(44.5)} = 1.4416$$

From Fig. 12 it is apparent that the tip contour does not have zero curvature at the outer rotor diameter of 180 mm, but that it is curved to the diameter where the axial width of the diffusor is 7 mm. It can be seen from Ref. 10 that this diameter is 215 mm. Hence, in accordance with Fig. 20 the tip contour is supposed to extend from P_m' to P_0' having

$$y_0'/x_0' = \frac{215 - 97.4}{2(37.5)} = 1.5680$$

The points P_0 and P_0' correspond to station P_0 of Fig. 18 so that the curvatures of the meridian at these locations are zero.

Since no direct solution of the problem of establishing the exponent b in $r/a = \theta^{-b}$ for given ratios y_0/x_0 is possible, the Calculator Program No. 110 of Appendix D has been established to obtain this relationship with an iterative process. Figure 19 shows b as function of y_0/x_0

and gives the maximum curvature k_m at station P_m of Fig. 18 by the dimensionless quantity $x_0 \, k_m$. From Fig. 19 for the hub contour

$$k_m = k_{mi} = \frac{(1.174)}{44.5} = (2.638)(10^{-2}) \text{ mm}^{-1}$$

so that the radius of curvature R_{ci} is

$$R_{ci} = \frac{1}{k_{mi}} = 37.90 \text{ mm}$$

For the tip contour

$$k_m' = k_{mo} = \frac{1.232}{37.5} = (3.285)(10^{-2}) \text{ mm}^{-1}$$

or

$$R_{co} = \frac{1}{k_{mo}} = 30.44 \text{ mm}$$

The exponents b were found to be 0.2552 for the inner and 0.3525 for the outer contour. They were used to establish the coordinates of the meridian contours of Fig. 20.

The calculated curvatures k_{mi} and k_{mo} introduced into Eq. C(14) give

$$-\int_0^n k_m \, dn = -0.6815 + 2.3747 \frac{R_1}{R_2} + 1.1456 \left(\frac{R_1}{R_2} - 0.287\right)^2 \qquad \text{C(15)}$$

From Eqs. C(12) and C(15) for $R_1/R_2 = R_{1o}/R_2 = 0.541$

$$\frac{V_{1o}}{V_{1i}} = e^{0.67712} = 1.9682$$

or

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$$\frac{V_1}{a_0} = \frac{V_{1o}}{a_0} (0.5081) \ e^{-\int_0^n k_m \, dn} = \frac{V_{1o}}{a_0} X \qquad\qquad C(16)$$

Thus, for chosen values of V_{1o}/a_0 the ratios V_1/a_0 at the different radii R_1 are known, and it is possible to determine the corresponding weight flow rates by

$$\dot{w} = k_{B1} \int_{R_{1i}}^{R_{1o}} 2 \pi \ R_1 \ V_1 \ \frac{p_1}{R_G \ T_1} \ dR_1$$

or

$$\dot{w} = 2 \pi \ R_2^2 \ k_{B1} \ \frac{P_0}{T_0} \ \frac{a_0}{R_G} \int_{R_{1i}/R_2}^{R_{1o}/R_2} \frac{R_1}{R_2} \ \frac{V_1}{a_0} \ \frac{p_1/P_0}{T_1/T_0} \ d\left(\frac{R_1}{R_2}\right)$$

Similar to Eqs. C(9) and C(10)

$$\frac{p_1/P_0}{T_1/T_0} = \left[1 - \frac{\gamma-1}{2} \left(\frac{V_1}{a_0}\right)^2\right]^{1/(\gamma-1)}$$

Then, since $R_{1i}/R_2 = 0.287$ and $R_{1o}/R_2 = 0.541$, the dimensionless mass flow rate $(\dot{m})*$ of Eq. C(11) is obtained also from

$$(\dot{m})* = 2 \ k_{B1} \sqrt{\gamma} \left(\frac{V_{1o}}{a_0}\right) \int_{0.287}^{0.541} \left(\frac{R_1}{R_2}\right) X \left[1 - \frac{\gamma-1}{2} \left(\frac{V_{1o}}{a_0} X\right)^2\right]^{1/(\gamma-1)} d\left(\frac{R_1}{R_2}\right) \quad C(17)$$

where X is defined by Eq. 16.

With Eqs. C(11) and C(17) the flow coefficient φ_1 can be related to V_{1o}/a_0 by determining $\overline{V}_1/a_0$ from Eq. C(7) for particular values of φ_1 and calculating $(\dot{m})*$ by Eq. C(11). Then, that ratio V_{1o}/a_0 has to be established which,

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introduced in Eq. C(16) and used in Eq. C(17), gives the same value of (m)*. Since the same blockage factor k_{B1} is used in both calculating procedures, its influence on the relationship between φ_1 and V_{1o}/a_0 is small, and a constant value $k_{B1} = 0.97$ will be assumed. For the ratios V_{1o}/a_0 thus determined, the flow angle β_{1o} at R_{1o} is given by

$$\tan \beta_{1o} = \frac{\omega R_{1o}}{V_{1o}} = \frac{(U_2/a_0)(R_{1o}/R_2)}{(V_{1o}/a_0)} = \frac{0.44903}{(V_{1o}/a_0)} \qquad C(18)$$

The rotor efficiencies η_{PR} of Fig. 17 which hold for $U_2/a_0 = 0.83$ can therefore be related to the flow angle β_{1o} at the tip of the inducer. With the calculated data it is possible also to establish the Mach number M_{W1} at the inducer tip radius by means of Eq. C(3). For $\gamma = 1.4$

$$M_{W1} = \frac{0.44903}{\left[\sin^2 \beta_{1o} - (0.2)(0.44903)^2 \cos^2 \beta_{1o} \right]^{\frac{1}{2}}} \qquad C(19)$$

These calculations have been performed on a Monroe 1655 Calculator. In particular, the evaluation of Eq. C(17) for the velocity ratios of Eq. C(16) has been carried out with Program No. 108 of Appendix D. Figure 21 shows the dimensionless mass flow rate $(\dot{m})*$ as functions of φ_1 and of V_{1o}/a_0. The relationship $(m)* = f_1(\varphi_1)$ has been obtained from Eqs. C(11) and C(10), and $(m)* = f_3(V_{1o}/a_0)$ is the result of the calculations with Program No. 108. Whereas $f_1(\varphi_1)$ depends solely on the rotor dimensions which are given by Fig. 12, the accuracy of the function $f_3(V_{1o}/a_0)$ depends on how well the assumed stream surface curvatures correspond to reality.

Figure 21 also shows the rotor efficiency η_{RP} as function of φ_1.
This curve has been obtained from the test data of Fig. 17, and represents
the best estimate of a continuous curve that can be drawn through all the
test points between $\varphi_1 \cong 0.11$ and $\varphi_1 \cong 0.275$. With this composite diagram the flow
functions φ_1 can be determined for chosen ratios V_{1o}/a_0, since corres-
ponding values must have the same dimensionless mass flow rate $(\dot{m})*$.
Hence, as shown in Fig. 21, it is also possible to obtain η_{RP} as a func-
tion of V_{1o}/a_0. Moreover, since by Eq. C(18) the relationship between
the flow angle β_{1o} and V_{1o}/a_0 is known for the velocity distribution of
Eq. C(16), the rotor efficiency η_{RP} is obtained as function of the angle
β_{1o} at the speed ratio $U_2/a_0 = 0.83$ for which the data of Fig. 17 hold.
Moreover, Eq. C(19) establishes the Mach number M_{W1} for different flow
angles β_{1o}. The data thus obtained are marked by circles in Fig. 22.
It can be seen that the maximum rotor efficiency occurs at a flow angle of
about 55°; that is, at an incidence angle i of about -2^O. The data points
marked by crosses in Fig. 22 are from Fig. 15 for $U_2/a_0 = 0.83$. Both
curves of η_{RP} have the same maximum at about the same flow angle, but
the efficiencies from Fig. 15 decrease more rapidly with flow angle on
either side of the maximum than the data from Fig. 21. Figure 15 was
obtained from the data of Ref. 10, shown in Fig. 13, by determining the
flow angle $(\beta_{1o}*)$ with Eq. C(4) on assuming that U_2/a_0 and M_{W1} of Fig. 13
are correct and that the rotor dimensions are those given by Fig. 12.
Inspite of the much smaller range of rotor efficiency with inlet flow
angle which the data from Fig. 15 exhibit, it is remarkable how well the
Mach numbers M_{W1} of the two approaches of Fig. 22 coincide.

For purposes of discussion the curves of η_{PR} and M_{W1} obtained from Fig. 21 are compared in Fig. 23 with the data of Fig. 13 at $U_2/a_0 = 0.83$ which are marked by crosses, and which represent the original values given by Ref. 10. It must be noted, however, that in Fig. 23 the curves from Fig. 13 are plotted against a scale marked β_{lo}** which is shifted by about 12° with respect to the horizontal scale β_{lo} that holds for the data from Fig. 21. This shift has been chosen such that the two curves for η_{RP} coincide as closely as possible.

The conclusions that can be drawn from the preceeding analyses are:

- (1) The curves of Fig. 13 are not consistent because, for the rotor dimensions of Fig. 12, the flow angles β_{lo} must be different than those of Fig. 13 if the velocity ratios U_2/a_0 and the Mach numbers M_{W1} of this figure are assumed to be correct, and doubt exists whether optimum efficiencies are reached at incidence angle i of about $+9^O$.

- (2) If the curves of Fig. 13 are plotted against the flow angle β_{lo}*, obtained from Eq. C(4) to establish the correct relationship between U_2/a_0 and M_{W1}, the resulting curves of Fig. 15 give optimum incidence angle i of about -2^O.

- (3) If other original values of Ref. 10 for $U_2/a_0 = 0.83$, presented in Fig. 17, are analyzed with the best possible procedure, the optimum incidence angle i is also about -2^O but, as shown in Fig. 22, the range in which the flow angle can vary for a specified off-design efficiency is about twice that of the curves of Fig. 15 described in point (2) above. However, the inlet Mach numbers M_{W1} of the two approaches lie on the same curve.

- (4) If the relations computed from Fig. 17 are compared with the original results of Fig. 13, it is seen from Fig. 23 that the two curves $\eta_{RP} = f(\beta_{1o})$ at $U_2/a_0 = 0.83$ can be made to coincide only if the flow angles of Fig. 13 are reduced by about 12°. In this case, however, different inlet Mach numbers M_{W1} occur.

- (5) The discrepancies in the data from Ref. 10 make it inadvisable to use Fig. 13 with reduced flow angles, or Fig. 15, where the range of flow angle for given off-design efficiency is very much smaller than that derived from Fig. 17.

- (6) It is not believed that the design criteria of Ref. 10 have general applicability. The inconsistencies in the data could be due to non-uniform inlet velocity distributions because of the shape of the inlet duct and its supporting fins. It is possible also that the flow angle measurements are in error or that the dimensions of the rotor are different from those given by Fig. 12.

Test data of radial compressor wheels are presented also in Ref. 2. The curves of Fig. 23b of Ref. 2 are redrawn in Fig. 24 of this report in a somewhat modified form, and with U_2/a_0 instead of with $U_2/\sqrt{T_0}$ as parameter. There is, in metric units for air,

$$\frac{U_2}{a_0} = \frac{U_2}{\sqrt{\gamma\ R_G\ g\ T_0}} = \frac{U_2}{\sqrt{T_0}}\ \frac{4.9874}{100}$$

for:

$\gamma = 1.4$

$R_G = \mathcal{R}/M = 847.83/28.964 = 29.272\ (m/^{\circ}K)$

$g = 9.81\ (m/s^2)$

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The incidence angle i' of Fig. 24 equals

$$i' = \beta_{1o}' - \beta_{Bo}$$

where β_{1o}' is the flow angle at R_{1o} obtained from Eq. C(1) by taking account of the blockage due to the inducer blade thickness, and β_{Bo} is the inducer blade angle at R_{1o}. Reference 2 does not give the dimensions and the inducer blade angles of the rotor for which Fig. 24 has been established. Hence Mach number M_{W1} and peripheral speed ratio U_2/a_0 cannot be related to each other by, say, Eq. C(3). Point D of Fig. 25, which gives the curves of Fig. 24 also corresponds to the design point of the Hybrid impeller with $M_{W1} = 0.4842$; $i' \cong + 0.5^{o}$, and $U_2/a_0 = 0.7156$. It can be noticed that for these values of M_{W1} and i' the parameter U_2/a_0 of Figs. 24 and 25 is very nearly equal to 0.7156. It was decided, therefore, to ignore the curves $U_2/a_0 =$ constant in Fig. 24 for the off-design performance calculations of the Hybrid compressor and to assume that $r_e = \eta_R/\eta_{RMAX}$ is only depending on M_{W1} and i' , not only because of the limited information given in Ref. 2 but also because these two quantities seem to be the most important variables that affect the rotor efficiency. The curve labeled "Max. Flow Rate" in Fig. 24 appears to represent the limit at which stable operation is possible, probably because of the flow separations that occur on the pressure, or concave, sides of the inducer blades at these negative incidence angles. The surge limit of Fig. 24 is that which occurs if a non-bladed diffusor is arranged after the impeller. Hence, for bladed diffusors, compressor surge may be initiated by separations in the diffusor at incidence angles i' smaller than those of Fig. 24.

APPENDIX D

CALCULATING PROGRAMS

FOR

MONROE MODEL 1655/56

ELECTRIC PROGRAMMABLE DISPLAY CALCULATOR

WITH

CARD READER CR-1

AND

MONROE MODEL 1880-22

SCIENTIFIC PROGRAMMABLE PRINTING CALCULATOR

PROGRAM No. 102

MONROE CALCULATOR 1655 WITH CARD READER CR-1

Description

Program 102 calculates the dimensionless flow rate of a radial compressor

from the conditions at the impeller discharge. From Eq. II (11) of Ref. (a)*,

$$\Phi_2 = \frac{\dot{w}\sqrt{(R_G/g)T_0}}{P_0\,A_2\,k_{B2}} = \mu\sqrt{\gamma}\,\cot\alpha_2\left(\frac{U_2}{a_0}\right)\frac{p_2/P_0}{T_2/T_0}$$

where:

$\dot{w}$ = weight flow rate (lbm/s)

R_G = gas constant (ft-lb/(lbm,$^{\circ}$R))

g = 32.174 (ft/s^2)

T_0 = total temperature ahead of rotor ($^{\circ}$R)

P_0 = total pressure ahead of rotor (psia)

$A_2 = 2\pi\,R_2\,b_2$ = rotor discharge area (in.^{2})

k_{B2} = restriction factor (-)

$A_1 = \pi\,(R_{lo}^2 - R_{li}^2)$ = rotor inlet area (in.^{2})

k_{B1} = restriction factor (-)

μ = slip factor (-)

$\gamma = c_p/c_v$ (-)

α_2 = absolute flow angle at rotor discharge ($^{\circ}$)

U_2 = peripheral rotor speed (ft/s)

$a_0 = \sqrt{g\,\gamma\,R_G\,T_0}$

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*(a) Vavra, M. H., "Basic Elements for Advanced Design of Radial
Flow Compressors," in AGARD-LS-39-70, "Advanced Compressors,"
Techn. Editing & Reprod. Ltd; London 1970.

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p_2 = static pressure out rotor discharge (psia)

T_2 = static temperature at rotor discharge (^{O}R)

From Eqs. I(20) and I(8) of Ref. (a)

$$\frac{p_2}{P_0} = (T_2'/T_0)^{\gamma(\gamma-1)}$$

$$\frac{T_2'}{T} = 1 + (\gamma-1)\, \mu \left(\frac{U_2}{a_0}\right)^2 \left[\frac{1}{\psi^2}\left(1 - \frac{\mu}{2\sin^2\alpha_2}\right) - \frac{1}{2\mu}\left(\frac{1}{\psi^2} - 1\right)\right]$$

From Eq. I(7) of Ref. (a)

$$\frac{T_2}{T_0} = 1 + (\gamma-1)\, \mu \left(\frac{U_2}{a_0}\right)^2 \left(1 - \frac{\mu}{2\sin^2\alpha_2}\right)$$

The velocity coefficient

$$\psi = \frac{W_2}{W_{2\ is}}$$

establishes the rotor loss in accordance with Ref. (a).

The following quantities will be used during the calculations:

$$A = 1 - \frac{\mu}{2\sin^2\alpha_2}$$

$$B = \frac{1}{2\mu}\left(\frac{1}{\psi^2} - 1\right)$$

$$C = (\gamma-1)\, \mu \left(\frac{U_2}{a_0}\right)^2$$

$$D = \mu\sqrt{\gamma}\, \cot \alpha_2 \left(\frac{U_2}{a_0}\right)$$

Then

$$T_2'/T_0 = F = 1 + C\left(\frac{1}{\psi^2} A - B\right)$$

$$p_2/P_0 = F^{\gamma/(\gamma-1)}$$

$$T_2/T_0 = 1 + C\,A$$

$$\Phi_2 = D\,\frac{(p_2/P_0)}{(T_2/T_0)}$$

$$X = \Phi_2\,A_2\,k_{B2} = \frac{\dot{w}\sqrt{(R_G/g)\,T_0}}{P_0}$$

$$\Phi_1 = \frac{X}{A_1\,k_{B1}} = \frac{\dot{w}\sqrt{(R_G/g)\,T_0}}{P_0\,A_1\,k_{B1}}$$

The flow function Φ_1 will be used in program No. 103 to establish the ratios p_1/P_0 and T_1/T_0. The area $A_1 = \pi\,(R_{1o}^2 - R_{1i}^2)$ must be introduced in square inches.

Enclosures: Operating Instructions (1 page)
              Program Listing (4 pages)

OPERATING INSTRUCTIONS PROGRAM No. 102

MONROE CALCULATOR 1655/6 WITH CARD READER CR-1

Set-Up: (RESET); (TO(0)); Depress (LOAD); Read Cards 1-3

Release (LOAD); (TO(0)); Depress (P); (RESUME)

P-COUNT			
0 0 1	ENTER:	γ	(RESUME)
0 1 2	" :	U_2/a_0	(")
0 1 4	" :	α_2	(")
0 2 3	" :	μ	(")
0 3 4	" :	ψ	(")
1 3 4	" :	A_2	(")
1 3 6	" :	k_{B2}	(")
1 4 1	" :	A_1	(")
1 4 3	" :	k_{B1}	(")
1 4 6	RESULTS:		

$\uparrow$ (1) $\rightarrow$ T_2/T_0

$\uparrow$ (0) $\rightarrow$ p_2/p_0

$\uparrow$ (4) $\rightarrow$ $\dfrac{\dot{w}\sqrt{(R_G/g)T_0}}{P_0}$

$\uparrow$ (3) $\rightarrow$ $\Phi_2 = \dfrac{\dot{w}\sqrt{(R_G/g)T_0}}{P_0 \, A_2 \, k_{B2}}$

$\uparrow$ (5) $\rightarrow$ $\Phi_1 = \dfrac{\dot{w}\sqrt{(R_G/g)T_0}}{P_0 \, A_1 \, k_{B1}}$

(RESUME)

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TURBO-PROPULSION LABORATORY, DEPT. OF AERONAUTICS, NPS,
PROGRAM No. 102 .... MONROE 1655 CALCULATOR
PAGE. 1 OF 4.
FLOW RATE THROUGH RADIAL COMPRESSOR FOR GIVEN
DATE: .. AUG 72   BY: M.H.VAR
·CONDITIONS AT DISCHARGE

REGISTERS

Register	Contents
0	$\frac{\gamma-1}{\gamma}$
2	γ
3	A
4	μ
5	$\sin^2\alpha_2$
6	U_2/a_0
7	$1/\psi^2$

Program listing

Address	Command	Code	E
00	HALT	4 0 1	γ
01	STR(2)	4 4 –	γ
02	–	0 6 2	
03	–	0 0 –	
04	÷	0 7 2	$\gamma-1$
05	RCL(2)	4 6 –	γ
06	=	0 2 0	$\frac{\gamma-1}{\gamma}$
07	INV	0 5 4	$\frac{\gamma}{\gamma-1}$
10	STR(0)	4 5 7	
11	HALT	4 0 1	
12	STR(6)	4 4 5	
13	HALT	4 0 1	α_2
14	SIN/COS	0 4 4	$\sin\alpha_2$
15	×	0 7 0	
16	=	0 2 0	$\sin^2\alpha_2$
17	STR(5)	4 4 4	$\sin\alpha_2$
20	INV.γ	0 5 4	μ
21	×	0 7 0	
22	HALT	4 0 1	$\frac{\mu}{\sin\alpha_2}$
23	STR(4)	4 4 –	
24	÷	0 7 2	
25	2	0 0 –	
26	1	0 6 –	$\frac{\mu}{2\sin\alpha_2}$
27	–	0 0 –	
30	=	0 2 0	$-A$
31	CHSGN	0 1 –	A
32	STR(3)	4 4 2	
33	HALT	4 0 1	ψ
34	INV	0 5 4	$1/\psi$
35	×	0 7 0	
36	–	0 6 2	$1/\psi^2$
37	STR(7)	4 4 6	

NOTES

- ENTER: γ
- ENTER: U_2/a_0
- ENTER: α_2
- ENTER: μ
- ENTER: ψ

BR PT: 0 , 1

Registers

Reg	Label
0	$\dfrac{\gamma}{\gamma-1}$ / P_2/P_0
1	C
2	γ
3	A
4	μ
5	$\sin^2\alpha_2$
6	U_2/a_0
7	$1/\gamma^2$
8	B

Program listing

BR PT	Address (P Count)	Command	Code	E
2	0	1	0 0 1	
	1	÷	0 7 2	$\tfrac{1}{\gamma^2}-1$
	2	2	0 0 2	
	3	÷	0 7 2	$\tfrac{1}{2}\!\left(\tfrac{1}{\gamma^2}-1\right)$
	4	RCL(4)	4 6 3	μ
	5	=	0 2 0	B
	6	STR(8)	4 4 7	
	7	RCL(2)	4 6 1	γ
	0	1	0 6 2	
	1	–	0 6 0	$\gamma-1$
	2	RCL(4)	4 6 3	μ
	3	×	0 7 0	$\mu(\gamma-1)$
	4	RCL(6)	4 6 5	U_2/a_0
	5	×	0 7 0	
	6	RCL(6)	4 6 5	U_2/a_0
	7	=	0 2 0	C
	0	STR(1)	4 4 0	
	1	RCL(7)	4 6 6	$1/\gamma^2$
	2	×	0 7 0	
	3	RCL(3)	4 6 2	A
	4	–	0 6 0	
	5	RCL(8)	4 6 7	B
	6	×	0 7 0	
	7	RCL(1)	4 6 0	C
	0	+	0 6 0	
	1	–	0 0 0	
	2	a^x	0 7 4	T_2/T_0
	3	RCL(0)	4 7 7	
	4	=	0 2 0	P_2/P_0
	5	STR(0)	4 5 7	
3	7	RCL(1)	4 6 0	C

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REGISTERS (stored values)

Reg 0	Reg 1	Reg 2	Reg 3	Reg 4	Reg 5	Reg 6
P_2/P_0	C	y	A	μ	$\sin^2\alpha$	U_2/g_0

BR PT	ADDRESS	COMMAND	CODE	E
4	1 0 0	$\times$	0 7 0	
	1 0 1	RCL(3)	4 6 2	A
	1 0 2	$+$	0 6 0	CA
	1 0 3	$-$	0 0 1	
	1 0 4	$=$	0 2 0	
	1 0 5	STR(1)	4 4 0	T_2/T_0
	1 0 6	$-$	0 0 1	
	1 0 7	$-$	0 6 2	
	1 1 0	RCL(5)	4 6 4	$\sin^2\alpha_2$
	1 1 1	$\div$	0 7 2	$\cos^2\alpha_2$
	1 1 2	RCL(5)	4 6 4	$\sin\alpha_2$
	1 1 3	$\times$	0 7 0	$\cot^2\alpha_2$
	1 1 4	RCL(2)	4 6 1	y
	1 1 5	$=$	0 2 0	$y\cot\alpha_2$
	1 1 6	$\sqrt{\ }$	0 5 6	$\sqrt{y\cot\alpha_2}$
5	1 1 7	$\times$	0 7 0	U_2/g_0
	1 2 0	RCL(6)	4 6 5	
	1 2 1	$\times$	0 7 0	μ
	1 2 2	RCL(4)	4 6 3	
	1 2 3	$\times$	0 7 0	
	1 2 4	I	0 0 1	$\mathcal{D}$
	1 2 5	$\times$	0 7 0	P_2/P_0
	1 2 6	RCL(0)	4 7 7	
	1 2 7	$\div$	0 7 2	T_2/T_0
	1 3 0	RCL(1)	4 6 0	ϕ_2
	1 3 1	$\times$	0 7 0	
	1 3 2	STR(3)	4 4 2	A_2
	1 3 3	HALT	4 0 0	
	1 3 4	$\times$	0 7 0	k_{B2}
	1 3 5	HALT	4 0 1	X
	1 3 6	$\div$	0 7 2	
	1 3 7	STR(4)	4 4 3	

NOTES: ENTER: A_2 (at address 1 3 3); ENTER: k_{B2} (at address 1 3 5)

Registers used in body: Reg 1 $= T_2/T_0$; Reg 3 $= \phi_2$; Reg 4 $= X$

BR PT	P COUNT	COMMAND	CODE			E	0	1	2	3	4	5	6	NOTES
6	0	HALT	4	0	1	A_1	P_2/P_0	T_2/T_0	X	ϕ_2	X	$\sin^2\alpha_2$	U_2/a_0	ENTER: A_1
	1	÷	0	7	2									
	2	HALT	4	0	1	k_{B1}								ENTER: k_{B1}
	3	=	0	2	0	ϕ_1	P_2/P_0	T_2/T_0	x	ϕ_2	X	ϕ_1		
	4	STR(5)	4	4	4									RESULTS:
	5	HALT	4	0	1									
	6	TO(0)	7	4	0									

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MONROE CALCULATOR 1655/6 WITH CARD READER CR-1

Description

Program 103 deals with the flow of a perfect gas with $\gamma = c_p/c_v = $ constant

that passes through a given area A. Because of boundary layers the effective

flow area is supposed to be k_B A. The total pressure P_t and the total

temperature T_t of the flow are known. To be determined is the average

static pressure p that exists at the flow area k_B A. The equation of

continuity can be expressed by a dimensionless flow function Φ where

$$\Phi = \sqrt{\frac{2\gamma}{\gamma-1}\left[\left(\frac{p}{P_t}\right)^{2/\gamma} - \left(\frac{p}{P_t}\right)^{(\gamma+1)/\gamma}\right]}$$

where

$$\Phi = \frac{\dot{w}\sqrt{(R_G/g)T_t}}{k_B A P_t} = \frac{\dot{m}\sqrt{g\,R_G\,T_t}}{k_B A P_t}$$

There are:

$\dot{w}$ = weight flow rate (lbm/s)

$\dot{m}$ = mass flow rate (slug/s)

R_G = gas constant (ft-lb/(lbm,$^\circ$R))

g = 32.174 (ft/s^2)

k_B A = effective cross-sectional area of channel where static

pressure p occurs

P_t, p   (psia)

T_t ($^\circ$R)

A   (in.^{2})

Figure D 103 shows a plot of Φ vs. $r = p/P_t$. At the critical pressure

ratio r_c the function $\Phi = \Phi_c$ has a maximum, hence no solutions occur if

$\bar{\Phi}$ is larger than Φ_c. There are:

$$r_c = \left(\frac{2}{\gamma + 1}\right)^{\gamma/(\gamma-1)} = \left[\left(\frac{2}{\gamma + 1}\right)^{1/(\gamma-1)}\right]^{\gamma}$$

and

$$\Phi_c = \sqrt{\frac{2\gamma}{\gamma + 1}} \left(\frac{2}{\gamma + 1}\right)^{1/(\gamma-1)}$$

If $\bar{\Phi}$ is smaller than Φ_c two solutions of $r = p/P_t$ are obtained, say, r_I if the velocity at the area A is subsonic, and r_{II} if the flow is super-sonic. These pressure ratios must be obtained with an iterative process, by assuming a value of r, say r_i, and verifying whether the corresponding value Φ_i equals the specified flow function $\bar{\Phi}$.

The following quantities are used in the calculations

$E1 = 2/\gamma$

$E2 = (\gamma+1)/\gamma$

$A = 2\gamma/(\gamma-1)$

$$B = \left(\frac{2}{\gamma + 1}\right)^{1/(\gamma-1)}$$

$$C = \sqrt{\frac{2\gamma}{\gamma + 1}} = \sqrt{\frac{2}{E2}}$$

With,

$$r = p/P_t$$

there are:

$$\Phi = \sqrt{A(r^{E1} - r^{E2})}$$

$$r_c = (p/P_t)_c = B^{\gamma}$$

$$\Phi_c = C B$$

Enclosures: Fig. D(103)

Operating Instruction (1 page)

Program Listing (3 pages)

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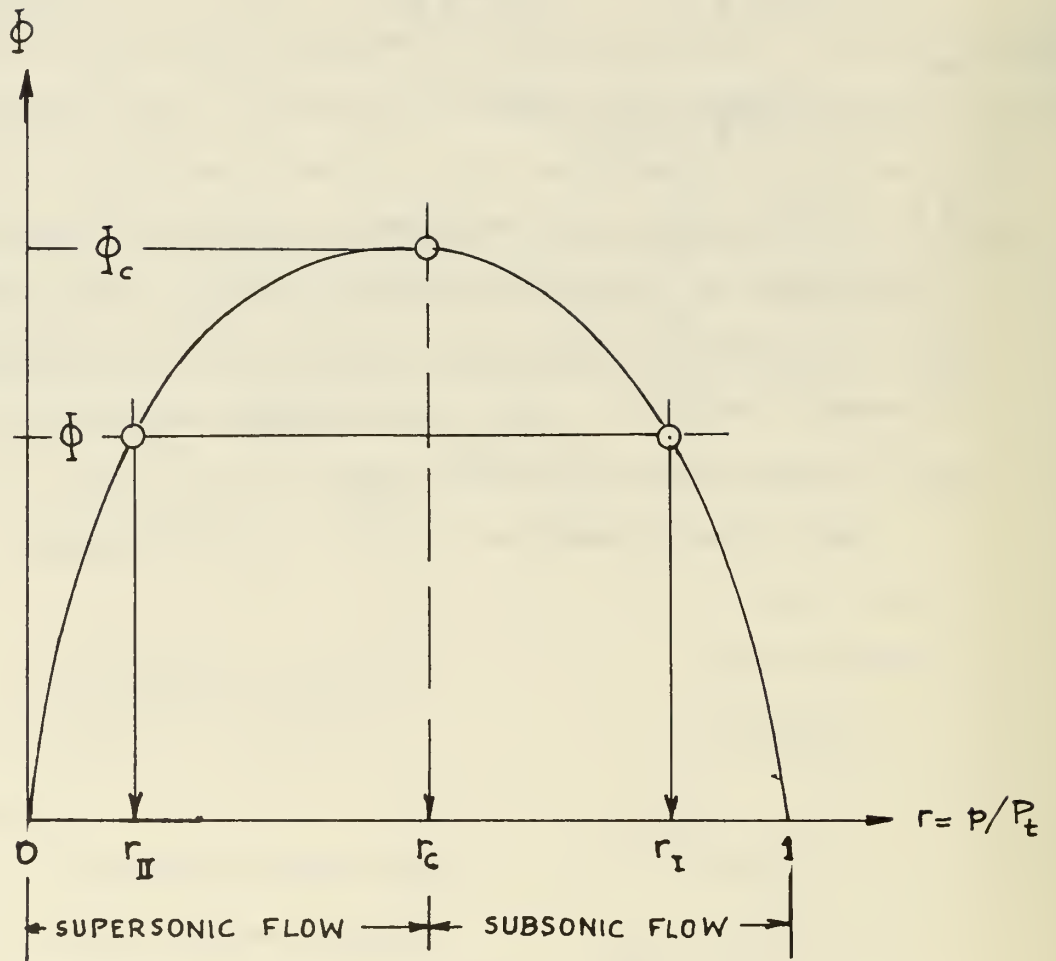
FIG. D(103) ISENTROPIC FLOW FUNCTION Φ

OPERATING INSTRUCTIONS PROGRAM No. 103

MONROE CALCULATOR 1655/6 WITH CARD READER CR-1

Set-Up: (RESET); (TO(0)); Depress (LOAD); Read Cards 1-3

Release (LOAD); (TO(0)); Depress (P); (RESUME)

P-COUNT		
0 0 1	ENTER: Φ (See Note 1)	(RESUME)
0 0 3	" γ (See Note 1)	(RESUME)
0 7 4	CHECK: (E) or $\uparrow(7) \rightarrow \Delta \Phi_c = \Phi - \Phi_c$	

$\Delta \Phi_c < 0$	$\Delta \Phi_c = 0$	$\Delta \Phi_c > 0$
(RESUME)	RESULT: $\uparrow(2) \rightarrow r_c$ $\uparrow(1) \rightarrow \Phi_c$	NO SOLUTION

| 1 0 1 | ENTER: r_i for Iteration | (RESUME) |
| 1 2 5 | CHECK: (E) or $\uparrow(7) \rightarrow \delta\Phi_i = \Phi_i - \Phi$ | |

$\delta\Phi_i \neq 0$	$\delta\Phi_i = 0$
(RESUME)	RESULT: $\uparrow(2) = r = p/P_t$ $\uparrow(1) = I$

(see Note 2)

(RESUME)
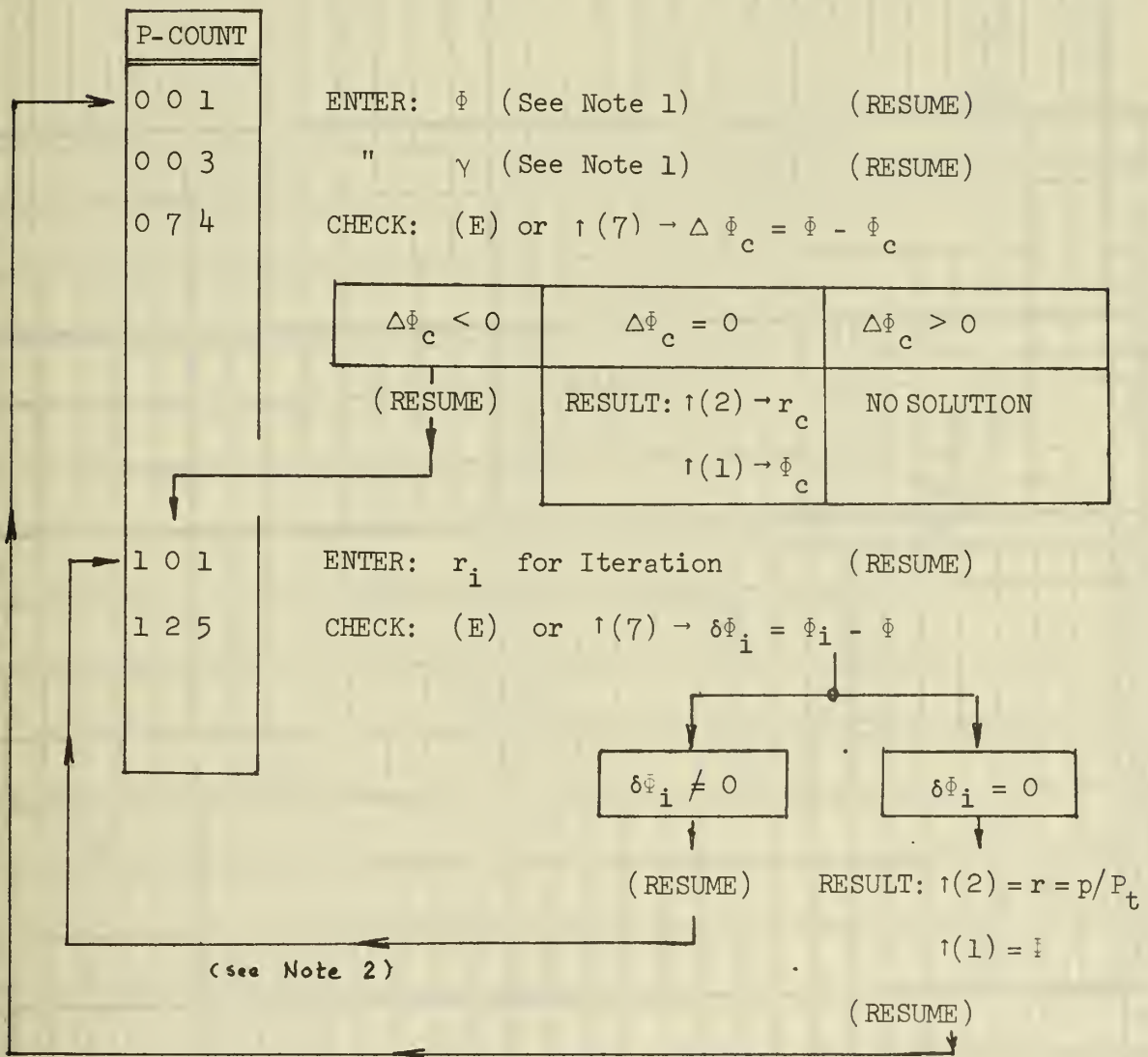
Note 1: If Program 103 is used immediately after Program 102:

Enter at P-Count 1: $\uparrow(5)$ for $\bar{\Phi}$

Enter at P-Count 3: $\uparrow(1)$ for γ

Note 2: Change of r_i (Reg. 2) to r_{i+1} for next iteration:

	SUBSONIC FLOW	SUPERSONIC FLOW
$\delta\Phi_i > 0$	$r_{i+1} > r_i$	$r_{i+1} < r_i$
$\delta\Phi_i < 0$	$r_{i+1} < r_i$	$r_{i+1} > r_i$

TURBO-PROPULSION LABORATORY, DEPT. OF AERONAUTICS, NPS ,
PROGRAM No. .103..... MONROE 1655 CALCULATOR
DETERMINATION OF PRESSURE RATIO FOR GIVEN ISENTROPIC
FLOW FUNCTION FOR DIFFERENT GAMMA

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DATE: AUG.72   BY: M.H.VA..

NOTES:

- ENTER: $\phi\,[M(5)$ of No.102$]$
- ENTER: $\gamma\,[M(2)$ of No.102$]$

REGISTERS (contents):

- Register 6: γ
- Register 5: $\dfrac{2}{\gamma+1}$
- Register 4: C
- Register 3: $-\dfrac{1}{\gamma}$
- Register 2: B
- Register 1: ϕ
- Register 0: ϕ_c

PROGRAM:

Address / P Count	Command	E
00	HALT	ϕ
01	STR(1)	
0 2	HALT	γ
3	STR.(6)	γ
4	+	
5	−	
6	.1.	$\gamma+1$
7	2	
0	=	$\dfrac{\gamma+1}{2}$
1	INV	$\dfrac{2}{\gamma+1}$
2	STR(5)	
3	×	γ
4	RcL(6)	$\dfrac{2\gamma}{\gamma+1}$
5	=	C
6	√	
7	STR(4)	γ
20	RcL(6)	
1	1	$\gamma-1$
2	−	$-\dfrac{1}{\gamma}$
3	=	
4	INV	$\dfrac{2}{\gamma+1}$
5	STR(3)	
6	RcL(5)	$-\dfrac{1}{\gamma-1}$, B
7	α^x	
30	RcL(3)	C
1	×	ϕ_c
2	STR(2)	
3	RcL(4)	
4	=	
5	STR(0)	B
6	RcL(2)	
37	α^x	

Register map (REGISTERS):

Reg	0	1	2	3	4	5	6
Label	Φ_c	Φ	B	$-\dfrac{1}{y-1}$	C	$\dfrac{z}{y+1}$	y

Other register contents: r_c (reg 2), A (reg 5), E1 (reg 4), E2 (reg 3), $\Phi-\Phi_c$ (reg 7), r_c (reg 2), Φ_c (reg 0)

Program:

BR PT	ADDRESS P COUNT	COMMAND	CODE	E
2	0	RCL(6)	4 6 5	y
	1	=	0 2 0	r_c
	2	STR(2)	4 4 1	$-\dfrac{1}{y-1}$
	3	RCL(3)	4 6 2	
	4	x	0 7 0	$-\dfrac{1}{y-1}$
	5	RCL(6)	4 6 5	y
	6	x	0 7 0	
	7	2	0 0 2	
4→5	0	=	0 2 0	A
	1	STR(5)	4 4 4	
	2	2	0 0 2	
	3	÷	0 7 2	
	4	RCL(6)	4 6 5	y
	5	=	0 2 0	E1
	6	STR(4)	4 4 3	
	7	RCL(6)	4 6 5	y
5→6	0	+	0 6 0	
	1	-	0 0 1	$y+1$
	2	÷	0 7 2	y
	3	RCL(6)	4 6 5	E2
	4	=	0 2 0	
	5	STR(3)	4 4 2	Φ
6→7	6	RCL(1)	4 6 0	
	7	-	0 6 2	Φ_c
	0	RCL(0)	4 7 7	$\Phi-\Phi_c$
	1	=	0 2 0	$\Phi-\Phi_c$
7	2	STR(7)	4 4 6	
	3	HALT	4 0	
	4	0		
	5	0		
	6	0		
	7	0		

NOTES: CHECK: $\Phi - \Phi_c = ?$

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ADDRESS / P COUNT	COMMAND	CODE	E	NOTES
0	HALT	40 1	r_i	ENTER: r_i for iteration
1	STR(2)	44 1	r_i	
2	α^x	0 74		
3	RCL(3)	46 2	E2	
4	=	20 0	r_i^{E2}	
5	STR(0)	45 7		
6	RCL(2)	46 1	r_i	
7	α^x	0 74		
0	RCL(4)	46 3	EI	
1	—	20 0...	r_i^{EI}	
2	RCL(0)	46 77	r_i^{E2}	
3	×	20 70		
4	RCL(5)	46 4	A	
5	=	20 0		
6	√	20 56	Φ_i	
7	STR(0)	45 7		
0	—	20 62	Φ	
1	RCL(1)	46 00	$\Phi_i-\Phi$	
2	=	20 0	$\Phi_i-\bar{\Phi}$	
3	STR(7)	44 46		
4	HALT	40 1		CHECK: $\Phi_i = \Phi^2$
5	SFSNS	52 3		Depr.(SENSE) if $\Phi_i = \Phi$
6	SKF)	54 0		
7	JUMP 00	0 0		
0	To(0)	74 0		

Registers: 0: Φ_c (r_i^{E2}); 1: Φ; 2: r_c (r_i); 3: E2; 4: EI; 5: A; 6: γ; 7: $\Phi_i-\Phi$ / $\Phi_i-\bar{\Phi}$; 0: Φ_i

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PROGRAM No. 104

MONROE CALCULATOR 1655/1656 WITH CARD READER CR-1

Description

This program can be used to determine the flow properties at the inlet

of a radial compressor rotor provided the absolute velocity V_1 at this

station is axial and uniform. The following quantities must be known:

$$\Phi_1 = \frac{\dot{w}\sqrt{(R_G/g)\ T_0}}{P_0\ A_1\ k_{B1}} = \frac{\dot{m}\sqrt{R_G\ g\ T_0}}{P_0\ A_1\ k_{B1}} = \text{dimensionless flow function}$$

p_1/P_0 = ratio of static and total pressure at inlet

U_2/a_0 = speed ratio

R_{1o}/R_2 = ratio of outer radius at inlet and outer rotor radius

$\gamma = c_p/c_v$ = specific heat ratio

The program determines:

T_1/T_0 = ratio of static and total temperatures at inlet

V_1/a_0 = ratio of absolute velocity at inlet and velocity of sound at T_0

W_{1o}/a_0 = ratio of relative velocity at R_{1o} and velocity of sound at T_0

β_{1o} = relative flow angle at R_{1o}

$M_{W1} = W_{1o}/a_1$ = Mach number of W_{1o}

Symbols:

$\dot{w}$ = weight flow rate (lbm/s)

$\dot{m}$ = mass flow rate (slug/s)

R_G = gas constant (ft-lb/(lbm,°R)

g = 32.174   (ft/s²)

T_0 = total inlet temperature (°R)

P_0 = total inlet pressure (psia)

$A_1 = \pi\ (R_{1o}^2 - R_{1i}^2)$ = area of inlet eye of rotor (in.²)

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k_{Bl} = restriction factor (-)

p_1 = static pressure at inlet (psia)

T_1 = static temperature at inlet ($^\circ$R)

U_2 = peripheral rotor speed at outer radius R_2 (ft/s)

$$a_0 = \sqrt{g\ \gamma\ R_G\ T_0} \qquad\qquad (ft/s)$$

R_{1i} = inner radius at inlet eye (in.)

R_{1o} = outer radius at inlet eye (in.)

R_2 = outer radius of impeller (in.)

Although English units are used in the above list, the program can be used for any consistent system of units.

Derivations:

$$T_1/T_0 = (p_1/P_0)^{(\gamma-1)/\gamma}$$

$$\dot{w} = A_1\ k_{Bl}\ V_1\ \frac{p_1}{R_G\ T_1} = A_1\ k_{Bl}\ \frac{V_1}{a_0}\ \frac{(p_1/P_0)}{(T_1/T_0)}\ \frac{\sqrt{g\ \gamma\ R_G\ T_0}}{R_G}\ \frac{P_0}{T_0}$$

or

$$\Phi_1 = \sqrt{\gamma}\ \frac{V_1}{a_0}\ \frac{(p_1/P_0)}{(T_1/T_0)}$$

and

$$\frac{V_1}{a_0} = \frac{\Phi_1}{\sqrt{\gamma}}\ \frac{T_1/T_0}{(p_1/P_0)}$$

The peripheral speed U_{1o} at R_{1o} is

$$U_{1o} = (R_{1o}/R_2)\ U_2$$

For axial entry

$$W_{1o}^2 = V_1^2 + U_{1o}^2$$

$$\tan\beta_{1o} = U_{1o}/V_1$$

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Thus

$$\frac{W_{1o}}{a_0} = \sqrt{\left(\frac{V_1}{a_0}\right)^2 + \left(\frac{U_2}{a_0}\right)^2 \left(\frac{R_{1o}}{R_2}\right)^2}$$

$$\tan\beta_{1o} = \frac{(R_{1o}/R_2)(U_2/a_0)}{(V_1/a_0)}$$

and

$$M_{W1} = \frac{W_{1o}}{a_1} = \frac{W_{1o}}{a_0}\frac{a_0}{a_1} = \frac{W_{1o}/a_0}{\sqrt{T_1/T_0}}$$

The flow angle β_{1o}', by taking account of the blade thickness, is

$$\tan\beta_{1o}' = \left(1 - \frac{t_u}{s}\right)\tan\beta_{1o} = k\,\tan\beta_{1o}$$

where

$$t_u = \frac{t}{\cos\beta_B}$$

$$s = \frac{2\pi R_{1o}}{Z_R}$$

where:

t = actual blade thickness at R_{1o}

β_B = blade inlet angle at R_{1o}

Z_R = number of rotor blade

Also

$$\cot\beta_{1o}' = \frac{(V_1/a_0)/k}{(R_{1o}/R_2)(U_2/a_0)}$$

with

$$k = 1 - \frac{t}{\cos\beta_B}\frac{Z_R}{2\pi R_{1o}}$$

If β_B is the blade angle at R_{1o}, the incidence angle i' is

$$i' = \beta_{1o}' - \beta_B$$

Enclosures: Operating Instructions (1 page)
             Program Listing (3 pages)

OPERATING INSTRUCTIONS PROGRAM No. 104

MONROE CALCULATOR 1655/6 WITH CARD READER CR-1

Set-Up: (RESET); (TO(0)); Depress (LOAD); Read Cards 1-2

Release (LOAD); (TO(0)); Depress (P); (RESUME)

P-COUNT	
0 0 1	ENTER: Φ_1 (see note) (RESUME)
0 0 3	" p_1/p_0 (see note) (")
0 0 5	" γ (")
0 3 6	" U_2/a_0 (")
0 4 0	" R_{10}/R_2 (")
0 6 7	" k (")
0 7 6	" β_B (")
1 0 1	RESULTS: ↑ (4) → (T_1/T_0)

↑ (3) → (V_1/a_0)

↑ (2) → (W_{10}/a_0)

↑ (1) → β_{10} (°)

↑ (0) → β'_{10} (°)

↑ (5) → M_{W1}

↑ (7) → i'(°)

(RESUME)

Note: If Program 104 is used immediately after Program 103, enter:

at P-Count 001: ↑ (1) to obtain Φ,

at P-Count 003: ↑ (2) to obtain p_1/P_0

REGISTERS

ADDRESS P COUNT	COMMAND	CODE	E	Registers (content)	NOTES
0 0	HALT	4 0 1			ENTER: Φ₁ [f(1) of PROG.103]
1	STR(6)	4 4 5		6: Φ₁	
0 2	HALT	4 0 1			ENTER: P₁/P₀ [f(2) of PROG.103]
3	STR(5)	4 4 4		5: P₁/P₀	
0 4	HALT	4 0 1	γ		ENTER: γ [f(6) of PROG.103]
5	STR(3)	4 4 2	γ	3: γ	
6	−	0 6 2			
7	−	0 0	Y−1		
0	÷	0 7 2	Y		
1	RCL(3)	4 6 2	(Y−1)/Y		
2	=	0 2 0		4: (Y−1)/Y	
3	RCL(3)	4 4 3			
4	√	4 6 2	√Y		
5	STR(3)	0 5 6		3: √Y	
6	RCL(5)	4 4 2	P₁/P₀		
7	dˣ	4 6 4	(Y−1)/Y		
2 0	RCL(4)	0 7 4	T₁/T₀		
1	×	4 6 3			
2	STR(4)	4 7 0	T₁/T₀	4: T₁/T₀	
3	RCL(6)	4 4 3	Φ₁		
4	÷	4 6 5			
5	RCL(3)	0 7 2	√Y		
6	÷	4 6 2			
2 7	RCL(5)	0 7 2	P₁/P₀		
3 0	×	4 6 4	V₁/a₀	3: V₁/a₀	
1	STR(3)	4 7 0			
2	=	4 4 2	(V₁/a₀)²		
3	STR(7)	0 2 0		7: (V₁/a₀)²	
4	HALT	4 4 6	U₂/a₀		ENTER: U₂/a₀
0 3 5	×	4 0 1			
6	HALT	4 7 0	R₁₀/R₂		ENTER: R₁₀/R₂
0 3 7	HALT	4 0 1			

M.H.V. 2/26/1

ADDRESS (P COUNT)	CODE	COMMAND	E	Registers (annotations)	NOTES
04 0	0 7 0	×	C	reg0: C	$C=(U_2/a_0)(R_{10}/R_2)$
1	4 5 7	STR(0)			
2	0 6 0	+	C^2		
3	4 6 6	RCL(7)	$(V_1/a_0)^2$	reg7: $(V_1/a_0)^2$	
4	0 2 0	=	$(W_1/a_0)^2$		
5	0 5 6	√	W_1/a_0		
6	4 4 4	STR(2)		reg2: W_1/a_0	
47	2 6 6	RCL(3)	V_1/a_0	reg3: V_1/a_0	
50 0	0 7 6	×			
1	4 7 7	RCL(0)	$\beta_{10}^{\,R}$		
2	0 2 0	=	$\beta_{10}^{\,\circ}$	reg1: β_{10}	
3	0 4 6	R→°		reg1: β_{10}	
4	4 4 0	STR(1)	T_1/T_0	reg4: T_1/T_0	
5	4 6 3	RCL(4)	$\sqrt{T_1/T_0}$		
6	0 5 6	÷			
57	0 7 2	÷	W_1/a_0		
60 0	4 6 1	RCL(2)	$1/M_{W_1}$		
1	0 2 0	=	M_{W_1}	reg5: M_{W_1}	
2	0 5 4	INV			
3	4 4 4	STR(5)			
4	4 6 2	RCL(3)	V_1/a_0		
5	0 7 2	÷			
66	4 0 1	HALT	k		ENTER: k
67	0 7 6	×	$k\,V_1/a_0$		
70 0	4 7 7	RCL(0)	C		
1	0 2 0	=	$\beta_{10}'^{\,R}$		
2	0 4 6	R→°	$\beta_{10}'^{\,\circ}$	reg0: β_{1b}'	
3	4 5 7	STR(0)	β_{1b}'		
4	0 6 2	−	β_{1b}		
75	4 0 1	HALT	i'		ENTER: β_{1b}
6	0 2 0	=			
77	4 4 6	STR(7)		reg7: i'	

BR PT: 2 ... 3

BR PT	ADDRESS P COUNT	COMMAND	CODE	E	A	M	0	1	2	3	4	5	6	7	8	9	X	Y	Z	RESULTS (NOTES)
		REGISTERS					β'_{10}	β_{10}	W_1/a_0	V_1/a_0	T_1/T_0	M_{w1}	Φ_1	ι'						
4	1 0 0	HALT	4 0 1																	
	1	To(o)	7 4 0																	

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MONROE CALCULATOR 1655/6 WITH CARD READER CR-1

Description

In Ref. (a)* the so-called adiabatic rotor efficiency η_R of a radial compressor wheel is related to the wheel efficiency η_W and to the velocity ratio

$$\Psi = \frac{W_2}{W_{2is}}$$

which is a convenient measure to express the rotor losses for performance calculations.

From Eq. a(21); that is, Eq. (21) of Ref. (a),

$$\Psi = \frac{W_2/W_{1o}}{\left[1 - \eta_W + \eta_W (W_2/W_{1o})^2 \right]^{\frac{1}{2}}}$$

From Eq. a(27)

$$\eta_W = \frac{\eta_R - C}{1 - C}$$

where, from Eq. a(25),

$$C = \frac{1 - (R_{1o}/R_2)^2}{(R_{1o}/R_2)^2 \cot^2 \beta_{1o} + 2\mu \left(1 - \mu/[2 \sin^2 \alpha_2] \right)}$$

From Eq. II(5) of Ref. (a)

$$\frac{W_2}{W_{1o}} = \frac{\left[1 - 2\mu \left(1 - \mu/[2 \sin^2 \alpha_2] \right) \right]^{\frac{1}{2}} \sin \beta_{1o}}{R_{1o}/R_2}$$

----
*See page 1 of Program 102

The following quantities are supposed to be known:

R_{1o}/R_2 = ratio of outer radius at impeller inlet and impeller exit radius

α_2 = absolute flow angle at impeller exit

μ = impeller slip factor

β_{1o} = relative flow angle at outer radius at impeller inlet

η_R = adiabatic rotor efficiency [see Eq. a(12)]

To be determined are:

η_W = wheel efficiency [see Eq. a(15)]

W_2/W_{1o} = ratio of relative velocity at impeller exit and relative velocity at outer radius at impeller inlet

$\Psi = W_2/W_{2is}$ = ratio of actual and isentropic relative velocities at impeller exit

The following quantities are used for the calculations

$$A = 2\mu \left(1 - \frac{\mu}{2\,\sin^2\alpha_2} \right)$$

$$B = \sqrt{1 - A}$$

Then

$$C = \frac{1 - (R_{1o}/R_2)^2}{(R_{1o}/R_2)^2 \cot^2\beta_{1o} + A} = \frac{D}{E}$$

$$W_2/W_{1o} = \frac{B\,\sin\beta_{1o}}{R_{1o}/R_2}$$

$$F = \left[1 - \eta_W + \eta_W\,(W_2/W_{1o})^2 \right]^{\frac{1}{2}}$$

$$\Psi = \frac{W_2/W_{1o}}{F}$$

Enclosures: Operating Procedure (1 page)

Program Listing (3 pages)

MONROE CALCULATOR 1655/6 WITH CARD READER CR-1

Set-Up: (RESET); (TO(0)); Depress (LOAD); Read Cards 1-3

Release (LOAD); (TO(0)); Depress (P); (RESUME)

P-COUNT		
0 0 1	ENTER: R_{1o}/R_2	(RESUME)
0 0 3	" : α_2	(")
0 1 2	" : μ	(")
0 3 7	" : β_{1o}	(")
0 6 7	" : η_R	(")
1 2 2	RESULTS: $\uparrow (4) \rightarrow W_2/W_{1o}$	
	$\uparrow (5) \rightarrow \eta_W$	
	$\uparrow (3) \rightarrow \psi$	
	(RESUME)	

TURBO-PROPULSION LABORATORY, DEPT. OF AERONAUTICS, NPS ,
PROGRAM No. 105...... MONROE 1655 CALCULATOR
RELATION BETWEEN ROTOR EFFICIENCIES AND VELOCITY RATIO.....
OF RADIAL COMPRESSOR IMPELLER...........................

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DATE: AUG. 72   BY: M.H. VAVRA

REGISTERS

BR PT	ADDRESS P COUNT	COMMAND	CODE	E	A	M	0	1	2	3	4	5	6	7	8	9	X	Y	Z	NOTES
0	00	HALT	4 0	R_{10}/R_2									R_{10}/R_2							ENTER: R_{10}/R_2
	01	STR(6)	4 5																	
	02	HALT	4 0	α_2																ENTER: α_2
	03	SIN/COS	0 4	$\sin\alpha_2$																
	04	$\times$	0 7																	
	05	$\times$	0 7	$\sin\alpha_2$																
	06	2	0 0																	
	07	=	0 2	$2\sin^2\alpha_2$				$2\sin^2\alpha_2$												
	00	STR(1)	4 4																	
0─	01	HALT	4 0	μ					μ											ENTER: μ
	02	STR(2)	4 4	μ																
	03	$\div$	0 7																	
	04	RCL(1)	4 6	$\dfrac{2\sin^2\alpha_2}{2\sin\alpha_2}$																
	05	1	0 6																	
─	06	−	0 0																	
	07	$\times$	0 7																	
2	00	2	0 0																	
	01	$\times$	0 7	μ																
	02	RCL(2)	4 6	−A				1−A												
	03	+	0 0	1−A																
	04	−	0 0																	
	05	1	0 6	1−A																
	06	STR(1)	4 4																	
	07	=	0 0	−A					A											
3─	00	CHSGN	0 3	+A																
	01	STR(2)	4 4																	
	02	RCL(1)	4 6	1−A																
	03	$\sqrt{\ }$	0 5	B				B												
	04	STR(1)	4 4					B	A											
03	05	HALT	4 0	β_{10}									R_{10}/R_2							ENTER: β_{10}
03	06	SIN/COS	0 4	$\sin\beta_{10}$				B	A											

BR PT	P COUNT	COMMAND	CODE	E (display)	Reg 1	Reg 2	Reg 3	Reg 4	Reg 5	Reg 6	NOTES
2	0	STR(3)	244	$\sin\beta_{10}$	B	A	$\sin\beta_b$			R_{10}/R_2	
	1	2.FUNC	630	$\cos\beta_{10}$							
	2	$\div$	270								
	3	RCL(3)	264	$\sin\beta_{10}$							
	4	$\times$	070	$\cot\beta_{10}$							
	5	RCL(6)	564	R_{10}/R_2							
	6	$\times$	070	$\dfrac{R_{10}\cot\beta_{10}}{R_2}$							
	7	+	060	$(R_{10}/R_2)\cot\beta_{10}\,]^2$							
	0	RCL(2)	164	A							
	1	=	020	E				E			
	2	STR(4)	344								
	3	RCL(6)	564	R_{10}/R_2							
	4	$\times$	070								
	5	$-$	260	$\left(R_{10}/R_2\right)^2$							
	6	$-$	070								
5	7	$\div$	262	$-D$							
3	0	RCL(4)	364	E							
	1	+	060	$-C$				$-C$			
	2	STR(4)	344	$-C$							
	3	$-$	060								
	4	=	020								
	5	STR(5)	444	$1-C$					$1-C$		
	6	HALT	104	η_R							ENTER: η_R
	7	+	060								
	0	RCL(4)	364	$-C$							
	1	$\div$	272	η_{a-c}							
	2	RCL(5)	464	$1-C$							
	3	=	020	η_w					η_w		
	4	STR(5)	444								
	5	RCL(1)	460	B							
	6	$\times$	070								
	7	RCL(3)	264	$\sin\beta_{10}$			$\sin\beta_{10}$				

REGISTERS

Reg	1	2	3	4	5	6
Label	B	A	$\sin\beta_{10}$	$-c$	η_W	R_{10}/R_2

BR PT	P COUNT	COMMAND	CODE	E (note)
4	00	÷	02	
	01	RCL(6)	465	R_{10}/R_2
	02	×	070	W_2/W_{10}
	03	STR(4)	443	
	04	×	070	$(W_2/W_{10})^2$
	05	RCL(5)	464	η_W
	06	─	062	η_W
	07	RCL(5)	464	η_W
	10	+	006	
	11	─	000	F^2
	12	=	020	F
	13	√	056	
	14	÷	072	W_2/W_{10}
	15	RCL(4)	463	$1/\psi$
	16	=	020	ψ
	17	INV	054	
5	20	STR(3)	442	ψ
	21	HALT	40	
	22	To(o)	740	

RESULTS:

Register labels (results block): ψ (reg 3), $\dfrac{W_2}{W_{10}}$ (reg 4), η_W (reg 5)

MONROE CALCULATOR 1655/6 WITH CARD READER CR-1

Description

This program is used to determine the flow properties at the discharge of a radial compressor wheel with the following equations of Ref. (a)*.

Eq. I (6): $\dfrac{T_{t2}}{T_0} = 1 + (\gamma-1)\,\mu\left(\dfrac{U_2}{a_0}\right)^2$

Eq. I (7): $\dfrac{T_2}{T_0} = 1 + (\gamma-1)\,\mu\left(\dfrac{U_2}{a_0}\right)^2\left[1 - \dfrac{\mu}{2\sin^2\alpha_2}\right]$

Eq. I (8): $\dfrac{T_2'}{T_0} = 1 + (\gamma-1)\,\mu\left(\dfrac{U_2}{a_0}\right)^2\left[\dfrac{1}{\psi^2}\left(1 - \dfrac{\mu}{2\sin^2\alpha_2}\right) - \dfrac{1}{2\mu}\left(\dfrac{1}{\psi^2} - 1\right)\right]$

Eq. I(20): $\dfrac{P_2}{P_0} = \left(\dfrac{T_2'}{T_0}\right)^{\gamma/(\gamma-1)}$

Eq. I(19): $\dfrac{P_{t2}}{P_0} = \left(\dfrac{P_2}{P_0}\right)\left(\dfrac{T_{t2}/T_0}{T_2/T_0}\right)^{\gamma/(\gamma-1)}$

Eq. II(6): $M_{v2} = \dfrac{\mu\; U_2/a_0}{\sin\alpha_2\;\sqrt{T_2/T_0}}$

Input data are:

$\dfrac{U_2}{a_0} = \dfrac{\text{peripheral speed of impeller at discharge}}{\text{velocity of sound at total inlet temperature } T_0}$

α_2 = absolute flow angle at impeller exit

μ = rotor slip factor

---

* See page 1 of Program 102

$$\gamma = c_p/c_v$$

$$\psi = W_2/W_{2is} = \text{velocity ratio}$$

The calculated values are :

T_0 = total temperature at impeller inlet

P_0 = total pressure at impeller inlet

T_2 = static temperature at impeller exit

P_2 = static pressure at impeller exit

T_{t2} = total temperature at impeller exit

P_{t2} = total pressure at impeller exit

M_{V2} = Mach number of absolute velocity V_2 at impeller

exit = $V_2/\sqrt{g \gamma R_G T_2}$

The following quantities are established during the calculations

$$A = (\gamma-1) \; \mu \left(\frac{U_2}{a_0}\right)^2$$

$$B = 1 - \frac{\mu}{2 \sin^2 \alpha_2}$$

$$C = \frac{1}{2\mu} \left(\frac{1}{\psi^2} - 1\right)$$

$$D = \frac{\mu^2 \left(U_2/a_0\right)^2}{\sin^2 \alpha_2}$$

$$E = \gamma/(\gamma-1)$$

Then:

$$\frac{T_{t2}}{T_0} = 1 + A$$

$$\frac{T_2}{T_0} = 1 + AB$$

$$\frac{T_2'}{T_0} = 1 + \left[A \frac{1}{\psi^2} B - C\right]$$

$$M_{V2} = \sqrt{\frac{D}{T_2/T_0}}$$

Enclosures: Operating Instructions (1 page)

Program Listing   (3 pages)

MONROE CALCULATOR 1655/6 WITH CARD READER CR-1

Set-Up: (RESET); (TO(O)); Depress (LOAD); Read Cards 1-3

Release (LOAD); (TO(O)); Depress (P); (RESUME)

P-COUNT
0 0 1
0 0 5
0 1 2
0 2 0
0 4 5
1 3 7

ENTER: U_2/a_0 (RESUME)

" : α_2 (")

" : γ (")

" : μ (")

" : ψ (")

RESULTS: ↑ (1) → T_{t2}/T_0

     ↑ (2) → P_{t2}/P_0

     ↑ (3) → T_2/T_0

     ↑ (4) → p_2/P_0

     ↑ (5) → M_{V2}

          (RESUME)

Note: N-switch must be in "Down" position.

Program worksheet — Registers, Code, Command, Address/P Count

P COUNT	COMMAND	E	NOTES / Registers
00	HALT	U_4/a_0	ENTER: U_2/a_0
01	×		
02	=	$(U_2/a_0)^2$	
03	STR(6)		Reg 6 = $(U_2/a_0)^2$
04	HALT	α_2	ENTER: α_2
05	SIN/COS	$\sin\alpha_2$	
06	×		
07	=	$\sin^2\alpha_2$	
0→	STR(5)		Reg 5 = $\sin^2\alpha_2$
1	HALT	γ	ENTER: γ
2	STR(7)	γ	Reg 7 = γ
3	−		
4	−		
5	×	$\gamma-1$	
6	STR(8)	μ	Reg 8 = $\gamma-1$
7	HALT	μ	ENTER: μ
0→2	STR(9)	$(\gamma-1)\mu$	Reg 9 = μ
1	×	$(U_2/a_0)^2$	
2	RCL(6)	A	
3	=		
4	STR(1)	γ	Reg 1 = A
5	RCL(7)		
6	÷	$\gamma-1$	
7	RCL(8)	E	
0→3	=	μ	
1	STR(2)		Reg 2 = E
2	RCL(9)		
3	÷	$\mu/2$	
4	2		
5	÷	$\sin^2\alpha$	
6	RCL(5)		
7	−		

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REGISTERS (top labels)

Reg	Content
1	A
2	E
3	B
4	C
5	D
6	$\sin^2\delta_2 (U_2/a_0)^2$
7	X ; $1/\psi^2$
8	$\gamma-1$
9	μ

Program listing:

Addr	Command	Code	E-register
040	$\sqrt{\ }$	1 0 0	
041	=	0 2 0	$-B$
042	CHSGN	0 3 0	B
043	STR(3)	4 4 2	
044	HALT	4 2 4	ψ
045	INV	1 0 4	$1/\psi$
046	×	0 5 4	$1/\psi$
047	–	0 7 0	
050	STR(7)	2 6 0	$1/\psi^2$
051	–	6 4 6	
052	÷	0 2 0	$1/x-1$
053	2	0 7 2	
054	÷	0 2 0	
055	RCL(9)	4 7 2	
056	=	0 2 0	μ
057	STR(4)	3 4 4	C
060	RCL(9)	4 7 4	μ
061	×	0 7 0	
062	×	0 7 0	μ^2
063	RCL(6)	4 6 5	$(U_2/a_0)^2$
064	÷	0 7 2	
065	RCL(5)	4 6 4	$\sin\delta_2$
066	=	0 2 0	D
067	STR(5)	4 4 4	
070	RCL(7)	4 6 6	$1/x^2$
071	×	0 7 0	
072	RCL(3)	4 6 2	B
073	–	0 6 0	
074	RCL(4)	4 6 3	C
075	×	0 7 0	
076	RCL(1)	4 6 0	A
077	+	0 6 0	

NOTES: ENTER : ψ (at address 044, HALT)

BR PT 2 (at 040) ; BR PT 3 (at 060)

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Register label row:

E	A	M	0	1 (A)	2 (E)	3 (B)	4 (C)	5 (D)	6	7	8	9	X	Y	Z
				A	E	B	C	D	U_2/a_0	$\sqrt[2]{1/4}$	$\gamma-1$	μ			

Program listing:

BR PT	Address	Command	E (register)
4	1-0	I	
	1-1	a^x	T_2/T_0
	1-2	RCL(2)	E
	1-3	=	P_2/P_0
	1-4	STR(4)	
	1-5	RCL(1)	A
	1-6	×	
	1-7	RCL(3)	B
	2-0	+	
	2-1	−	
	2-2	=	T_2/T_0
	2-3	STR(3)	T_2/T_0
	2-4	INV	T_0/T_2
	2-5	×	
	2-6	RCL(5)	D
	2-7	=	
	3-0 (230 / 5)	√	M_{V2}
	3-1	STR(5)	M_{V2}
	3-2	−	
	3-3	+	
	3-4	RCL(1)	A
	3-5	÷	T_{t2}/T
	3-6	STR(1)	T_{t2}/T_0
	3-7	RCL(3)	T_2/T_2
3-	3-0	a^x	E
	3-1	RCL(2)	P_2/P_0
	3-2	×	
	3-3	RCL(4)	P_{t2}/P_0
	3-4	=	
	3-5	STR(2)	
3-6		HALT	
1-	3-7	To(0)	

Register contents noted in grid:
- Reg 4 (C): P_2/P_0
- Reg 3 (B): T_2/T_0
- Reg 5 (D): M_{V2}
- Reg 1 (A): T_{t2}/T_0

RESULTS:

0	1	2	3	4	5	6	7	8	9
	$\dfrac{T_{t2}}{T_0}$	$\dfrac{P_{t2}}{P_0}$	$\dfrac{T_2}{T_0}$	$\dfrac{P_2}{P_0}$	M_{V2}				

MONROE CALCULATOR 1655 WITH CARD READER CR-1

Description

This program calculates Eq. C(17) of Appendix C.

$$(\dot{m})^* = 2k_{B1}\sqrt{\gamma'} \int_{0.287}^{0.541} \left(\frac{R_1}{R_2}\right) X \left(\frac{V_{1o}}{a_0}\right)\left[1 - \frac{\gamma-1}{2}\left(X\frac{V_{1o}}{a_0}\right)^2\right]^{1/(\gamma-1)} d\left(\frac{R_1}{R_2}\right)$$

where $\quad X = \dfrac{V_1/a_0}{V_{1o}/a_0}$

For five equal increments of R_1/R_2 between 0.287 and 0.541 the ratio X can be calculated from Eqs. C(15) and C(16). The following table gives the data that have to be entered in the program in the order required, starting from $i = 0$. The quantity z_i is used in the process of integration.

i	0	1	2	3	4	5
X_i	0.5081	0.5749	0.6544	0.7493	0.8631	1.0
$(R_1/R_2)_i$	0.287	0.3378	0.3886	0.4394	0.4902	0.541
z_i	2	1	1	1	1	2

With $\Delta(R_1/R_2) = (0.541 - 0.287)/5 = 0.0508$ and

$$N_i = \left(\frac{R_1}{R_2}\right)_i X_i \left[\frac{V_{1o}}{a_0}\right]\left[1 - \frac{\gamma-1}{2}\left(X_i\frac{V_{1o}}{a_0}\right)^2\right]^{1/(\gamma-1)}$$

there is with the trapezoidal method of integration

$$\int_{0.287}^{0.541} = \left(N_0/2 + N_1 + N_2 + N_3 + N_4 + N_5/2\right)\Delta\left(\frac{R_1}{R_2}\right)$$

or

$$S = \int_{0.287}^{0.541} = 0.0508 \sum_{i=0}^{5} N_i / z_i$$

Hence

$$(m)* = 2k_{B1} \sqrt{\gamma} \; S$$

Further, from Eq. C(18)

$$\cot \beta_{1o} = \frac{V_{1o}/a_0}{(U_2/a_0)(R_{1o}/R_2)} = \frac{V_{1o}/a_0}{0.44903}$$

From Eq. C(19)

$$M_{W1} = \frac{0.44903}{\left[\sin^2\beta_{1o} - \frac{\gamma-1}{2}(0.44903)^2 \cos^2\beta_{1o}\right]^{\frac{1}{2}}}$$

The program can be used for different values of γ, k_{B1}, U_2/a_0 and R_{1o}/R_2. It can be adapted also to integrations with more than five equal increments between R_{1i}/R_2 and R_{1o}/R_2. In this case the increment $\Delta(R_1/R_2)$ must be entered in addresses 75 to 103 (octal).

Enclosures: Operating Instruction (1 page)

Program Listing (4 pages)

OPERATING INSTRUCTIONS PROGRAM No. 108

MONROE CALCULATOR 1655/6 WITH CARD READER CR-1

<u>Set-Up</u>: (RESET); (TO(0)); Depress (LOAD); Read Cards 1-4;

Release (LOAD); (TO(0)); Depress (P); (RESUME)

P-COUNT			
0 0 1	ENTER:	γ	(RESUME)
0 2 2	"	k_{B1}	(")
0 2 5	"	(U_2/a_0)	(")
0 2 7	"	(R_{1o}/R_2)	(")
0 4 1	"	(V_{1o}/a_0)	(")
0 4 5	"	X_i $(^+)$	(")
0 6 3	"	$(R_1/R_2)_i$ $(^+)$	(")
0 6 5	"	Z_i $(^+)$	(")

If i $\neq$ 5   If i = 5

(RESUME)   Depress (SENSE)

(RESUME)

1 4 5   RESULTS: $\uparrow (0) \rightarrow (\dot{m})*$

$\uparrow (1) \rightarrow \beta_{1o}{}^o$

$\uparrow (3) \rightarrow M_{W1}$

Release (SENSE)

(RESUME)

Introduce new value of (V_{1o}/a_0)

$(^+)$ Enter val·   with equal indices i of Table   on p. 1 of Program

Descripti   sequentially for i = 0, 1, 2, 3, 4, 5.

BR PT	ADDRESS P COUNT	COMMAND	CODE			E	A	M	0	1	2	3	4	5	6	7	8	9	X	Y	Z	NOTES
0	0 0	HALT	4 0 1			γ																ENTER: γ
	1	STR(1)	4 4 0			γ				γ												
	2	—	0 0 6																			
	3	1	0 0 0																			
	4	÷	0 0 0			$\gamma-1$																
	5	STR(2)	4 4 7								$\gamma-1$											
	6	2	4 0 2																			
	7	=	2 0 0			$\frac{\gamma-1}{2}$									$\frac{\gamma-1}{2}$							
	0	STR(5)	4 4 4																			
	1	RCL(2)	4 6 6			$\frac{\gamma-1}{}$																
	2	INV	0 5 0			$\frac{1}{\gamma-1}$								$\frac{1}{\gamma-1}$								
	3	STR(4)	4 4 5																			
	4	RCL(1)	4 6 6			γ																
	5	$\sqrt{}$	0 5 0			$\sqrt{\gamma}$																
	6	×	0 7 0																			
	7	2	0 0 2			$2\sqrt{\gamma}$																
	0	×	0 7 0			$2\sqrt{\gamma}$																
	2 1	HALT	4 0 1			k																ENTER: $k_{B_1} = k$
	2	=	0 2 0			$2k\sqrt{\gamma}$										$2k\sqrt{\gamma}$						
	3	STR(6)	4 4 5			$2k\sqrt{\gamma}$																
	2 4	HALT	4 0 7			U_2/a_0																ENTER: U_2/a_0
	5	×	0 7 0																			
	2 6	HALT	4 0 1			R_{1o}/R_2																ENTER: R_{1o}/R_2
	2 7	=	0 2 0			b			b													$b = (U_2/a_0)(R_{1o}/R_2)$
	3 0	STR(2)	4 4								b											
	1	0																				
	2	0																				
	3	0																				
	4	0																				
	5	0																				
	6	0																				
	3 7	STR(0)	4 5 7						O	γ	b		$\frac{1}{\gamma-1}$	$\frac{\gamma-1}{2}$	$2k\sqrt{\gamma}$							Clears (O)

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Register headings (top): reg0 = 0, reg1 = Y / ν, reg2 = b, reg3 = νX_i, reg4 = $\frac{1}{Y-1}$, reg5 = $\frac{Y-1}{2}$, reg6 = $2k/\sqrt{Y}$

Register headings (bottom): reg1 = ν, reg2 = b, reg3 = νX_i, reg4 = $\frac{1}{Y-1}$, reg5 = $\frac{Y-1}{2}$, reg6 = $2k\sqrt{8}$

BR PT	ADDRESS P COUNT	COMMAND	CODE	E	NOTES
2	0 4 0	HALT	4 01	ν	ENTER: $(V_{10}/a_0) = \nu$
	4 1	STR(1)	4 40		
	4 2	RCL(1)	4 60	ν	
	4 3	×	0 70		
	4 4	HALT	4 01	X_i	ENTER: (X_i); $i \to 5, 2$
	4 5	×	0 70	νX_i	
	4 6	STR(3)	4 42		
	4 7	×	0 70	$(\nu X_i)^2$	
	5 0	RCL(5)	4 64	$\frac{Y-1}{2}$	$c_i = \frac{Y-1}{2}(\nu X_i)^2$
	5 1	=	0 20	c_i	
	5 2	CHSGN	0 13	$-c_i$	
	5 3	+	0 60		
	5 4	−	0 01	$1-c_i$	
	5 5	α^x	0 74	$-\frac{1}{Y-1}$	$g_i = (1-c_i)^{1/(Y-1)}$
	5 6	RCL(4)	4 63	g_i	
	5 7	×	0 70	νX_i	
	6 0	RCL(3)	4 62	$(R_i/R_2)_i$	ENTER: (R_i/R_2); $i \to 5, 1$
	6 1	×	0 70		
	6 2	HALT	4 01	N_i	
	6 3	÷	0 72	z_i	ENTER: z_i; $i = 0 \to 5, 1$ If $i = 5$, depress [SENSE]
	6 4	HALT	4 01		
	6 5	+	0 60	N_i/z_i	● $\sum(N_i/z_i)$
	6 6	RCL(0)	4 77	◉	② $\sum(N_i/z_i)$
	6 7	=	0 20	◎	
3	7 0	STR(0)	4 57		
	7 1	SFSNS	5 23		
	7 2	SKFI	5 40		
	7 3	JUMP 42	6 42	5 $\sum(N_i/z_i)$	
	7 4	×	0 70		
	7 5	.	0 2(?)		← $\Delta R/R_2 = .050800$
	7 6	0	0 00		
	7 7	5	0 05		

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Register usage:

Reg	Contents
0	$(\dot{m})^*$
1	ν ; β_{10}
2	b
3	νX_i ; $\sin^2\beta_{10}$
4	$\dfrac{1}{\gamma-1}$
5	$\dfrac{\gamma-1}{2}$
6	$2k\sqrt{\gamma}$

Program listing:

P COUNT	COMMAND	CODE	E / A (operand)	NOTES
-10 0	0	00		$\Delta R/R_2 = .050800$
1	8	01		
2	0	00		
-10 3	0	00		
4	×	00 07	s	
5	RCL(6)	46	$\Sigma(N\sqrt{c_i})\dfrac{\Delta R}{R_2}$	
6	=	02	$2k\sqrt{\gamma}$	
7	STR(0)	20	$(\dot{m})^*$	
-10 0	RCL(1)	46	ν	
1	÷	07		
2	RCL(2)	46	b	
3	Σx	00	$\cot\beta_{10}$	
4	-	00		
5	=	00		
6	R→°	44	β_{10}^{R}	
-1 7	STR(1)	40	$\beta_{10}°$	
-1 2 0	SIN/COS	00	$\beta_{10}°$	
1	×	07	$\sin\beta_{10}$	
2	=	02		
3	STR(3)	40	$\sin^2\beta_{10}$	
4	2.FUNC	03	$\cos^2\beta_{10}$	
5	×	07		
6	RCL(2)	46	b	
-12 7	×	07	$b\cos\beta_{10}$	$d = \dfrac{\gamma-1}{2} b^2\cos^2\beta_{10}$
-13 0	×	07	$b^2\cos^2\beta_{10}$	
1	RCL(5)	46	$\dfrac{\gamma-1}{2}$	
2	-	02	d	$f = d - \sin^2\beta_{10} - \dfrac{\gamma-1}{2} b^2\cos^2\beta_{10}$
3	RCL(3)	46	$\sin^2\beta_{10}$	
4	=	02	f	$-f = \sin^2\beta_{10} - \dfrac{\gamma-1}{2} b^2\cos^2\beta_{10}$
5	CHSGN	03	$-f$	
6	√	05	$\sqrt{-f}$	
-13 7	INV	05 4	$\sqrt{1-f}$	

BR PT: 4 ; 5

M.H.V 2/4

BR ADDRESS / STEP COUNT	COMMAND	CODE	E	A	M	0	1	2	3	4	5	6	7	8	9	X	Y	Z	NOTES
6 1 0	×	0 7 0				$(\dot{m})^*$	$\beta_{10}°$	b	$\sin^2\beta_{10}$	$\frac{1}{\gamma-1}$	$\frac{\gamma-1}{2}$	$2k\sqrt{\delta}$							
1	RCL(2)	4 6 1	b																
2	=	0 2 0																	
3	STR(3)	4 4 2	M_{W1}						M_{W1}										
4 1 4	HALT	4 0 1				$(\dot{m})^*$	$\beta_{10}°$		M_{W1}										RESULTS
5	0	0 0																	Clears (0)
6	STR(0)	4 5 7																	To repeat with new value V_{10}/a_0
7 1 4	TO(2)	7 4 2																	

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MONROE CALCULATOR 1655 WITH CARD READER CR-1

Description

This program calculates the flow conditions after an axial row of
blades for known entrance conditions. Figure D(109)1 shows such as
cascade located between station (e) and station (d). It is assumed
that the conditions at the mean radii R_{me} and R_{md}, at entrance and
discharge, respectively, are representative of the average flow properties
ahead of and after the cascade. The effective flow area at station (e)
is taken as

$$A_e \ k_{Be} = 2\pi \ R_{me} \ h_e \ k_{Be}$$

where k_{Be} is a blockage factor that takes account of the boundary layers
at the inner and outer wall contours. Similarly, at discharge station (d)

$$A_d \ k_{Bd} = 2\pi \ R_{md} \ h_d \ k_{Bd}$$

Figure D(109)2 shows a diffusor cascade of a subsonic axial compressor
where the flow angle is reduced from α_e to α_d. Figure D(109)4 shows a
stator of a turbine blading where the subsonic velocity V_e ahead of the
row is accelerated to a supersonic velocity V_d because of the converging-
diverging area change of the flow channel. Figures D(109)3 and 5
represent the flow processes in the bladings of Fig. D(109)2 and 4,
respectively in entropy diagrams, by assuming that the processes are
adiabatic and that the fluids have constant specific heat ratios γ.
In general, from the equation of continuity

$$A_e \ k_{Be} \ \rho_e \ V_e \ \cos \alpha_e = A_d \ k_{Bd} \ \rho_d \ V_d \ \cos \alpha_d$$

With ρ_e and ρ_d from

$$\rho = p/g \ R_G \ T$$

and the Mach numbers M_e and M_d from

$$M = V/\sqrt{g \ \gamma \ R_G \ T}$$

there is

$$M_d = \frac{A_e}{A_d} \frac{k_{Be}}{k_{Bd}} \ \frac{\cos \alpha_e}{\cos \alpha_d} \ \frac{p_e}{\sqrt{T_e}} \ M_e \ \frac{\sqrt{T_d}}{p_d}$$

To obtain dimensionless relations the static pressure p and the static temperatures T will be taken as multiples of the constants P_0 and T_0, respectively. Then

$$M_d = K \ \frac{\sqrt{T_d/T_0}}{(p_d/P_0)} \qquad\qquad \text{D109(1)}$$

where

$$K = \frac{A_e}{A_d} \frac{k_{Be}}{k_{Bd}} \frac{\cos \alpha_e}{\cos \alpha_d} \ M_e \ \frac{p_e/P_0}{\sqrt{T_e/T_0}} \qquad\qquad \text{D109(2)}$$

The dimensionless quantity K is known from the cascade geometry and the inlet conditions. It is assumed that the ratios P_{te}/P_0, T_{te}/T_0 and the Mach number M_e are known, where P_{te} and T_{te} are the total pressure and the total temperature at station (e). Then, from

$$T_{te} = T_e \left[1 + \frac{\gamma-1}{2} \ M_e^{\ 2}\right]$$

and

$$P_{te} = p_e \left[1 + \frac{\gamma-1}{2} \ M_e^{\ 2}\right]^{\gamma/(\gamma-1)}$$

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there are

$$\frac{T_e}{T_0} = \frac{T_{t2}/T_0}{1 + \frac{\gamma-1}{2} M_e^2}$$ D109(3)

and

$$\frac{P_e}{P_0} = \frac{P_{te}/P_0}{\left[1 + \frac{\gamma-1}{2} M_e^2\right]^{\gamma/(\gamma-1)}}$$ D109(4)

These quantities establish the value of K of Eq. 2, if the flow areas, the blockage factors, and the flow angles at stations (e) and (d) are known.

Since $T_{td} = T_{te}$ for an adiabatic process, there is similar to Eq. 3

$$\frac{T_d}{T_0} = \frac{T_{te}/T_0}{1 + \frac{\gamma-1}{2} M_d^2}$$ D109(5)

The losses in the row of the blade are expressed by the total pressure loss coefficient Y_t defined by

$$Y_t = \frac{P_{te} - P_{td}}{P_{te} - P_e}$$ D109(6)

Hence

$$\frac{P_{td}}{P_0} = \frac{P_{te}}{P_0} - Y_t \left(\frac{P_{te}}{P_0} - \frac{P_e}{P_0}\right)$$ D109(7)

and, similar to Eq. 4,

$$\frac{P_d}{P_0} = \frac{P_{td}/P_0}{\left[1 + \frac{\gamma-1}{2} M_d^2\right]^{\gamma/(\gamma-1)}}$$ D109(8)

Because of the above exponential expression it is not possible to obtain a closed solution for M_d by substituting Eqs. 5 and 8 into Eq. 1. It is necessary to choose a particular value $M_d = M_d^*$, which is used to determine

T_d/T_0 and p_d/P_0 by Eqs. 5 and 8. These values are introduced into Eq. 1.,
and M_d* must be iterated until the result of Eq. 1 equals M_d*. For given
flow conditions at station (e) there always occur two solutions, one for
which M_d is subsonic, the other for which M_d is supersonic.

All input data are dimensionless with the exception of the cross-
sectional areas A_e and A_d. The dimensions of these areas are arbitrary but
the units for A_e and A_d must be equal. As seen from the operating
instructions, the calculated ratios p_e/P_0 and T_e/T_0 must be read before the
iteration for M_d. If the condition $M_d = M_d*$ has been satisfied, the final
results are obtained by depressing the (SENSE) switch.

The velocity V_d after the cascade is

$$V_d = M_d \; a_0 \sqrt{\frac{T_d}{T_0}}$$

where a_0 is the velocity of sound corresponding to T_0. The velocity V_d
is obtained with the keyboard operation

↑ (8) $\sqrt{}$ x ↑ (0) x (Value of a_0) =

at P-Count 173.

Enclosures: Figure D(109)

                    Operating Instruction (1 page)

                    Program Listing (4 pages)

FIG. D(109)1

FIG. D(109)2

FIG. D(109)4

FIG. D(109)3

FIG. D(109)5

FIG. D(109)   FLOW THROUGH CASCADE

MONROE CALCULATOR 1655 WITH CARD READER CR-1

<u>Set-Up</u>: (RESET); (TO(0)); Depress (LOAD); Read Cards 1-4

Release (LOAD); (TO(0)); Depress (P); (RESUME)

P-COUNT				
0 0 1	ENTER:	Y		(RESUME)
0 1 7	" :	A_e		(")
0 2 1	" :	k_{Be}		(")
0 2 3	" :	A_d		(")
0 2 5	" :	k_{Bd}		(")
0 3 0	" :	$\alpha_e(^{\circ})$		(")
0 3 7	" :	$\alpha_d(^{\circ})$		(")
0 4 7	" :	M_e		(")
0 5 6	" :	T_{te}/T_0		(")
0 7 3	" :	P_{te}/P_0		(")
1 0 6	" :	Y_t		(")
1 1 3	RESULT:	$\uparrow(0) \rightarrow pe/P_0$;	$\uparrow(4) \rightarrow T_e/T_0$	
1 1 4	ENTER:	$M_d{}^*$ for Iteration		(RESUME)
1 5 4	.	CHECK OF ITERATION:	$\uparrow(0) = M_d$;	$\uparrow(4) = M_d{}^*$

If: $M_d \neq M_d{}^*$ $\downarrow$ If: $M_d = M_d{}^*$

(RESUME)   Depress (SENSE)

(Improved Value $M_d{}^*$)   (RESUME)

1 7 3	RESULTS:	$\uparrow(0) \rightarrow M_d$
		$\uparrow(4) \rightarrow M_d{}^*$
		$\uparrow(2) \rightarrow P_{td}/P_0$
		$\uparrow(1) \rightarrow K$
		$\uparrow(7) \rightarrow p_d/P_0$
		$\uparrow(8) \rightarrow T_d/T_0$

$\downarrow$

Release (SENSE)

(RESUME)

(New Data)

TURBO-PROPULSION LABORATORY, DEPT. OF AERONAUTICS, NPS ,
PROGRAM No. ...109... MONROE 1655 CALCULATOR
FLOW CONDITIONS AFTER CASCADE FOR GIVEN INLET CONDITIONS....
FLOW DEFLECTIONS AND TOTAL PRESSURE LOSS COEFFICIENT

PAGE..1..OF...4
DATE:..8/6/72.   BY: M.H.Vav

REGISTERS / NOTES

ADDRESS P COUNT	COMMAND	CODE	E	Registers	NOTES
0 0	HALT	4 0 1	γ		ENTER: γ
1	STR(1)	4 4 0		R1 = γ	
2	−	0 6 2			
3	÷	0 0 1	$\gamma-1$		
4	÷	0 7 2	$\gamma-1$	R2 = $\gamma-1$	
5	STR(2)	4 4 −	$\frac{\gamma-1}{\gamma}$		
6	2	0 0 2	γ		
7	=	0 0 0			
0	STR(6)	4 4 5	γ	R6 = $\frac{\gamma-1}{2}$	
−	RCL(1)	4 6 0			
	÷	0 7 2	$\frac{\gamma-1}{\gamma}$		
	RCL(2)	4 6 1			
−	=	0 2 0	$\frac{\gamma-1}{\gamma}\ \frac{\gamma}{\gamma-1}$		
−	STR(5)	4 4 4		R5 = $\frac{\gamma}{\gamma-1}$	
−	HALT	4 0 1			
	X	0 7 0			
2 0	HALT	4 0 1			ENTER: A_e
	÷	0 7 2			
2	HALT	4 0 1			ENTER: k_{be}
	÷	0 7 2			
2	HALT	4 0 1			ENTER: A_d
	=	0 2 0	B		ENTER: k_{Bd} ; $B=(A_e k_{be})/(A_d k_{Bd})$
2	STR(1)	4 4 0	α_e	R1 = B	
	HALT	4 0 1			ENTER: α_e
3	SIN/COS	0 4 0	$\cos\alpha_e$		
	2.FUNCT	0 3 6			
	X	0 7 0			
	RCL(1)	4 6 0	B		
	=	0 2 0			
	STR(1)	4 4 0	α_d	R1 = $B\cos\alpha_e$	
3	HALT	4 0 1			
3	SIN/Cos	0 4 0			ENTER: $\alpha_d°$

BR PT: 0   244   (1)

M U V

Register header labels: Register 5 = $\frac{\gamma}{\gamma-1}$, Register 6 = $\frac{\gamma-1}{2}$

BR PT	ADDRESS P COUNT	COMMAND	CODE	E	A	M	0	1	2	3	4	5	6	7	8	9	X	Y	Z	NOTES
2	(4) 0	2.FUNCT	0 3 6	$\cos\alpha$								$\frac{\gamma}{\gamma-1}$	$\frac{\gamma-1}{2}$							
	1	÷	0 7 2																	
	2	RCL(1)	4 6 0	$B\cos\alpha_e$																
	3	=	0 2 0	$(B\cos\alpha_e/\cos\alpha)^{-1}$																
	4	INV	0 5 4	$B\cos\alpha_e/\cos\alpha$																
	5	X	0 7 0																	
	46	HALT	4 0 1	M_e					M_e											ENTER: M_e
	47	STR(2)	4 4 -	M_e																
	50	=	0 2 0	C				C												$C = \dfrac{A_e\,h_{Be}\,\cos\alpha_e}{A_s\,h_{ss}\,\cos\alpha_s}\,M_e$
	1	STR(1)	4 4 0	C																
	2	RCL(2)	4 6 -	M_e																
	3	TO(6)	7 4 6	Z_{1e}																
	4	X	0 7 0																	
	55	HALT	4 0 1	T_{te}/T_o						T_{te}/T_o										ENTER: T_{te}/T_o
	56	STR(3)	4 4 2	T_e/T_o							T_e/T_o									
	57	=	0 2 0																	
3	60	STR(4)	4 4 3	$\sqrt{T_e/T_o}$																
	1	√	0 5 6	$1/\sqrt{T_e/T_o}$																
	2	INV	0 5 4																	
	3	X	0 7 0																	
	4	RCL(1)	4 6 0	C																
	5	=	0 2 0	C'				C'												$C' = C/\sqrt{T_e/T_o}$
	66	STR(1)	4 4 0	C'																
	67	RCL(2)	4 6 1	M_e																
	70	TO(7)	7 4 7	Z_{2e}																
	1	X	0 7 0																	
	2	HALT	4 0 1	P_{te}/P_o						P_{te}/P_o										ENTER: P_{te}/P_o
	73	STR(2)	4 4 -	P_e/P_o			P_e/P_o													
	74	X	0 7 0																	
	5	STR(0)	4 5 7	C'																
	6	RCL(1)	4 6 0	K																
	77	=	0 2 0																	

ADDRESS BR PT P COUNT	COMMAND	CODE	E	A	M	0	1	2	3	4	5	6	7	8	9	X	Y	Z	NOTES
4 0 0	STR(1)	4 4 0	K			P_e/P_0	K	P_{te}/P_0	P_{te}/T_0	T_e/T_0	$\frac{Y}{Y-1}$	$\frac{Y-1}{2}$								
1	RCL(0)	4 7 7	P_e/P_0																
2	−	0 6 2																	
3	RCL(2)	4 6 1	P_{te}/P_0																
4	×	0 7 0	$\frac{P_e-P_{te}}{P_0}$																
1 0 5	HALT	4 0 1	Y_t																ENTER: Y_t
6	+	0 6 0	$\frac{Y_t \cdot P_{te}}{P_0}$																
7	RCL(2)	4 6 1	P_{te}/P_0																
0	=	0 2 0	P_{td}/P_0			P_e/P_0		P_{td}/P_0		T_e/T_0										RESULTS: $\uparrow(0) \to P_e/P_0$; $f(4) \to T_e/T_0$
1 0 1	STR(2)	4 4 1																	ENTER: M_d^* for Iteration
1 2	HALT	4 0 1	M_d^*																
1 3	HALT	4 0 1	M_d^*					M_d^*												
1 4	STR(4)	4 4 3	Z_{1d}^*																
5	To(7)	7 4 7											P_d/P_0						
6	×	0 7 0																	
1 7	RCL(2)	4 6 1	P_{td}/P_0																
2 0	=	0 2 0	P_d/P_0																
2 1	STR(7)	4 4 6	P_0/P_d			$K\frac{P_0}{P_d}$														
2	INV	0 5 4																	
3	×	0 7 0	K																
4	RCL(1)	4 6 0	KP_0/P_d																
5	=	0 2 0																	
6	STR(0)	4 5 7	M_d^*																
2 7	RCL(4)	4 6 3	Z_{1d}^*					M_d^*												
3 0	To(6)	7 4 6	T_e/T_0																
1	×	0 7 0	T_d/T_0																
2	RCL(3)	4 6 2	T_d/T_0																
3	=	0 2 0	V_d/T_0																
1 4	STR(8)	4 4 7													T_d/T_0				
5	√	0 5 6																	
6	×	0 7 0																	
1 3 7	JUMP 50	6 5 0																	

REGISTERS

BR PT	ADDRESS P COUNT	COMMAND	CODE	E	0	1	2	3	4	5	6	7	NOTES
6	14 0	X	07 0	M						$\frac{\gamma}{\gamma-1}$	$\frac{\gamma-1}{2}$		SUBROUTINE: $z_1 = f(M,\gamma)$
	1	X	07 0	M^2									
	2	RCL(6)	46 5	$\frac{\gamma-1}{2}$									
	3	+	06 0	$\frac{\gamma-1}{2}M^2$									
	4	-	00 1										
	5	=	02 0	z_1^{-1}									$z_1 = \sqrt{/(1+\frac{\gamma-1}{2}M^2)}$
	6	INV	05 4	z_1									
	7	RCLP	05 7	z_1									
	15 0	RCL(0)	47 7	$\frac{KP_{t0}}{P_d}$ M_d	$\frac{KP_{t0}}{P_d}$	K	P_{td}/P_0 M_d^*	T_{d0}/T_0		$\frac{\gamma}{\gamma-1}$	$\frac{\gamma-1}{2}$	P_d/P_0 T_d/T_0	
	1	=	02 0	M_d									
	2	STR(0)	45 7		M_d								CHECK: $M_d = M_d^*$?; If $M_d = M_d^*$ depress (SENSE)
	3	HALT	40 1										
	4	SFSNS	52 3										
	5	SKF1	54 0										
	6	JUMP 13	6 13										
	7	JUMP 72	67 2										
7	16 0	X	07 0	M									SUBROUTINE $z_2 = f(M,\gamma)$
	1	X	07 0	M^2									
	2	RCL(6)	46 5	$\frac{\gamma-1}{2}$									
	3	+	06 0	$\frac{\gamma-1}{2}M^2$									
	4	-	00 1	$1+\frac{\gamma-1}{2}M^2$									
	5	a^x	07 4	$\frac{\gamma}{\gamma-1} \frac{1}{z_2}$									
	6	RCL(5)	46 4	z_2									
	7	=	02 0										
	17 0	INV	05 4		M_d	K	P_{td}/P_0	T_{d0}/T_0	M_d^*	$\frac{\gamma}{\gamma-1}$	$\frac{\gamma-1}{2}$	P_d/P_0 T_d/T_0	$z_2 = \sqrt{/[(1+\frac{\gamma-1}{2}M^2)^{(\gamma-1)}]}$
	1	RCLP	05 7										RESULTS
	2	HALT	40 1										
	3	To(0)	74 0										

MONROE CALCULATOR 1655 WITH CARD READER C-R1

Description

The curve of Fig. D(110) has the characteristics that its curvature k at the point P_O is zero and that k increases gradually with increasing angle θ. To be found is that curve which has the angle $\delta_m = \pi/2$ between the tangents of the curve at P_O and P_m such that particular distances x_O/a and y_O/a are obtained. For

$$r/a = \theta^{-b} \qquad\qquad 110(1)$$

there is *

$$\tan \Psi = -\frac{\theta}{b} \qquad\qquad 110(2)$$

For $0 < b < 1$ there is $\pi/2 < \Psi < \pi$ and since

$$\vartheta = \Psi - \pi/2$$

one obtains

$$\cot \vartheta = -\tan(\Psi - \pi/2) = \theta/b \qquad\qquad 110(3)$$

and

$$\sin \vartheta = \sqrt{\frac{1}{1 + (\theta/b)^2}} \qquad\qquad 110(4)$$

where $\qquad 0 < \vartheta < \pi/2$

The curvature k at $P(r/a, \theta)$ is

$$k = \frac{1 - b(1-b)/\theta^2}{a\theta^{-b}\left[1 + (b/\theta)^2\right]^{3/2}} \qquad\qquad 110(5)$$

----

*Vavra, M. H., "Aerothermodynamics and Flow in Turbomachines," pp. 293/298, John Wiley & Sons, New York, 1960.

At $P_o \, (r_o/a, \; \theta_o)$ the curvature k_o is zero, hence, by Eq. 5

$$\theta_o = \sqrt{b(1-b)}$$ 110(6)

From Eq. 1

$$\frac{r_o}{a} = \theta_o^{-b} = [b(1-b)]^{-\frac{b}{2}}$$ 110(7)

and from Eq. 4

$$\vartheta_o = \sin^{-1} \sqrt{\frac{1}{1 + (\theta_o/b)^2}}$$ 110(8)

From Fig. D(110) for $P(r/a, \; \theta)$

$$\delta = (\theta + \vartheta) - (\theta_o + \vartheta_o) = E - E_o$$

and for $P_m \left(\dfrac{r_m}{a}, \; \theta_m \right)$, where $\delta_m = \pi/2$,

$$\delta_m = \frac{\pi}{2} = (\theta_m + \vartheta_m) - (\theta_o + \vartheta_o) = E_m - E_o$$ 110(9)

where, according to Eq. 4

$$\vartheta_m = \sin^{-1} \sqrt{\frac{1}{1 + (\theta_m/b)^2}}$$ 110(10)

From Fig. D(110) the coordinates x_o/a and y_o/a are

$$\frac{x_o}{a} = \frac{r_o}{a} \cos \vartheta_o - \frac{r_m}{a} \sin \vartheta_m$$ 110(11)

$$\frac{y_o}{a} = \frac{r_o}{a} \sin \vartheta_o + \frac{r_m}{a} \cos \vartheta_m$$ 110(12)

From Eq. 3

$$\frac{b}{\theta} = \tan \vartheta$$

Hence

$$1 + (b/\theta)^2 = 1 + \tan^2 \vartheta = \frac{1}{\cos^2 \vartheta}$$

Introduced into Eq. 5, with Eqs. 1 and 6,

$$a\,k = \frac{1 - (\theta_o/\theta)^2}{r/a} \cos^3 \vartheta \qquad\qquad 110(13)$$

Hence at P_m the curvature k_m is obtained from

$$a\,k_m = \frac{1 - (\theta_o/\theta_m)^2}{r_m/a} \cos^3 \vartheta_m \qquad\qquad 110(14)$$

It is not possible to calculate the parameters of a curve with $\delta_m = \pi/2$ that has a given ratio y_o/x_o with a closed solution. It is necessary to choose a value of b which establishes θ_o, r_o/a and ϑ_o. Then the angle θ_m must be varied until $\delta_m = 90^o$ by Eq. 9. With θ_m, the quantities r_m/a and ϑ_m are obtained from Eqs. 1 and 10. Then the coordinates x_o/a and y_o/a of Eqs. 11 and 12 establish the ratio y_o/x_o. If this ratio differs from that of the desired curve the quantity b must be varied until agreement is reached

From Eqs. 11 and 14 it is possible also to express the curvature k_m as a multiple of $1/x_o$ or

$$k_m\, x_o = (a\,k_m)\ (x_o/a) \qquad\qquad 110(15)$$

Enclosures: Figure D(110)

                  Operating Instruction (1 page)

                  Program Listing (4 pages)

FIG. D(110)   CURVE $r/a = \theta^{-b}$

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MONROE CALCULATOR 1655/6 WITH CARD READER CR-1

Set-Up: (RESET); (TO(0)); Depress (LOAD); Read Cards 1-4

Release (LOAD); TO(0)); Depress (P); (RESUME)

P-COUNT		
0 0 3	ENTER: b	[Resume]
0 1 5	ENTER: $\theta_m(^\circ)$ for Iteration	["]
0 3 7	CHECK of ITERATION: $\uparrow$ (1) $= \delta_m = 90^\circ$?	

$\delta_m \neq 90^\circ$ $\qquad\qquad$ $\delta_m = 90^\circ$

(RESUME) $\qquad\qquad\qquad$ Depress (SENSE)

(New Value of θ_m°) $\qquad\qquad\qquad$ (RESUME)
(See Note 1)

0 5 7 $\qquad$ RESULTS: $\uparrow(1) \to r_o/a$

$\uparrow(0) \to r_m/a$

$\uparrow(8) \to \vartheta_o^\circ$

$\uparrow(7) \to \vartheta_m^\circ$

Release (SENSE)

(RESUME)

1 7 6 $\qquad$ RESULTS: $\uparrow(2) \to y_o/x_o$; $\uparrow(0) \to k_m\, x_o$

$\uparrow(1) \to x_o/a$; $\uparrow(5) \to \theta_o^\circ$

$\uparrow(4) \to y_o/a$; $\uparrow(3) \to \theta_m^\circ$

New Value of b (See Note 2) $\qquad$ (RESUME)

Note 1: $\delta_m < 90^\circ \to$ Increase θ_m ; $\delta_m > 90^\circ \to$ Decrease θ_m

Note 2: To increase $y_o/x_o \to$ Increase b

To decrease $y_o/x_o \to$ Decrease b

TURBO-PROPULSION LABORATORY, DEPT. OF AERONAUTICS, NPS,
PROGRAM No. 110 MONROE 1655 CALCULATOR
CALCULATION OF CURVE $r/a = \theta^{-b}$ WITH ZERO CURVATURE
AT ONE POINT AND $\delta_{max} = 90°$
PAGE 1 OF 4
DATE: 8/7/72 BY: M.H.Vavra

Registers used: reg 6 = b, reg 5 = θ_0^R, reg 4 = ϑ_0^R, reg 3 = θ_m^R, reg 2 = ϑ_m^R, reg 1 = δ_m

Address	Command	Code	E (register)	Notes
0 0	–	01	–	
0 1	↑	00 62		
0 2	HALT	40	b	ENTER: b
0 3	STR(6)	45	b	
0 4	X	07	$1-b$	
0 5	RCL(6)	46	b	
0 6	=	00	$b(1-b)$	
0 7	√	05	θ_0^R	
1 0	STR(5)	44	θ_0^R	
1 1	TO(7)	47	$\sin\vartheta_0$	
1 2	SIN⁻¹/COS⁻¹	42	ϑ_0^R	
1 3	STR(4)	43	ϑ_0^R	
1 4	HALT	40	$\theta_m°$	ENTER: $\theta_m°$ $(0 \le \theta_m \le 180°)$
1 5	SIN/COS	40		
1 6	2FUNCT	36	$\cos\theta_m$	
1 7	SIN⁻¹/COS⁻¹	42		
2 0	2FUNCT	36	θ_m^R	
2 1	STR(3)	44	θ_m^R	
2 2	TO(7)	47	$\sin\vartheta_m$	
2 3	SIN⁻¹/COS⁻¹	42	ϑ_m^R	
2 4	STR(2)	44	ϑ_m^R	
2 5	+	06	θ_m^R	
2 6	RCL(3)	46	θ_m^R	
2 7	–	06		
3 0	RCL(5)	46	θ_0^R	
3 1	–	06		
3 2	RCL(4)	46	ϑ_0^R	
3 3	=	00	$\delta_m°$	
3 4	R→	04	$\delta_m°$	
3 5	STR(1)	44	δ_m	$\delta_m = \vartheta_m + \theta_m - (\theta_0 + \vartheta_0)$
3 6	HALT	40		
3 7	SFSNS	53		CHECK: $\delta_m = 90°$? If true: [SENSE]

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REGISTERS (top labels):
- 1: δ_m°
- 2: ϑ_m^R
- 3: θ_m^R
- 4: ϑ_0^R
- 5: θ_0^R
- 6: b
- 7: ϑ_m° (and θ_m°)
- 8: ϑ_0° (and ϑ_0°)

NOTES: RESULTS: r_m/a, r_0/a, ϑ_m°, ϑ_0°

Address	Command	Code	E (register / note)
0	SKF1	540	
1	JUMP 14	614	
2	RCL(5)	464	θ_0^R
3	TO(6)	746	r_0/a
4	STR(1)	440	
5	RCL(3)	462	θ_m^R
6	TO(6)	746	r_m/a
7	STR(0)	457	
0	RCL(2)	446	ϑ_m^R
1	R→	046	ϑ_m°
2	STR(7)	446	
3	RCL(4)	463	ϑ_0^R
4	R→°	046	ϑ_0°
5	STR(8)	447	
6	HALT	401	ϑ_e^e
7	RCL(8)	467	$\sin\vartheta_0$
0	SIN/COS	000	
1	x	070	$\dfrac{r_0}{a}\sin\vartheta_0$
2	RCL(1)	460	
3	=	020	
4	STR(4)	443	$\dfrac{r_0\sin\vartheta_0}{a}$
5	2.FUNC	036	$\cos\vartheta_0$
6	x	070	
7	RCL(1)	460	r_0/a
0	=	020	$\dfrac{r_0\cos\vartheta_0}{a}$
1	STR(1)	044	ϑ_m^R
2	RCL(2)	046	ϑ_m°
3	R→°	046	$\sin\vartheta_m$
4	SIN/COS	040	
5	x	070	r_m/a
6	RCL(0)	077	$\dfrac{r_m}{a}\sin\vartheta_m$
7	−	062	

BR PT: 2

BR PT: 3

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M.H.V. 3/2/1

Registers (header labels):

0	1	2	3	4	5	6
r_m/a	$\dfrac{r_o\cos\vartheta_o}{a}$	ϑ_m^R	θ_m^R	$\dfrac{r_o\sin\vartheta_o}{a}$	θ_o^R	b

Program listing:

P COUNT	COMMAND	CODE	E / A	Register filled	NOTES
0	RCL(1)	4 6 0	$r_o\cos\vartheta_o$		
1	=	0 2 0	$-x_o/a$		
2	CH SGN	0 1 3	x_o/a		
3	STR(1)	4 4 0		1: x_o/a	
4	2.FUNCT	0 3 6	$\cos\vartheta_m$		
5	X	0 7 0			
6	RCL(0)	4 7 7	r_m/a		
7	÷	0 6 0	$r_m\cos\vartheta_m$		
0	RCL(4)	4 6 3	$r_o\sin\vartheta_o$		
1	=	0 2 0	y_o/a		
2	STR(4)	4 4 3		4: y_o/a	
3	RCL(5)	4 6 4	θ_o^R		
4	÷	0 7 2			
5	RCL(3)	4 6 2	θ_m^R		
6	X	0 7 0	θ_o/θ_m		
7	÷	0 6 2	$(\theta_o/\theta_m)^2$		
0	+	0 0 0	$\left(\dfrac{\theta_o}{\theta_m}\right)^2 - 1$		$Y = (1-(\theta_o/\theta_m)^2)/(r_m/a)$
1	÷	0 7 2	r_m/a		
2	RCL(0)	4 1 7			
3	=	0 2 0	$-Y$		
4	CH SGN	0 1 3	Y		
5	STR(0)	4 5 7		0: Y	
6	RCL(2)	4 6 1	ϑ_m^R		
7	R→	0 4 6	ϑ_m°		
0	SIN/COS	0 4 0	$\cos\vartheta_m$		
1	2.FUNCT	0 3 6			
2	α^x	0 7 4			
3	3	0 0 3	$\cos\vartheta_m^3$		
4	X	0 7 0			
5	RCL(0)	4 7 7	Y		
6	X	0 7 0	$a\,k_m$		
7	JUMP 45	6 4 5			

BR PT: 4 ... 5 ... 3

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PROGRAM No. ...110.... MONROE 1655 CALCULATOR

ADDRESS / P COUNT	COMMAND	CODE	E	0	1	2	3	4	5	6	NOTES
14 0	a^x	0 74	θ							b	SUBROUTINE: $r/a = \theta^{-b}$
1	RCL(6)	4 65	b								
2	=	0 20	θ^b								
3	INV	0 54	θ^{-b}								
4	RCLP	5 57	r/a								
4 5	RCL(1)	4 60	x_0/a	"Y"	x_0/a	ϑ_m^R	θ_m^R	y_0/a	θ_0^R	b	
6	=	0 20	$x_0 k_m$	$x_0 k_m$							
4 7	STR(0)	4 57	$x_0 k_m$								
5 0	RCL(4)	4 63	y_0/a								
1	÷	0 72	x_0/a								
2	RCL(1)	4 60	y_0/x_0								
3	=	0 20	y_0/x_0			y_0/x_0					
4	STR(2)	4 1	θ_0^R								
5	RCL(5)	4 64	θ_0°								
6	R→°	4 6	θ_0°								
5 7	JUMP 71	6 71									
6 0	÷	0 72	θ							b	SUBROUTINE: $\sin\vartheta = \dfrac{1}{\sqrt{1+(\theta/b)^2}}$
1	RCL(6)	4 65	b								
2	×	0 70	θ/b								
3	+	0 60	$(\theta/b)^2$								
4	-	0 0 1									
5	=	0 20	$1+(\theta/b)^2$								
6	√	0 56	$\sin\vartheta$								
7	INV	0 54									
7 0	RCLP	5 57	θ_0°	$x_0 k_m$	x_0/a	y_0/x_0	θ_m^R	y_0/a	θ_0°	b	
1	STR(5)	4 4	θ_0°								
2	RCL(3)	4 62	θ_m^R								
3	R→°	0 46	θ_m°								
4	STR(3)	4 42					θ_m°				
7 5	HALT	4 01		$x_0 k_m$	x_0/a	y_0/x_0	θ_m°	y_0/a	θ_0°	b	RESULTS: $\dfrac{y_0}{x_0}, \dfrac{y_0}{a}, \dfrac{x_0}{a}, x_0 k_m; \theta_0^{\circ}, \theta_m^{\circ}; \vartheta_0^{\circ}, \theta_m^{\circ}$
6	TO(0)	7 40									

BR PT: 6   7

PROGRAM NO. 517

MONROE CALCULATOR 1880-22

Description

Program 517 calculates the conditions after the diffusor, the
honeycomb flow straightener, and the discharge duct of the Hybrid
compressor. Details of these calculations are given in Section III.3
of "Hybrid Compressor Design Report." The compressor is supposed to
operate as an exhauster such that the static pressure (p_6) at the compressor
discharge is 14.7 psia. The total temperature at the impeller inlet (T_0)
is taken to be 520°R. Basic data to be used in the program are the
conditions after the rotor obtained by the method described in Section III.2
of "Hybrid Compressor Design Report."

Both diffusor rows are considered as a unit and it is assumed that
the flow angle α_4 after the second diffusor blade row is constant, equal
to 21°. The program contains program 109, described in Appendix D, which
by an iterative procedure establishes the Mach number $M_{V4} = M_4$ of the flow
after the diffusor with losses that are a multiple of its design pressure
loss coefficient.

After calculating the diffusor performance program 517 determines
the overall compressor performance in accordance with Section III.4.
Examples of print-outs are given in Tables XI and XII of the aforementioned
report.

Enclosures: Operating Instructions (1 page)
              List of Print-Out of Results (1 page) .
              Program Listing (12 pages)
              Main Data Storage (1 page)

MONROE CALCULATOR 1880-22

Set-Up: Read 2 Magnetic Cards starting at Branch Point 0 0

P-COUNT		
0 0 4 3	ENTER: $(k_{B2}/k_{B4})\cos\alpha_4 = 1.161\ 218$	(RESUME)
0 0 4 7	" : $(Y_t)_{i=i_o} = 0.2089$	(")
0 0 5 1	" : $V_S/V_4 = 1.039$	(")
0 0 5 5	" : $V_5/V_4 = 0.8764$	(")
0 0 5 9	" : $V_6/V_4 = 0.722$	(")
0 0 7 9	" : $\alpha_4\ (^o) = 21^o$	(")
0 0 8 5	" : $\alpha_2\ (^o)$	(")
0 0 9 4	" : T_{t2}/T_0	(")
0 0 9 8	" : P_{t2}/T_0	(")
0 1 0 2	" : T_2/T_0	(")
0 1 0 6	" : P_2/P_0	(")
0 1 1 0	" : M_{V2}	(")
0 1 4 1	" : $Y_t/(Y_t)_{i=i_o}$	(")
0 1 6 7	" : M_4* FOR ITERATION	(")
0 2 3 5		

PRINT-OUT: IDENTIFIER -4.

$$\Delta M = M_4 - M_4*$$

$$M_4*$$

IF $\Delta M \neq 0$ IF $\Delta M \cong 0$

(RESUME)   ENTER: 0
                            (RESUME)

0 4 3 9	ENTER: $\dot{w}\sqrt{(R_G/g)T_0}/P_0$	(RESUME)
0 4 6 7	" : U_2/a_0	(")

PRINT-OUT OF RESULTS
  (see list attached)

SEE NOTE
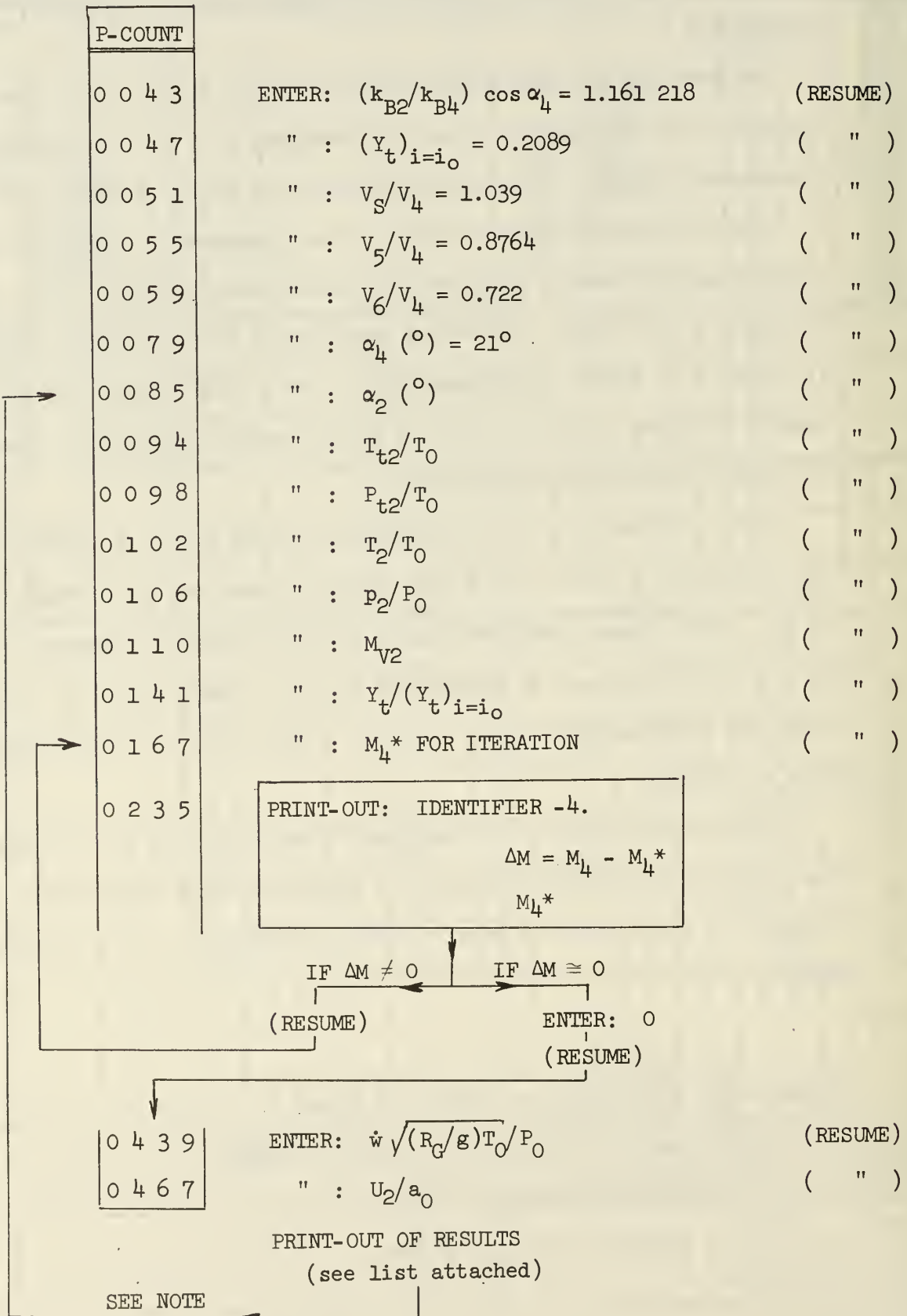
NOTE: After "Print-out of Results" the program
       automatically returns to P-Count 0085 for new data.

MONROE CALCULATOR 1880-22

LIST OF PRINT-OUT OF RESULTS:

· · · · · · · · · · ·

U_2/a_0

α_2 ($^\circ$)

P_{t4}/P_0

p_4/P_0

T_4/T_0

$M_{V4} = M_4$

V_4/a_0

P_{t4}'/P_0

p_4'/P_0

P_{t4}''/P_0

p_4'/P_0

P_{t5}/P_0

P_{t6}/P_0

p_6/P_0

P_0 (psia)

$\dot{w}$ (lbm/s)

HP   (HP)

N   (rpm)

η_T (–)

· · · · · · · · · · ·

STEP			SYMBOL	COMMAND	COMMENTS	ENTER	STORE	PRINT
0	0	0		2				
		1		9				
		2		.				
		3		3				
		4		6				
		5		4				
		6		0				
		7		7				
		8		7	$E = \sqrt{(R_G/g)\,T_0}$			
		9		↓( )( )				
0	1	0		2				
		1		0	✗		$E \rightarrow 20$	
		2		1				
		3		7				
		4		6				
		5		.				
		6		5				
		7		4	$F = R_G(\gamma/(\gamma-1)\,T_0/550$			
		8		↓( )( )				
		9		2				
0	2	0		1	✗		$F \rightarrow 21$	
		1		2				
		2		3				
		3		2				
		4		9				
		5		0				
		6		.				
		7		2				
		8		1				
		9		↓( )( )	$G = a_0\, 720/(\pi D_2)$			
0	3	0		2				
		1		2			$G \rightarrow 22$	
		2		/				
		3		/				
		4		/				
		5		/	NO OP.			
		6		/				
		7		/				
		8		/				
		9		/				
0	4	0		SET D.P.				
		1		4				
		2		HALT	ENTER: $C = \frac{k_{B3}}{k_{B4}}/\cos\alpha_1 = 1.162218$	C		
		3		↓( )( )				
		4		0				
		5		0			$C \rightarrow 00$	
		6		HALT	ENTER: $(Y_t)_{i=i_0} = 0.2089 = Y_{t0}$	Y_{t0}		
		7		↓( )( )				
		8		0				
		9		1			$Y_{t0} \rightarrow 01$	

STEP	SYMBOL	COMMAND	COMMENTS	ENTER	STORE	PRINT
0 5 0		HALT	ENTER: $V_S/V_A = 1.039$	V_S/V_4		
1		↓( )( )				
2		0				
3		2			$V_S/V_4 \to 02$	
4		HALT	ENTER: $V_S/V_4 = 0.8764$	V_S/V_4		
5		↓( )( )			$V_S/V_4 \to 03$	
6		0				
7		3				
8		HALT	ENTER: $V_6/V_4 = 0.722$	V_6/V_f		
9		↓( )( )				
0 6 0		0				
1		4			$V_6/V_a \to 04$	
2		.				
3		4	$\gamma-1$			
4		÷				
5		1				
6		.				
7		4	γ			
8		=	$(\gamma-1)/\gamma$			
9		↓( )( )				
0 7 0		0				
1		5			$\frac{\gamma-1}{\gamma} \to 05$	
2		3				
3		.				
4		5	$\gamma/(\gamma-1)$			
5		↓( )( )				
6		0			$\frac{\gamma}{\gamma-1} \to 06$	
7		6				
8		HALT	ENTER: $\alpha_4 = 21$	α_4		
9		↓( )( )				
0 8 0		0				
1		7			$\alpha_4 \to 07$	
2	+	IND/SYMB	↑ SYMBOL. ADDRESS +			
3		+	↓			
4		HALT	ENTER: α_2	α_2		
5		↓( )( )				
6		2				
7		9			$\alpha_2 \to 29$	
8		SIN/COS				
9		2NDFUNC	$\cos \alpha_2$			
0 9 0		↓( )( )				
1		1				
2		0			$\cos \alpha_2 \to 10$	
3		HALT	ENTER: T_{t2}/T_0	T_{t2}/T_0		
4		↓( )( )				
5		1				
6		1			$T_{t2}/T_0 \to 11$	
7		HALT	ENTER: P_{t2}/P_0	P_{t2}/P_0		
8		↓( )( )				
9		1				

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STEP			SYMBOL	COMMAND	COMMENTS	ENTER	STORE	PRINT
1	0	0		2			$P_{t2}/P_0 \to 12$	
		1		HALT	ENTER: T_2/T_0	T_2/T_0		
		2		↓( )( )				
		3		1				
		4		3			$T_2/T_0 \to 13$	
		5		HALT	ENTER: P_2/P_0	P_2/P_0		
		6		↓( )( )				
		7		1				
		8		4			$P_2/P_0 \to 14$	
		9		HALT	ENTER: $M_{V2} = M_2$	M_{V2}		
1	1	0		↓( )( )				
		1		1				
		2		5			$M_2 \to 15$	
		3		↑( )( )				
		4		1				
		5		3	T_2/T_0			
		6		√	$\sqrt{T_2/T_0}$			
		7		1/x	$1/\sqrt{T_2/T_0}$			
		8		×				
		9		↑( )( )				
1	2	0		1				
		1		5	M_2			
		2		×				
		3		↑( )( )				
		4		1				
		5		4	P_2/P_0			
		6		×				
		7		↑( )( )				
		8		1				
		9		0	$\cos \alpha_2$			
1	3	0		×				
		1		↑( )( )				
		2		0				
		3		0	C			
		4		=	K			
		5		↓( )( )				
		6		0				
		7		8			$K \to 08$	
		8		/	↑ NO OP.			
		9		/				
1	4	0		HALT	ENTER: Y_t / Y_{to}	Y_t/Y_{to}		
		1		×				
		2		↑( )( )				
		3		0				
		4		1	Y_{to}			
		5		CHSGN	$-Y_{to}$			
		6		×				
		7		(				
		8		↑( )( )				
		9		1				

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STEP			SYMBOL	COMMAND	COMMENTS	ENTER	STORE	PRINT
1	5	0		2	P_{t2}/P_0			
		1		−				
		2		f( )( )				
		3		1				
		4		4	P_2/P_0			
		5		)				
		6		+				
		7		↑( )( )				
		8		1				
		9		2	P_{t2}/P_0			
1	6	0		=	P_{tA}/P_0			
		1		↓( )( )				
		2		3				
		3		0			$P_{tA}/P_0 \to 40$	
		4	X	IND/SYMB	↑ SYMBOL. ADDRESS X			
		5		X				
		6		HALT	ENTER: M_4^* FOR ITERATION OF M_4	M_4^*		
		7		↓( )( )				
		8		1				
		9		6			$M_4^* \to 16$	
1	7	0		X				
		1		X	M_4^{*2}			
		2		.				
		3		2	$(\gamma-1)/2$			
		4		+				
		5		1				
		6		a^x	$1 + \frac{\gamma-1}{2} M_4^{*2} = A1$			
		7		↓( )( )				
		8		1				
		9		7			$A1 \to 17$	
1	8	0		↑( )( )				
		1		0				
		2		6	$\gamma/(\gamma-1) = 3.5$			
		3		=	$\left(1 + \frac{\gamma-1}{2} M_4^{*2}\right)^{3.5} =$			
		4		1/x				
		5		X				
		6		↑( )( )				
		7		1				
		8		0	P_{tA}/P_0			
		9		=	P_4/P_0			
1	9	0		↓( )( )				
		1		1				
		2		1			$P_4/P_0 \to 31$	
		3		↑( )( )				
		4		1				
		5		1	T_{t2}/T_0			
		6		÷				
		7		↑( )( )				
		8		1				
		9		7	$A1$			

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STEP			SYMBOL	COMMAND	COMMENTS	ENTER	STORE	PRINT
2	0	0		$=$	T_4/T_0			
		1		$\downarrow()()$				
		2		3				
		3		2			$T_4/T_0 \rightarrow 32$	
		4		$\sqrt{\ }$	$\sqrt{T_4/T_0}$			
		5		$\div$				
		6		$\uparrow()()$				
		7		3				
		8		1	p_4/P_0			
		9		$\times$				
2	1	0		$\uparrow()()$				
		1		0				
		2		8	K			
		3		$=$	M_4			
		4		$\downarrow()()$				
		5		3				
		6		3			$M_4 \rightarrow 33$	
		7		$-$				
		8		$\uparrow()()$				
		9		1				
2	2	0		6	M_4^*			
		1		$=$	$\Delta M = M_4 - M_4^*$			
		2		$\downarrow(\ )$				
		3		0			$\Delta M \rightarrow 0$	
		4		4	↑ PRINT IDENTIFIER $-4.$			
		5		CHSGN				
		6	EC	177	↓			$-4.$
		7		$\uparrow(\ )$				
		8		0	ΔM			
		9		PRINT A				ΔM
2	3	0		$\uparrow()()$				
		1		1				
		2		6	M_4^*			
		3		PRINT A				M_4^*
		4		HALT	IF $\Delta M \cong 0$; ENTER: 0			
		5		JUMP	↑			
		6		$=$	GO TO S.A $\div$ IF $\Delta M = 0$			
		7		IND/SYMB				
		8		$\div$	↓			
		9		JUMP	↑ GO TO S.A. $\times$ IF $\Delta M \neq 0$ FOR			
2	4	0		IND/SYMB	BETTER APPROXIMATION OF M_4			
		1		$\times$	↓			
		2	$\div$	IND/SYMB	↑ SYMBOL. ADDRESS $\div$			
		3		$\div$	↓			
		4		$\uparrow()()$				
		5		3				
		6		2	T_4/T_0			
		7		$\sqrt{\ }$	$\sqrt{T_4/T_0}$			
		8		$\times$				
		9		$\uparrow()()$				

STEP	SYMBOL	COMMAND	COMMENTS	ENTER	STORE	PRINT
2 5 0		3				
1		3	M_4			
2		x	V_4/a_0			
3		↓( )( )				
4		3				
5		4			$V_6/a_0 \rightarrow 34$	
6		(				
7		↑( )( )				
8		0				
9		7	α_4			
2 6 0		SIN/COS				
1		)	$\sin \alpha_4$			
2		x	$(V_4/a_0) \sin \alpha_4$			
3		x	$[(V_4/a_0) \sin \alpha_4]^2$			
4		•				
5		2	$(\gamma-1)/2$			
6		+				
7		↑( )( )				
8		3				
9		2	T_4/T_0			
2 7 0		=	T_4*/T_0			
1		1/x	T_0/T_4*			
2		X				
3		↑( )( )				
4		1				
5		1	T_{t2}/T_0			
6		a^x	$(T_{t2}/T_0)(T_0/T_4*)$			
7		↑( )( )				
8		0				
9		6	$\gamma/(\gamma-1) = 3.5$			
2 8 0		x				
1		↑( )( )				
2		3				
3		1	P_4/P_0			
4		=	P_{t4}'/P_0			
5		↓( )( )				
6		3				
7		5	-		$\dfrac{P_{t4}'}{P_0} \rightarrow 35$	
8		↑( )( )				
9		3				
2 9 0		4	V_4/a_0			
1		x				
2		↑( )( )				
3		0				
4		2	$V_5/V_4 = 1.039$			
5		x	V_5/a_0			
6		x	$(V_5/a_0)^2$			
7		•				
8		2	$(\gamma-1)/2 = .2$			
9		CHSGN	$-.2$			

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STEP			SYMBOL	COMMAND	COMMENTS	ENTER	STORE	PRINT
3	0	0		+				
		1		↑( )( )				
		2		1				
		3		1	T_{t2}/T_0			
		4		÷	T_4'/T_0			
		5		↑( )( )				
		6		1				
		7		1	T_{t2}/T_0			
		8		a^x				
		9		↑( )( )				
3	1	0		0				
		1		6	$\gamma/(\gamma-1) = 3.5$			
		2		×				
		3		↑( )( )				
		4		3				
		5		5	P_{t4}'/P_0			
		6		×	P_4'/P_0			
		7		↓( )( )				
		8		3				
		9		6			$\frac{P_4'}{P_0} \to 36$	
3	2	0		/	NO OP			
		1		.				
		2		3				
		3		+	$.3(P_4'/P_0)$			
		4		(				
		5		.				
		6		7				
		7		×				
		8		↑( )( )				
		9		3				
3	3	0		5	P_{t4}'/P_0			
		1		)	$.7\ (P_{t4}'/P_0)$			
		2		÷	P_{t4}''/P_0			
		3		↓( )( )				
		4		3				
		5		7			$\frac{P_{t4}''}{P_0} \to 37$	
		6		↑( )( )				
		7		3				
		8		5	P_{t4}'/P_0			
		9		×				
3	4	0		↑( )( )				
		1		3				
		2		6	P_4'/P_0			
		3		=	P_4''/P_0			
		4		↓( )( )				
		5		3				
		6		8			$\frac{P_4''}{P_0} \to 38$	
		7		↑( )( )				
		8		3				
		9		4	V_4/a_0			

STEP			SYMBOL	COMMAND	COMMENTS	ENTER	STORE	PRINT
3	5	0		X				
		1		↑( )( )				
		2		0				
		3		3	$V_5/V_4 = 0.8764$			
		4		X	V_5/a_0			
		5		X	$(V_5/a_0)^2$			
		6		•				
		7		2	$(\gamma-1)/2$			
		8		CHSGN	$-.2$			
		9		+				
3	6	0		↑( )( )				
		1		1				
		2		1	T_{t2}/T_0			
		3		=	T_5/T_0			
		4		1/x	T_0/T_5			
		5		X				
		6		↑( )( )				
		7		1				
		8		1	T_{t2}/T_0			
		9		a^x	T_{t2}/T_5			
3	7	0		↑( )( )				
		1		0				
		2		6	$\gamma/(\gamma-1) = 3.5$			
		3		X				
		4		↑( )( )				
		5		3				
		6		8	$p_4"/P_0$			
		7		X	P_{t5}/P_0			
		8		↓( )( )				
		9		3				
3	8	0		9			$P_{t5} \rightarrow 39$	
		1		•			P_0	
		2		6	0.6			
		3		+	$0.6 (P_{t5}/P_0)$			
		4		(				
		5		↑( )( )				
		6		3				
		7		8	$p_4"/P_0$			
		8		X				
		9		•				
3	9	0		4				
		1		)				
		2		=	P_{t6}/P_0			
		3		↓( )( )				
		4		4				
		5		0			$P_{t6} \rightarrow 40$	
		6		↑( )( )			P_0	
		7		3				
		8		4	V_4/a_0			
		9		X				

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STEP			SYMBOL	COMMAND	COMMENTS	ENTER	STORE	PRINT
4	0	0		↑( )( )				
		1		0				
		2		4	$V_6/V_4 = .722$			
		3		x	V_6/a_0			
		4		x	$(V_6/a_0)^2$			
		5		.				
		6		2	$(\gamma-1)/2 = .2$			
		7		CHSGN	$-.2$			
		8		+				
		9		↑( )( )				
4	1	0		1				
		1		1	T_{t2}/T_0			
		2		÷	T_6/T_0			
		3		↑( )( )				
		4		1				
		5		1	T_{t2}/T_0			
		6		a^x	T_6/T_{t2}			
		7		↑( )( )				
		8		0				
		9		6	$\gamma/(\gamma-1) = 3.5$			
4	2	0		x				
		1		↑( )( )				
		2		4				
		3		0	P_{t6}/P_0			
		4		=	P_6/P_0			
		5		↓( )( )				
		6		4				
		7		1			$\frac{P_6 \to 41}{T_0}$	
		8		1/x	P_0/P_6			
		9		x				
4	3	0		1				
		1		4	$P_{ATM} = 14.7$ psia			
		2		.				
		3		7				
		4		=	P_0 (psia)			
		5		↓( )( )				
		6		4				
		7		2			$P_0 \to 42$	
		8		HALT	ENTER: $X = \dot{w}\sqrt{(R_G/g)T_0}/P_0$	X		
		9		x				
4	4	0		↑( )( )				
		1		4				
		2		2	P_0			
		3		÷				
		4		↑( )( )				
		5		2				
		6		0	E			
		7		x	$\dot{w}$ (lbm/s)			
		8		↓( )( )				
		9		4				

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STEP			SYMBOL	COMMAND	COMMENTS	ENTER	STORE	PRINT
4	5	0		3			$\dot{w} \rightarrow 43$	
		1		(				
		2		↑( )( )				
		3		1				
		4		1	T_{t2}/T_0			
		5		−				
		6		1				
		7		)	$(T_{t2}/T_0) - 1$			
		8		×				
		9		↑( )( )				
4	6	0		2				
		1		1	F			
		2		=	HP			
		3		↓( )( )				
		4		4				
		5		4			$HP \rightarrow 44$	
		6		HALT	ENTER: U_2/a_0	U_2/a_0		
		7		↓( )( )				
		8		2				
		9		8			$\dfrac{U_2}{a_0} \rightarrow 28$	
4	7	0		×				
		1		↑( )( )				
		2		2				
		3		2	G			
		4		=	N (rpm			
		5		↓( )( )				
		6		4				
		7		5			$N \rightarrow 45$	
		8		↑( )( )				
		9		3				
4	8	0		0	P_{t4}/P_0			
		1		a^x				
		2		↑( )( )				
		3		0				
		4		5	$(\gamma-1)/\gamma = .4/1.4$			
		5		−	$(P_{t4}/P_0)^{\gamma-1/\gamma}$			
		6		1				
		7		÷	$(P_{t4}/P_{t_0})^{\frac{\gamma-1}{\gamma}} - 1$			
		8		(				
		9		↑( )( )				
4	9	0		1				
		1		1	T_{t2}/T_0			
		2		−				
		3		1				
		4		)	$(T_{t2}/T_0) - 1$			
		5		=	η_T			
		6		↓( )( )				
		7		4				
		8		6			$\eta_T \rightarrow 46$	
		9	EC	176	PRINT LINE OF DOTS			. . . .

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STEP			SYMBOL	COMMAND	COMMENTS	ENTER	STORE	PRINT
5	0	0		2				
		1		8	SET-UP POINTER 28 (FIRST REG.			
		2		↓ ( )	TO BE PRINTED & STR. 49			
		3		•				
		4		↓ ( )( )				
		5		4				
		6		9				
		7	PRINT A	IND/SYMB	SYMBOL. ADDRESS "PRINT A"			
		8		PRINT A				
		9		↑ ( )( )	RCL ACC. TO POINTER			
5	1	0		IND/SYMB				
		1		PRINT A				DATA
		2		SET D.P	SET DEC. POINT TO 4			
		3		4				
		4		1				
		5		↑ ( )( )	ADD 1 TO POINTER, STR 49			
		6		+	AND SET UP NEW POINTER			
		7		4				
		8		9				
		9		↓ ( )( )				
5	2	0		4				
		1		9				
		2		↓ ( )				
		3		•				
		4		−				
		5		4				
		6		5				
		7		=	NEW POINTER − 45			
		8		BRANCH	IF NEW POINTER = 45, I.E. IF N			
		9		=	IS TO BE PRINTED SET DP TO ZERO			
5	3	0		IND/SYMB	WITH S.R. ⊕			
		1		⊕				
		2		↑ ( )( )				
		3		4				
		4		9	NEW POINTER			
		5		−				
		6		4				
		7		7				
		8		=	NEW POINTER − 47			
		9		JUMP				
5	4	0		=	GO TO S.A. √ IF NEW POINTER			
		1		IND/SYMB	= 47, OR DO NOT PRINT			
		2		√				
		3		JUMP	GO TO S.A "PRINT A" IF NEW			
		4		IND/SYMB	POINTER R ≤ 46			
		5		PRINT A				
		6	√	IND/SYMB	SYMBOL. ADDRESS √			
		7		√				
		8	EC	176	PRINT LINE OF DOTS			. . . .
		9		JUMP				

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STEP			SYMBOL	COMMAND	COMMENTS	ENTER	STORE	PRINT
5	5	0		IND/SYMB	JUMP TO S.A. ADD. + TO			
		1		+	PROCESS NEW DATO			
		2	Φ	IND/SYMB	SUBROUTINE Φ SETS D.POINT TO 0			
		3		Φ	FOR PRINTING OF N			
		4		SET D.P				
		5		0				
		6		RESUME				
		7						
		8						
		9						
5	6	0						
		1						
		2						
		3						
		4						
		5						
		6						
		7						
		8						
		9						
		0						
		1						
		2						
		3						
		4						
		5						
		6						
		7						
		8						
		9						
		0						
		1						
		2		IND/SYMB				
		3						
		4						
		5						
		6						
		7						
		8						
		9						
		0						
		1						
		2						
		3						
		4						
		5						
		6						
		7						
		8		COMMAND	COMMENTS	ENTER	STORE	PRINT
		9		IND/SYMB	JUMP TO S.A. ADD. + TO			
				+	PROCESS NEW DATO			

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REGISTER			CONTENTS 1	CONTENTS 2	CONTENTS 3
0	0		$C = (k_{B2}/k_{B4})/\cos 21° = 1.16$ 1 218		
		1	$Y_{to} = .2089$		
		2	$V_S/V_4 = 1.039$		
		3	$V_5/V_4 = .8764$		
		4	$V_6/V_4 = .722$		
		5	$(Y-1)/Y = .4/1.4$		
		6	$Y/(Y-1) = 1.4/.4 = 3.5$		
		7	$\alpha_4 = 21°$		
		8	K		
		9			
	1	0	$\cos \alpha_2$		
		1	T_{t2}/T_0		
		2	P_{t2}/P_0		
		3	T_2/T_0		
		4	p_2/P_0		
		5	$M_{V2} = M_2$		
		6	M_4*		
		7	$A1 = 1 + [(Y-1)/2] M_4*^2$		
		8			
		9			
	2	0	$E = 29.364\ 077$		
		1	$F = 176.54$		
		2	$G = 23290.21$		
		3			
		4			
		5			
		6			
		7			
		8	U_2/a_0	PRINT-OUT OF INPUT	
		9	α_2		
	3	0	P_{t4}/P_0		
		1	p_4/P_0		
		2	T_4/T_0		
		3	M_4	LINE UP	
		4	V_4/a_0	OF CALCULATED DATA	
		5	P_{t4}'/P_0	FOR PRINTING.	
		6	p_4'/P_0		
		7	P_{t4}''/P_0		
		8	p_4''/P_0		
		9	P_{t5}/P_0		
	4	0	P_{t6}/P_0		
		1	p_6/P_0		
		2	P_0 (psia)		
		3	$\dot{w}$ (lbm/s)		
		4	HP		
		5	N (rpm)		
		6	η_T		
		7			
		8			
		9	POINTER		

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18. SUPPLEMENTARY NOTES

19. KEY WORDS *(Continue on reverse side if necessary and identify by block number)*

Hybrid compressor concept.
Aerodynamic Design
Design- and Off-Design Performance
Losses in Radial Compressor Wheels
Performance of Drive Air Turbine

20. ABSTRACT *(Continue on reverse side if necessary and identify by block number)*

This report presents the aerodynamic calculations and describes the mechanical features of a test rig that has been designed at the Turbopropulsion Laboratory, Department of Aeronautics, for research work on a special type of centrifugal compressor. This so-called Hybrid compressor consists of a centrifugal rotor with 180° flow deflection in the meridional plane followed by an axial flow diffusor. The report establishes a method to predict the off-design performance of the subject compressor, which can be applied also to conventional centrifugal compressors. Extensive use is made of modern programmable calculators, and

DD FORM 1 JAN 73 **1473** EDITION OF 1 NOV 65 IS OBSOLETE
(Page 1) S/N 0102-014-6601 |

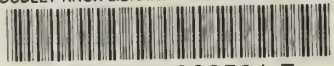Item 19 continued:

    Description of Test Rig
    Torque Measurement
    Programs for Programmable Calculators

Item 20 continued:

    programs are presented to show the effectiveness of these tools in
    engineering endeavors.

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